NOTICE OF THE SCAQMD REFINERY COMMITTEE MEETING

REFINERY COMMITTEE:
Dr. Clark E. Parker, Sr., Chair
Mayor Larry McCallon, Vice Chair
Mayor Ben Benoit
Dr. Joseph Lyou
Mayor Pro Tem Judith Mitchell

Saturday, January 20, 2018 – 9:00 a.m.

Holiday Inn Los Angeles Gateway
- Torrance Gateway Ballroom
19800 S. Vermont Avenue
Torrance, CA 90502

AGENDA

Items are expected to be completed in the order listed below. However, items may be taken in any order.

1. Welcome / Opening Remarks
   Dr. Clark E. Parker, Sr.
   Committee Chair

2. Overview
   SCAQMD staff will provide review of the latest refinery activities.
   Wayne Nastri
   Executive Officer

3. Staff Presentation - PR1410 Update
   SCAQMD staff will provide information on the development of the proposed rule 1410 including public process, MHF technology, and possible rule concepts.
   Dr. Philip Fine
   Deputy Executive Officer
   Planning and Rules
4. **Public Comments**

Members of the public may address the Committee concerning any agenda item before or during consideration of that item (Govt. Code Section 54954.3). Speakers may be limited to three (3) minutes each. The agenda for this meeting is posted at SCAQMD Headquarters, 21865 Copley Drive, Diamond Bar, CA, and Torrance Gateway Ballroom at 19800 S. Vermont Avenue, Torrance, CA, at least 72 hours in advance of the meeting. At the end of the agenda, an opportunity is provided for public comment on matters within the Committee’s authority.

5. **Closing Remarks**

Adjournment

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**Document Availability**

All documents (i) constituting non-exempt public records, (ii) relating to an item on the agenda, and (iii) having been distributed to at least a majority of the Committee after the agenda is posted, are available prior to the meeting for public review at the South Coast Air Quality Management District Public Information Center, 21865 Copley Drive, Diamond Bar, CA 91765, and will also be available at the meeting site on the day of the meeting.

**Americans with Disabilities Act**

The agenda and documents in the agenda packet will be made available, upon request, in appropriate alternative formats to assist persons with a disability [Govt. Code Section 54954.2(a)]. Disability-related accommodations will also be made available to allow participation in the meeting. Any accommodations must be requested as soon as practicable. Requests will be accommodated to the extent feasible. Please contact Lisa Tanaka-O’Malley at 909-396-3327 from 7 a.m. to 5:30 p.m. Tuesday through Friday, or send the request to lomalley@aqmd.gov.
Status Update on PR1410 – Hydrogen Fluoride Storage and Use at Petroleum Refineries
PUBLIC PROCESS

• Six working group meetings conducted since April 2017

• Presentations provided:
  - Refineries’ Current Mitigations
  - CEC’s Potential Transportation Fuel Supply and Price Impacts of HF Ban
  - API RP 751 Safe Operation of Hydrofluoric Acid (HF) Alkylation Units
  - Alternative Alkylation Technologies (DuPont/CB&I/Chevron)
  - Cal-OSHA Process Safety Management Regulation
  - TRAA’s Modified HF (MHF)/HF Alkylation Dangers
  - SCAQMD’s Proposed Rule Concepts

• Five technical discussion meetings with Torrance Refining Company (TORC)

• Two refinery site visits & Torrance refinery community/neighborhood tour

• Interagency meeting with US EPA and Cal-OSHA
GENESIS OF PR1410 RULEMAKING

• “Near-miss” accident at Torrance refinery on February 18, 2015

• Community concerns on the alkylation unit safety, potential HF release and corresponding risk

• Hazards and human health risk due to exposure to HF are greater than those of sulfuric acid

• Additional information made available
  - More studies and documentation on MHF
  - Viable alternative technologies have matured and are being implemented

• SCAQMD staff conducted independent assessment
<table>
<thead>
<tr>
<th></th>
<th>HF</th>
<th>Sulfuric Acid</th>
</tr>
</thead>
<tbody>
<tr>
<td>Appearance</td>
<td>Colorless, fuming liquid/gas</td>
<td>Colorless, oily liquid</td>
</tr>
<tr>
<td>Vapor Density</td>
<td>0.7 (relative to air)</td>
<td>3.4 (relative to air)</td>
</tr>
<tr>
<td>Boiling Point</td>
<td><strong>67 °F</strong></td>
<td><strong>554 °F</strong></td>
</tr>
<tr>
<td>Hazards</td>
<td>Severe skin and deep tissue burns, changing the bone structure</td>
<td>Severe irritation and skin burn, carcinogenic</td>
</tr>
<tr>
<td>Rate of Onset</td>
<td>Immediate &amp; delayed</td>
<td>Immediate</td>
</tr>
<tr>
<td>Isolating Distance*</td>
<td>At least 330 ft.</td>
<td>At least 150 ft.</td>
</tr>
</tbody>
</table>

* Isolate leak area in all directions as an immediate precautionary measure (source: https://cameochemicals.noaa.gov)
“NEAR-MISS” ACCIDENT

Each settler tank contains 47,000 lb of MHF

(Courtesy of the US Chemical Safety Board)
ASSESSMENT OF MHF TECHNOLOGY

• Staff has assessed the scientific information provided by TORC on MHF
• Assessing the safety of MHF technology is very complex and uncertainty still exists
• Summary results of MHF assessment:
  ❑ Some, but uncertain, HF mitigation benefits offered by MHF (≤ 35%)
  ❑ Ability to prevent formation of vapor/aerosol cloud is uncertain
    ✓ Conditions of testing are different from current operating conditions
    ✓ Large hole sizes were not considered
  ❑ Ignoring all the uncertainties, best case scenario with all existing mitigation measures added at TORC, HF reduction is 89% leaving 11% released
• In case of breach in one settler tank at TORC, potential release of 5,200 lb HF assuming all passive mitigation functioning properly
HF REDUCTION BENEFITS OFFERED BY MHF

Lab Tests and Modeling

Modeling Only (TORC)


* Airborne Reduction Factor
INITIAL RULE CONCEPTS

• HF mitigation tiered at three different levels and with different timeline
  ▪ Tier I Mitigation – Require existing mitigation with some enhancements
  ▪ Tier II Mitigation – Above and beyond Tier I Mitigation (API recommendations)
  ▪ Tier III Mitigation – Greatly enhanced protection (failsafe systems)

• Option to change to alternative technologies in lieu of Tier II and/or Tier III Mitigation
TIER I MITIGATION

- HF point sensors
- Alarm set points
- Open path monitors – 4 sided
  (TORC and/or Valero would need to install)
- Video cameras + monitor screens in remote control room
- HF sensitive paint
- Water mitigation
  (TORC would need to install water curtain)
- Acid evacuation system

- Emergency isolation block valves
- Backup power
- Baffles
  (TORC would need to install)
- Acid settler pans
- Flange shrouds
  (Valero would need to install)
- Pump barriers
- Safety audits

✓ Cost Range: $2.5 – $6 MM (for mitigation not yet installed)
TIER II MITIGATION

• Automated systems (water mitigation, emergency block valves) at alarm set points of HF sensors & open path monitors
• State-of-the-art high definition cameras (increase number of cameras & monitors)
• More HF sensors to compensate for non-operating sensors
• More comprehensive barriers (e.g., enclosure around acid settler tanks)

✓ Cost Range: $50 – $100 MM
TIER III MITIGATION (POTENTIAL APPROACHES)

• Complete, full enclosure of alkylation unit with roll-up doors, comprehensive water spray (worker safety), sensors & drainage capabilities
  - Possibly build whole new containment system parallel to existing unit to reduce downtime
  - Need to address potential “unintended secondary consequences” (e.g., flammable gases)

• Negatively pressured enclosure venting to scrubber with drainage

• Fully automated systems including acid evacuation at alarm set points

• Underground storage (acid dump tank, fresh storage, etc.)

✔ Cost Range: $50 – $150 MM (based on chlorine gas containment and handling facility)
TORRANCE REFINING COMPANY

Approx. Footprint
270 ft x 290 ft

ESP

Settler Tanks

Blast Wall

(Source: Google Maps)
Approx. footprint: 130 ft x 220 ft

MHF Unloading Area
Water Curtain
Settler

(Source: Google Maps)
## COMPARISON OF ALTERNATIVES TO HF

<table>
<thead>
<tr>
<th>Catalyst Type</th>
<th>Sulfuric Acid</th>
<th>Solid Acid</th>
<th>Ionic Liquid</th>
</tr>
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<tbody>
<tr>
<td><strong>Technology Name</strong></td>
<td><strong>CDAlky® (CB&amp;I)</strong></td>
<td><strong>ConvExSM (DuPont/STRATCO)</strong></td>
<td><strong>AlkyClean® (CB&amp;I)</strong></td>
</tr>
<tr>
<td><strong>Cost</strong></td>
<td>Less than conventional sulfuric acid unit (30–50% less acid consumption)</td>
<td>~40–60% less than a grassroots sulfuric acid unit</td>
<td>Information not available</td>
</tr>
<tr>
<td><strong>Associated Hazards</strong></td>
<td>Sulfuric acid</td>
<td>Sulfuric acid</td>
<td>No known hazards</td>
</tr>
<tr>
<td><strong>Commercial Applications/Status</strong></td>
<td>One US Gulf Coast refinery start-up in 2020 at comparable capacity (23,000 b/d) and 13 refineries worldwide</td>
<td>None, new technology</td>
<td>Petrochemical plant in China at lower capacity (2,700 b/d)</td>
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## EXISTING COST ANALYSIS OF TECHNOLOGY CONVERSION

### Conversion to sulfuric acid

<table>
<thead>
<tr>
<th>Cost Range</th>
<th>Conditions</th>
<th>Reference</th>
</tr>
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<tbody>
<tr>
<td>$100 – $200 MM</td>
<td>US Gulf Coast cost; Alkylation unit only</td>
<td>Norton Engineering (2016)</td>
</tr>
<tr>
<td>$210 – $330 MM</td>
<td>US Gulf Coast &amp; Midwest costs; Alkylation unit (~23,000 b/d) and acid regeneration</td>
<td>DuPont (2018)</td>
</tr>
<tr>
<td>$600 – $900 MM</td>
<td>TORC cost; Alkylation unit and acid regeneration</td>
<td>Burns &amp; McDonnell (2017)</td>
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POTENTIAL TIMING FOR IMPLEMENTATION

• 2018 – Rule adoption
• 6-12 months after adoption – Require Tier I Mitigation measures
• 2-3 years after adoption – Require Tier II Mitigation or alternative technology
• 2021 – Alternative technology assessment completed
• 8 years after adoption – Require Tier III Mitigation or alternative technology