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## TESORO LOS ANGELES REFINERY

#### INTEGRATION AND COMPLIANCE PROJECT

## FINAL ENVIRONMENTAL IMPACT REPORT

VOLUME III: Appendix C through F

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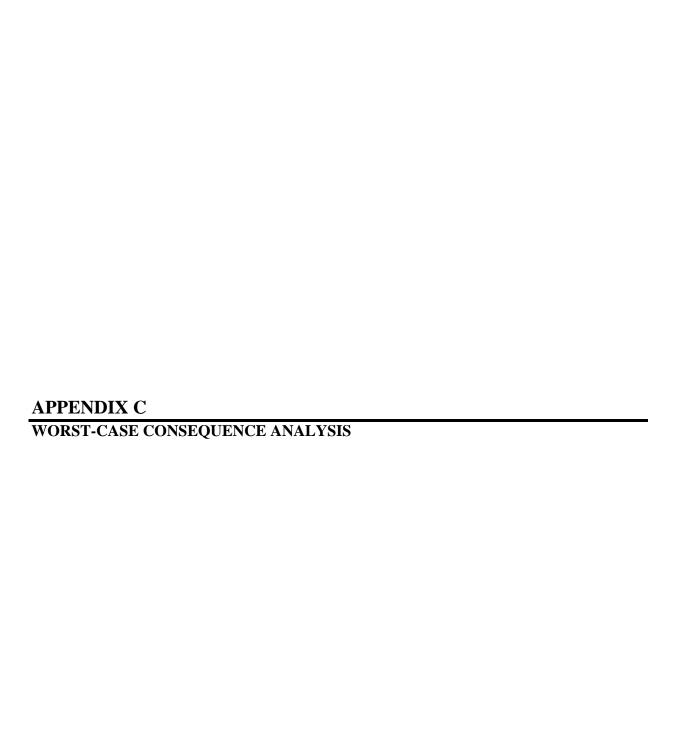
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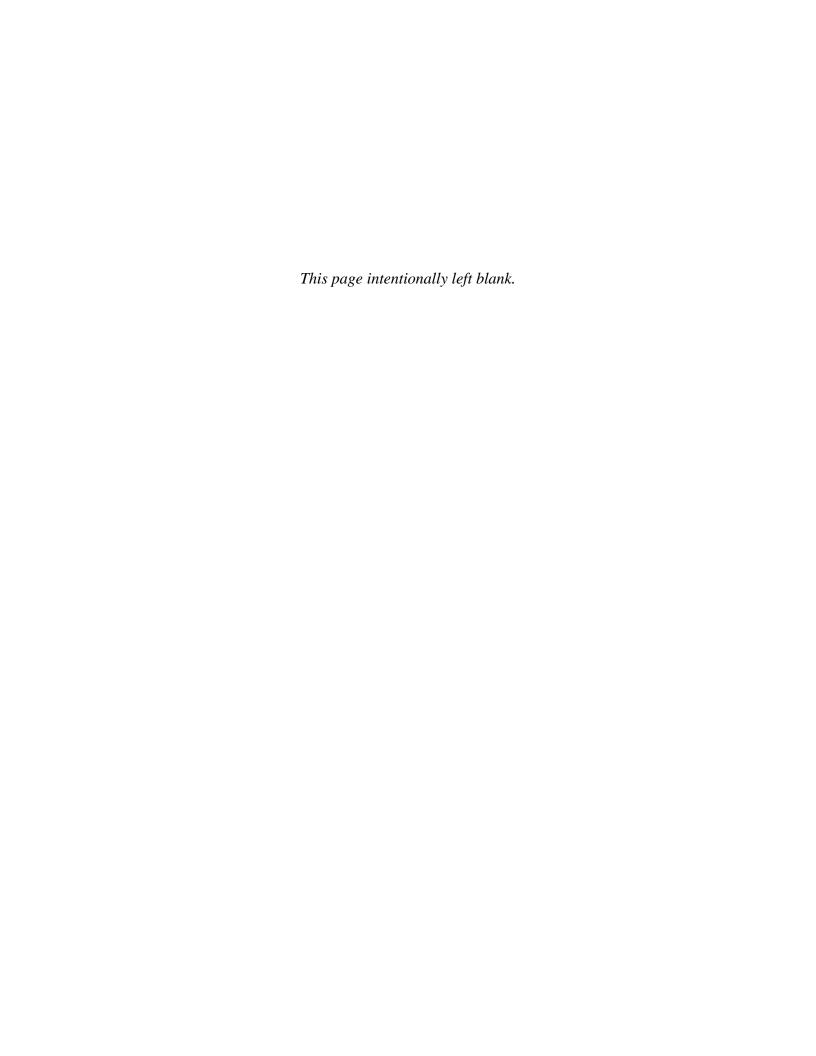
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# WORST-CASE CONSEQUENCE ANALYSIS FOR THE TESORO LOS ANGELES REFINERY

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### WORST-CASE CONSEQUENCE ANALYSIS FOR THE TESORO LOS ANGELES REFINERY

#### **PREFACE**

In April 2015, Quest prepared a Worst Case Consequence Analysis for the Tesoro Los Angeles Refinery Integration and Compliance Project. The objective of the analysis was to determine the largest potential hazard impacts to the public from the proposed project. This analysis was used to support the March 2016 Draft Environmental Impact Report (DEIR).

The analysis has been revised for the Final Environmental Impact Report (FEIR) to include updates and technical corrections identified during review of the document to respond to public comments on the DEIR. Updates and corrections include the following:

- The worst case consequence for pipelines is generated from the Interconnecting Pipelines. However, to provide a comprehensive pipeline analysis, the replacement pipeline was added to the analysis (Section 2.1.1.10 was added, Tables 4-1 and 4-2 were updated, and Figure 4-4 was updated and replaced).
- A clarifying paragraph was added to Section 3.0 Modeling Methodology.
- Correct largest hazard description for railcar unloading in Table 4-2.

The corrections, clarifications, and updates made after April 2015 are minor in nature. The overall results and conclusion of this report are unchanged.



#### 1.0 INTRODUCTION

Quest Consultants Inc.® was retained by Environmental Audit, Inc. and Tesoro Refining & Marketing Company LLC (Tesoro) to perform a worst-case consequence analysis on the proposed Los Angeles Refinery changes. The primary authors of this report are John B. Cornwell and David W. Johnson, and their resumes are listed in Appendix A. The objective of the study was to compute the potential increase or decrease in hazards to the public due to the proposed changes to the facility.

The study was divided into three tasks.

- Task 1. Determine the maximum credible potential releases, and their consequences, for existing process units, transfer systems, and storage areas.
- Task 2. Determine the maximum credible potential releases, and their consequences, for the modifications to the facility which have been proposed by Tesoro.
- Task 3. Determine whether the consequences associated with the proposed modifications generate potential hazards that are larger or smaller than the potential hazards which currently exist.

Potential hazards from the existing and proposed equipment are associated with accidental releases of toxic and flammable materials. Hazardous events associated with these types of releases include toxic vapor clouds, flash fires, torch fires, pool fires, and vapor cloud explosions.

For each type of hazard identified (toxic, radiant, overpressure), maximum distances to potentially injurious levels (vulnerability/hazard zones) are determined. The hazard levels used are those that have been developed by the U.S. Environmental Protection Agency (EPA) and American Industrial Hygiene Association (AIHA) for risk management purposes.



#### 2.0 OVERVIEW OF TESORO LOS ANGELES REFINERY

#### 2.1 Facility Location

The Tesoro Los Angeles Refinery is comprised of two parts, one which is located in Wilmington, California and the other which is located across the street in Carson, California. Both are in the Los Angeles area. The proposed project will better integrate the Wilmington and Carson operations and will comply with federal, state, and local regulations. The layout of the Wilmington facility is shown in Figure 2-1; the Carson facility is shown in Figure 2-2; and the new proposed Carson tankage is presented in Figure 2-3.

#### 2.1.1 Wilmington Operations

Proposed modifications for the Wilmington Operations are described further in the following subsections.

#### 2.1.1.1 FCCU Shutdown

The Wilmington FCCU will be shut down and the equipment will be permanently removed from service. Shutting down this unit will eliminate hazards associated with it.

#### 2.1.1.2 HCU Modification

The Wilmington Hydrocracker Unit (HCU) capacity would be increased approximately 15 percent, the overall integrated Refinery capacity would remain unchanged. The reactor and fractionation sections will be modified to increase the production of ultra-low sulfur diesel and gasoline.

Additionally, to recover propane for the Propane Sales Treating Unit (PSTU), the HCU product recovery section will be modified by installing two new water cooled exchangers, one knockout drum, and associated piping and instrumentation.

#### 2.1.1.3 DCU Fresh Feed Heater (H-100)

The existing equipment description of the Wilmington Delayed Coking Unit Fresh Feed Heater in the Title V permit will be revised to conform to SCAQMD/Industry standards. The description will be changed from the 'design heat release' basis (252 million Btu/Hr) to the industry standard 'maximum heat release' basis (302.4 million Btu/Hr). No physical modifications will be made to the heater. These modifications do not produce changes in hazards, and this unit was not evaluated in the analysis

#### 2.1.1.4 <u>Propane Sales Treating Unit (PSTU)</u>

A new PSTU will be constructed at the Wilmington Operations. The PSTU conditions liquid propane for sale using absorbers and dryers to meet sales specifications.

#### 2.1.1.5 CRU3 Modification

The Wilmington Operations Catalytic Reformer Unit 3 (CRU3) will be modified to recover Hydrocracker propane from the refinery fuel gas system.



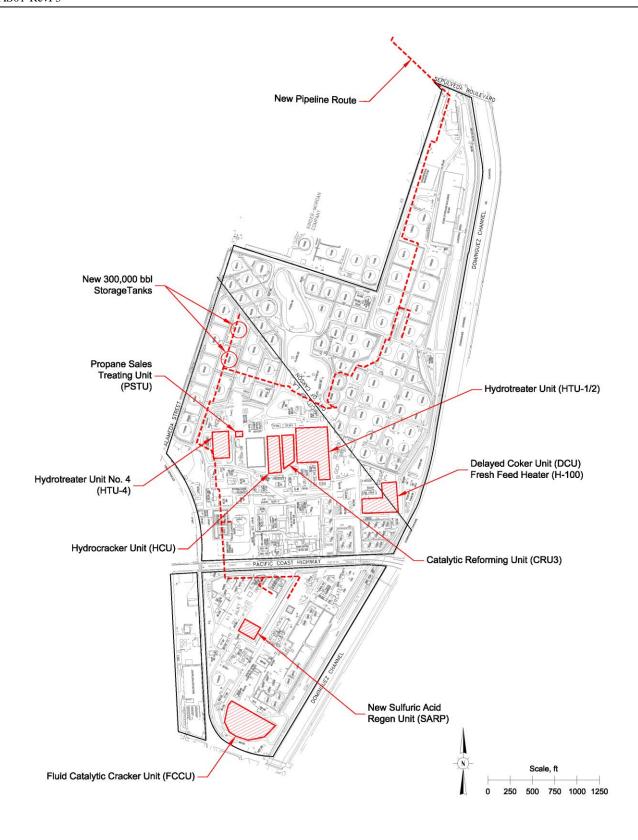


Figure 2-1
Plot Plan of Wilmington Operations at Tesoro Los Angeles Refinery



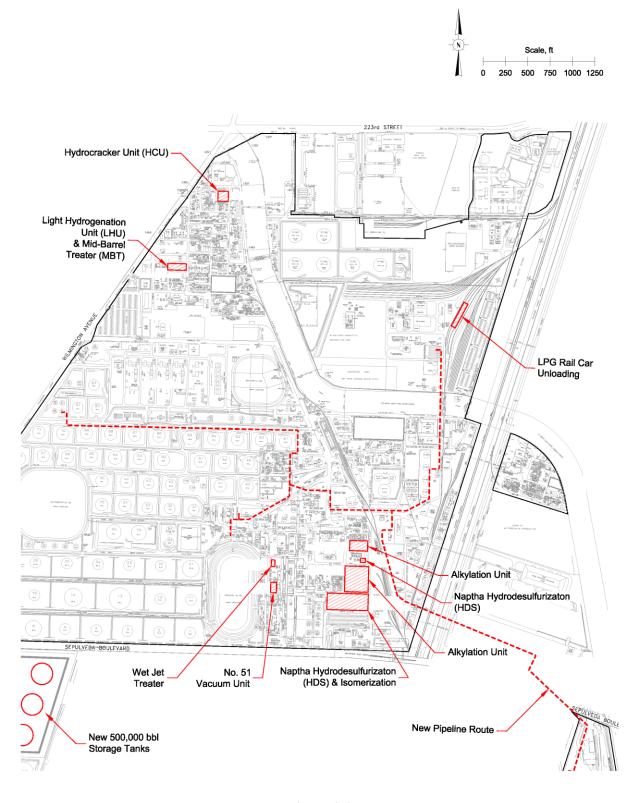
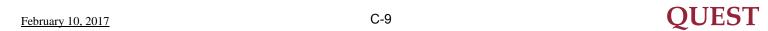


Figure 2-2 Plot Plan of Carson Operations at Tesoro Los Angeles Refinery





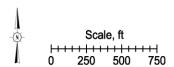


Figure 2-3 Plot Plan of New 500,000 bbl. Storage Tanks



#### 2.1.1.6 <u>HTU-1 and 2 Modifications (HTU-1/2)</u>

The Wilmington Operations Hydrotreater Unit 1 (HTU-1) will be modified to hydrotreat approximately 20,000 BPD of FCCU gasoline to comply with the federally mandated Tier 3 gasoline specifications. HTU-2 feed will be separated from HTU-1 feed.

#### 2.1.1.7 HTU-4 Modification

The Wilmington Operations Hydrotreater Unit No. 4 (HTU-4) will be modified to fully utilize the existing hydrotreating capacity to produce ultra-low sulfur diesel, to recover jet fuel, and to reduce energy consumption. These modifications do not produce changes in hazards, and this unit was not evaluated in the analysis.

#### 2.1.1.8 New Sulfuric Acid Regeneration Plant

The proposed new Sulfuric Acid Regeneration Plant (SARP) will be constructed in the Wilmington operations area and will remove impurities from and recycle the Wilmington and Carson Operations spent sulfuric acid to produce fresh sulfuric acid.

#### 2.1.1.9 Wilmington Storage Tanks

Two new 300,000 barrel internal floating roof storage tanks (Tanks 300035 and 300036) will replace two existing 80,000 barrel fixed-roof storage tanks (Tanks 80035 and 80036) in the north tank area of Wilmington Operations.

Tanks 80038, 80044, 80060, 80067, 80074, 80211, 80215, and 80217 will have increased utilization, increased throughput, or conversion to internal floating roofs. None of these changes will affect the hazard zone associated with each tank.

#### 2.1.1.10 Replace Existing Section of Crude Oil Pipeline

The proposed project will replace 5,000 feet of 12-inch diameter piping with 24-inch diameter piping within the confines of the Wilmington Operations to allow the tank loading rate to increase from 5,000 bbl/hr to 15,000 bbl/hr when filling internal floating roof tanks.

#### 2.1.2 Carson Operations

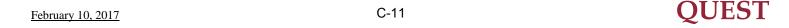
Proposed modifications to the Carson Operations are described in the following subsections.

#### 2.1.2.1 No. 51 Vacuum Unit Modifications

The No. 51 Vacuum Unit (51VAC) will be modified to provide the flexibility to increase diesel production by decreasing vacuum gas oil production by approximately 8,000 BPD.

#### 2.1.2.2 New Wet Jet Treater

One new 50,000 BPD Wet Jet Treater (WetJet) will be installed at Carson Operations to remove mercaptans and to reduce the total acid number (TAN), or organic acid content, in jet fuel.



#### 2.1.2.3 HCU Modification

The Carson Operations Hydrocracker (HCU) will be modified to add flexibility of running the distillate recovered from the No. 51 Vacuum and the Fluid Feed Hydrodesulfurization (FFHDS) Units. The HCU capacity will be increased by 10 percent.

#### 2.1.2.4 LHU Modifications

The Carson Operations Light Hydrotreating Unit (LHU) will be modified to more effectively remove sulfur from FCCU gasoline to comply with the federally mandated Tier 3 gasoline sulfur specification.

#### 2.1.2.5 Naphtha HDS Unit Modification

The Carson Operations Naphtha Hydrodesulfurization (Naptha HDS) unit will be modified with the installation of new equipment to allow removal of contaminants from unit feed and sulfur from pentanes.

#### 2.1.2.6 <u>Naphtha Isomerization Unit Modifications</u>

The Carson Operations Naphtha Isomerization Unit (ISOM) will be modified to recover propane and heavier material from the Unit off-gas.

#### 2.1.2.7 <u>Alkylation Modification</u>

The Carson Operations Alkylation Unit (ALKY) will be modified to separate amylenes to feed the Carson Operations Alkylation Unit.

#### 2.1.2.8 Mid-Barrel Distillate Treater Modifications

The existing Mid Barrel Distillate Treater (MBT) will be modified to remove sulfur from heavy FCCU naptha as well as to continue to treat straight run diesel.

#### 2.1.2.9 <u>Steam System Balance Modification</u>

The Carson Operations steam system balance will be impacted due to Tier 3 conformance and the shifting of distillates draws. Implementing the projects described above will result in an increased steam demand at the Carson Operations. The increased steam demand will be met by a combination of; installing waste heat steam generators, generating more steam from the existing Cogen Units and reducing steam demand from existing steam turbines.

#### 2.1.2.10 Carson Storage Tanks

Up to six new 500,000 barrel floating roof crude oil storage tanks will be constructed adjacent to the Carson Crude Terminal.

Tanks 14, 31, 62, 63, 64, 502, and 959 will have increased utilization. This will not affect the hazard zones associated with each tank.



#### 2.1.3 Modifications to Supporting Equipment

#### 2.1.3.1 Interconnecting Pipeway

The proposed project will require an interconnecting pipeway between the Wilmington and Carson Operations. The pipeway will be comprised of one pipe bundle of up to 15 pipelines ranging from 4 inches to 12 inches in diameter. The pipeway is proposed to exit the Carson Operations and be routed underneath S. Alameda Street to land near the Tesoro Coke Barn. The pipeway would then be routed underneath E. Sepulveda Boulevard to connect to the Wilmington Operations. The pipeway would then be routed above ground on pipe racks or ground level pipe supports into the respective product and supply manifolds within the Refinery.

#### 2.1.3.2 <u>Liquid Petroleum Gas (LPG) Rail Loading/Unloading</u>

The LPG Rail Car Unloading facilities at Wilmington will be modified to allow increased receiving capacity of approximately 4,000 BPD at Wilmington of Alkylation Unit feedstocks (propane, propylene, butane, butylene, etc.). Butane is received from rail cars into pressurized tanks for use in the Refinery process. LPG Rail Unloading facilities will be used to transfer LPG to and from the Refinery to supplement Alkylation Unit feed and remove products

The LPG rail loading modifications will allow the Refinery to transfer up to about 15,000 BPD of LPG, resulting in the increase of about 4,000 BPD or ten rail cars per day at the Refinery. It is expected that these additional rail cars would be added onto existing trains that visit the Refinery.



#### 3.0 MODELING METHODOLOGY

For any one of the hazards that are inherent to the existing or proposed process systems at the Tesoro Los Angeles Refinery facility to impact an area, a loss of containment (LOC) must occur. If the hydrocarbons normally contained within the piping or equipment at the site are released, the resulting flash fire, vapor cloud explosion (VCE), torch fire, pool fire, or toxic vapor cloud has specific consequences that can be described by modeling.

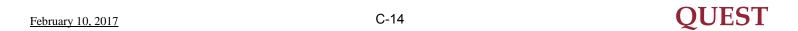
To describe the hazards at any facility handling or storing hazardous materials, release scenarios are developed to simulate the potential LOC events. This first requires calculations of material release rates and the properties of the material following release. Following these calculations, hazard models are applied to describe the extent of a toxic or flammable vapor cloud (flash fire), torch fire radiation, pool fire radiation, Boiling Liquid Expanding Vapor Explosion (BLEVE) or overpressure from a vapor cloud explosion. With the results of these calculations, the extent of the potential impacts can be determined.

In the current study, the facility was divided up into 19 sections that generally correspond to the units in the facility. The units and the potential changes to them are described in Section 2. The units requiring evaluation are listed in Table 4-1. As described above, the hazards associated with the release of flammable and/or toxic fluids are well known. However, the extent or size of a particular hazard following an accidental release is a function of the fluid's composition, temperature, pressure, inventory, pipe size, normal flowrate, release orientation, etc. Not all of these parameters will change within a portion of a unit, but many will change as a fluid passes through a unit. In Quest's accident selection methodology, thousands of potential releases and hazard zone calculations are made, but only the largest (worst case) results are presented in Section 4.

#### 3.1 CANARY Consequence Analysis Models

When performing site-specific consequence analysis studies, the ability to accurately model the release, dilution, and dispersion of gases and aerosols is important if an accurate assessment of potential exposure is to be attained. For this reason, Quest uses a modeling package, CANARY by Quest®, that contains a set of complex models that calculate release conditions, initial dilution of the vapor (dependent upon the release characteristics), and the subsequent dispersion of the vapor introduced into the atmosphere. The models contain algorithms that account for thermodynamics, mixture behavior, transient release rates, gas cloud density relative to air, initial velocity of the released gas, and heat transfer effects from the surrounding atmosphere and the substrate. The release and dispersion models contained in the QuestFOCUS package (the predecessor to CANARY by Quest®) were reviewed in a United States Environmental Protection Agency (EPA) sponsored study [TRC, 1991] and an American Petroleum Institute (API) study [Hanna, Strimaitis, and Chang, 1991]. In both studies, the QuestFOCUS software was evaluated on technical merit (appropriateness of models for specific applications) and on model predictions for specific releases. One conclusion drawn by both studies was that the dispersion software tended to overpredict the extent of the gas cloud travel, thus resulting in too large a cloud when compared to the test data (i.e., a conservative approach).

A study prepared for the Minerals Management Service (MMS) [Chang, et al., 1998] reviewed models for use in modeling routine and accidental releases of flammable and toxic gases. The MMS recommends CANARY for use when evaluating toxic and flammable gas releases. The specific models (e.g., SLAB) contained in the CANARY software package have also been extensively reviewed.



CANARY also contains models for pool fire, torch fire, and boiling liquid expanding vapor explosions (BLEVEs) radiation. These models account for impoundment configuration, material composition, target height relative to the flame, target distance from the flame, atmospheric attenuation (includes humidity), wind speed, and atmospheric temperature. Both are based on information in the public domain (published literature) and have been validated with experimental data.

#### 3.2 The QMEFS Model for Vapor Cloud Explosions

For vapor cloud explosion (VCE) calculations, Quest uses a model that is a variation of the Baker-Strehlow-Tang (BST) method. The Quest Model for Estimation of Flame Speeds (QMEFS) [Melton & Marx, 2009] is based on experimental data involving vapor cloud explosions, and is related to the amount of confinement and/or obstruction present in the volume occupied by the vapor cloud.

Quest's QMEFS model is based on the premise that the strength of the blast wave generated by a VCE is dependent on the reactivity of the flammable gas involved, the presence (or absence) of structures such as walls or ceilings that partially confine the vapor cloud, the spatial density of obstructions within the flammable cloud [Baker, et al., 1994, 1998], the average size of those obstacles, and the overall size of the confined or congested space [Mercx, 1994a, 1994b, 1997; Mercx, Van den Berg, & Van Dongen, 1996]. This model reflects the results of several international research programs on vapor cloud explosions, which show that the strength of the blast wave generated by a VCE increases as the degree of confinement and/or obstruction of the cloud increases. The following quotations illustrate this point.

"On the evidence of the trials performed at Maplin Sands, the deflagration [explosion] of truly unconfined flat clouds of natural gas or propane does not constitute a blast hazard." [Hirst and Eyre, 1982] (Tests conducted by Shell Research Ltd., in the United Kingdom.)

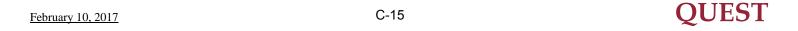
"Both in two- and three-dimensional geometries, a continuous accelerating flame was observed in the presence of repeated obstacles. A positive feedback mechanism between the flame front and a disturbed flow field generated by the flame is responsible for this. The disturbances in the flow field mainly concern flow velocity gradients. Without repeated obstacles, the flame front velocities reached are low both in two-dimensional and three-dimensional geometry." [van Wingerden and Zeeuwen, 1983] (Tests conducted by TNO in the Netherlands.)

"The current understanding of vapor cloud explosions involving natural gas is that combustion only of that part of the cloud which engulfs a severely congested region, formed by repeated obstacles, will contribute to the generation of pressure." [Johnson, Sutton, and Wickens, 1991] (Tests conducted by British Gas in the United Kingdom.)

Researchers who have studied case histories of accidental vapor cloud explosions have reached similar conclusions.

"It is a necessary condition that obstacles or other forms of semi-confinement are present within the explosive region at the moment of ignition in order to generate an explosion." [Wiekema, 1984]

"A common feature of vapor cloud explosions is that they have all involved ignition of vapor clouds, at least part of which have engulfed regions of repeated obstacles." [Harris and Wickens, 1989]



The strength of the blast wave predicted by the QMEFS VCE model is directly related to the size of the obstructed or partially confined volume that is filled with a flammable mixture of gas and air, and fuel reactivity.

#### 3.3 Hazards Identification and Modeling Endpoints

The potential hazards associated with this facility are common to most oil processing facilities worldwide, and are a function of the materials being processed, processing systems, procedures used for operating and maintaining the facility, and hazard detection and mitigation systems. The hazards that are likely to exist are identified by the physical and chemical properties of the materials being handled and the process conditions. For hydrocarbon fuel and petrochemical facilities, the common hazards are:

- toxic gas clouds (e.g., gas with hydrogen sulfide, sulfur dioxide, or sulfur trioxide)
- flash fires
- torch fires
- pool fires
- boiling liquid expanding vapor explosions (BLEVEs)
- vapor cloud explosions (VCEs)

When comparing a toxic hazard to a flammable or explosive hazard, the magnitude of the hazard's impact must be identically defined. For instance, it would not be meaningful to compare human exposure to nonlethal overpressures (low overpressures which break windows) to human exposure to lethal fire radiation (34,500 Btu/(hr•ft²) for five seconds). Thus, in order to compare the hazards of toxic gases, fires, and explosions on humans, equivalent levels of hazard must be defined.

The endpoint hazard criterion defined in this study corresponds to a hazard level which might cause an injury. With this definition, the injury level must be defined for each type of hazard (toxic, radiant heat, or overpressure exposure). Fortunately, data exist which approximate an equivalent injury level for each of the hazards listed. Table 3-1 presents the endpoint hazard criteria used by federal agencies and national associations for this type of analysis.

#### 3.4 Weather Conditions

The weather conditions at the time of an accidental release (a LOC event) can influence the extents of the resulting hazards. For the purposes of a consequence-based study, a set of weather conditions – consisting of atmospheric stability and wind speed – must be assigned for each calculation. Atmospheric stability is classified by the letters A through F. In general, the most unstable atmosphere is characterized by stability class A. Stability A would correspond to an atmospheric condition where there is strong solar radiation and moderate winds. This combination of radiation and wind allows for rapid fluctuations in the air and thus greater mixing of the released gas with time. Stability D is characterized by fully overcast or partial cloud cover during both daytime and nighttime. The atmospheric turbulence is not as great during D conditions as during A conditions; thus, the gas will not mix as quickly with the surrounding atmosphere. Stability F corresponds to the most "stable" atmospheric conditions. Stability F generally occurs during the early morning hours before sunrise (thus, no solar radiation) and under low wind. The combination of low wind and lack of solar heating allows for an atmosphere which appears calm or still and thus restricts the ability to actively mix with the released gas.



#### Table 3-1 Consequence Analysis Hazard Levels (Endpoint Criteria for Consequence Analysis)

	Injury Threshold				
Hazard Type	Exposure Duration	Hazard Level	Reference		
Sulfur Dioxide (SO <sub>2</sub> ) exposure	Up to 60 min	3 ppm	ERPG-2 [AIHA, 2011]		
Sulfur Trioxide (SO <sub>3</sub> ) exposure	Up to 60 min 2.5 ppm		ERPG-2 [AIHA, 2011]		
Hydrogen Sulfide (H <sub>2</sub> S) exposure	Up to 60 min	30 ppm	ERPG-2 [AIHA, 2011]		
Radiant heat exposure	40 sec	1,600 Btu/(hr•ft²) †	40 CFR 68 [EPA, 1996]		
Explosion overpressure	Instantaneous	1.0 psig ‡	40 CFR 68 [EPA, 1996]		
Flash fires (flammable vapor clouds)	Instantaneous	LFL	40 CFR 68 [EPA, 1996]		

ERPG-2. The maximum airborne concentration below which it is believed nearly all individuals could be exposed for up to one hour without experiencing or developing irreversible or other serious health effects or symptoms that could impair an individual's ability to take protective action.

For vapor dispersion calculations, the typical worst-case weather assumption is a stable atmosphere with low wind, which tends to produce longer vapor dispersion distances. The conditions chosen for the dispersion analyses are:

Atmospheric Stability Class F

Wind Speed 4.5 mph (2.0 m/s)

For fire radiation, higher wind speeds generally result in longer impact distances due to flame bending. Atmospheric stability does not affect the size or characteristics of a flame. Thus, a worst-case wind speed for fire radiation was chosen as:

Wind Speed 20 mph (8.9 m/s)

For all calculations, annual average air temperature and relative humidity values were taken from local meteorological data [weatherspark, 2014]:

Air Temperature 65°F (18.3 °C)

Relative Humidity 70%



<sup>40</sup> CFR 68. United States Environmental Protection Agency RMP endpoints.

<sup>†</sup> Corresponds to second-degree skin burns.

<sup>&</sup>lt;sup>‡</sup> An overpressure of 1 psi may cause partial demolition of houses, which can result in serious injuries to people, and shattering of glass windows, which may cause skin laceration from flying glass.

## 4.0 IMPLEMENTATION OF WORST-CASE CONSEQUENCE MODELING METHODOLOGY

The results of the worst-case consequence modeling calculations for the existing and proposed processes are presented in this section. In addition, for several processes, the vulnerability zone which extends the greatest distance from the point of release is overlaid onto the local area in order to determine possible public exposure to the defined hazard levels.

#### 4.1 Accident Selection

The inherent flammable hazards associated with refineries are well known. A review of the Los Angeles Refinery process shows that there are multiple release scenarios that could result in fire or explosion hazards that may generate significant impacts. The hazards from the various release scenarios are identified in the following sections.

#### 4.2 Releases Resulting in the Largest Downwind Hazard Zones

When the hazard identification and consequence modeling calculations described in Section 3.0 are completed for the accidents selected in Section 4.1 for both the existing facility and the proposed changes to the facility, the releases which generate the largest hazard zones can be defined for the facility and associated pipeway. Table 4-1 summarizes the worst-case releases identified and Table 4-2 summarizes the maximum hazard zones for each worst-case release. In Table 4-2, P indicates a proposed modification and E indicates an existing unit.

#### 4.3 <u>Worst-Case Consequences</u>

#### 4.3.1 Flash Fires

Flash fires are the result of a release, formation of a flammable vapor cloud and ignition of the cloud. Flash fire hazard zones are defined by the maximum extent of the LFL portion of the vapor cloud. For example, a release from the line feeding the Carson light hydrotreater unit (LHU) stabilizer column could result in a flash fire.

In this release scenario, the flash fire is the maximum hazard. For the LHU, this scenario is the worst-case scenario because it goes further than the other scenarios chosen for the LHU, so it is used to define the vulnerability zone for the LHU.

An example hazard footprint and vulnerability zone associated with this "worst-case" event is illustrated in Figure 4-1. The vulnerability zone (the circle) depicts the potential area that could be affected due to a release from the feed line to the LHU stabilizer column. This presentation is misleading since all locations within this zone cannot be simultaneously exposed to potential flash fire hazard from any single accident. There are other possible hazard zones following this loss of containment that form smaller footprints. The scenario that creates the maximum hazard footprint is just one of the many possible outcomes found when considering variables such as hole size, orientation, wind speed, atmospheric stability, and wind direction. The hazard footprint in Figure 4-1 (the cross hatching) shows what would be expected if the pipe were to rupture, and low speed wind is blowing to the northeast, and the atmosphere is stable, and the release is oriented horizontal, and the gas is ignited after reaching a maximum extent.

As shown in Table 4-2, a large fraction of the worst-case release scenarios are flash fires.



Table 4-1 Summary of Unit Worst-Case Scenarios

Unit	Description of Release		
Carson Refinery			
51 Vacuum	Vacuum column LGO product		
Alkylation	Olefin feed from surge drums		
HCU	Reactor 3 effluent		
Mid-Barrel Hydrotreater	Reactor effluent		
Naptha HDS	Debutanizer bottoms liquid		
Naptha Isomerization	Hot flash drum liquid		
LHU	Feed to stabilizer column		
Wet Jet Treater	Liquid to reactors		
New Crude Tanks	500,000 bbl. crude tank fire		
Wilmington Refinery			
FCCU	Unit Shutdown – not evaluated		
HTU-1/2	Liquid from HP Separator to Stripper		
HTU4	No change in hazards – not evaluated		
CRU3	Total liquid from depropanizer reflux receiver		
PSTU	Liquid from depropanizer reflux receiver to treater		
HCU	Liquid from 1st stage surge drum and DEA contactor		
SARP	Vapor from discharge of main compressor		
Replace Crude Tanks	300,000 bbl. crude tank fire		
Replace Portion of Crude Transfer Pipeline	Crude oil release		
Other			
Interconnecting Pipeway	<i>n</i> -Butane release		
Rail Car Unloading	LPG BLEVE at loading/unloading area		



Table 4-2 Summary of Worst-Case Hazard Distances

Summary of Worst-Case Hazaru Distances						
T.L.	Case ID (P/E)	Distance to I	Largest			
Unit		Proposed (P)	Existing (E)	Hazard (P/E)		
Carson Refinery						
51 Vacuum	51V-03/02	150	155	Flash Fire		
Alkylation	AU-04/04	360	585	Flash Fire		
HCU	HC-08/08	1245	1250	Toxic		
Mid-Barrel Hydrotreater	MBT-01/01	275	400	Torch Fire/ Toxic		
Naptha HDS	IO-03/01	865	1035	Flash Fire		
Naptha Isomerization	IS-02/01	665	530	Flash Fire		
LHU	LH-04/04	600	585	Flash Fire		
Wet Jet Treater	WJ-10	205	DNCE	Flash Fire		
New Crude Tanks	TNK500k	340	DNCE	Pool Fire		
Wilmington Refinery						
FCCU	CCU Shutdown					
HTU1/2	HT-04/04	1170	1065	Flash Fire		
HTU4	Modifications do not affect vulnerability zone					
CRU3	CR-04/20	1595	2190	Toxic		
PSTU	CR-05/20	1085	2190**	Toxic		
HCU	HC-07/10	1320	1450	Flash Fire		
SARP	SAR-03A	1905	DNCE	Toxic		
Replace Crude Tanks	TNK300k	265	190	Pool Fire		
Replace Portion of Crude Transfer Pipeline	PL12/24	<u>120</u>	<u>70</u>	Pool Fire		
Other						
Interconnecting Pipeway	IC-01	380	DNCE	Flash Fire		
Rail Car Unloading	C4BLEV	1700	1700	BLEVE <u>Fireball</u>		

DNCE = Does Not Currently Exist

NCR = No Calculations Required



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<sup>\*\*</sup> Existing hazard in CRU3 unit. See Figure 4-2

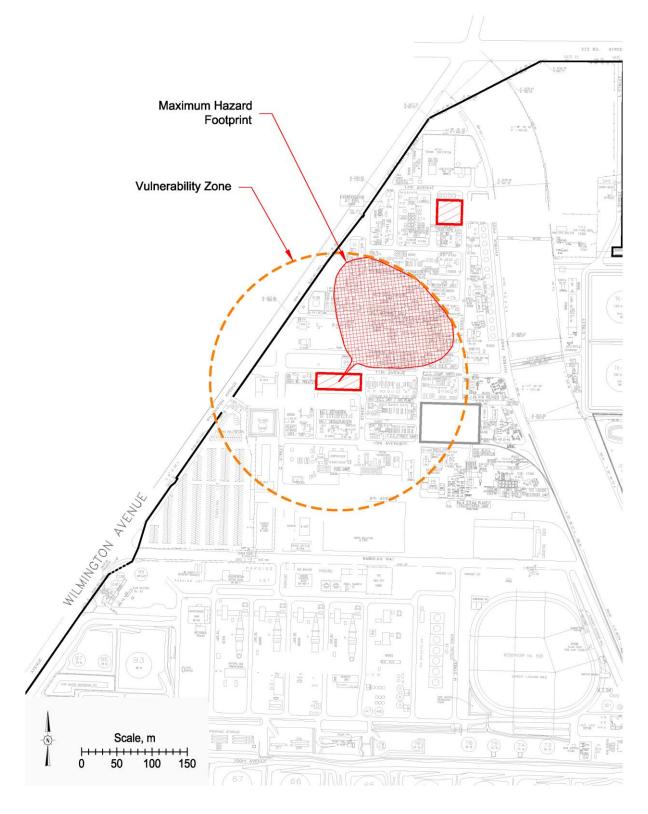


Figure 4-1 Example Vulnerability Zone



#### **4.3.2** Fire Radiation

Fire radiation hazards for this facility are a result of torch fires, pool fires, or BLEVEs. Consequence results for the units where fire radiation is the worst-case scenario are shown in Table 4-2.

The largest fire radiation hazard shown in the table is an LPG rail car BLEVE.

#### 4.3.3 Toxic Vapor Clouds

H<sub>2</sub>S, SO<sub>2</sub>, and SO<sub>3</sub> are the only toxic components in any of the processed fluids in the modified areas of the facility. A release of a stream containing H<sub>2</sub>S, SO<sub>2</sub>, or SO<sub>3</sub> may produce a toxic vapor cloud. The hazard zone of a toxic vapor cloud containing H<sub>2</sub>S, SO<sub>2</sub>, or SO<sub>3</sub> is defined by the ERPG-2 concentration level (30 ppm H<sub>2</sub>S, 3 ppm SO<sub>2</sub>, 2.5 ppm SO<sub>3</sub>).

Releases of material containing H<sub>2</sub>S produce worst-case vulnerability zones in four areas (Carson HCU and Wilmington CRU3, and PSTU). Releases of material containing SO<sub>2</sub> and SO<sub>3</sub> produce worst-case vulnerability zones in one unit (Wilmington SARP). The results from the toxic vapor cloud analysis are listed in Table 4-2.

#### **4.3.4** Vapor Cloud Explosions (VCE)

One of the possible results of a flammable fluid or gas release is the potential ignition of the vapor which could then result in a VCE. There are no LOC events that could result in VCEs that are not also possible in the existing refinery configuration. No new vulnerability zones are produced by VCE events.

#### 4.4 Summary of Maximum Vulnerability Zones

The maximum vulnerability zones for the existing equipment and proposed changes are presented in Figure 4-2 and 4-3 for the Wilmington operation and Figure 4-3 for the Carson operation. Figures 4-4 and 4-5 show the vulnerability zones for the new pipeway in the Wilmington and Carson operation areas. Figure 4-6 shows the vulnerability zone for the new 500,000 bbl. storage tanks.

Many of the units have vulnerability zones that are the same size or larger for the existing facility (solid blue lines) than for those that would be produced following the proposed changes (dashed orange lines). New units do not have existing vulnerability zones, so the proposed vulnerability zones would be larger (Carson Wet Jet, Wilmington PSTU and SARP units).

The potential hazard zones from releases originating inside the facility at the Carson operation are dominated by the toxic hazards from the HCU and at the Wilmington operation by toxic hazards in the CRU3, PTSU, and SARP areas. The largest potential hazard zone occurring within any modified area is found in the Wilmington SARP area and covers a vulnerability zone with a radius of 1,905 feet.



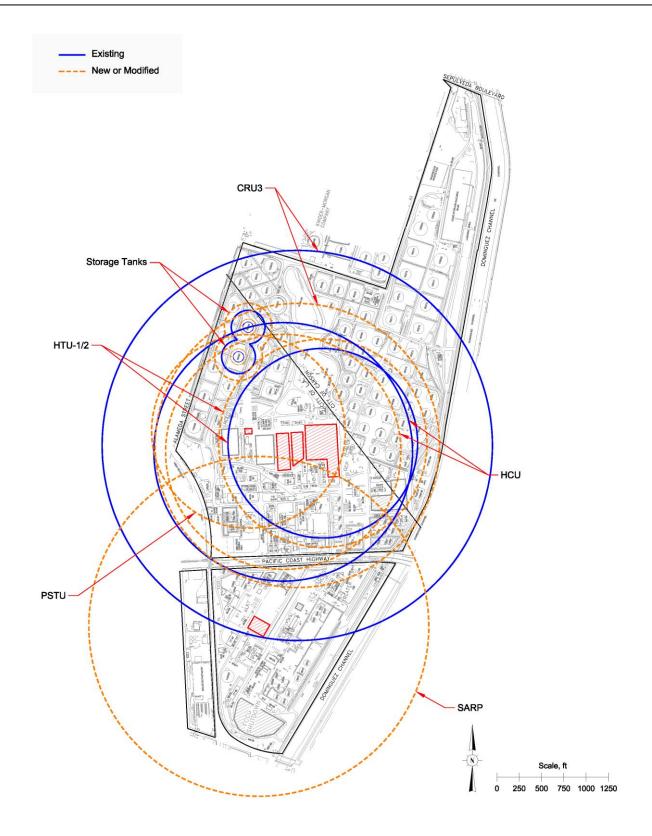
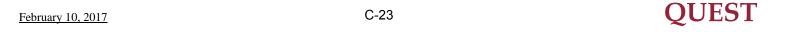


Figure 4-2 Vulnerability Zones for Wilmington Operations



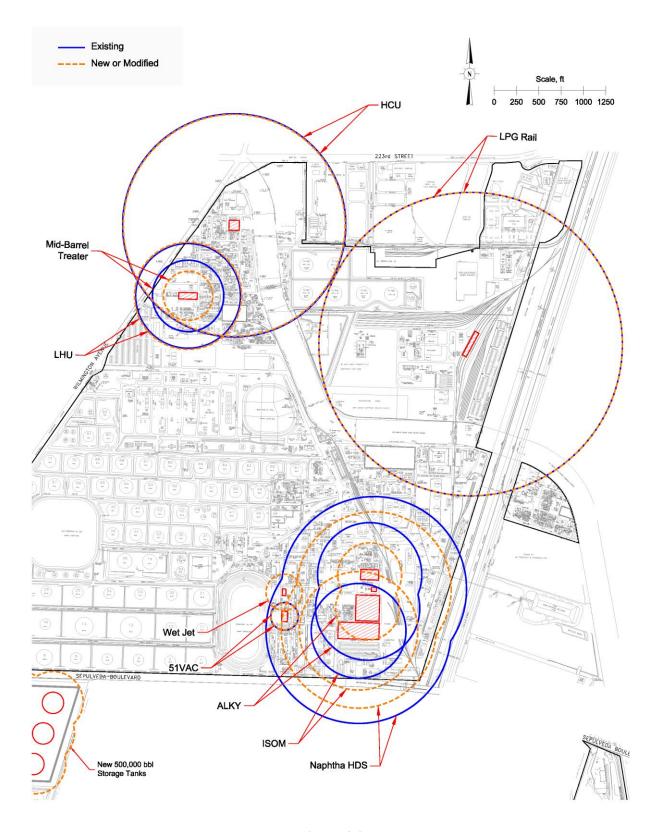
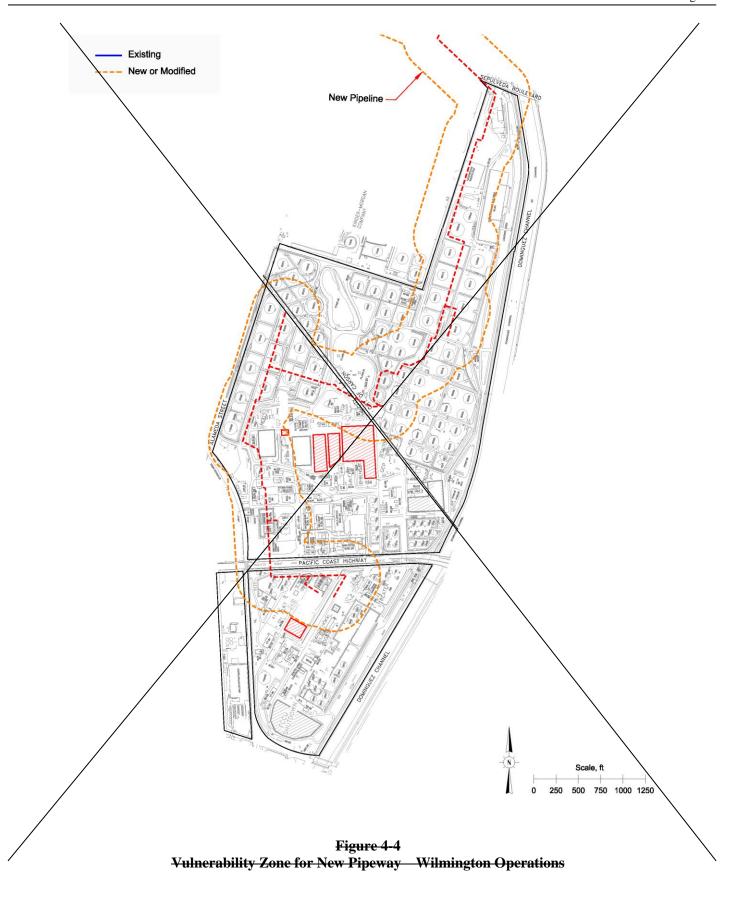
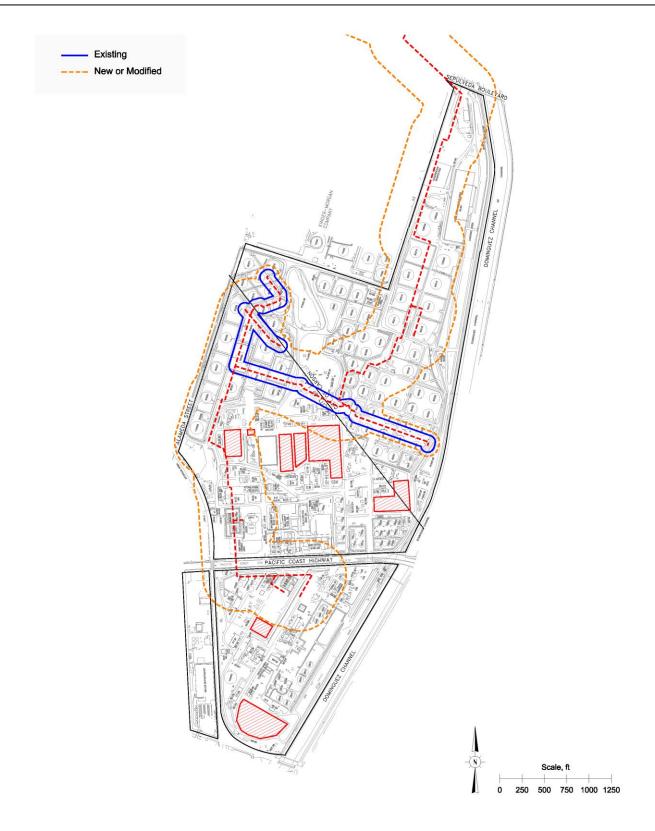


Figure 4-3 Vulnerability Zones for Carson Operations









<u>Figure 4-4</u> <u>Vulnerability Zone for New Pipeway – Wilmington Operations</u>

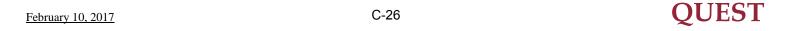
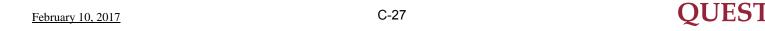




Figure 4-5 Vulnerability Zones for New Pipeway – Carson Operations



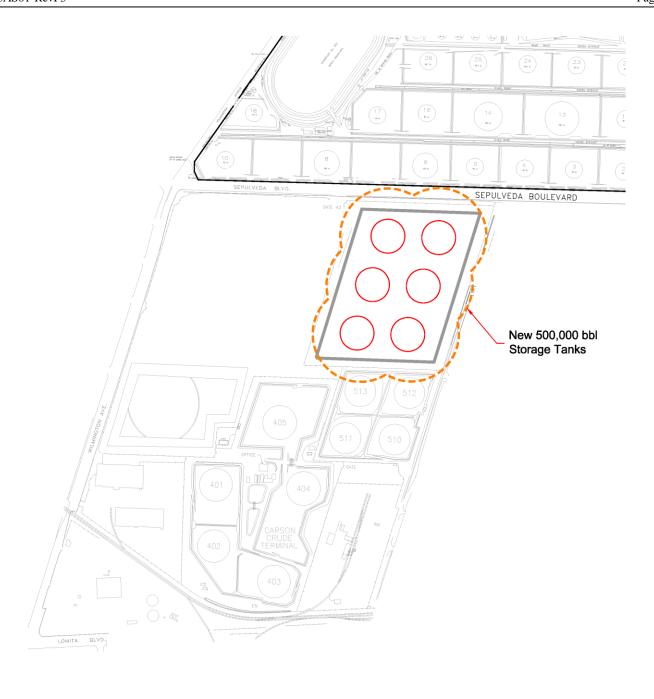




Figure 4-6 Vulnerability Zone for New 500,000 bbl. Storage Tanks

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#### 5.0 CONCLUSIONS

The primary conclusions drawn from the worst-case consequence modeling results are that for most potential releases, the proposed changes result in similar or smaller potential vulnerability zones than those posed by the existing facility configuration.

With the maximum vulnerability zones defined for each release evaluated under the existing and proposed refinery configurations, the areas can be divided into three categories, dependent on their potential to impact the public. The categories are defined as:

• Areas with no potential off-site impacts for proposed refinery configurations (hazard zones are contained onsite within the facility fence line).

Carson: Alkylation, Wet Jet, 51VAC, MBT Wilmington: HTU-1/2, 80,000 to 300,000 bbl. tank replacement

• Areas with potential off-site impacts, but no public residential exposure under proposed refinery configurations where project modified impacts are similar to or smaller than existing impacts.

Carson: HCU, Naptha HDS, LHU, Rail Loading/Unloading

Wilmington: PSTU, CRU3, HCU

 Areas with potential off-site impacts, but no public residential exposure under proposed refinery configurations where project modified impacts are larger than existing impacts.

Carson: Naptha Isomerization, new 500,000 bbl. Tanks, New Pipeway

Wilmington: New Pipeway

• Areas with potential public residential exposure.

Carson: none

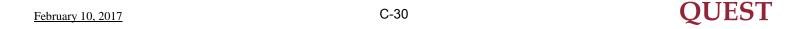
Wilmington: New SARP

These conclusions are driven by the nature of the proposed changes to the Tesoro Los Angeles Refinery. The consequences are determined by the process conditions at the time of release. The proposed changes to the Tesoro Los Angeles Refinery are not expected to significantly change those conditions. Thus, for the purposes of this study, using the hazard endpoints developed by the U.S. EPA and AIHA, the off-site hazard increases associated with the proposed project are limited to adjacent industrial areas near the facility.



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## APPENDIX A

## **RESUMES**



# John B. Cornwell Quest Consultants Inc.® Principal Engineer

### **EDUCATION**

1978 M.S., Mechanical Engineering University of Texas, Austin, Texas

1975 B.S., Chemical Engineering University of Texas, Austin, Texas

#### **EXPERIENCE**

1989 - Present Quest Consultants Inc., Norman, Oklahoma Principal Engineer

Directs the company's hazards analysis and risk analysis efforts. Directs the use of the company's state-of-the-art phenomenological models to determine the extent of potential flammable/toxic/explosive hazards. Presents the technology behind the studies to corporate and regulatory groups.

Directs quantitative risk analysis studies (QRAs) involving:

- LNG import and export terminals
- LPG storage/marketing terminals
- LPG import terminals
- Refinery complexes
- Alkylation units (HF and H<sub>2</sub>SO<sub>4</sub>)
- Ammonia plants
- Transportation of toxic materials (road and rail)
- Pipeline networks (natural gas, LPG, ammonia, liquids)
- Exploration and production systems (oil and natural gas)
- Gas plants

Directs development of computer software, CANARY by Quest<sup>®</sup>, that provides analysis tools for the company. Oversees the use of public domain (e.g. DEGADIS, SLAB, LNGFIRE3) and special application software.

1985 - 1989 Energy Analysts, Inc., Norman, Oklahoma Principal Engineer

Directed the development of computer models to simulate the hazards associated with accidental releases of toxic/flammable materials. These models were contained in a commercially available software package named EAHAP.

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### John B. Cornwell

Modeled the simulation of heavier-than-air gases and momentum jet releases of gases and aerosols. Directed the comparison analysis of several heavier-than-air gas dispersion models against the large-scale test data produced by the Thorney Island Trials, Desert Tortoise Ammonia Releases, and the Goldfish Hydrofluoric Acid Releases.

Directed numerous risk analysis/assessment studies using results of the consequence modeling and in-house risk modeling capabilities. Prepared and reviewed California RMPPs (Risk Management and Prevention Plans).

Los Alamos National Laboratory, Los Alamos, New Mexico
 Staff Member/Research Scientist, Advanced Technologies Division
 Security Clearance Level Q (DoE)

Evaluated advanced energy systems, including advanced fusion devices, liquid oxygen/liquid hydrogen turbogenerators, advanced photovoltaic systems, and conventional petroleum-based turbine systems.

1981 - 1984 Energy Analysts, Inc., Norman, Oklahoma Senior Engineer

> Directed the development of advanced simulation models for the dispersion of heavierthan-air vapors. Developed compatible thermodynamic systems and methodologies for predicting transient vaporization history of cryogenic fluids.

> Directed development of a risk analysis model for use in conjunction with results of vapor dispersion and fire radiation analyses. The risk analysis model was employed in studies requiring the time-varying/site-dependent risk profile for petrochemical facilities and the surrounding area.

Evaluated transient fire hazards and the analysis of toxic combustion products.

1978 - 1981 University of Texas, Austin, Texas Research Scientist, Center for Energy Studies

Developed a series of mathematical models to evaluate geopressured/geothermal resources along the Texas gulf coast.

### PROFESSIONAL MEMBERSHIPS

American Institute of Chemical Engineers Air and Waste Management Association American Nuclear Society



### John B. Cornwell

#### **PUBLICATIONS**

Authored papers on hazards analysis modeling, risk analysis methodologies, project siting issues, and model-to-test data analysis.

#### RELEVANT PROJECT EXPERIENCE

**Quantitative Risk Analysis for an LNG Import Terminal:** *Project Manager* for a full QRA of an LNG import terminal on Mexico's gulf coast. QRA was submitted to Mexico's Department of the Environment (SEMARNAT). Other studies completed under this contract included a qualitative risk analysis and siting study per Mexico's Secretary of Energy, Energy Regulation Commission (CRE). Terminal is now under construction. *Client: Shell Global Solutions*.

**Quantitative Risk Analysis of a Refrigerated LPG Import Terminal:** *Project Manager* for a study that included refrigerated LPG ship loading/unloading and cavern storage. Full QRA was completed and submitted for review to Chinese authorities. *Client: Caltex Corporation (now part of ChevronTexaco).* 

**LNG Facility Siting Safety Study for a Pacific Ocean Gravity Based Structure (GBS) for Use as an Import Terminal:** Participant in a study to determine if a proposed LNG import terminal could be built upon a GBS in the Mexican waters off Baja California. The study applied Mexico's NOM-EM-001-SECRE-2002 to the design. The project involved vapor dispersion, fire radiation, and vapor cloud explosion modeling for numerous hypothetical releases of LNG. *Client: ChevronTexaco* 

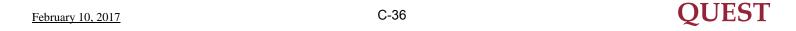
**Quantitative Risk Analysis for an Existing HF Alkylation Unit:** *Project Manager* for a full QRA of an existing HF alkylation unit. QRA was used to develop potential mitigation options. *Client: Sunoco* 

**Quantitative Risk Analysis for Natural Gas Transmission Pipeline:** *Project Manager* for a full QRA of a natural gas transmission line spanning the Gulf of Mexico from Alabama to Florida. Torch fire and flash fire radiation hazards were defined. QRA was submitted to US FERC as part of project permitting. *Client: Willbros Engineers, Inc.* 

Quantitative Risk Analysis of a Refrigerated and Pressurized LPG Storage Depot: *Project Manager* for a full QRA of a LPG storage depot and a nearby chemical facility. Analysis of terrorist threat included. Facility had been target of failed domestic terrorism in 1999. *Client: City of Elk Grove, California.* 

Quantitative Risk Analysis for Natural Gas Gathering Pipeline Network: *Project Manager* for a full QRA of a natural gas gathering network in Venezuela. Wellhead, compression and pipeline releases were evaluated. Toxic (Hydrogen Sulfide) and fire radiation hazards were defined. QRA was submitted to Petroleos de Venezuela (PDVSA) for review and approved per PDVSA standard IR-S-02. *Client: Petroleos de Venezuela*.

**Quantitative Risk Analysis for an Existing HF Alkylation Unit:** *Project Manager* two full QRAs of an existing HF alkylation unit were conducted to identify the possible risk benefit afforded by the use of acid additive. *Client: Texaco* 



### John B. Cornwell

**Quantitative Risk Analysis for an LNG Import Terminal:** *Project Manager* for a full QRA of an LNG import terminal on Mexico's Pacific coast. QRA was submitted to Mexico's Department of the Environment (SEMARNAT). Other studies completed under this contract included a qualitative risk analysis and siting study per Mexico's Secretary of Energy (CRE). *Client: Sempra Energy*.

**LNG Carrier Spill Hazards Analysis:** *Project Manager* for an analysis of possible large scale LNG carrier releases in Boston Harbor. Results used by U.S. Department of Energy in designing LNG tanker operations in Boston Harbor following September 11, 2001 terrorist attacks. *Client: U.S. Department of Energy.* 

Comparative Quantitative Risk Analysis for an HF Alkylation Unit Upgrade: *Project Manager* for a comparative (before and after) set of QRAs of an existing HF alkylation unit. The QRAs were used to demonstrate the benefits associated with three mitigation measures (individually or in concert); rapid dump system, water curtains, and water cannons. *Client: Ampol* 

**LNG Facility Siting Safety Study for Gulf of Mexico Gravity Based Structure (GBS) for Use as an Import Terminal:** Participant in a study to determine if the proposed LNG import terminal could be built upon a GBS in the Gulf of Mexico. The study included meshing the import terminal design with applicable LNG standards. This involved vapor dispersion, fire radiation, and vapor cloud explosion modeling for numerous hypothetical releases of LNG. *Client: ChevronTexaco* 

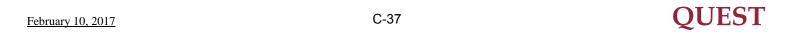
**Consequence Analysis Course:** *Instructor* for an introductory course covering the principals of consequence analysis. Course covers accidental releases and the methods to predict the extent of potential fire, explosion and toxic hazards. Course is provided through the Mary Kay O'Conner Process Safety Center located at Texas A&M University. *Client: Texas A&M University, College Station, Texas* 

**Quantitative Risk Analysis for an LNG Import Terminal:** *Project Manager* for a full QRA of an LNG import terminal on Mexico's Pacific coast. QRA was submitted to Mexico's Department of the Environment (SEMARNAT). Other studies completed under this contract included a qualitative risk analysis and siting study per Mexico's Secretary of Energy (CRE). *Client: ConocoPhillips*.

**Quantitative Risk Analysis for Natural Gas Gathering Pipeline Network:** *Project Manager* for a full QRA of a natural gas gathering network. Wellhead and pipeline releases were evaluated. Toxic (Hydrogen Sulfide) and fire radiation hazards were defined. QRA was submitted to US EPA's technical staff for review and approved. *Client: Union Pacific Resources*.

**Quantitative Risk Analysis for an HF Alkylation Unit Addition to Existing Refinery:** *Project Manager* for a full QRA of a new HF alkylation unit to be added to an existing refinery. QRA was submitted to local and Federal Israeli authorities. Evaluation included acid additive as well as water spray mitigation systems. *Client: Paz Ashdod Refinery Limited.* 

**Quantitative Risk Analysis for a Proposed Gas-to-Liquids Facility:** *Project Manager* for a full QRA of a new gas-to-liquids facility along the Nigerian coast. QRA was submitted to local and Federal Nigerian authorities. *Client: Chevron Energy and Technology* 



# David W. Johnson Quest Consultants Inc.® Principal Engineer

### **EDUCATION**

1969 Ph.D., Chemical Engineering

University of Oklahoma, Norman, Oklahoma

1965 B.S., Chemical Engineering

University of Texas, Austin, Texas

#### **EXPERIENCE**

1989 - Present Quest Consultants Inc., Norman, Oklahoma Principal Engineer

Facilitated HAZOP, SIL/LOPA, What If?, HAZID, and HEMP (bowtie) reviews for numerous projects, including:

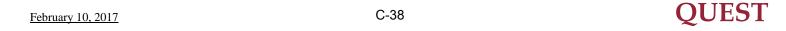
- Chemical complex
- Oil and gas processing facilities
- Refinery units
- LNG baseload (export) facilities
- LNG import facilities
- Offshore oil and gas processing

Performed consequence modeling for siting and safety studies of several liquefied natural gas (LNG) facilities. Involved in numerous consequence analysis, risk analysis, and facility siting studies involving refineries, gas plants, pipelines, and petrochemical plants.

Responsible for Quest's testing and research programs, and for the development and implementation of analytical models for predicting accidental release rates, aerosol formation, pool spreading, heat transfer, and vaporization rates.

Directed all major aspects of several experimental programs involving releases of hazardous fluids.

- On-site tests conducted to determine if the flammable cloud produced by emergency venting of ullage gas from a crude oil pipeline surge tank could reach associated process areas.
- Two field-test programs conducted to evaluate the efficacy of additives designed to reduce the amount of aerosol formed during accidental releases from HF alkylation units.
- Release tests conducted for the Petroleum Environmental Research Foundation (PERF) to determine the potential for a hydrocarbon/sulfuric acid emulsion to form an aerosol upon its release.



### David W. Johnson

• Aerosol release tests conducted for the CCPS at the DOE Nevada Test Site.

Assisted in development of RMPPs for several refinery units in California, including alkylation, hydrotreating, hydrocracking, catalytic cracking, delayed coking, and product storage. This work included a review of unit HAZOPs, selection of potential release scenarios, estimation of accident frequencies, and supervision of hazard modeling.

1983 - 1989 Energy Analysts, Inc., Norman, Oklahoma Principal Engineer

Conducted HAZOP study for a proposed refinery expansion in the Philippines. Trained refinery personnel as HAZOP leaders for future HAZOP studies.

Responsible for the technical content of the final safety analysis report (FSAR) for the Big Hill Strategic Petroleum Reserve (SPR) site. Tasks completed included identification and analysis of hazards; review of site layout and design; and equipment, piping, and instrumentation evaluation. Made recommendations to improve site operations.

Developed risk models in the areas of fire and thermal radiation, rate of fluid release from containment, and Gaussian dispersion for EAHAP hazards analysis computer code.

Designed and participated in several large-scale outdoor fire and fluid release tests designed to determine the burning and release characteristics of hydrocarbon fluids.

1977 - 1983 Applied Technology Corporation, Norman, Oklahoma Vice President

Developed mathematical models in the areas of fire radiation, vapor dispersion, and heat transfer. Applied these models to LNG facility safety studies.

Designed and conducted several large-scale outdoor tests involving fire and materials combustion. Tests included the burning and subsequent extinguishment of hexane, LPG, and carbon disulfide pool fires.

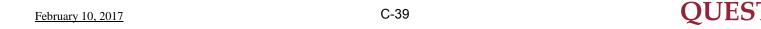
1970 - 1977 University Engineers, Inc., Norman, Oklahoma Senior Engineer

Project manager of a semi-works seawater desalination project utilizing direct contact heat transfer and freezing to produce potable water.

Involved in several large-scale outdoor fire tests to study the flammability characteristics of thermal insulation products.

1965 Celanese Fibers Corporation, Rock Hill, South Carolina Development Engineer

Adapted existing plant equipment for new and more productive uses, developed computer models describing machine operations, and assisted in plant start-up.



### David W. Johnson

#### PROFESSIONAL MEMBERSHIPS

National Society of Professional Engineers American Institute of Chemical Engineers Oklahoma Society of Professional Engineers

#### **PUBLICATIONS**

Authored more than twenty-five papers in the areas of physical properties, kinetics, and process plant safety.

### RELEVANT PROJECT EXPERIENCE

**Process Hazards Analysis (PHA) of a Large LNG Liquefaction Facility**: *Directed* the HAZOP and LOPA studies for a large scale grass roots LNG facility in Texas. Studies for both the FEED and EPC were performed as well as Management of Change (MOC) reviews. *Client: Sabine Pass LNG*.

**Process Hazards Analysis (PHA) of a Large LNG Liquefaction Facility**: *Directed* the HAZOP and LOPA studies for a large scale grass roots LNG facility in Australia. Studies for both the FEED and EPC were performed as well as Management of Change (MOC) reviews. *Client: Gladstone LNG*.

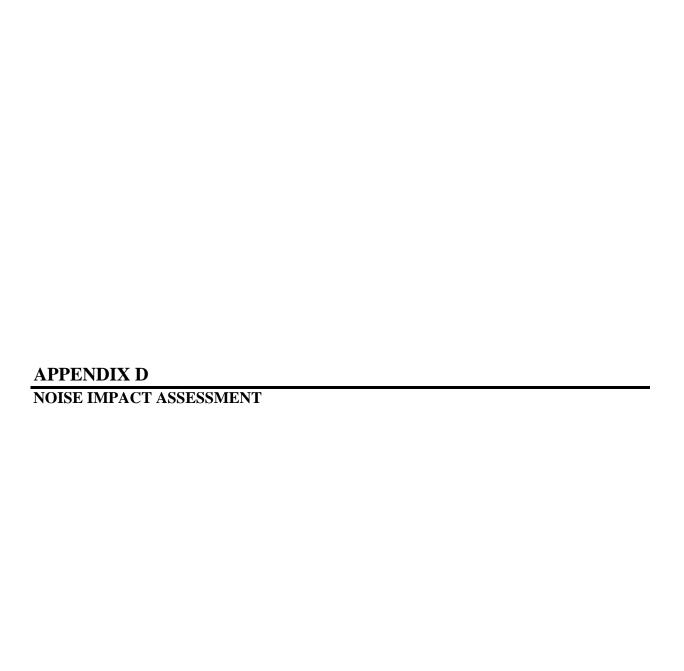
Process Hazards Analysis (PHA) of Multiple Nitrogen Rejection (NRU) and Cryogenic Processing Units: *Directed* the HAZOP and MOC studies for multiple nitrogen rejection and cryogenic units in Texas, New Mexico, and Wyoming. *Client: BCCK Engineering*.

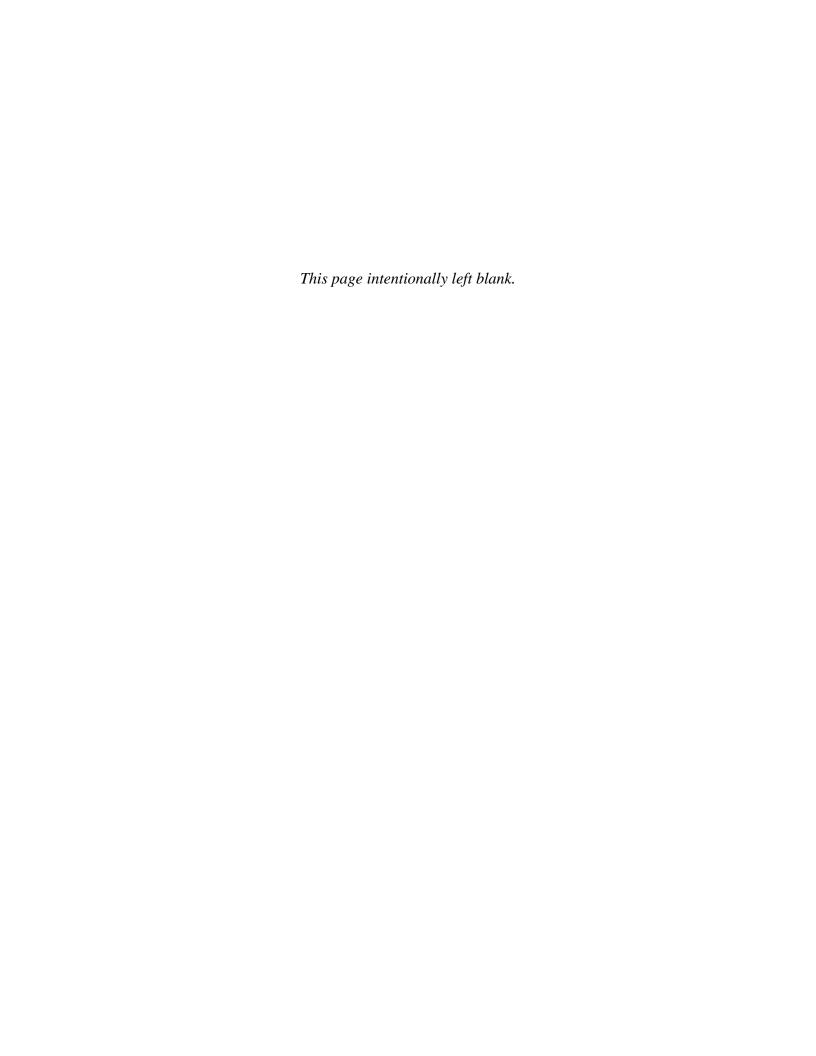
**Process Hazards Analysis (PHA) of a Refinery Crude Unit**: *Directed* the HAZOP for a refinery crude unit. *Client: Caltex Corporation (now part of ChevronTexaco)*.

**Development of an Improved Hydrogen Fluoride Alkylation Catalyst**: *Project Manager* for a research project involving the large scale outdoor release of anhydrous hydrogen fluoride (HF) and hydrogen fluoride mixed with vapor pressure reducing additives. The purpose of the testing was to validate lab scale results with respect to the reduction of aerosol formation of the released HF. *Client: Mobil Research and Development Corporation (now a part of Exxon/Mobil)*.

**Development of an Improved Hydrogen Fluoride Alkylation Catalyst:** *Project Manager* for a research project involving the large scale outdoor release of anhydrous hydrogen fluoride (HF) and hydrogen fluoride mixed with vapor pressure reducing additives. The purpose of the testing was to validate lab scale results with respect to the reduction of aerosol formation of the released HF. *Client: Texaco Inc.(now a part of ChevronTexaco)*.









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## Navcon Engineering Report No. 143110d (Rev D)

## NOISE IMPACT ASSESSMENT

for the

Tesoro LA Refinery Integration and Compliance Project

Prepared for: Environmental Audit, Inc. 1000-A Ortega Way Placentia, CA 92870-7162 Ph. 714-632-8521 Prepared by: Navcon Engineering Network 701 West Las Palmas Drive Fullerton, CA 92835 Ph. 714-441-3488 This page intentionally left blank.

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### 1.0 INTRODUCTION

This report documents the results of the Tesoro Refining & Marketing Company, LLC Los Angeles Refinery Integration and Compliance Project (Project) noise impact assessment. The principal objectives were as follows:

- 1. To determine whether the noise impact during the facility construction will exceed the Project's thresholds of significance, and
- 2. To determine whether noise impact associated with the operation of the new equipment will exceed the Project's thresholds of significance (refer to **Section 4.1**).

The noise impact assessment included the following tasks:

- 1. An environmental noise survey was conducted to document the current ambient noise environment in the residential communities closest to the refinery (refer to **Section 4.2**).
- A three dimensional acoustical model was developed to predict the residential noise impact from the construction activities and from the operation of the new equipment (refer to Section 4.3).
- 3. A noise impact assessment was conducted by comparing the noise levels predicted from the construction activities and operation of the new equipment the thresholds of significance (refer to **Section 4.4**).

The noise impact assessment project was conducted by Hans Forschner and Jim Steedman of Navcon Engineering under the direction of Debbie Bright Stevens, Senior Vice President, Environmental Audit Inc.

### 2.0 TESORO LA REFINERY INTEGRATION AND COMPLIANCE PROJECT OVERVIEW

The purpose of the Tesoro LA Refinery Integration and Compliance Project is to further integrate the Tesoro Wilmington Operations with the Tesoro Carson Operations. As part of the proposed project the operation of the adjacent facilities will be redesigned to comply with federally mandated Tier 3 gasoline specification and State and local regulations mandating emission reductions.

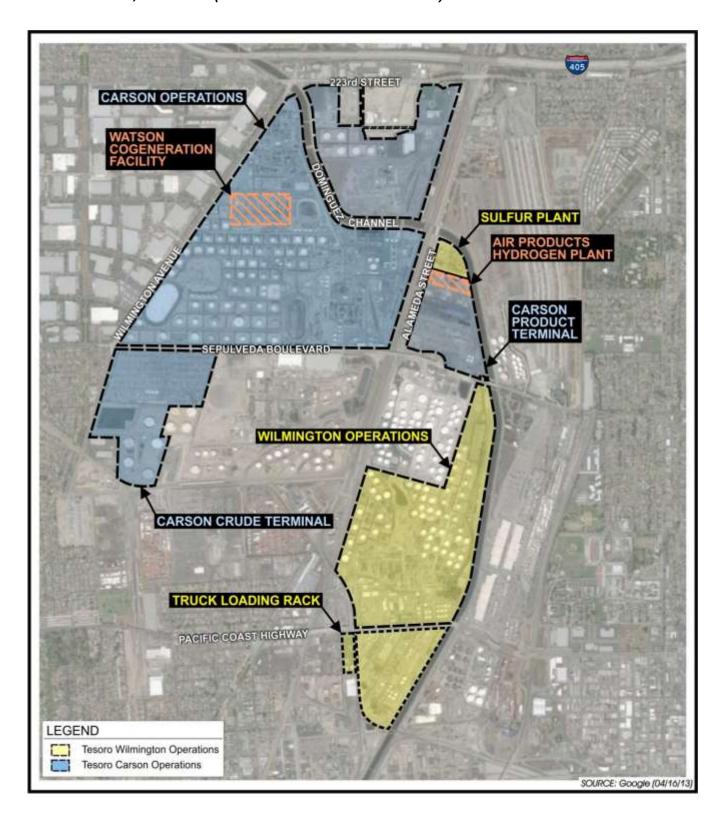
The Tesoro Wilmington Operations is located within Wilmington, a community under the jurisdiction of the City of Los Angeles, at 2101 East Pacific Coast Highway, Wilmington, Los Angeles County, California 90744. The Tesoro Carson Operations is located at 2350 E 223rd Street, Carson, California, 90745. *Aerial Photo 2-1* depicts the Site Location Map. Both new and modified equipment, as well as connecting piping, will be located within portions of the Refinery under both the City of Carson jurisdiction and the City of Los Angeles jurisdiction.

The Wilmington Operations are bounded to the north by Sepulveda Boulevard, to the west by Alameda Street, to the south by railroad tracks, and to the east by the Dominguez Channel (see *Aerial Photo 2-1*). The Wilmington Operations are bisected by Pacific Coast Highway, with the larger portion of the Wilmington Operations to the north of Pacific Coast Highway and the smaller portion to the south. The Refinery and all adjacent areas are zoned for heavy industrial use (M3-1).

The Carson Operations are bounded by Wilmington Avenue to the west, 223rd Avenue to the north, Alameda Street to the east, and Sepulveda Boulevard to the south. The Dominguez Channel flows through the Carson Operations, dividing the property into two sections: Northeastern and Southern (see *Aerial Photo 2-1*). Several industrial/commercial facilities and the 405 Freeway border the Carson Operations to the north. The Alameda Corridor and other industrial facilities, including the Tesoro Coke Barn, the Air Products Hydrogen Plant, and the Tesoro Sulfur Plant, are located to the east of the Carson Operations. Commercial and residential areas are located to the west of the Carson Operations. The Phillips 66 Refinery and tank farms occupy the area located to the south of the Tesoro Carson Operations.

The Carson Operations and all adjacent properties are zoned manufacturing heavy (MH). The closest residential area to the Carson Operations is approximately 250 feet southwest of the Refinery on the southwest corner of the Sepulveda Boulevard/Wilmington Avenue intersection.

## Aerial Photo 2-1, Site Plan (Source: Environmental Audit)



### 3.0 EXECUTIVE SUMMARY

The principal objective of this study was to assess whether the Tesoro LA Refinery Integration and Compliance Project will result in a significant noise impact to the surrounding communities based upon the project's thresholds of significance. The project's thresholds of significance were derived from the project's applicable noise regulations.

The results of the noise analysis concluded that:

- The proposed Tesoro LA Refinery Integration and Compliance Project construction noise will not represent a significant noise impact to the residential communities.
- The proposed Tesoro LA Refinery Integration and Compliance Project operations noise will not represent a significant noise impact to the residential communities.

### 4.0 ENVIRONMENTAL NOISE

## 4.1 Noise Impact Assessment Criteria & Thresholds of Significance

The Tesoro LA Refinery Integration and Compliance Project noise impact assessment criteria are based upon the noise metrics, limits, methods and procedures contained in the City of Los Angeles Municipal Code, the City of Los Angeles Noise Element, the City of Carson Municipal Code, the California Department of Health Services, the Federal Rail Administration, and the Federal Highway Administration. The regulations and codes are described in detail in Tesoro LA Refinery Integration and Compliance Project EIR.

The Tesoro LA Refinery Integration and Compliance Project noise impact assessment was conducted by applying the most stringent limits from each of the regulations listed above. The Project noise limits are described in three thresholds of significance.

- NOI-1 Construction of the proposed Project would have a significant noise impact if construction noise levels exceed the local noise ordinances, or if the noise ordinance is currently exceed, if ambient Community Noise Exposure Levels (CNEL) would be increased by three (3) dBA or more at a noise sensitive receptor during the construction period.
- NOI-2 Operation of the proposed project would have a significant noise impact if proposed project operational noise levels exceed any of the local noise ordinances at the site boundary or, if the noise threshold is currently exceed, ambient CNEL noise levels would be increased by three (3) dBA or more at a noise sensitive receptor.
- **NOI-3** Operation of the new equipment would have a significant noise impact if Daytime ambient noise level (Leq,day) or Nighttime ambient noise level (Leq,night) would be increased by three (3) dBA or more at a noise sensitive receptor.

## 4.2 Environmental Noise Survey

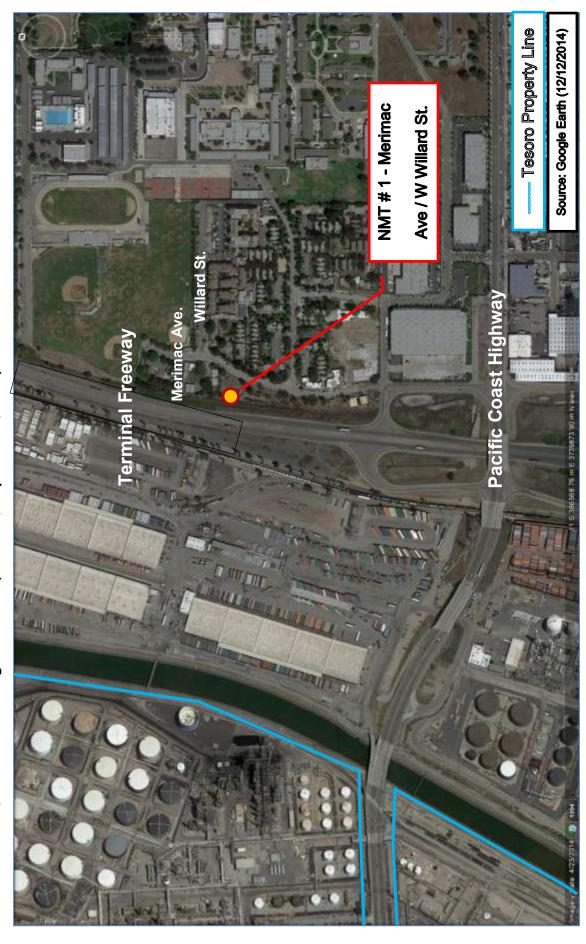
Environmental noise surveys were conducted to characterize the existing ambient noise environment. No immediate residential communities are located to the North or North-East of the facilities. The surveys were conducted between August 29<sup>th</sup>, 2014 and September 18<sup>th</sup>, 2014 and focused on the closest residential communities located to the South-East, South-West and West of the Tesoro Refineries.

The noise monitoring locations are shown in *Aerial Photo 4-1*, *Aerial Photo 4-2*, *Aerial Photo 4-3* and *Photo 4-1* through *Photo 4-4*. The noise data was collected using stationary noise monitoring terminals (NMT). Each NMT was placed in a weatherproof enclosure and collected data continuously throughout the survey period.

The noise monitoring terminals were based upon Larson Davis (LD) Model 831 sound level analyzers, LD PRM813 pre-amplifiers and 377B02 microphones. The analyzers meet the American National Standards Institute (ANSI) S1.4, 1983 specification for Type I (Precision) sound level meters. The system sensitivities were set immediately prior to each survey using a Bruel & Kjaer (B&K) Type 4230 Sound Level Calibrator. The system sensitivities were checked immediately following each survey using the B&K 4230 calibrator to confirm that the sensitivity had not changed. The NMTs are calibrated on an annual basis in accordance with the National Institute of Standards Technology (NIST).

The hourly Leq and L90 levels are presented in *Graphic 4-1* through *Graphic 4-4*. The daytime noise levels (Ld), evening noise levels (Le), nighttime noise levels (Ln) and community noise equivalent noise levels (CNEL) are presented in *Table 4-1*.

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Aerial Photo 4-1, Noise Monitoring Locations (NMT # 1, Sep. 18 - 19, 2014)

Navcon Engineering Report No. 143110d (Rev D), Tesoro LA Refinery Noise Impact Analysis

Aerial Photo 4-2, Noise Monitoring Locations (NMT # 2, Aug. 31 - Sep. 1, 2014, NMT # 3, Aug. 29 – Aug. 30, 2014)

Aerial Photo 4-3, Noise Monitoring Locations (NMT # 4, August 29 – August 30, 2014)



Navcon Engineering Report No. 143110d (Rev D), Tesoro LA Refinery Noise Impact Analysis

Photo 4-1 NMT-1 Merimac Ave / W Willard St.



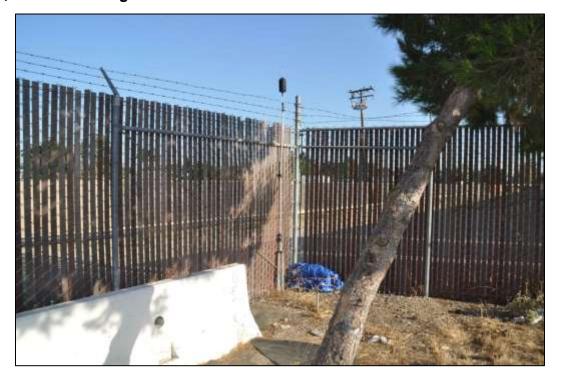
Photo 4-2 NMT-2 Mauretania St / Goodrich Ave.

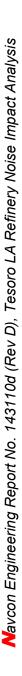


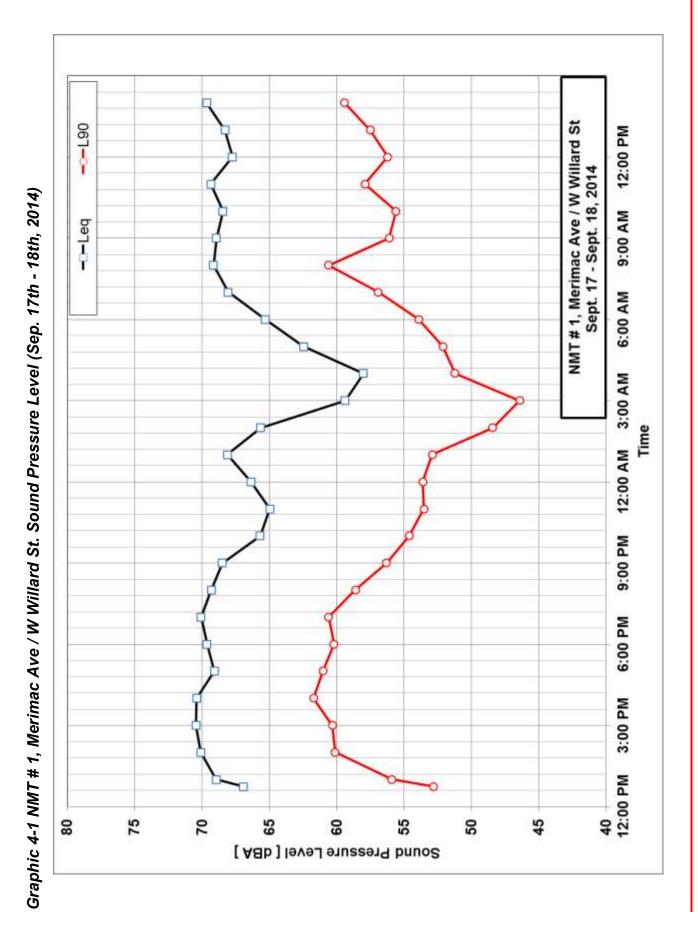
Photo 4-3 NMT-3 Drumm Ave / E Sandison St.

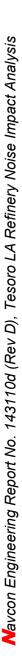


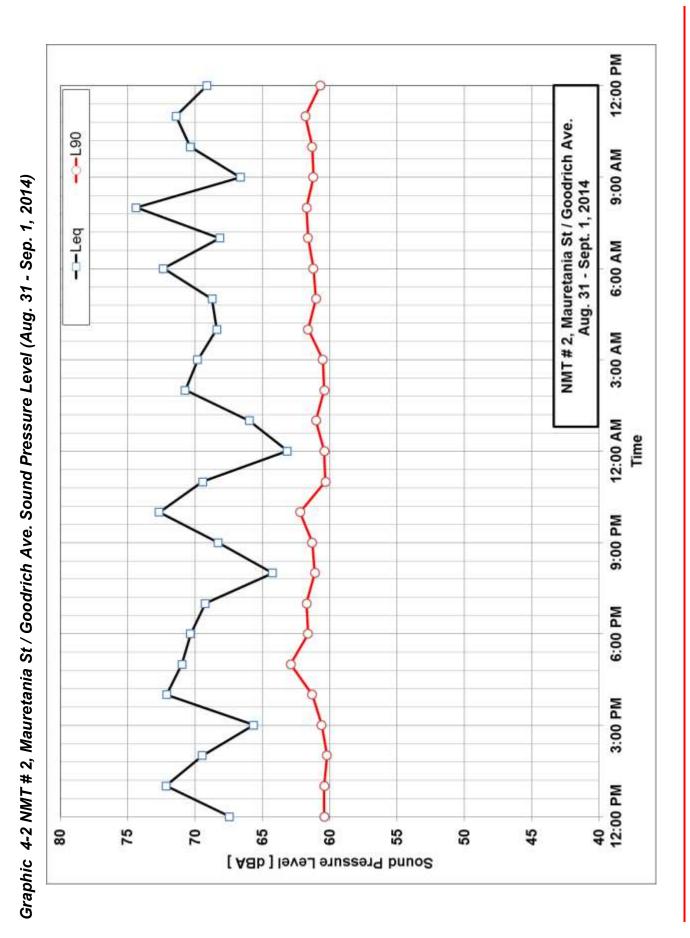
Photo 4-4, NMT-4 Wilmington Ave / E Pacific St.

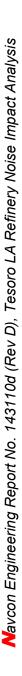


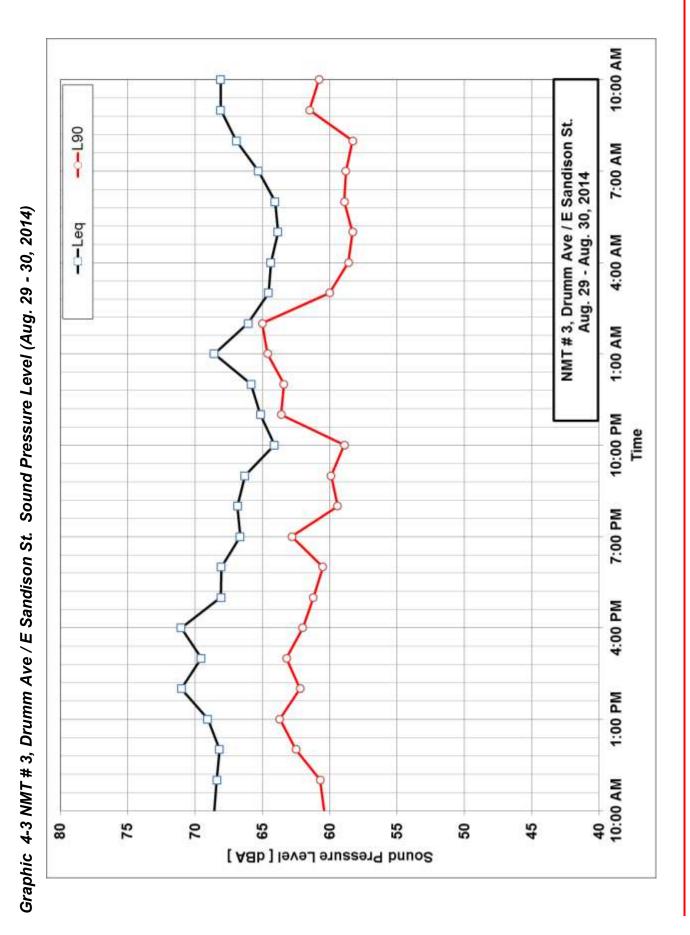


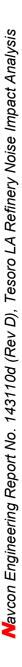












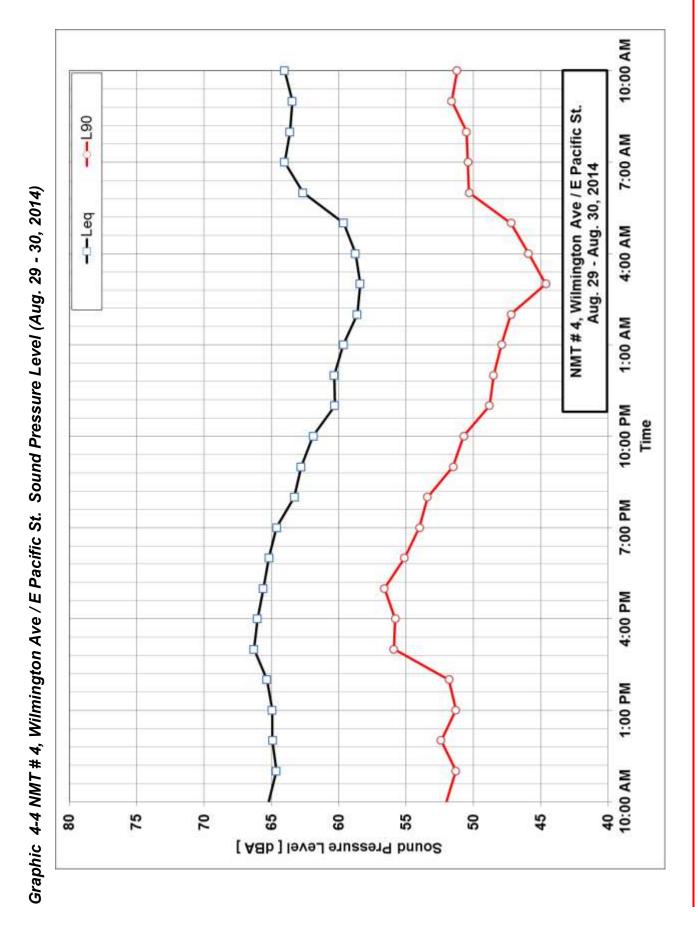


Table 4-1, Noise Monitoring Terminals - Daytime/Evening/Nighttime Levels & CNELs

	Average Hourly Leq				
Time	NMT-1	NMT-2	NMT-3	NMT-4	
00:00:00	66.4	63.1	65.8	60.3	
01:00:00	68.1	66.0	68.6	59.6	
02:00:00	65.6	70.7	66.0	58.6	
03:00:00	59.4	69.8	64.5	58.4	
04:00:00	58.0	68.4	64.4	58.8	
05:00:00	62.5	68.7	63.8	59.6	
06:00:00	65.3	72.3	64.1	62.7	
07:00:00	68.0	68.2	65.3	64.0	
08:00:00	69.1	74.4	66.9	65.8	
09:00:00	68.9	66.6	68.1	64.9	
10:00:00	68.4	70.3	68.5	65.2	
11:00:00	69.3	71.4	68.4	64.6	
12:00:00	67.7	67.4	68.2	64.9	
13:00:00	68.3	72.1	69.1	64.9	
14:00:00	70.1	69.5	71.0	65.3	
15:00:00	70.4	65.6	69.5	66.3	
16:00:00	70.4	72.1	71.0	66.0	
17:00:00	69.1	71.0	68.1	65.6	
18:00:00	69.6	70.3	68.0	65.2	
19:00:00	70.1	69.2	66.6	64.6	
20:00:00	69.3	64.2	66.8	63.3	
21:00:00	68.5	68.3	66.3	62.8	
22:00:00	65.7	72.7	64.1	61.9	
23:00:00	65.0	69.4	65.1	60.3	
CNEL	72.8	76.4	72.7	68.2	
Ldn	72.3	76.3	72.4	67.7	
Leq,day	68.2	69.6	67.8	64.3	
Leq,even	62.3	60.7	59.6	56.6	
Leq,night	64.9	69.8	65.4	60.3	

**CNEL** = The Community Noise Equivalent Level (average level with 5 dB penalty added between 7 pm and 10 pm and a 10 dB penalty added between 10 pm and 7 am)

**Ldn** = Day/Night Noise Equivalent Level (average level with a 10 dB penalty added between 10 pm and 7 am)

**Leq,day** = The Daytime averaged sound pressure level (averaged 7 am to 7 pm)

**Leq,even** = The Evening averaged sound pressure level (averaged 7 pm to 10 pm)

**Leq,night** = The Nighttime averaged sound pressure level (averaged 10 pm to 7 am)

### 4.3 Acoustical Noise Models

The Tesoro LA Refinery Project noise impact was determined by (1) developing three dimensional noise models of the Project, (2) predicting the Project noise levels at the selected community locations and (3) comparing the predicted the noise with the existing community ambient noise levels at the locations described in **Section 4.2**.

The noise models were developed using the noise modeling software, SoundPLAN™. SoundPLAN™ is a standards based program with more than twenty national and international noise modeling guidelines. The following noise prediction standards were used during the performance of this project:

- ISO 9613-1, Acoustics Attenuation of sound during propagation outdoors Part 1: Calculation of the absorption of sound by the atmosphere
- ISO 9613, Acoustics -- Attenuation of sound during propagation outdoors Part 2, Acoustics Attenuation of Sound During Propagation Outdoors

The noise model geometry is presented in *Figure 4-1* through *Figure 4-7*. The sides of the tanks, containers, buildings, etc. were modeled as reflective surfaces and also as diffractive bodies (the yellow and gray shaded surfaces). The Noise Sources are shown as red spheres (point sources) and red surfaces (area sources). A light blue line outlines the perimeter of each operation. The surrounding roads are displayed as grey surfaces. Most of the ground within the refinery and adjacent areas are covered with gravel, concrete or asphalt. Therefore, it was modeled as a hard reflective surface with an absorption coefficient of 0.25.

### **Construction Noise Model:**

- The Project will include 23 construction activities scheduled over a 5 year period. The
  Construction Noise Model represents a worst case scenario by assuming that all
  construction activities are performed at the same time.
- The construction equipment noise emission levels were based upon FHWA Roadway Construction Noise Model (RCNM Manual).

- The construction equipment was modeled as a line of stationary point sources along the pipe-ways. The noise level predicted from each point source location and the maximum predicted was used for the noise impact assessment.
- During plant operation the construction activities were assumed to take place during a single twelve hour work shift (7 am to 7 pm). During project related shutdowns / turnarounds, the construction activities were assumed to be conducted during two twelve hour shifts (i.e., 24 hours per day).

## **Operational Noise Model:**

- The operational noise model includes all new noise producing equipment.
- The sound power emission levels of the new equipment were estimated using the equipment dimensions (L x W x H) and a sound pressure level of 85 dBA at a distance of 3 foot. The equipment dimensions were provided by Tesoro engineers. Refineries in general are specifying an 85 dBA noise limit for all new equipment. The 85 dBA noise limit originates from the regulation set forth by the Occupational Safety Health Administration (OSHA).

The detailed noise model input data is presented in **Section 5.0, Appendix A, Three Dimensional Noise Model Input Data**.

Figure 4-1 Model Geometry with Topo Data - 3D View Wilmington Operation from South

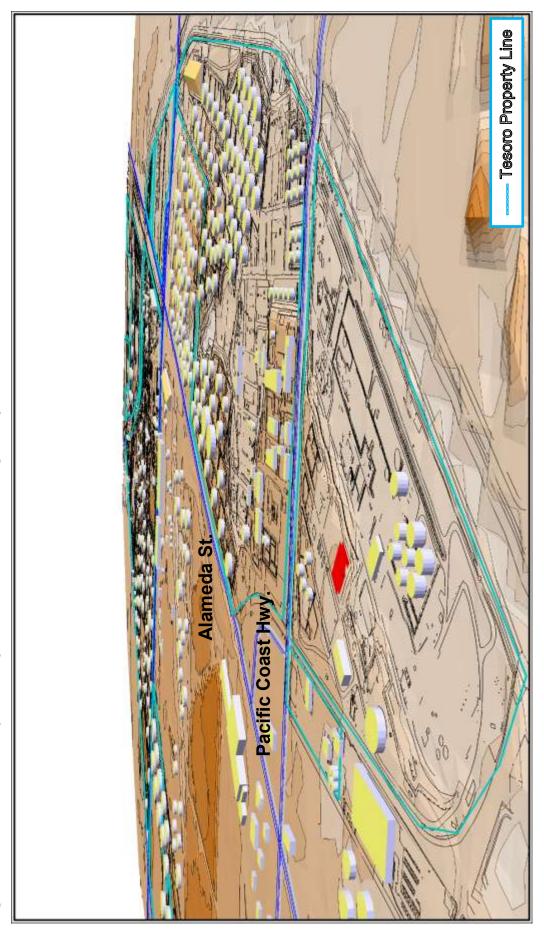
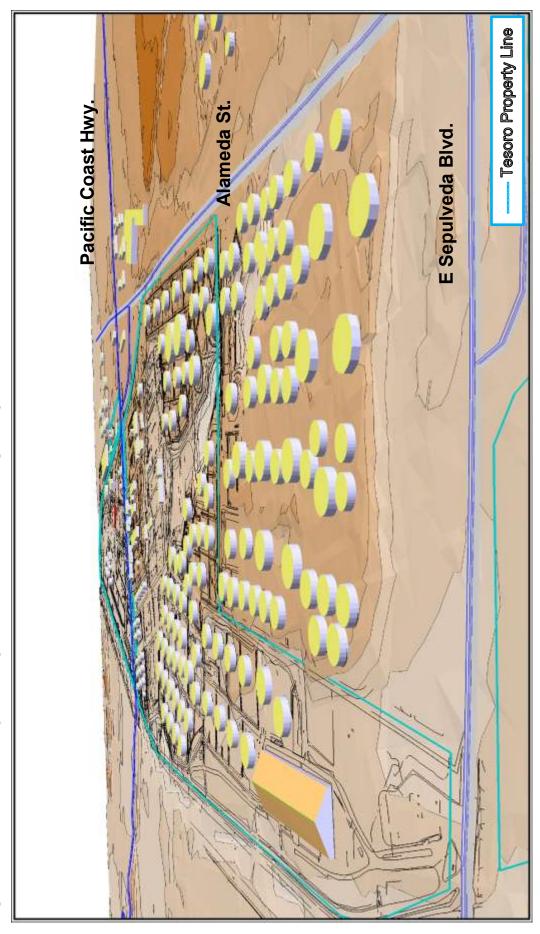
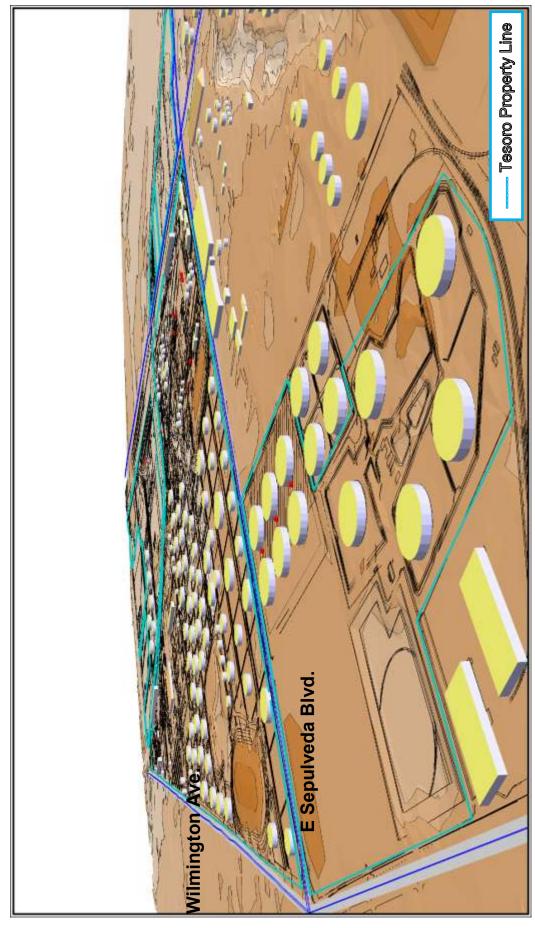


Figure 4-2 Model Geometry with Topo Data - 3D View Wilmington Operation from North





Tesoro Property Line E Sepulveda Blvc Alameda St.

Figure 4-4 Model Geometry with Topo Data - 3D View Carson Operation from South East

Tesoro Property Line ameda St

Figure 4-5 Model Geometry with Topo Data - 3D View Carson Operation from East



Figure 4-6 Model Geometry Construction Tesoro Refinery (Carson, Wilmington) - 2D View

NMT # 2, Mauretania St / Goodrich Ave. NMT # 1, Merimac Ave / W Willard St. NMT # 3, Drumm Ave / E Sandison St. NMT # 4, Wilmington Ave / E Pacific St. Tesoro Property Line ameda St.

Figure 4-7 Model Geometry New Equipment Tesoro Refinery (Carson, Wilmington) - 2D View

### 4.4 Acoustical Noise Model Assessment

The 3D acoustical model was used to generate noise contour maps over the refinery property and adjacent residential communities.

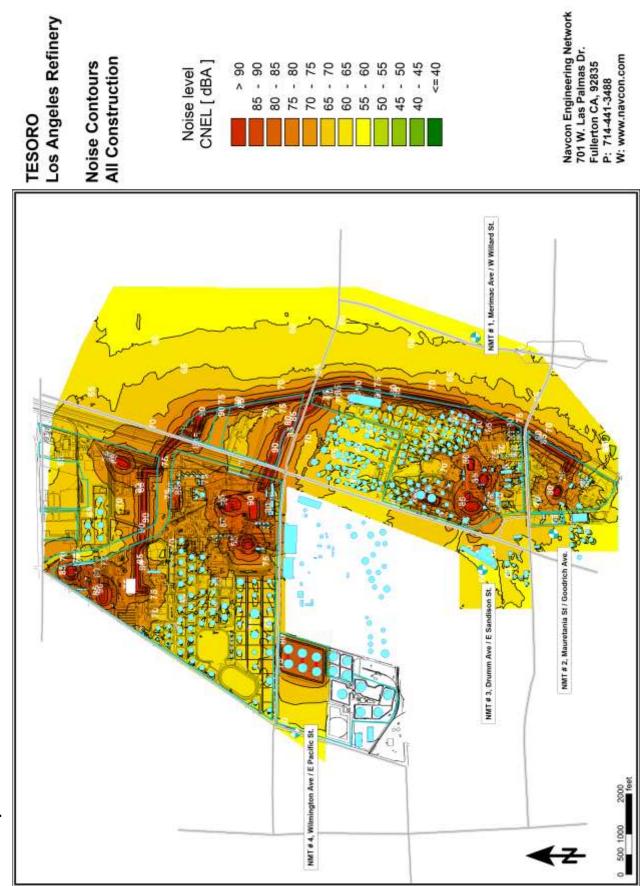
- The Plant Construction Noise contours are shown in Noise Map 4-1, Noise Map 4-2 and
   Noise Map 4-3 (CNEL, Leg,day, Leg,night respectively).
- The Plant Operational Noise contours are shown in Noise Map 4-4 and Noise Map 4-5
   (CNEL and Leq,day/Leq,night respectively).

The 3D acoustical model was used to predict the noise level at the four sensitive receptor locations.

- The sensitive receptor locations are listed in Table 4-2.
- The change in noise level predicted during the Plant Construction is listed in Table 4-3.
- The change in noise level predicted during the Plant Operation is listed in *Table 4-4*.

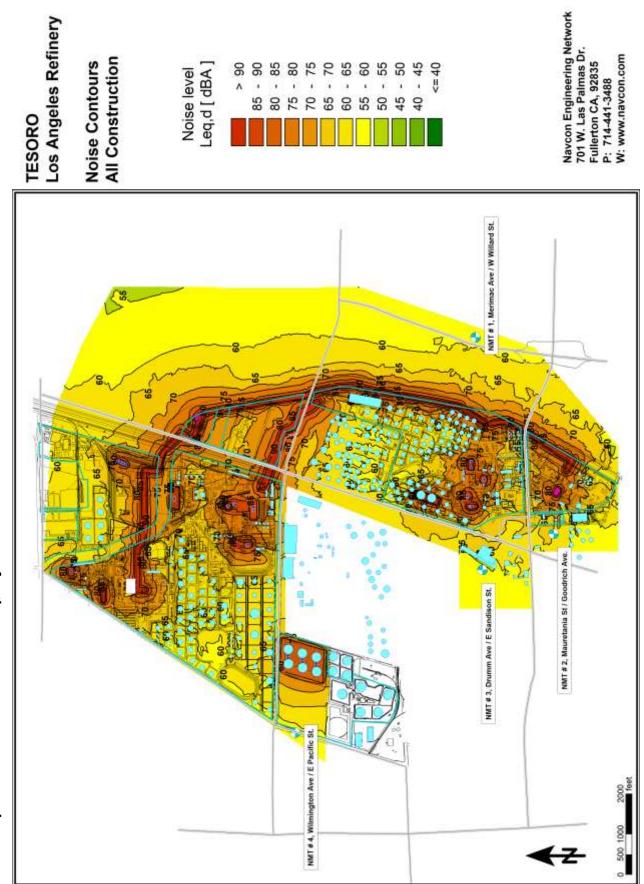
The noise level predictions indicate that the Tesoro LA Refinery Integration and Compliance Project are below all of the significance thresholds and do not exceed any of the significance thresholds.

Noise Map 4-1 Plant Construction CNEL Contours



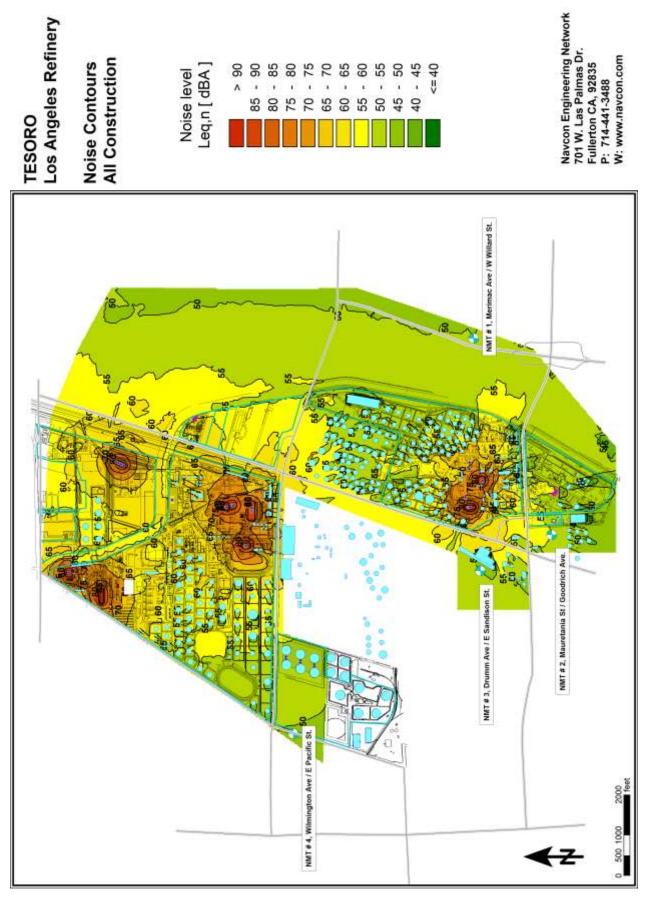
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Noise Map 4-2 Plant Construction Leq, day Contours



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Noise Map 4-3 Plant Construction Leq, night Contours



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- 65 - 60 - 55 - 50

65 55 50 50

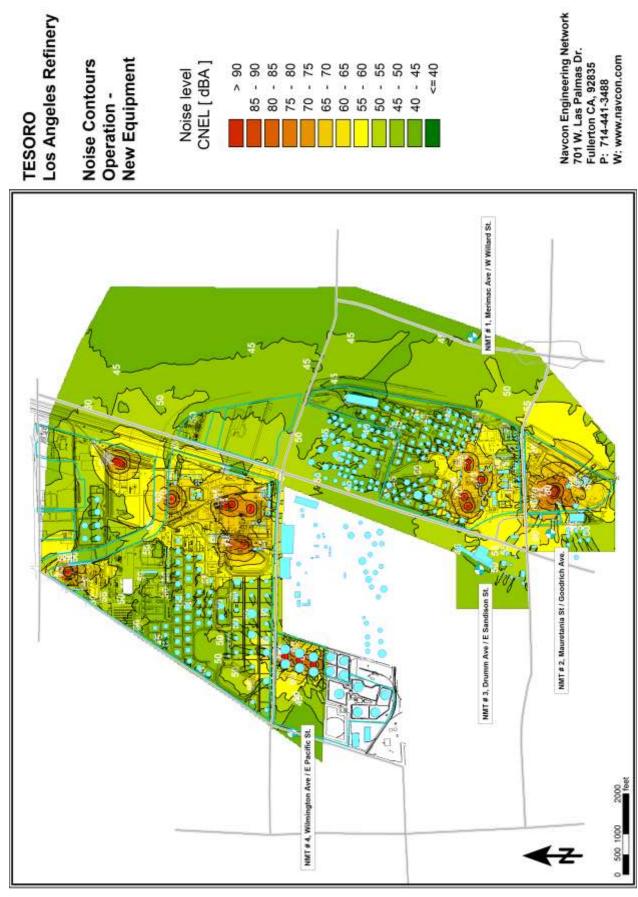
<= 40

45

- 80

12 2

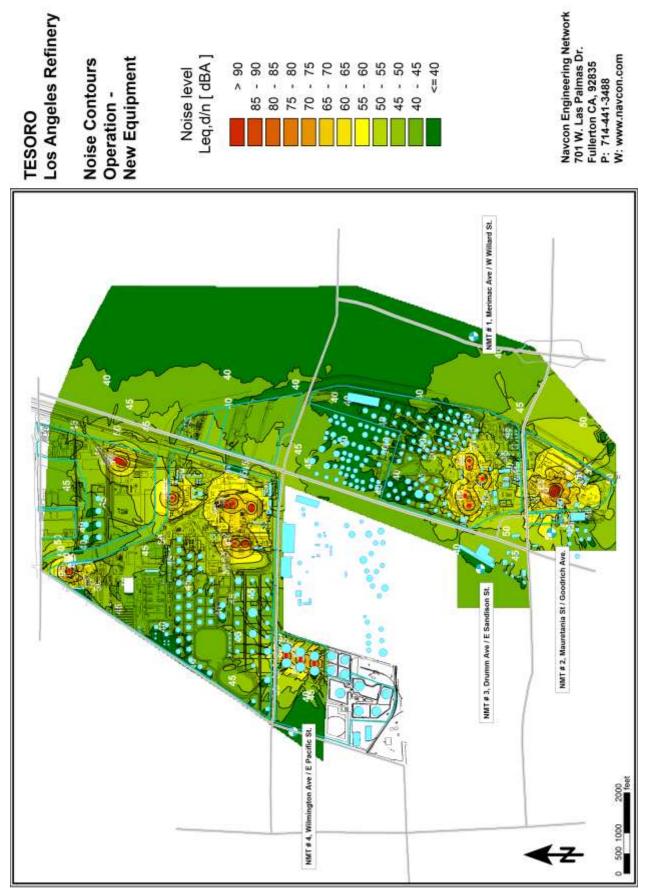
Noise Map 4-4, Plant Operation CNEL Contours (New Equipment Only)



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2

Noise Map 4-5, Plant Operation Leg, day / Leg, night Contours (New Equipment Only)



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Table 4-2, Project Sensitive Receptor Locations

NMT	Address	City, State
#1	Merrimac Ave. / W Willard St.	Long Beach, CA
#2	Mauretania St. / Goodrich Ave.	Los Angeles, CA
#3	Drumm Ave. / E Sandison St.	Los Angeles, CA
#4	Wilmington Ave. / E Pacific St.	Carson, CA

Table 4-3, NOI-1 Construction Noise CNEL (Baseline vs. Baseline & Construction)

	Baseline 2014		Co	Construction			Baseline & Construction			Overall Change		
Receptor Location	CNEL	p'bə7	Leq,n	CNEL	p'bə7	Leq,n	CNEL	p'bə7	Leq,n	CNEL	p'bə7	Leq,n
NMT#1, Merrimac Ave. / W Willard St.	72.8	69.2	64.9	59.0	57.7	50.2	73.0	69.5	65.1	0.2	0.3	0.1
NMT #2, Mauretania St. / Goodrich Ave.	76.4	70.1	69.8	64.4	63.7	54.9	76.7	71.0	69.9	0.3	0.9	0.1
NMT#3, Drumm Ave. / E Sandison St.	72.7	68.4	65.4	58.6	57.2	50.0	72.9	68.7	65.6	0.2	0.3	0.1
NMT #4, Wilmington Ave. / E Pacific St.	68.2	65.0	60.3	59.0	58.2	49.6	68.7	65.8	60.6	0.5	0.8	0.4

**Note**: The noise level predictions indicate that the construction activities will have a negligible impact at the residential locations. The largest increase in the Community Noise Exposure Level (CNEL) is predicted to be 0.3 dBA. The largest daytime increase (Leq,day) is predicted at 0.9 dBA while the largest nighttime increase (Leq,night) is predicted at 0.4 dBA. The predicted change in noise level is less than the threshold of significance, 3 dB (refer to **Section 4.1**).

Table 4-4, NOI-2 & NOI-3 New Equipment CNEL, Leq,d/n (Baseline vs. Baseline with Equip.)

			Measured ine Levels		Predicted New Equipment Levels			2014 Baseline + New Equipment			Predicted Change (+ increase)		
Receptor Location	CNEL	Ped,d	Leq,n	CNEL	p'bə7	Leq,n	CNEL	Ped,d	Leq,n	CNEL	Ped,d	Leq,n	
NMT #1, Merrimac Ave. / W Willard St.	72.8	69.2	64.9	45.5	38.8	38.8	72.8	69.2	64.9	0.0	0.0	0.0	
NMT #2, Mauretania St. / Goodrich Ave.	76.4	70.1	69.8	58.9	52.2	52.2	76.5	70.2	69.9	+ 0.1	+ 0.1	+ 0.1	
NMT #3, Drumm Ave. / E Sandison St.	72.7	68.4	65.4	45.2	38.6	38.6	72.7	68.4	65.4	0.0	0.0	0.0	
NMT #4, Wilmington Ave. / E Pacific St.	68.2	65.0	60.3	42.4	35.8	35.8	68.2	65.0	60.3	0.0	0.0	0.0	

**Note**: The noise level predictions indicate that the Plant operation will have a negligible impact at the residential locations. The largest increases in the Community Noise Exposure Level (CNEL), the daytime level (Leq,day) and the nighttime level (Leq,night) is predicted to be 0.1 dBA. The predicted change in noise level is less than the threshold of significance, 3 dB (refer to **Section 4.1**).

# 5.0 APPENDIX A, THREE DIMENSIONAL NOISE MODEL INPUT DATA

Table 5-1, Noise Model Operational Data Proposed Project

No.	Plant	Equipment	Number of New Equipment	Lw, dBA
		Heat Exchanger	5	n/a
1	No. 51 Vacuum Unit Modifications ( C )	Pumps (Electric)	3	102
		Coalescers	2	n/a
		Heat Exchanger	3	n/a
2	нси (с)	Pumps (Electric)	2	106
		Knockout drum	1	n/a
3	Interconnecting Pipelines	Pumps (Electric)	2	n/a
		Steam Generators	1	n/a
4	HCU Modification (W)	Air Cooler		103
		Pumps (Electric)	2	100
5	Liquid Petroleum Gas (LPG) Rail Unloading (C)	Pumps (Electric)	4	102
3	Liquid Petroleum Gas (LPG) Rail Unloading (C)	Ten additional rail cars		n/a
		Pumps (Electric)	4	101
		Heat Exchanger	11	n/a
6	HTU-4 (W)	Surge drum	1	n/a
		Salt dryer	1	n/a
		Coalescer	1	n/a

Table 5-2, Noise Model Operational Data Proposed Project (Cont'd)

No.	Plant	Equipment	Number of New Equipment	Lw, dBA
		tower	1	n/a
		caustic scrubber	1	n/a
		K/O drums	2	n/a
		coalescer	1	n/a
7	Naphtha HDS Unit Modification ( C )	accumulator	1	n/a
		condensate pot	1	n/a
		heat exchnagers	14	n/a
		air cooler	1	108
		pumps (electric)	6	101
		Gas Treater	1	n/a
		Tower	1	n/a
8	Naphtha Isomerization Unit Modifications (C)	Flash drum	2	n/a
		Heat Exchanger	n/a	
		Pumps (Electric)	4	101
		Heat Exchanger	6	n/a
9	Alkylation Modification(C)	Filter/Coalescer	1	n/a
9	Aikylation Woulineation (C)	Truck loading rack	1	n/a
		Pumps (Electric)	2	101
10	Mid Barrel Distillate Treater	Piping		n/a

Table 5-3, Noise Model Operational Data Proposed Project (Cont'd)

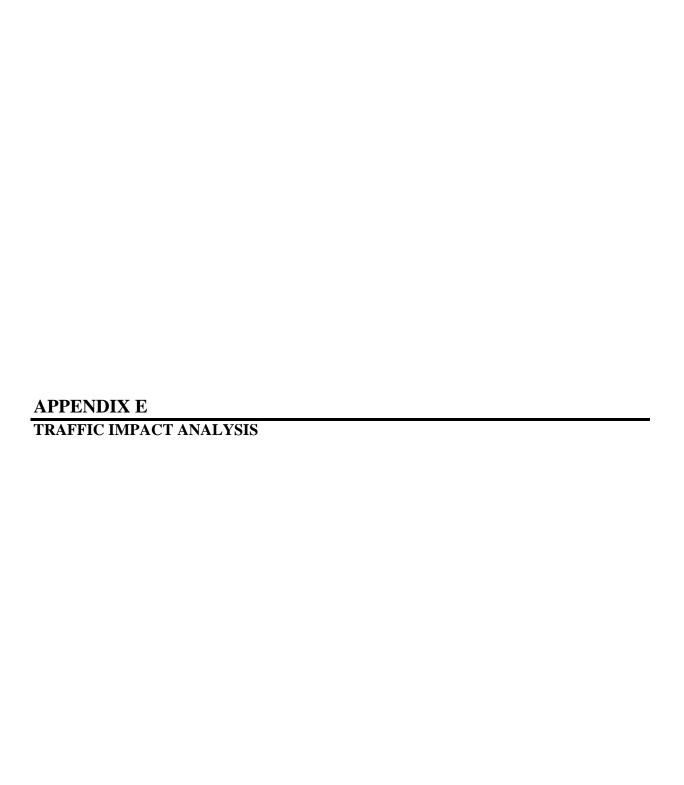
No.	Plant	Equipment	Number of New Equipment	Lw, dBA
		Heat Exchanger	5	n/a
		Steam Nozzle	1	n/a
10	LHU Modifications (C)	Coalescer	1	n/a
		Salt Dryer		n/a
		Condensate pot	1	n/a
		Pumps (Electric)	6	101
13	New Wet Jet Treater ( C )	Reactors 2	2	n/a
13	New Wet Jet Treater ( C )	Product Separators	2	n/a
		loading facility	1	n/a
14	New Crude Tankage ( C )	Pumps (Electric)	5	105
		Pumps (Electric)	4	101
15	PTSU ( W )	Absorbers		n/a
		Dryers		n/a
		Heat Exchanger	3	n/a
15	CRU-3 ( W )	Pumps (Electric)	4	101
		Depropanizer tower	1	n/a
		Heat Exchanger	5	n/a
16	HTU-1 ( W )	Pumps (Electric)	1	101
		Feed Surge Drum		n/a
16	HTU-2 ( W )	Pumps (Electric)	2	101

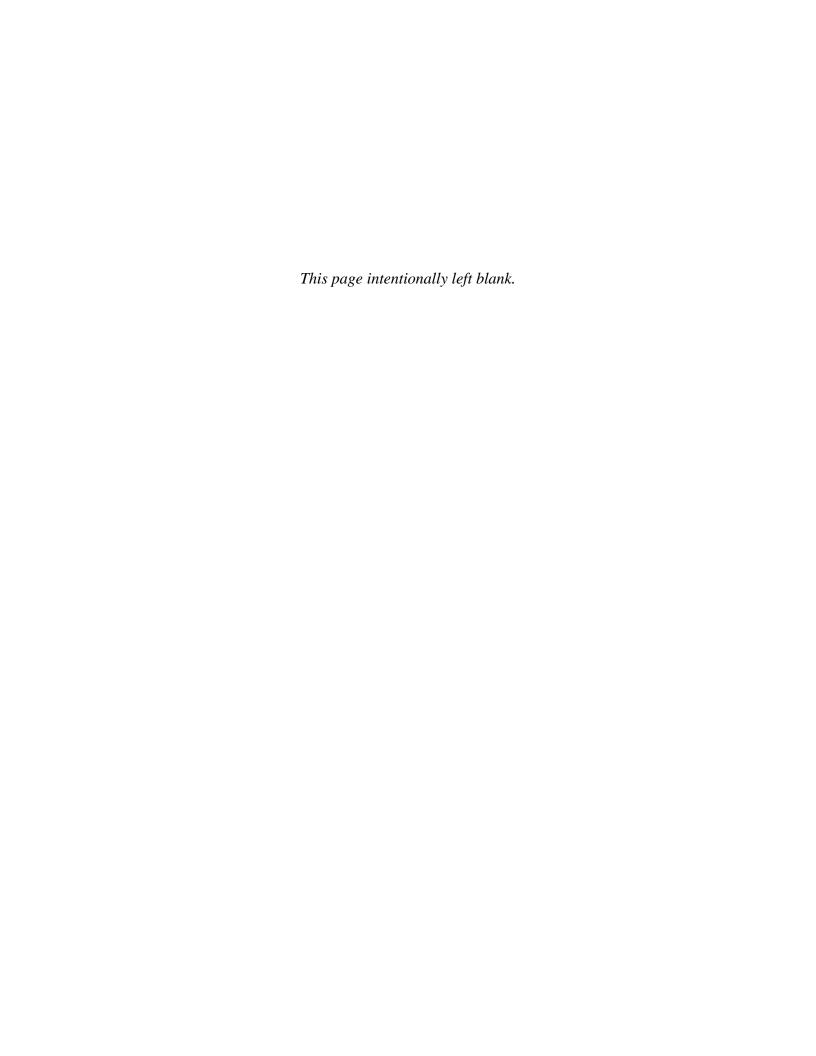
Table 5-4, Noise Model Operational Data Proposed Project (Cont'd)

No.	Plant	Equipment	Number of New Equipment	Lw, dBA
		Pumps (Electric)	8	102
		Gas Fired Furnace	1	106
		Air Heater	1	n/a
17	Sulfuric Acid Regeneration Plant ( W )	Steam Generator	1	107
		Blower	n/a	
		Heat Exchanger	n/a	
		Compressor	1	108
18, 19	SCAQMD Rule 1114 –Coker Venting( C )	Venturi	1	109
21	Wilmington Replacement Crude Tanks ( W )	None		n/a

Table 5-5, Noise Model Input Data Construction Noise Emission Levels

		Octave Band Sound Power Level [ dBA]							Sound Power	
Name	Shift (1/2)	63Hz	125Hz	250Hz	500Hz	1kHz	2kHz	4kHz	8kHz	Lw
No. 01 No 51 Vacuum Unit Mod Construction	2	92	108	118	118	120	118	112	104	125
No. 02 HCU Construction ( C )	2	92	107	117	118	119	117	111	103	124
No. 03-11 Horiz. Drilling Equipment New Pipeline	1	82	97	107	108	109	107	101	93	114
No. 3 Interconnecting Pipe Construction	1	97	112	123	123	124	123	116	108	130
No. 04 HCU Modification Construction ( W )	2	91	106	117	117	118	116	110	102	123
No. 05 Rail Car Unloading Construction	2	90	105	116	116	117	116	109	101	123
No. 06 HTU-4 Construction	2	92	107	118	118	119	118	111	103	125
No. 07 Alky Construction	2	92	107	118	118	119	118	111	103	125
No. 08 Naphtha Isomerization Construction	2	89	104	115	115	117	115	108	100	122
No. 09 Alkylation Construction	2	90	105	116	116	117	116	109	101	123
No. 10 LHU Modifications Construction	2	92	107	118	118	119	118	111	103	125
No. 13 New Wet Jet Treater Construction	1	92	107	118	118	119	118	111	103	125
No. 14 New Crude Tank Construction	1	95	110	121	121	122	120	114	106	127
No. 15 PSTU Construction	1	93	108	119	119	120	119	112	104	126
No. 16 HTU-1 Construction	1	93	108	118	119	120	118	112	104	125
No. 17 Sulfuric Acid Regeneration Plant	1	95	110	120	121	122	120	114	106	127
No. 18, 19 Coker Unit Construction	1	91	106	116	117	118	116	110	102	123
No. 20 Drilling Equipment New Electrical	1	93	109	119	119	121	119	113	105	126
No. 20 Electrical Line Construction	1	93	109	119	119	121	119	113	105	126
No. 21 Crude Tanks Equipment Construction	1	97	112	122	123	124	122	116	108	129
No. 22 Naphtha Isom Equipment	1	89	104	115	115	116	114	108	100	121





Submitted by:



TESORO LOS ANGELES REFINERY INTEGRATION
AND COMPLIANCE PROJECT

Traffic Impact Analysis

Draft Report

Submitted to:

**South Coast Air Quality Management District** 

April 27, 2015

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# 1.0 INTRODUCTION

This report summarizes the methodology and results of a traffic impact analysis for the proposed Tesoro Refining & Marketing Company LLC (Tesoro) Los Angeles Refinery Integration and Compliance Project (proposed Project) located in the Cities of Los Angeles and Carson, California. This report follows guidelines provided by the South Coast Air Quality Management District, the California Department of Transportation, Los Angeles County and the Cities of Los Angeles and Carson.

The traffic study will look at several scenarios to describe baseline and future conditions without the project, during the construction of the project, and in the operational phase of the project. This includes analysis of baseline conditions, peak construction activities, and year 2021 traffic conditions which represent future traffic growth and operating conditions at study locations due to ambient growth, a cumulative interchange realignment project at I-405/Wilmington Avenue, and traffic generated by the proposed project. Therefore this analysis addresses the proposed project's contribution to cumulative traffic growth and congestion.

## 1.1 PROJECT DESCRIPTION

In June 2013, Tesoro purchased the BP West Coast Products LLC (BP) Carson Refinery, which will be further integrated with the adjacent Tesoro Los Angeles Refinery – Wilmington Operations to form the Tesoro Los Angeles Refinery (Refinery). The Refinery includes: (1) the Wilmington Operations located at 2101 East Pacific Coast Highway in the Wilmington District of the City of Los Angeles; and (2) the Carson Operations, which is the former BP Carson Refinery located at 2350 East 223rd Street in the City of Carson. The proposed project will be designed to better integrate the Tesoro Wilmington Operations and Tesoro Carson Operations.

The proposed project will occur at both the Wilmington and Carson Operations of the Tesoro Los Angeles Refinery. Tesoro will further integrate the recently purchased adjacent BP Carson Refinery (currently referred to as the Tesoro Los Angeles Refinery Carson Operations) with the existing Tesoro Los Angeles Refinery (currently referred to as the Tesoro Los Angeles Refinery Wilmington Operations). Together, the Wilmington and Carson Operations comprise the complete Tesoro Los Angeles Refinery (the Refinery).

The Tesoro Los Angeles Refinery is approximately 950 contiguous acres in size and operates within the Cities of Los Angeles and Carson. The Tesoro Wilmington Operations is located within Wilmington, a community under the jurisdiction of the City of Los Angeles, at 2101 East Pacific Coast Highway, Wilmington, Los Angeles County, California 90744. The Tesoro Carson Operations is located at 2350 East 223rd Street, Carson, California, 90745.

As part of the proposed project, both new and modified equipment, as well as connecting piping, will be located within portions of the Refinery under both the City of Carson jurisdiction and the City of Los Angeles jurisdiction.

The Wilmington Operations are bounded to the north by Sepulveda Boulevard, to the west by Alameda Street, to the south by railroad tracks, and to the east by the Dominguez Channel. The Wilmington Operations are bisected by Pacific Coast Highway, with the larger portion of the Wilmington Operations to the north of Pacific Coast Highway and the smaller portion to the south. The Refinery and all adjacent areas in the Cities of Carson and Los Angeles are zoned for heavy industrial use.

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The Carson Operations are bounded by Wilmington Avenue to the west, 223rd Avenue to the north, Alameda Street to the east, and Sepulveda Boulevard to the south. The Dominguez Channel flows through the Carson Operations, dividing the property into two sections: Northeastern and Southern. Several industrial/commercial facilities and the 405 Freeway border the Carson Operations to the north. The Alameda Corridor and other industrial facilities, including the Tesoro Coke Barn, the Air Products Hydrogen Plant, and the Tesoro Sulfur Recovery Plant (SRP), are located to the east of the Carson Operations. Commercial and residential areas are located to the west of the Carson Operations. The Phillips 66 Refinery and tank farms occupy the area located to the south of the Tesoro Carson Operations. Additionally, the SRP (considered to be a portion of the Tesoro Wilmington Operations) is located at 23208 South Alameda Street in the City of Carson.

Construction activities for the proposed Project are expected to begin in third quarter of 2015 and are expected to be completed by first quarter of 2021, based on preliminary project engineering. The preliminary construction schedule for each component of the proposed project varies. The construction activities for most of the components are expected to overlap from about December 2015 to February 2017. Construction work shifts are expected to last about ten hours per day during most portions of the construction schedule. During normal construction periods, one work shift per day is expected.

Construction period employee trips will access the proposed Project site at three parking lots: parking for 550 workers will be provided from 223<sup>rd</sup> street at the northern portion of the proposed Project site, parking for 200 workers will be provided off of Alameda Street to the immediate north of Sepulveda Boulevard, and parking for 200 workers will be provided from Sepulveda Boulevard to the east of Alameda Street.

Completion of the proposed Project will result in the permanent addition of approximately ten daily truck roundtrips from the proposed Project site:

- There will be no increase in workers as compared to baseline conditions following completion of the construction phase
- Eight trucks per day will transport spent sulfuric acid from the Carson Plant to the new Sulfuric Acid Plant at Wilmington
- One truck per day will transport other materials and supplies to or from the Refinery

The project site location as well as the location of the construction worker parking lots is shown in Figure 1.



### 1.2 STUDY AREA

The following thirteen (13) intersections were identified for inclusion in the traffic impact analysis:

- 1. Wilmington Avenue/I-405 Northbound Ramps;
- 2. Wilmington Avenue/I-405 Southbound Ramps;
- 3. Wilmington Avenue/223<sup>rd</sup> Street;
- 4. Alameda Street/I-405 Northbound Ramps;
- 5. Alameda Street/223<sup>rd</sup> Street (along Alameda Street);
- 6. Alameda Street/223<sup>rd</sup> Street (along 223<sup>rd</sup> Street);
- 7. Alameda Street/Sepulveda Boulevard (along Alameda Street);
- 8. Alameda Street/Sepulveda Boulevard (along Sepulveda Boulevard);
- 9. I-405 Southbound Ramps/223<sup>rd</sup> Street;
- 10. Terminal Island Freeway (SR-103)/Sepulveda Boulevard;
- 11. Santa Fe Avenue/Sepulveda Boulevard;
- 12. SR-710 SB Ramps/Willow Street; and
- 13. SR-710 NB Ramps/Willow Street.

**Figure 2** illustrates the study area including the locations of the study intersections analyzed in this report. The existing lane configurations of the study intersections are illustrated in **Figure 3**.





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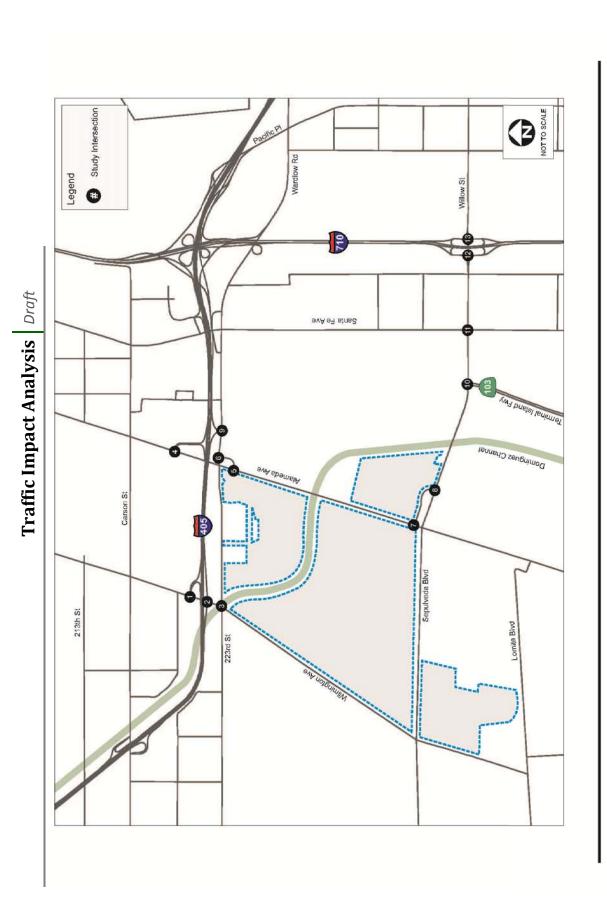


FIGURE 2 Study Intersection Locations

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FIGURE 3
Baseline Intersection Lane Configurations

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## 1.3 STUDY ANALYSIS PERIODS

Traffic Operations are evaluated for each of the following scenarios during the weekday a.m. peak hour and the p.m. peak hour:

- Baseline (Existing) Conditions
- Baseline Conditions Plus Construction Conditions (2015)
- Year 2021 Without Project
- Year 2021 With Project Operations

Baseline (existing) conditions are obtained from turning movement traffic counts taken in August 2014 during the peak hours of operations (6:00 a.m. to 9:00 a.m. and 4:00 p.m. to 6:00 p.m.) as well as existing roadway signal and geometric conditions. These conditions include the trips to and from the proposed Project site and the parking lots to be used for the construction trips associated with the proposed Project. Based on traffic counts of those driveways, there are a total of 1,312 daily trips generated by these parking areas in the baseline conditions: 135 daily trips from the 223<sup>rd</sup> Street parking lot, 912 daily trips from the Alameda Street parking lot, and 265 daily trips from the Sepulveda Boulevard parking lot.

The trips associated with the construction of the proposed Project were added to the baseline traffic counts to evaluate construction conditions. The proposed Project will have several phases requiring a variable number of construction-related trips. For this analysis, the peak number of trips to be generated over the two-year construction period was used to determine the potential for significant impacts at the study locations<sup>1</sup>. It was assumed the trips associated with current operations on the proposed Project site would occur at the same rate as in the baseline conditions.

The I-405/Wilmington Avenue Interchange began a major improvement project in November 2013 which is expected to be completed by late 2015 or early 2016. The geometrics at the study locations associated with the interchange are assumed to be the pre-construction configuration in the near-term construction period analysis—the construction activities prior to the traffic counts did not change the number of lanes or connections provided by the interchange. The I-405/Wilmington Avenue Interchange construction involves periodic closures and openings of geometric and operational improvements on a constant (daily, weekly, and monthly) but inconsistent basis over the course of its construction period, and while these many iterations of the I-405/Wilmington Avenue interchange construction period conditions were not specifically analyzed in this study, it is recommended that the construction schedule of the Interchange be integrated into the traffic management planning and scheduling for trips associated with the proposed Project for the duration of the overlapping construction periods.

Ambient (background traffic) Year 2021 Conditions were forecasted based on the annualized ambient growth as determined from the Southern California Association of Governments (SCAG) regional travel

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<sup>&</sup>lt;sup>1</sup> As explained in more detail in *Section 3.0 Construction Conditions*, below, during the majority of the construction period, only one work shift per day is expected. However, during peak construction activities, the project is expected to require two shifts per day, a day and night shift.

demand model. The proposed Project area annualized growth was calculated based on the growth between the two analysis years of the travel demand model (2012 to 2035) along Wilmington Avenue and Alameda Street from 223<sup>rd</sup> to Sepulveda Boulevard and along Sepulveda Boulevard and 223<sup>rd</sup> Street from Wilmington Avenue to Alameda Street. The annualized growth rate was calculated to be 0.4 percent per year. The completion of the I-405/Wilmington Avenue Interchange improvement project is assumed in the 2021 Project Operations scenario. The proposed Project operations are estimated to not increase the number of on-site workers after the opening of the proposed project, however approximately ten additional truck round-trips per work day would result from the proposed Project to support its operations.

### 2.0 BASELINE CONDITIONS

This section presents an overview of the existing roadway system and transit operations within the study area and the methodology used to determine existing traffic volumes.

### 2.1 ROADWAY CONFIGURATIONS

The existing configurations of the roadways within the study area are described as follows:

Wilmington Avenue, oriented in a north-south direction, is a four-lane roadway with a raised median. Wilmington Avenue provides access to the project site as well as regional access through its connection to the I-405 freeway. On-street parking is prohibited along Wilmington Avenue in the study area.

Alameda Street, oriented in a north-south direction, consists of two lanes in each direction. On-street parking is prohibited along Alameda Street in the study area. Alameda Street bisects and provides direct access to the project site.

Santa Fe Avenue, oriented in a north-south direction, consists of two lanes in each direction with a raised median and on-street parking permitted in the study area. Santa Fe Avenue runs parallel to the I-710 freeway and consists of multiple bus routes.

*223<sup>rd</sup> Street*, oriented in an east-west direction, consists of two lanes in each direction with on-street parking allowed in some sections of the study area. 223<sup>rd</sup> Street provides access to the project site. East of the project site, 223<sup>rd</sup> Street transitions to Wardlow Road.

Sepulveda Boulevard, oriented in an east-west direction, consists of two lanes in each direction. Onstreet parking is prohibited along Sepulveda Boulevard in the study area. East of the I-710 freeway, Sepulveda Boulevard transitions to Willow Street.

### 2.2 BASELINE TRANSIT OPERATIONS

The Los Angeles County Metropolitan Transportation Authority (Metro) and the Long Beach Transit (LBT) operate bus lines within the area of the project site. A description of the transit service follows:

Metro Line 202 – This line operates between Wilmington and Watts. Within the study area, this line travels north and south along Alameda Street Service is provided at 60 minute headways during weekday peak periods, late night, and owl service. Weekend and holiday service is not provided.



Long Beach Line 191/192 – These lines operate between Downtown Long Beach and Lakewood. Within the study area, the lines travel north and south along Santa Fe Avenue. Service is provided on weekdays, weekends, and holidays. They currently provide 20 minute headways during peak periods.

Long Beach Line 101/102/103/104 – These lines operate between Wilmington and Long Beach. Within the study area, the lines travel east and west along Sepulveda Boulevard beginning at Santa Fe Avenue. Service is provided at 20 minute headways during weekday peak periods. Weekend and holiday service is limited.

# 2.3 BASELINE TRAFFIC VOLUMES

Vehicle turning movement counts at the study intersections were collected in August 2014 during the a.m. (6:00a.m. to 9:00 a.m.) and p.m. (4:00p.m. and 6:00 p.m.) peak periods. The traffic counts are a reasonable estimate of conditions during the baseline period. Detailed traffic count sheets are provided in **Appendix A. Figure 4** shows the existing peak hour volumes at the study intersections.

#### 2.4 Traffic Operations Analysis Methodology

The efficiency of traffic operations on a facility can be described in terms of Level of Service (LOS). The level of service concept is a measure of average operating conditions at an intersection during an hour. Levels range from 'A' to 'F', with 'A' representing excellent (free-flow) conditions and 'F' representing a roadway operating at its design capacity.

Traffic operating conditions in the vicinity of the project were evaluated using methodologies described in each project area agencies' traffic analysis guidelines. The non-freeway ramp study intersections are analyzed using the Intersection Capacity Utilization (ICU) methodology for intersection analysis. ICU methodology defines the LOS by the volume-to-capacity (V/C) ratio for the turning movements and intersection characteristics at the signalized intersections. The ICU value is determined by summing the V/C ratio of the critical movements, plus a factor for a yellow signal time. Intersections located in the City of Los Angeles are also analyzed with the Circular 212 methodology which calculates the delay of critical movements in the intersection—those results are similar to the ICU calculation and are included in the appendix. The Caltrans ramp intersections are under Caltrans' jurisdiction and are analyzed using the Highway Capacity Manual (HCM) methodology. HCM methodology defines the LOS by the average vehicle delay experienced by all vehicles traveling through the intersection. **Table 1** presents the both the V/C ratio and average delay associated with each LOS grade as well as a qualitative description of intersection operations at that grade.



**TABLE 1: INTERSECTION LEVEL OF SERVICE DEFINITIONS** 

Level of Service	Description	Signalized Intersection Volume-to-Capacity Ratio (V/C)	Signalized Intersection Delay (seconds)
А	Free flowing, virtually no delay. Minimal Traffic.	<u>≤</u> 0.600	<u>≤</u> 10
В	Free flow and choice of lanes. Delays are minimal. All cars clear intersection easily.	>0.600 to 0.699	>10 and <u>&lt;</u> 20
С	Good operation. Delays starting to become a factor but still within acceptable limits.	>0.700 to 0.799	>20 and <u>&lt;</u> 35
D	Approaching unstable flow. Queues at intersection are quite long but most cars clear intersection on their green signal. Occasionally, several vehicles must wait for a second green signal. Congestion is moderate.	>0.800 to 0.899	>35 and <u>&lt;</u> 55
E	Severe Congestion and delay. Most of the available capacity is used. Many cars must wait through a complete signal cycle to clear the intersection.	>0.900 to 0.999	>55 and <u>&lt;</u> 80
F	Excessive delay and congestion. Most cars must wait through more than one on one signal cycle. Queues are very long and drivers are obviously irritated.	> 1.000	> 80

Study location significance criteria are based on the location of each analyzed facility. The Cities in the study area consider LOS D to be the minimum acceptable LOS. The threshold of significance is considered to be a Project-related change in V/C ratio of 0.02 or greater if the final LOS is 'E' or 'F'.<sup>2</sup>

The City of Los Angeles has a sliding scale of acceptable effects for service levels 'C', 'D', 'E' and 'F'<sup>3</sup>. For example, a greater effect is allowed under LOS 'C' than LOS 'D' before being considered significant. Thus, a project would have a significant impact on transportation/circulation during construction if it would increase an intersection's V/C ratio in accordance with the following guidelines:

- V/C ratio increase greater than or equal to 0.040 if final LOS is 'C',
- V/C ratio increase greater than or equal to 0.020 if final LOS is 'D', or
- V/C ratio increase greater than or equal to 0.010 if final LOS is 'E' or 'F'.

However since the analysis intersection located in the City of Los Angeles is forecasted to operate at no worse than LOS 'B' in any of the analysis scenarios, there is no impact determined at the intersection of Alameda Street Ramp at 223<sup>rd</sup> Street in the City of Los Angeles.



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<sup>&</sup>lt;sup>2</sup> City of Carson General Plan Update Transportation and Infrastructure Element, October 11, 2004, City of Long Beach General Plan Transportation Element, 1991 based on Los Angeles County Congestion Management Program Guidelines.

<sup>&</sup>lt;sup>3</sup> City of Los Angeles Department of Transportation Traffic Study Policies and Procedures, August 2014

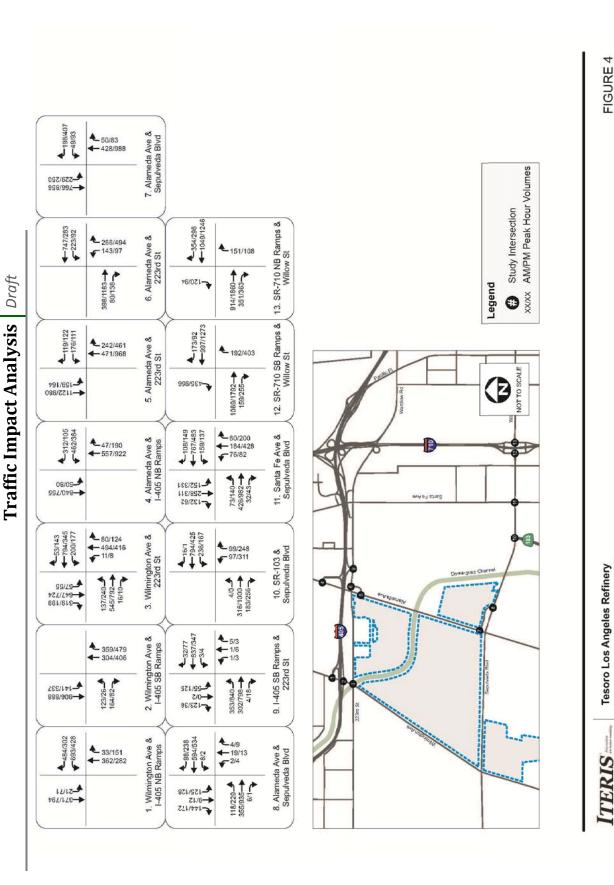


FIGURE 4 Baseline Intersection Volumes

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Caltrans has not adopted specific thresholds of significance for determining whether an impact is significant and relies on the local-defined County and City standards for significance thresholds. The transportation/traffic questions on the CEQA checklist XVI: Transportation/Traffic a) and b) state:

- a) Conflict with an applicable plan, ordinance or policy establishing measures of effectiveness for the performance of the circulation system, taking into account all modes of transportation including mass transit and non-motorized travel and relevant components of the circulation system, including but not limited to intersections, streets, highways and freeways, pedestrian and bicycle paths, and mass transit?
- b) Conflict with an applicable congestion management program including, but not limited to level of service standards and travel demand measures, or other standards established by the county congestion management agency for designated roads or highways?

Therefore the Caltrans CEQA Checklist defers to locally defined thresholds. For the purposes of this analysis, intersection locations under the jurisdiction of Caltrans will use the significance threshold of the City in which it is located.

#### 2.5 **BASELINE INTERSECTION LEVELS OF SERVICE**

LOS analysis was conducted to evaluate existing intersection operations during the a.m. and p.m. peak hours. Table 2 summarizes the existing level of service at the study intersections. LOS calculation worksheets are included in **Appendix B**.



TABLE 2: BASELINE EXISTING CONDITIONS (2014) INTERSECTION LEVELS OF SERVICE

Intersection		Agency / LOS Methodology	AM Peak Hour			PM Peak Hour		
			V/C Ratio	Delay (sec)	LOS	V/C Ratio	Delay (sec)	LOS
1	Wilmington Ave/I-405 NB Ramps	Caltrans / HCM	0.499	21.4	С	0.395	18.5	В
2	Wilmington Ave/I-405 SB Ramps	Caltrans / HCM	0.355	44.2	D	0.629	15.7	В
3	Wilmington Ave/223 <sup>rd</sup> St	Carson / ICU	0.643	-	В	0.690	-	В
4	Alameda St/I-405 NB Ramps	Caltrans / HCM	0.690	21.2	С	0.665	23.2	С
5	Alameda St/223 <sup>rd</sup> St (along Alameda St)	Carson / ICU	0.460	-	Α	0.570	-	Α
6	Alameda St/223 <sup>rd</sup> St (along 223 <sup>rd</sup> St)	LA / ICU	0.349	-	А	0.634	-	В
7	Alameda St/Sepulveda Blvd (along Alameda St)	Carson / ICU	0.374	-	А	0.537	-	А
8	Alameda St/Sepulveda Blvd (along Sepulveda Blvd)	Carson / ICU	0.415	-	А	0.742	-	С
9	I-405 SB Ramps/223 <sup>rd</sup> St	Caltrans / HCM	0.472	23.4	С	0.327	24.3	С
10	Terminal Island Fwy (SR-103)/Sepulveda Blvd	Long Beach / ICU	0.390	-	А	0.579	-	А
11	Santa Fe Ave/Sepulveda Blvd	Long Beach / ICU	0.624	-	С	0.781	-	С
12	I-710 SB Ramps/Willow St	Uncontrolled Intersection						
13	I-710 NB Ramps/Willow St	Uncontrolled Intersection						

Notes:

V/C = Volume to Capacity Ratio, LOS = Level of Service, Delay = Average Vehicle Delay (Seconds)

As shown in **Table 2**, the study intersections are currently operating at LOS D or better.

### 3.0 CONSTRUCTION CONDITIONS

Construction activities for the proposed Project are expected to begin in fourth quarter of 2015 and are expected to be completed by fourth quarter, 2019, based on preliminary project engineering. The preliminary construction schedule for each component of the proposed project varies. The construction activities for most of the components are expected to overlap from about December 2015 to February 2017. Construction work shifts are expected to last about ten hours per day during most portions of the construction schedule. During normal construction periods, one work shift per day is expected. However, during peak construction activities, the proposed project is expected to require two work shifts – one day and one night shift.

Due to the temporary nature of construction trips, in general construction-related traffic is considered less than significant; however detailed analysis of construction period conditions were conducted due to several factors. First, the proposed Project is expected to involve a large number of workers and therefore generate a large number of worker trips as compared to typical development projects in

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southern California. Second, a cumulative construction event at the I-405/Wilmington interchange will overlap with the first phases of the proposed Project construction. Since the I-405/Wilmington interchange is expected to be utilized by many of the proposed Project construction trips, construction period analysis of the proposed Project include analysis at the beginning of the construction of the I-405/Wilmington Interchange (baseline conditions) in its pre-construction geometry. For these reasons detailed analysis of construction period conditions for the peak construction period (2015) was conducted to identify potential significant impacts and recommend construction period traffic management strategies to mitigate those impacts.

#### 3.1 PROJECT CONSTRUCTION TRIP GENERATION AND DISTRIBUTION

Construction conditions are analyzed for the construction phase with the maximum number of construction trips during the two-year construction period. The peak construction period trip generation is shown below in **Table 3**. In total 950 workers will travel to and from the proposed Project site during the highest trip-generation phase of construction of the proposed project. These include 875 day shift workers and 75 night shift workers. In addition to worker trips, 120 truck trips would be generated during the peak trip-generating construction phase throughout the work day.

**Total One-**Type **Work Shift Total Round Trips** Way Trips Supervisors 6 am - 5:30 pm 40 80 **Dayshift Workers** 7:00 am - 5:30 pm 835 1,670 **Nightshift Workers** 7:00 pm - 7:00 am 75 150 Trucks Throughout the day 120 240 1,070 2,140 Total

Table 3: Construction Period Daily Trip Generation

In converting daily trip generation values into peak hour analysis periods, two adjustments were made. First, it was assumed that auto trips had a 10 percent carpool rate. Second, given the work shift hours for each type of worker, not all project trips are expected to occur within the peak hour for overall traffic volume in the study area and the following peak hour project trip generation assumptions were made:

- Supervisors would arrive before the a.m. peak hour and 50 percent would leave in the p.m. peak hour
- 50 percent of day shift workers would arrive during the a.m. peak hour and 50 percent would leave in the p.m. peak hour
- 50 percent of night shift workers would leave in the a.m. peak hour and 50 percent would arrive in the p.m. peak hour
- Truck trips are distributed evenly throughout the ten hour work day with 12 inbound and 12 outbound trips per peak hour. A passenger car equivalency (PCE) factor of 2.0 is applied to the truck trips to account for their larger size and slower turning speeds at intersections.

Of the 2,140 total daily construction-related trips shown in **Table 3**, PCE trips occurring in the peak hours are forecasted to be 454 PCE in the a.m. peak hour and 472 PCE trips in the p.m. peak hour as shown in Table 4.

TABLE 4: CONSTRUCTION PERIOD PEAK HOUR TRIP GENERATION

Turno	A	M Peak Hour			PM Peak H	our
Туре	In	Out	Total	In	Out	Total
Auto	376	34	410	34	394	428
Truck (PCE)	24	24	48	24	24	48
Total	400	58	458	58	418	476

Trip distribution assumptions were used to determine the origin and destination of new vehicle trips associated with the project. Trip distribution for the employee trips of the proposed Project was developed using the weighted distribution of workers, from the 2010 United States Census, in Los Angeles, Orange, Riverside, and San Bernardino Counties via the arterial network to Cities near the study area (e.g. Carson, Compton, Long Beach, portions of Los Angeles, and Torrance) and the regional freeway network for Cities more than two miles from the proposed Project site. As shown in Figure 5, distribution of employee trips was approximately 30 percent from I-405 north of the proposed Project site, 25 percent from I-405 south of the proposed Project site, 30 percent from I-710 north of the proposed Project site and 15 percent from local access along arterials. Truck trip distribution was assumed to occur to/from the north along I-710. The assignment of project-related trips shown in **Figure 6** is based on the trip distribution percentages.

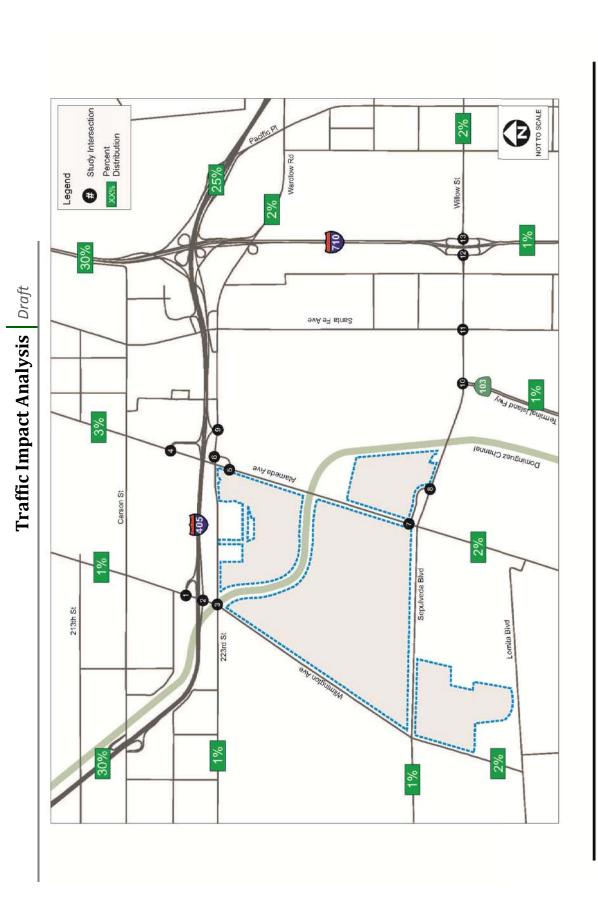


FIGURE 5 Proposed Project Construction Trip Distribution

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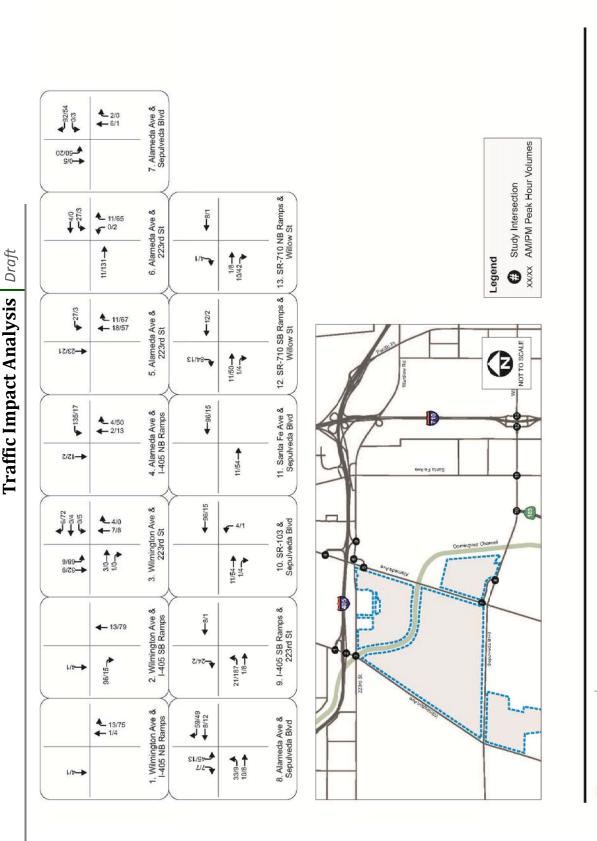


FIGURE 6 Proposed Project Construction Trip Assignment

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#### 3.2 Construction Period Intersection Levels of Service

LOS analysis was conducted to evaluate existing plus construction intersection operations during the a.m. and p.m. peak hours. **Figure 7** shows the baseline plus construction peak hour volumes at the study intersections. **Table 5** summarizes the LOS at the study intersections as compared to baseline LOS to determine if a threshold of significance was exceeded. LOS calculation worksheets are included in **Appendix B**.

Caltrans has undertaken a major construction project to modify the I-405/Wilmington interchange starting November 2013. The interchange construction is expected to finish in late 2015 or early 2016—potentially overlapping with the construction period of the proposed Project. The project will reconfigure existing on- and off-ramps from northbound and southbound I-405, construct a new onramp to southbound I-405, reconstruct Wilmington Avenue and Lenardo Drive, and construct a new bridge over the Torrance Lateral Channel.

The construction of the I-405/Wilmington Interchange will have periodic lane and ramp closures that, while temporary, have the potential to effect the proposed Project–related construction trips' interaction with the roadway network and demand placed on study intersections. While the Year 2015 With Project Construction Conditions (Pre- I-405/Wilmington Interchange) does not account for each possible iteration of lane closures<sup>4</sup>, it does include the construction period analysis of the proposed Project at the beginning of the construction of the I-405/Wilmington Interchange (baseline conditions) in its pre-construction geometry. These conditions are shown in **Table 5.** Further the Year 2021 scenarios assume the completion of the interchange in its post-construction configuration.

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<sup>&</sup>lt;sup>4</sup> The I-405/Wilmington Avenue Interchange construction involves periodic closures and openings of geometric and operational improvements on a constant (daily, weekly, and monthly) but inconsistent basis over the course of its construction period

FIGURE 7 Proposed Project Construction Period Intersection Volumes

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INTERSECTION LOS

Table 5: Baseline Existing Conditions Plus Project Construction Conditions (Pre- I-405/Wilmington Interchange)

			Û	cisting Co	Existing Conditions			Ä	Existing Plus Construction Conditions	s Constr	uction C	onditions		a.m. Change	p.m. Change	
	Intersection	a.m	a.m. Peak Hour	ını	p.m	p.m. Peak Hour	ını	a.m.	a.m. Peak Hour	ını	p.m.	Peak Hour	'n	in V/C	in V/C	Significant Impact?
		V/C Ratio	Delay (sec)	SOI	V/C Ratio	Delay (sec)	SOT	V/C Ratio	Delay (sec)	SOT	V/C Ratio	Delay (sec)	SOT	Delay	Delay	
1	Wilmington Ave/I-405 NB Ramps	0.499	21.4	C	0.395	18.5	В	0.500	21.5	S	0.395	18.6	В	0.1 s	0.1 s	No
2	Wilmington Ave/I-405 SB Ramps	0.355	44.2	۵	0.629	15.7	В	0.439	57.9	ш	0.641	16.5	В	13.7 s	0.8 s	Yes <sup>1</sup>
ж	Wilmington Ave/223 <sup>rd</sup> St	0.643	1	В	0.690	1	В	0.653	1	В	969.0		В	0.010	900.0	No
4	Alameda St/I-405 NB Ramps	0.690	21.2	C	0.665	23.2	C	0.807	25.6	C	0.683	23.8	C	4.4 s	0.6 s	No
2	Alameda St/223 <sup>rd</sup> St (along Alameda St)	0.460	1	۷	0.570		٧	0.484		٧	0.604		В	0.024	0.034	No
9	Alameda St/223 <sup>rd</sup> St (along 223 <sup>rd</sup> St)	0.349	1	⋖	0.634	1	В	0.358	1	۷	969.0	-	В	0.009	0.062	No
7	Alameda St/Sepulveda Blvd (along Alameda St)	0.374	1	⋖	0.537	1	۷	0.406	1	۷	0.552	-	4	0.032	0.015	No
8	Alameda St/Sepulveda Blvd (along Sepulveda Blvd)	0.415	1	A	0.742	-	С	0.452	-	А	0.751	-	С	0.037	0.009	No
6	I-405 SB Ramps/223 <sup>rd</sup> St	0.472	23.4	U	0.327	24.3	U	0.502	24.6	U	0.395	23.7	U	1.2 s	-0.6 s	No
10	Terminal Island Fwy (SR- 103)/Sepulveda Blvd	0.390		A	0.579	-	А	0.421	-	Α	0.595	-	А	0.031	0.016	No
11	Santa Fe Ave/Sepulveda Blvd	0.624	ı	U	0.781	ı	U	0.654	ı	U	0.798	1	U	0:030	0.017	No
12	I-710 SB Ramps/Willow St						ñ	Uncontrolled Intersection	ed Inters	ection						No
13	I-710 NB Ramps/Willow St						Ď	Uncontrolled Intersection	ed Inters	ection						No
1	1 = Significant temporary impact based on LOS E operation with the addition of construction-related trips.	on LOS E	operatio	n with th	ne additic	in of cons	struction	-related	trips.							

<sup>1</sup> = Significant temporary impact based on LOS E operation with the addition of construction-related trips.

Notes:

V/C = Volume to Capacity Ratio, LOS = Level of Service, Delay = Average Vehicle Delay (Seconds), s = seconds

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As shown in **Table 5**, construction-related trips are forecast to result in a significant impact during construction conditions at the Wilmington Ave/I-405 Southbound Ramps under their pre-construction configuration. This is due to the large number of project-related trips utilizing the Southbound ramp to access the proposed Project site in the a.m. peak hour.

It should be emphasized that this exceedance of the threshold of significance is temporary in nature and does not represent a significant impact that would require permanent mitigation by the applicant. However, it does indicate that inbound trips to the proposed Project during the construction period should avoid the I-405/Wilmington interchange while it is under construction

In order to reduce the proposed Project's construction-related trips on the Wilmington Avenue/I-405 Southbound Ramps intersection prior to the completion of the I-405/Wilmington Avenue Interchange Modification Project, it is recommended that proposed Project workers be advised of the construction schedule and potential restrictions and closures associated with the Interchange Modification Project. It is recommended that the Project workers be encouraged to avoid the Wilmington Avenue/I-405 Southbound Ramps intersection during morning peak travel periods by traveling either outside of the morning peak travel time or along alternative routes. The operational conditions of all other study locations, operating at LOS C or better during peak hours, demonstrate the adequacy of several alternative routes for proposed Project construction period trips.

The I-405/Wilmington Avenue Interchange Modification Project maintains several sources of information about current construction conditions through a web site (http://i405wilmington.com), a bilingual, toll-free hotline (887) 481-0004 and an email notification system.

The protocols for the dissemination of information to proposed Project workers and potential alternative schedules or routing during construction activities for the proposed project should be provided in the form of a construction staging and/or traffic management plan, to be approved by the Cities of Carson and Los Angeles.

#### 4.0 YEAR 2021 CONDITIONS

Year 2021 conditions were forecasted by applying ambient growth from year 2014 with the 0.4 percent per year growth as calculated from the SCAG travel demand model. The proposed Project operations are estimated to not increase the number of on-site workers after the construction phase, however approximately ten additional truck round-trips per work day would result from the proposed Project to support its operations. The peak hour estimates of these project-related trips were used to develop a year 2021 with proposed Project scenario that was compared against the year 2021 conditions without the proposed Project to determine if any significant impacts would occur due to the operation of the proposed Project.

#### 4.1 YEAR 2021 WITHOUT PROJECT INTERSECTION LEVELS OF SERVICE

**Figure 8** shows the year 2021 without project peak hour volumes at the study intersections. A level of service analysis was conducted to evaluate year 2021 without project intersection operations during the a.m. and p.m. peak hours. **Table 6** summarizes the year 2021 without project LOS at the study intersections. LOS calculation worksheets are included in **Appendix B**.

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Table 6: Year 2021 Without Project Conditions Intersection LOS

		Agency /	a.r	n. Peak Ho	our	p.n	n. Peak Ho	our
	Intersection	LOS Methodology	V/C Ratio	Delay (sec)	LOS	V/C Ratio	Delay (sec)	LOS
1	Wilmington Ave/I-405 NB Ramps	Caltrans / HCM	0.512	21.7	С	0.420	18.4	В
2	Wilmington Ave/I-405 SB Ramps	Caltrans / HCM	0.364	21.8	С	0.362	15.7	В
3	Wilmington Ave/223 <sup>rd</sup> St	Carson / ICU	0.656	-	В	0.703	-	С
4	Alameda St/I-405 NB Ramps	Caltrans / HCM	0.687	23.4	С	0.681	23.5	С
5	Alameda St/223 <sup>rd</sup> St (along Alameda St)	Carson / ICU	0.470	-	Α	0.581	-	Α
6	Alameda St/223 <sup>rd</sup> St (along 223 <sup>rd</sup> St)	LA / ICU	0.355	-	Α	0.647	-	В
7	Alameda St/Sepulveda Blvd (along Alameda St)	Carson / ICU	0.380	-	Α	0.548	-	Α
8	Alameda St/Sepulveda Blvd (along Sepulveda Blvd)	Carson / ICU	0.422	-	Α	0.758	-	С
9	I-405 SB Ramps/223 <sup>rd</sup> St	Caltrans / HCM	0.484	23.5	С	0.514	19.1	В
10	Terminal Island Fwy (SR-103)/Sepulveda Blvd	Long Beach / ICU	0.396	-	Α	0.590	-	Α
11	Santa Fe Ave/Sepulveda Blvd	Long Beach / ICU	0.636	-	В	0.798	-	С
12	I-710 SB Ramps/Willow St		U	ncontrolle	d Intersed	ction		
13	I-710 NB Ramps/Willow St		U	ncontrolle	d Intersed	ction		
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V/C = Volume to Capacity Ratio, LOS = Level of Service, Delay = Average Vehicle Delay (Seconds)



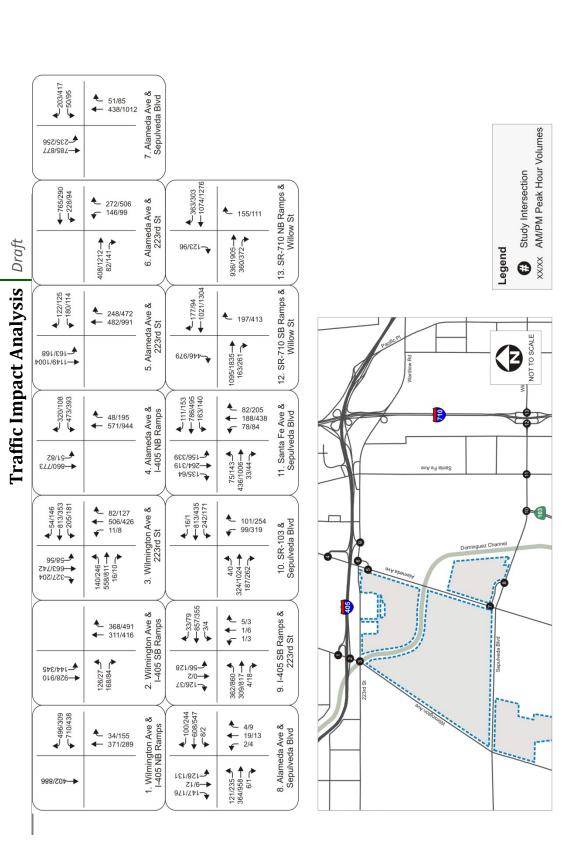


FIGURE 8 Year 2021 Without Proposed Project Intersection Volumes

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#### 4.2 YEAR 2021 WITH PROJECT INTERSECTION LEVELS OF SERVICE

A level of service analysis was conducted to evaluate year 2021 with project conditions during the a.m. and p.m. peak hours. The following trip generation assumptions for the operation of the proposed Project were made:

- There will be no increase in workers as compared to baseline conditions following completion of the construction phase
- Eight trucks per day will transport spent sulfuric acid from the Carson Plant to the new Sulfuric Acid Plant at Wilmington
- One truck per day will transport other materials and supplies to or from the Refinery

Overall ten truck roundtrips over 10 daytime hours are estimated to occur with the completion of the proposed Project. Based on the above assumptions, the estimated worst-case a.m. and p.m. trips were estimated: two inbound and two outbound truck trips in each peak hour, resulting in four inbound and four outbound PCE trips per peak hour as shown in **Table 7**.

a.m. Peak Hour p.m. Peak Hour Type In Out In Out Auto 0 0 0 0 4 Truck (PCE) 4 4 4 Total Δ 4 4 4

TABLE 7: PROPOSED PROJECT OPERATION PEAK HOUR TRIPS

Trip distribution assumptions were used to determine the origin and destination of vehicle trips associated with the operation of the proposed Project. As shown in Figure 9, distribution of proposed Project trips was 25 percent from I-405 north of the proposed Project site, 25 percent from I-405 south of the proposed Project site, 25 percent from I-710 north of the proposed Project site and 25 percent from local access along Willow Street east of the proposed Project site based on the equitable distribution of trips to major destinations outside of the study area. The assignment of project-related trips shown in Figure 10 is based on the trip distribution percentages.

The resulting year 2021 peak hour traffic volumes at the study intersections with the proposed project are shown in Figure 11. Table 8 summarizes the year 2021 with project LOS compared to without project conditions at the study intersections. LOS calculation worksheets are included in Appendix B.

As shown in **Table 8**, the proposed Project is not forecasted to cause a study location to exceed a threshold of significance and therefore the project would have a less than significant impact on area roadway facilities.

It should be noted that an Existing Conditions plus Project Operations was not conducted in addition to the Year 2021 Plus Project Operations scenario since the Year 2021 Plus Project Operations scenario was developed in this study as an existing conditions plus ambient growth to Year 2021 plus Project Operations. If levels of significance are not exceeded under the Year 2021 levels of ambient traffic, they will not be under lower levels of existing traffic.

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FIGURE 9 Proposed Project Operations Distribution

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Traffic Impact Analysis

FIGURE 10 Proposed Project Operations Trip Assignment

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Traffic Impact Analysis

FIGURE 11 Year 2021 With Proposed Project Operations Intersection Volumes

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TABLE 8: YEAR 2021 WITH PROJECT INTERSECTION LOS

			Year 2021		Without Project	)ject		<b>&gt;</b>	Year 2021 With Project Operations	With Pr	oject Op	erations		a.m. Change	p.m. Change	9
	Intersection	a.m	a.m. Peak Hour	our	p.m	p.m. Peak Hour	our	a.m	a.m. Peak Hour	ur	p.m.	p.m. Peak Hour	our	in V/C	in V/C	Significant Impact?
		V/C Ratio	Delay (sec)	SOT	V/C Ratio	Delay (sec)	SOT	V/C Ratio	Delay (sec)	ros	V/C Ratio	Delay (sec)	ros	Delay	Delay	
1	Wilmington Ave/I-405 NB Ramps	0.512	21.7	U	0.420	18.4	В	0.512	21.7	U	0.420	18.4	В	0 s	s 0	o N
2	Wilmington Ave/I-405 SB Ramps	0.364	21.8	)	0.362	15.7	В	0.365	21.8	C	698.0	15.8	В	s 0	0.1 s	No
3	Wilmington Ave/223 <sup>rd</sup> St	0.656	1	В	0.703	1	C	0.657	1	В	0.703	1	C	0.001	0	No
4	Alameda St/I-405 NB Ramps	0.687	23.4	3	0.681	23.5	Э	289.0	23.4	C	0.682	23.6	0	s 0	0.1 s	No
2	Alameda St/223 <sup>rd</sup> St (along Alameda St)	0.470	•	۷	0.581	•	∢	0.471	1	Α	0.581	1	4	0.001	0	O Z
9	Alameda St/223 <sup>rd</sup> St (along 223 <sup>rd</sup> St)	0.355	1	٨	0.647	1	В	0.355	1	Α	0.647	ı	В	0	0	o N
7	Alameda St/Sepulveda Blvd (along Alameda St)	0.380	1	Α	0.548	1	⋖	0.381	1	Α	0.549	ı	٨	0.001	0.001	o N
8	Alameda St/Sepulveda Blvd (along Sepulveda Blvd)	0.422	1	А	0.758	1	C	0.423	1	А	0.759	ı	C	0.001	0.001	No
6	I-405 SB Ramps/223 <sup>rd</sup> St	0.484	23.5	U	0.514	19.1	В	0.484	23.5	U	0.514	19.1	В	0 s	0s	N 0
10	Terminal Island Fwy (SR- 103)/Sepulveda Blvd	0.396	1	Α	0.590		٨	0.397	1	Α	0.591		A	0.001	0.001	N O
11	Santa Fe Ave/Sepulveda Blvd	0.636	1	В	0.798	1	С	0.637	1	В	0.799	ı	С	0.001	0.001	No
12	I-710 SB Ramps/Willow St						) ]	Uncontrolled Intersection	ed Inters	ection						ı
13	I-710 NB Ramps/Willow St							Uncontrolled Intersection	ed Inters	ection						1

Notes: V/C = Volume to Capacity Ratio, LOS = Level of Service, Delay = Average Vehicle Delay (Seconds)

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#### 5.0 CONCLUSIONS

As shown in **Table 5**, under the Baseline Existing Conditions (2014) Plus Project Construction Conditions scenario, temporary construction-related trips are forecast to result in a potentially significant impact at the Wilmington Ave/I-405 Southbound Ramps under the I-405/Wilmington Interchange preconstruction configuration. This is due to the large number of temporary project-related trips utilizing the southbound ramp to access the proposed Project site in the a.m. peak hour.

It should be emphasized that this exceedance of the threshold of significance is temporary in nature and does not represent a significant impact that would require permanent mitigation by the applicant. However, it does indicate that inbound trips to the proposed Project during the construction period should avoid the I-405/Wilmington interchange while it is under construction.

In order to reduce the proposed Project's construction-related trips on the Wilmington Avenue/I-405 Southbound Ramps intersection prior to the completion of the I-405/Wilmington Avenue Interchange Modification Project, it is recommended that proposed Project workers be advised of the construction schedule and potential restrictions and closures associated with the Interchange Modification Project. Workers should be encouraged to avoid the Wilmington Avenue/I-405 Southbound Ramps intersection during morning peak travel periods by traveling either outside of the morning peak travel time or along alternative routes. The operational conditions of all other study locations, operating at LOS C or better during peak hours, demonstrate the adequacy of several alternative routes for proposed Project construction period trips.

The protocols for the dissemination of information to proposed Project workers and potential alternative schedules or routing during construction activities for the proposed project should be provided in the form of a construction staging and/or traffic management plan, to be approved by the Cities of Carson and Los Angeles.

As shown in **Table 12**, the proposed Project is not forecasted to cause a study location to exceed a threshold of significance in year 2021 and therefore the project would have a less than significant impact on area roadway facilities.

It should be noted that an Existing Conditions plus Project Operations was not conducted in addition to the Year 2021 Plus Project Operations scenario since the Year 2021 Plus Project Operations scenario was developed in this study as an existing conditions plus ambient growth to Year 2021 plus Project Operations. If levels of significance are not exceeded under the Year 2021 levels of ambient traffic, they will not be under lower levels of existing traffic.



# **APPENDIX A: TRAFFIC COUNTS**



626.991.7522 www.ctcounters.com

File Name: Wilmington\_405NBRamps Site Code: 00000000

Start Date : 8/20/2014

Page No : 1

**Groups Printed- Unshifted** 

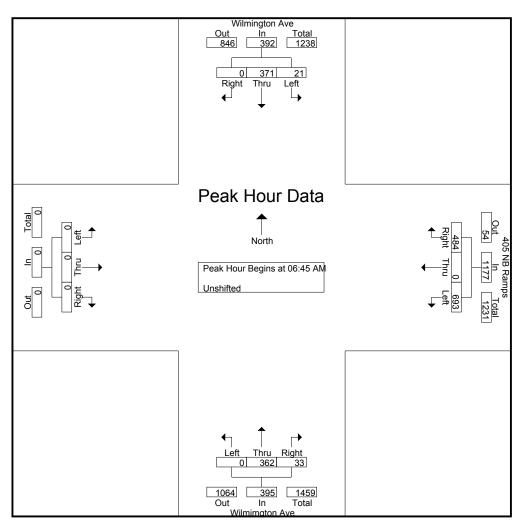
						rintea- U							
		nington Ave	e		NB Ramps			nimgton Av	e				
		uthbound			stbound			orthbound			stbound		
Start Time	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Int. Total
06:00 AM	10	78	0	159	0	78	0	46	24	0	0	0	395
06:15 AM	6	84	0	174	0	85	0	44	9	0	0	0	402
06:30 AM	1	80	0	172	0	94	0	96	14	0	0	0	457
06:45 AM	7	95	0	180	0	137	0	124	5	0	0	0	548_
Total	24	337	0	685	0	394	0	310	52	0	0	0	1802
1													
07:00 AM	4	75	0	187	0	111	0	71	10	0	0	0	458
07:15 AM	6	94	0	161	0	108	0	90	13	0	0	0	472
07:30 AM	4	107	0	165	0	128	0	77	5	0	0	0	486
07:45 AM	3	98	0	130	0	148	0	99	13	0	0	0	491
Total	17	374	0	643	0	495	0	337	41	0	0	0	1907
1			1			1			1			1	
08:00 AM	3	105	0	161	0	109	0	95	18	0	0	0	491
08:15 AM	5	86	0	146	0	125	0	80	9	0	0	0	451
08:30 AM	7	105	0	118	0	110	0	80	14	0	0	0	434
08:45 AM	4	99	0	115	0	99	0	63	14	0	0	0	394
Total	19	395	0	540	0	443	0	318	55	0	0	0	1770
04.00 704	10	10.5	ا م ا	00	0	<b>5.</b> 1		<b>7</b> 0	24	Ō	0	0.1	4.5.5
04:00 PM	18	195	0	99	0	71	0	59	24	0	0	0	466
04:15 PM	15	166	0	100	0	59	0	60	26	0	0	0	426
04:30 PM	16	190	0	105	0	78	0	67	39	0	0	0	495
04:45 PM	21	201	0	108	0	76	0	82	46	0	0	0	534
Total	70	752	0	412	0	284	0	268	135	0	0	0	1921
05:00 PM	20	190	0	111	0	76	0	<i>C</i> 1	22	0	0	0	400
05:00 PM 05:15 PM	20 14	213	0	111 104	0	76 72	0	61 72	32 34	0	0	0	490
					0	72	0		- 1		0		509
05:30 PM	9	174	0	102	0	66	0	74	33	0	0	0	458
05:45 PM	13 56	176	0	109	0	104	0	62 269	40	0	0	0	504
Total	56	753	0	426	0	318	0	269	139	0	0	0	1961
C 1 T 1	106	2611	ا م	2706	0	1934	0	1500	422	0	0	ا م	0261
Grand Total	186	2611	0	2706	0		0	1502	422	0	0	0	9361
Appreh %	6.6	93.4	0	58.3	0	41.7	0	78.1	21.9	0	0	0	
Total %	2	27.9	0	28.9	0	20.7	0	16	4.5	U	0	0	

626.991.7522 Appendix E www.ctcounters.com

File Name: Wilmington\_405NBRamps

Site Code : 00000000 Start Date : 8/20/2014

		Wilming	gton Ave			405 NB	Ramps		1	Wilmim	gton Av	e					
		South	bound			Westl	ound			North	bound			Eastb	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 0	6:00 AM	to 11:45	AM - Peak	1 of 1												
Peak Hour for Ent	ire Interse	ection Be	gins at 06:	45 AM													
06:45 AM	7	95	0	102	180	0	137	317	0	124	5	129	0	0	0	0	548
07:00 AM	4	75	0	79	187	0	111	298	0	71	10	81	0	0	0	0	458
07:15 AM	6	94	0	100	161	0	108	269	0	90	13	103	0	0	0	0	472
07:30 AM	4	107	0	111	165	0	128	293	0	77	5	82	0	0	0	0	486
Total Volume	21	371	0	392	693	0	484	1177	0	362	33	395	0	0	0	0	1964
% App. Total	5.4	94.6	0		58.9	0	41.1		0	91.6	8.4		0	0	0		
PHF	.750	.867	.000	.883	.926	.000	.883	.928	.000	.730	.635	.766	.000	.000	.000	.000	.896

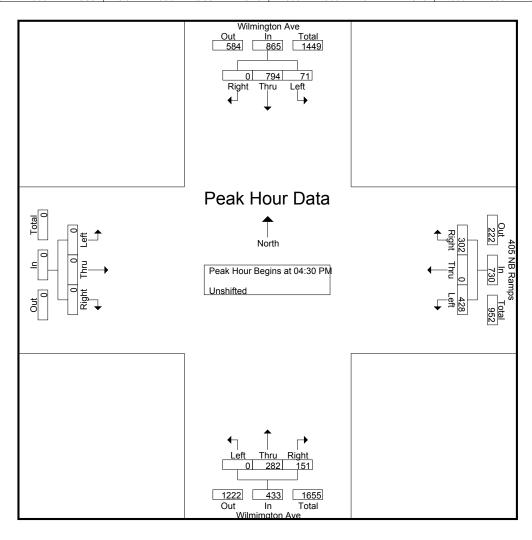


626.991.7522 Appendix E www.ctcounters.com

File Name: Wilmington\_405NBRamps

Site Code : 00000000 Start Date : 8/20/2014

		Wilming	ton Ave			405 NB	Ramps		1	Wilmim	gton Av	e					
		South	oound			Westl	oound			North	bound			Easth	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 1	2:00 PM	to 05:45	PM - Peak	1 of 1												
Peak Hour for Ent	ire Interse	ection Beg	gins at 04	:30 PM													
04:30 PM	16	190	0	206	105	0	78	183	0	67	39	106	0	0	0	0	495
04:45 PM	21	201	0	222	108	0	76	184	0	82	46	128	0	0	0	0	534
05:00 PM	20	190	0	210	111	0	76	187	0	61	32	93	0	0	0	0	490
05:15 PM	14	213	0	227	104	0	72	176	0	72	34	106	0	0	0	0	509
Total Volume	71	794	0	865	428	0	302	730	0	282	151	433	0	0	0	0	2028
% App. Total	8.2	91.8	0		58.6	0	41.4		0	65.1	34.9		0	0	0		
PHF	.845	.932	.000	.953	.964	.000	.968	.976	.000	.860	.821	.846	.000	.000	.000	.000	.949



626.991.7522 www.ctcounters.com

File Name: Wilmington\_405SBRamps Site Code: 00000000

Start Date : 8/20/2014

Page No : 1

**Groups Printed- Unshifted** 

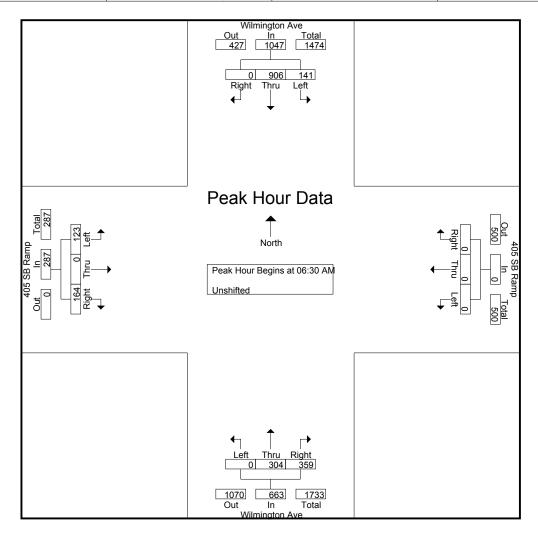
						Timea- U							
		nington Av	e		SB Ramp			nington Ave	e		SB Ramp		
		uthbound			estbound			rthbound			stbound		
Start Time	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Int. Total
06:00 AM	38	198	0	0	0	0	0	53	100	15	0	31	435
06:15 AM	40	211	0	0	0	0	0	41	107	12	0	34	445
06:30 AM	35	227	0	0	0	0	0	84	98	27	0	43	514
06:45 AM	43	222	0	0	0	0	0	78	89	50	0	46	528
Total	156	858	0	0	0	0	0	256	394	104	0	154	1922
07:00 AM	25	240	0	0	0	0	0	62	81	19	0	35	462
07:15 AM	38	217	0	0	0	0	0	80	91	27	0	40	493
07:30 AM	46	217	0	0	0	0	0	64	79	18	0	37	461
07:45 AM	24	212	0	0	0	0	0	85	94	27	0	63	505
Total	133	886	0	0	0	0	0	291	345	91	0	175	1921
1						1			1			i	
08:00 AM	48	210	0	0	0	0	0	98	103	23	0	47	529
08:15 AM	43	187	1	0	0	0	0	92	83	24	0	47	477
08:30 AM	46	181	0	0	0	0	0	66	79	27	0	51	450
08:45 AM	26	191	0	0	0	0	0	70	90	24	0	42	443_
Total	163	769	1	0	0	0	0	326	355	98	0	187	1899
1			1			1			1			1	
04:00 PM	86	212	0	0	0	0	0	81	117	10	0	19	525
04:15 PM	77	190	0	0	0	0	0	81	125	6	0	25	504
04:30 PM	79	218	0	0	0	0	0	98	142	6	0	17	560
04:45 PM	88	220	0	0	0	0	0	119	110	11	0	15	563
Total	330	840	0	0	0	0	0	379	494	33	0	76	2152
0.500.505			اها			. 1			40-1	_		- 1	
05:00 PM	83	220	0	0	0	0	0	84	105	7	0	29	528
05:15 PM	87	230	0	0	0	0	0	105	122	2	0	21	567
05:30 PM	75 75	203	0	0	0	0	0	97	125	11	0	10	521
05:45 PM	78	203	0	0	0	0	0	93	126	6	0	12	518
Total	323	856	0	0	0	0	0	379	478	26	0	72	2134
a .m . l	1105	1200	. 1	0		ا ۾		1.621	20.55	2.52	0	1	10000
Grand Total	1105	4209	1	0	0	0	0	1631	2066	352	0	664	10028
Apprch %	20.8	79.2	0	0	0	0	0	44.1	55.9	34.6	0	65.4	
Total %	11	42	0	0	0	0	0	16.3	20.6	3.5	0	6.6	

626.991.7522 Appendix E www.ctcounters.com

File Name: Wilmington\_405SBRamps

Site Code : 00000000 Start Date : 8/20/2014

	,	Wilming	ton Ave			405 SB	Ramp		,	Wilming	gton Ave	•		405 SB	Ramp		
		South	ound			Westl	ound			North	bound			Eastb	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 0	6:00 AM	to 11:45	AM - Peak	1 of 1		_				_				_		
Peak Hour for Ent	ire Interse	ction Beg	gins at 06:	:30 AM													
06:30 AM	35	227	0	262	0	0	0	0	0	84	98	182	27	0	43	70	514
06:45 AM	43	222	0	265	0	0	0	0	0	78	89	167	50	0	46	96	528
07:00 AM	25	240	0	265	0	0	0	0	0	62	81	143	19	0	35	54	462
07:15 AM	38	217	0	255	0	0	0	0	0	80	91	171	27	0	40	67	493
Total Volume	141	906	0	1047	0	0	0	0	0	304	359	663	123	0	164	287	1997
% App. Total	13.5	86.5	0		0	0	0		0	45.9	54.1		42.9	0	57.1		
PHF	.820	.944	.000	.988	.000	.000	.000	.000	.000	.905	.916	.911	.615	.000	.891	.747	.946

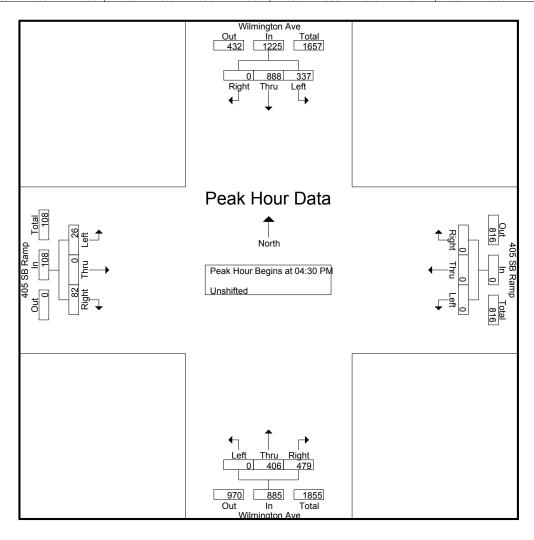


626.991.7522 Appendix E www.ctcounters.com

File Name: Wilmington\_405SBRamps

Site Code : 00000000 Start Date : 8/20/2014

		Wilming	ton Ave			405 SB	Ramp		,	Wilmin	gton Ave	e		405 SB	Ramp		
		Southl	oound			Westl	ound			North	bound			Easth	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 1	2:00 PM	to 05:45	PM - Peak	1 of 1												
Peak Hour for Ent	ire Interse	ection Be	gins at 04	:30 PM													
04:30 PM	79	218	0	297	0	0	0	0	0	98	142	240	6	0	17	23	560
04:45 PM	88	220	0	308	0	0	0	0	0	119	110	229	11	0	15	26	563
05:00 PM	83	220	0	303	0	0	0	0	0	84	105	189	7	0	29	36	528
05:15 PM	87	230	0	317	0	0	0	0	0	105	122	227	2	0	21	23	567
Total Volume	337	888	0	1225	0	0	0	0	0	406	479	885	26	0	82	108	2218
% App. Total	27.5	72.5	0		0	0	0		0	45.9	54.1		24.1	0	75.9		
PHF	.957	.965	.000	.966	.000	.000	.000	.000	.000	.853	.843	.922	.591	.000	.707	.750	.978



626.991.7522 www.ctcounters.com

File Name: Wilmington\_223rd Site Code: 00000000

Start Date : 8/20/2014

Page No : 1

**Groups Printed- Unshifted** 

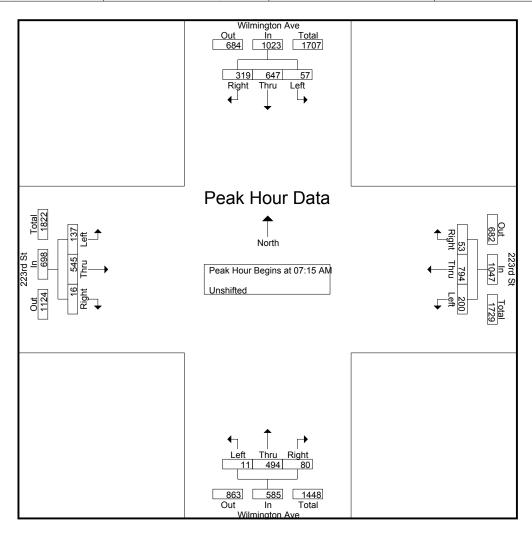
						rimea- C							
	Wiln	nington Ave	e	2	223rd St		Wiln	nington Av	e	2	23rd St		
	Sou	ıthbound		W	estbound		No	rthbound		Ea	stbound		
Start Time	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Int. Total
06:00 AM	11	152	49	35	33	15	3	125	7	28	36	0	494
06:15 AM	6	169	69	36	56	11	1	117	3	26	52	3	549
06:30 AM	6	185	74	42	148	12	3	138	4	33	64	0	709
06:45 AM	12	183	77	50	130	10	2	119	22	38	66	3	712
Total	35	689	269	163	367	48	9	499	36	125	218	6	2464
07:00 AM	13	169	82	51	132	12	7	109	8	27	99	7	716
07:15 AM	9	161	75	55	231	13	3	114	21	32	112	5	831
07:30 AM	22	148	90	54	235	12	3	117	14	33	140	5	873
07:45 AM	12	177	78	38	178	13	1	143	17	32	149	2	840
Total	56	655	325	198	776	50	14	483	60	124	500	19	3260
1			1			1			1			1	
08:00 AM	14	161	76	53	150	15	4	120	28	40	144	4	809
08:15 AM	16	155	73	45	128	15	6	97	15	27	102	0	679
08:30 AM	14	149	58	34	102	12	3	108	23	42	78	5	628
08:45 AM	12	152	71	32	103	8	2	112	16	19	68	6	601
Total	56	617	278	164	483	50	15	437	82	128	392	15	2717
04.00 PM	10	166	47.	25	<b>60</b>	21		100	22	60	212	ر - ا	750
04:00 PM	18	166	47	25	62	21	1	109	23	69	213	5	759
04:15 PM	14	173	36 58	40	68	23	3	112 86	24	63 70	210	4	770
04:30 PM 04:45 PM	8 14	167 178	58 49	43 40	87 70	64 35	4	86 126	20 40	70 59	184 185	4 2	795 700
Total	54	684	190	148	287	143	9	433	107	261	792	15	799 3123
Total	54	084	190	148	287	143	9	433	107	201	192	15	3123
05:00 PM	20	190	42	50	101	28	1	83	38	48	191	1	793
05:15 PM	13	189	50	44	87	16	2	121	26	63	232	3	846
05:30 PM	16	148	51	22	56	26	2	126	35	63	226	5	776
05:45 PM	14	162	44	25	49	26	4	136	40	55	184	7	746_
Total	63	689	187	141	293	96	9	466	139	229	833	16	3161
Total	03	007	107	141	273	70		400	137	22)	033	10	3101
Grand Total	264	3334	1249	814	2206	387	56	2318	424	867	2735	71	14725
Apprch %	5.4	68.8	25.8	23.9	64.7	11.4	2	82.8	15.2	23.6	74.5	1.9	
Total %	1.8	22.6	8.5	5.5	15	2.6	0.4	15.7	2.9	5.9	18.6	0.5	
			1									1	

626.991.7522 Appendix E www.ctcounters.com

File Name: Wilmington\_223rd

Site Code : 00000000 Start Date : 8/20/2014

		Wilmin	gton Ave	e		223	rd St			Wilmin	gton Ave	•		223	rd St		
		South	bound			Westl	oound			North	bound			Easth	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 0	6:00 AM	I to 11:45	AM - Peak	1 of 1		_				_				-		
Peak Hour for Ent	ire Interse	ction Be	gins at 0'	7:15 AM													
07:15 AM	9	161	75	245	55	231	13	299	3	114	21	138	32	112	5	149	831
07:30 AM	22	148	90	260	54	235	12	301	3	117	14	134	33	140	5	178	873
07:45 AM	12	177	78	267	38	178	13	229	1	143	17	161	32	149	2	183	840
08:00 AM	14	161	76	251	53	150	15	218	4	120	28	152	40	144	4	188	809
Total Volume	57	647	319	1023	200	794	53	1047	11	494	80	585	137	545	16	698	3353
% App. Total	5.6	63.2	31.2		19.1	75.8	5.1		1.9	84.4	13.7		19.6	78.1	2.3		
PHF	.648	.914	.886	.958	.909	.845	.883	.870	.688	.864	.714	.908	.856	.914	.800	.928	.960

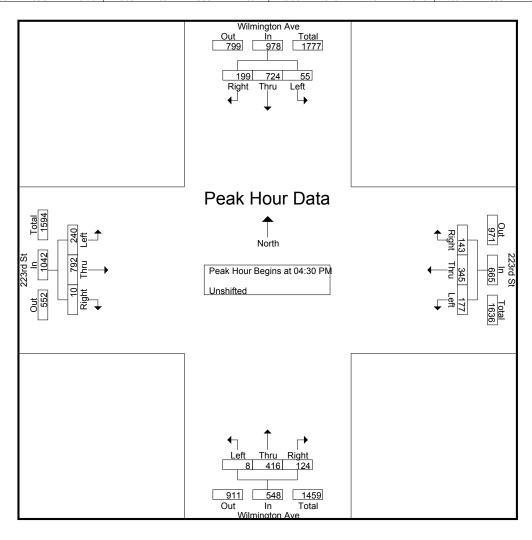


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File Name: Wilmington\_223rd

Site Code : 00000000 Start Date : 8/20/2014

	,	Wilming	ton Ave			223	rd St		,	Wilmin	gton Ave			223	rd St		
		South	ound			Westl	oound			North	bound			Easth	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 1:	2:00 PM	to 05:45	PM - Peak	1 of 1												
Peak Hour for Ent	ire Interse	ction Beg	gins at 04	:30 PM													
04:30 PM	8	167	58	233	43	87	64	194	4	86	20	110	70	184	4	258	795
04:45 PM	14	178	49	241	40	70	35	145	1	126	40	167	59	185	2	246	799
05:00 PM	20	190	42	252	50	101	28	179	1	83	38	122	48	191	1	240	793
05:15 PM	13	189	50	252	44	87	16	147	2	121	26	149	63	232	3	298	846
Total Volume	55	724	199	978	177	345	143	665	8	416	124	548	240	792	10	1042	3233
% App. Total	5.6	74	20.3		26.6	51.9	21.5		1.5	75.9	22.6		23	76	1_		
PHF	.688	.953	.858	.970	.885	.854	.559	.857	.500	.825	.775	.820	.857	.853	.625	.874	.955



626.991.7522 www.ctcounters.com

File Name: Alameda\_405NBRamps

Site Code : 00000000 Start Date : 8/20/2014

Page No : 1

**Groups Printed- Unshifted** 

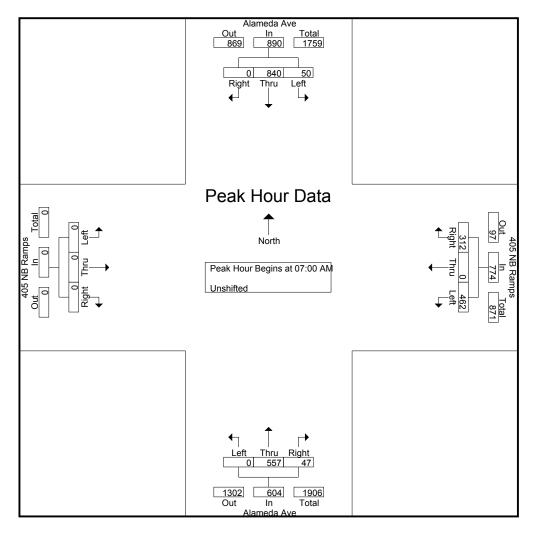
					Groups P	<u>rinted- U</u>							
		meda Ave		405	NB Ramps			meda Ave		405 N	NB Ramps		
	Sou	thbound		W	estbound		No	rthbound		Ea	stbound		
Start Time	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Int. Total
06:00 AM	18	93	0	138	0	30	0	69	20	0	0	0	368
06:15 AM	8	133	0	144	0	31	0	65	13	0	0	0	394
06:30 AM	11	164	0	153	0	64	0	105	14	0	0	0	511
06:45 AM	17	137	0	132	0	51	0	99	15	0	0	0	451
Total	54	527	0	567	0	176	0	338	62	0	0	0	1724
07:00 AM	19	200	0	123	0	63	0	120	13	0	0	0	538
07:15 AM	12	207	0	104	0	64	0	124	13	0	0	0	524
07:30 AM	7	219	0	117	0	88	0	165	14	0	0	0	610
07:45 AM	12	214	0	118	0	97	0	148	7	0	0	0	596
Total	50	840	0	462	0	312	0	557	47	0	0	0	2268
08:00 AM	12	185	0	95	0	59	0	123	16	0	0	0	490
08:15 AM	8	133	0	84	0	61	0	111	13	0	0	0	410
08:30 AM	7	155	0	83	0	41	0	79	10	0	0	0	375
08:45 AM	6	146	0	92	0	37	0	85	14	0	0	0	380
Total	33	619	0	354	0	198	0	398	53	0	0	0	1655
04:00 PM	19	156	0	111	0	40	0	189	39	0	0	0	554
04:15 PM	21	179	0	121	0	32	0	198	37	0	0	0	588
04:30 PM	19	188	0	110	0	29	0	224	58	0	0	0	628
04:45 PM	17	175	0	106	0	28	0	255	53	0	0	0	634
Total	76	698	0	448	0	129	0	866	187	0	0	0	2404
05:00 PM	26	188	0	84	0	13	0	221	49	0	0	0	581
05:15 PM	18	204	0	84	0	35	0	222	30	0	0	0	593
05:30 PM	19	212	0	89	0	26	0	196	29	0	0	0	571
05:45 PM	10	141	0	105	0	37	0	157	39	0	0	0	489
Total	73	745	0	362	0	111	0	796	147	0	0	0	2234
Grand Total	286	3429	0	2193	0	926	0	2955	496	0	0	0	10285
Apprch %	7.7	92.3	0	70.3	0	29.7	0	85.6	14.4	0	0	0	
Total %	2.8	33.3	0	21.3	0	9	0	28.7	4.8	0	0	0	

626.991.7522 Appendix E www.ctcounters.com

File Name: Alameda\_405NBRamps

Site Code : 00000000 Start Date : 8/20/2014

		Alame	da Ave			405 NB	Ramps			Alame	da Ave			405 NB	Ramps		
		South	bound			Westl	ound			North	bound			Eastb	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 0	6:00 AM	to 11:45	AM - Peak	1 of 1		-				-				_		
Peak Hour for Ent	ire Interse	ection Be	gins at 07:	:00 AM													
07:00 AM	19	200	0	219	123	0	63	186	0	120	13	133	0	0	0	0	538
07:15 AM	12	207	0	219	104	0	64	168	0	124	13	137	0	0	0	0	524
07:30 AM	7	219	0	226	117	0	88	205	0	165	14	179	0	0	0	0	610
07:45 AM	12	214	0	226	118	0	97	215	0	148	7	155	0	0	0	0	596
Total Volume	50	840	0	890	462	0	312	774	0	557	47	604	0	0	0	0	2268
% App. Total	5.6	94.4	0		59.7	0	40.3		0	92.2	7.8		0	0	0		
PHF	.658	.959	.000	.985	.939	.000	.804	.900	.000	.844	.839	.844	.000	.000	.000	.000	.930

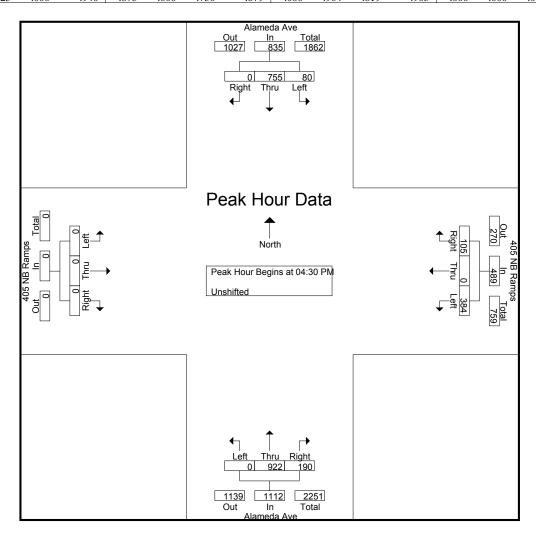


626.991.7522 Appendix E www.ctcounters.com

File Name: Alameda\_405NBRamps

Site Code : 00000000 Start Date : 8/20/2014

		Alame	da Ave			405 NB	Ramps			Alame	da Ave			405 NB	Ramps		
		South	bound			Westl	ound			North	bound			Easth	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 1	2:00 PM	to 05:45 P	M - Peak	1 of 1												
Peak Hour for Ent	ire Interse	ection Be	gins at 04:3	30 PM													
04:30 PM	19	188	0	207	110	0	29	139	0	224	58	282	0	0	0	0	628
04:45 PM	17	175	0	192	106	0	28	134	0	255	53	308	0	0	0	0	634
05:00 PM	26	188	0	214	84	0	13	97	0	221	49	270	0	0	0	0	581
05:15 PM	18	204	0	222	84	0	35	119	0	222	30	252	0	0	0	0	593
Total Volume	80	755	0	835	384	0	105	489	0	922	190	1112	0	0	0	0	2436
% App. Total	9.6	90.4	0		78.5	0	21.5		0	82.9	17.1		0	0	0		
PHF	.769	.925	.000	.940	.873	.000	.750	.879	.000	.904	.819	.903	.000	.000	.000	.000	.961



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File Name : 223rd\_Alameda\_onAlameda

Site Code : 00000000 Start Date : 8/20/2014

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**Groups Printed- Unshifted** 

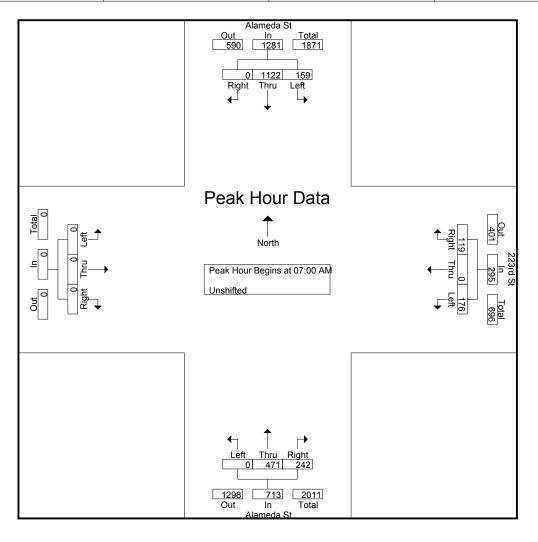
		ameda St			23rd St	Time C	Al	ameda St					
		thbound			estbound			rthbound			stbound		
Start Time	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Int. Total
06:00 AM	30	195	0	31	0	12	0	63	38	0	0	0	369
06:15 AM	34	239	0	50	0	11	0	68	33	0	0	0	435
06:30 AM	30	277	0	43	0	21	0	92	50	0	0	0	513
06:45 AM	32	243	0	39	0	20	0	95	55	0	0	0	484
Total	126	954	0	163	0	64	0	318	176	0	0	0	1801
07:00 AM	31	290	0	39	0	28	0	99	62	0	0	0	549
07:15 AM	35	273	0	41	0	27	0	102	65	0	0	0	543
07:30 AM	42	280	0	47	0	31	0	145	63	0	0	0	608
07:45 AM	51	279	0	49	0	33	0	125	52	0	0	0	589
Total	159	1122	0	176	0	119	0	471	242	0	0	0	2289
08:00 AM	40	251	0	42	0	28	0	120	26	0	0	0	507
08:15 AM	33	181	0	37	0	32	0	92	23	0	0	0	398
08:30 AM	32	203	0	40	0	26	0	81	12	0	0	0	394
08:45 AM	26	207	0	27	0	26	0	77	18	0	0	0	381_
Total	131	842	0	146	0	112	0	370	79	0	0	0	1680
04:00 PM	47	212	0	25	0	24	0	198	108	0	0	0	614
04:15 PM	25	240	0	27	0	17	0	212	107	0	0	0	628
04:30 PM	39	259	0	35	0	38	0	237	108	0	0	0	716
04:45 PM	39	235	0	27	0	26	0	277	112	0	0	0	716
Total	150	946	0	114	0	105	0	924	435	0	0	0	2674
05:00 PM	41	239	0	21	0	34	0	229	118	0	0	0	682
05:15 PM	45	247	0	28	0	24	0	225	123	0	0	0	692
05:30 PM	41	251	0	17	0	18	0	205	98	0	0	0	630
05:45 PM	28	209	0	16	0	21	0	177	95	0	0	0	546
Total	155	946	0	82	0	97	0	836	434	0	0	0	2550
Grand Total	721	4810	0	681	0	497	0	2919	1366	0	0	0	10994
Apprch %	13	87	0	57.8	0	42.2	0	68.1	31.9	0	0	0	
Total %	6.6	43.8	0	6.2	0	4.5	0	26.6	12.4	0	0	0	

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File Name : 223rd\_Alameda\_onAlameda

Site Code : 00000000 Start Date : 8/20/2014

		Alamo	eda St			2231	rd St			Alam	eda St						
		South	oound			Westl	ound			North	bound			Eastb	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 0	6:00 AM	to 11:45	AM - Peak	1 of 1		_				_				_		
Peak Hour for Ent	ire Interse	ection Be	gins at 07	:00 AM													
07:00 AM	31	290	0	321	39	0	28	67	0	99	62	161	0	0	0	0	549
07:15 AM	35	273	0	308	41	0	27	68	0	102	65	167	0	0	0	0	543
07:30 AM	42	280	0	322	47	0	31	78	0	145	63	208	0	0	0	0	608
07:45 AM	51	279	0	330	49	0	33	82	0	125	52	177	0	0	0	0	589
Total Volume	159	1122	0	1281	176	0	119	295	0	471	242	713	0	0	0	0	2289
% App. Total	12.4	87.6	0		59.7	0	40.3		0	66.1	33.9		0	0	0		
PHF	.779	.967	.000	.970	.898	.000	.902	.899	.000	.812	.931	.857	.000	.000	.000	.000	.941

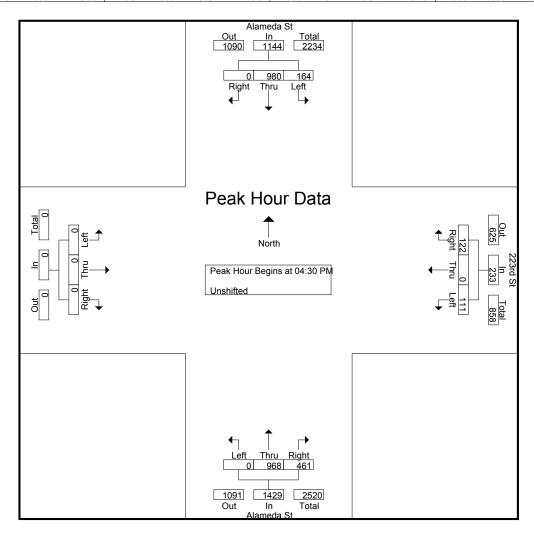


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File Name : 223rd\_Alameda\_onAlameda

Site Code : 00000000 Start Date : 8/20/2014

		Alam	eda St			2231	rd St			Alam	eda St						
		South	bound			Westl	ound			North	bound			Easth	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 1	2:00 PM	to 05:45	PM - Peak	1 of 1												
Peak Hour for Ent	ire Interse	ection Be	gins at 04	:30 PM													
04:30 PM	39	259	0	298	35	0	38	73	0	237	108	345	0	0	0	0	716
04:45 PM	39	235	0	274	27	0	26	53	0	277	112	389	0	0	0	0	716
05:00 PM	41	239	0	280	21	0	34	55	0	229	118	347	0	0	0	0	682
05:15 PM	45	247	0	292	28	0	24	52	0	225	123	348	0	0	0	0	692
Total Volume	164	980	0	1144	111	0	122	233	0	968	461	1429	0	0	0	0	2806
% App. Total	14.3	85.7	0		47.6	0	52.4		0	67.7	32.3		0	0	0		
PHF	.911	.946	.000	.960	.793	.000	.803	.798	.000	.874	.937	.918	.000	.000	.000	.000	.980



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File Name : 223rd\_Alameda\_on223rd

Site Code : 00000000 Start Date : 8/20/2014

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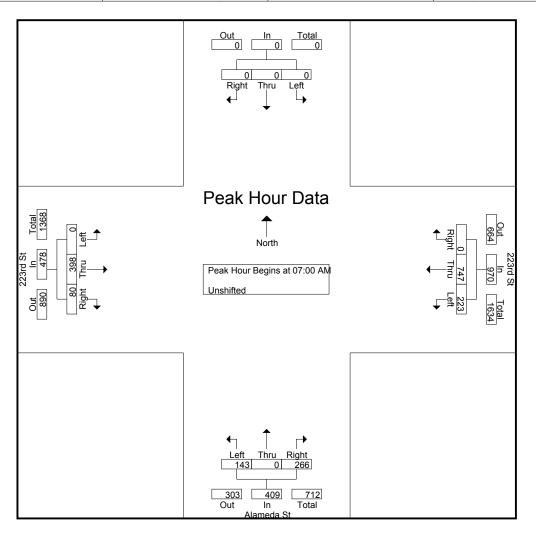
						rintea- U							
					23rd St			ameda St			23rd St		
		thbound		W	estbound			rthbound			stbound		
Start Time	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Int. Total
06:00 AM	0	0	0	34	78	0	18	0	49	0	53	10	242
06:15 AM	0	0	0	37	107	0	18	0	50	0	57	20	289
06:30 AM	0	0	0	40	158	0	29	0	50	0	57	19	353
06:45 AM	0	0	0	40	169	0	33	0	54	0	77	19	392
Total	0	0	0	151	512	0	98	0	203	0	244	68	1276
07:00 AM	0	0	0	53	179	0	35	0	59	0	79	16	421
07:15 AM	0	0	0	51	180	0	41	0	63	0	102	18	455
07:30 AM	Õ	0	0	63	207	0	40	0	67	Ö	110	19	506
07:45 AM	Õ	0	0	56	181	0	27	0	77	Ö	107	27	475
Total	0	0	0	223	747	0	143	0	266	0	398	80	1857
08:00 AM	0	0	0	48	148	0	28	0	39	0	120	26	409
08:15 AM	0	0	0	45	132	0	33	0	55	0	118	24	407
08:30 AM	ő	0	0	41	106	0	28	0	28	ő	105	24	332
08:45 AM	Õ	0	0	36	110	0	20	0	22	Õ	123	20	331_
Total	0	0	0	170	496	0	109	0	144	0	466	94	1479
						1							
04:00 PM	0	0	0	22	62	0	32	0	124	0	268	20	528
04:15 PM	0	0	0	24	69	0	19	0	116	0	304	21	553
04:30 PM	0	0	0	27	45	0	30	0	112	0	307	48	569
04:45 PM	0	0	0	21	81	0	24	0	128	0	290	34	578_
Total	0	0	0	94	257	0	105	0	480	0	1169	123	2228
05:00 PM	0	0	0	20	88	0	24	0	138	0	282	35	587
05:15 PM	0	0	0	26	74	0	24	0	144	0	248	27	543
05:30 PM	0	0	0	16	67	0	22	0	112	0	282	20	519
05:45 PM	0	0	0	19	65	0	15	0	111	0	274	20	504_
Total	0	0	0	81	294	0	85	0	505	0	1086	102	2153
Grand Total	0	0	0	719	2306	0	540	0	1598	0	3363	467	8993
Apprch %	0	0	0	23.8	76.2	0	25.3	0	74.7	0	87.8	12.2	
Total %	0	0	0	8	25.6	0	6	0	17.8	0	37.4	5.2	

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File Name: 223rd\_Alameda\_on223rd

Site Code : 00000000 Start Date : 8/20/2014

						223	rd St			Alam	eda St			223	rd St		
		Southb	ound			Westl	oound			North	bound			Easth	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 0	6:00 AM	to 11:45	AM - Peak	1 of 1		_				_				_		
Peak Hour for Ent	ire Interse	ction Beg	ins at 07	:00 AM													
07:00 AM	0	0	0	0	53	179	0	232	35	0	59	94	0	79	16	95	421
07:15 AM	0	0	0	0	51	180	0	231	41	0	63	104	0	102	18	120	455
07:30 AM	0	0	0	0	63	207	0	270	40	0	67	107	0	110	19	129	506
07:45 AM	0	0	0	0	56	181	0	237	27	0	77	104	0	107	27	134	475
Total Volume	0	0	0	0	223	747	0	970	143	0	266	409	0	398	80	478	1857
% App. Total	0	0	0		23	77	0		35	0	65		0	83.3	16.7		
PHF	.000	.000	.000	.000	.885	.902	.000	.898	.872	.000	.864	.956	.000	.905	.741	.892	.917

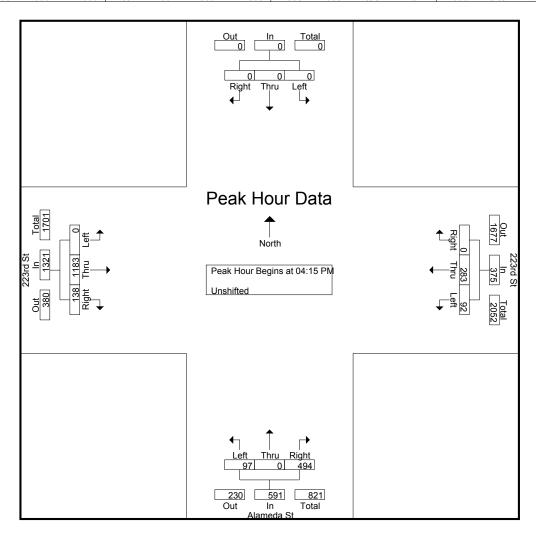


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File Name : 223rd\_Alameda\_on223rd

Site Code : 00000000 Start Date : 8/20/2014

																	_
						223	rd St			Alam	eda St			223	rd St		
		South	bound			Westl	bound			North	bound			Eastl	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 1	2:00 PM	to 05:45	PM - Peak	1 of 1		_										
Peak Hour for Ent	ire Interse	ection Be	gins at 04	4:15 PM													
04:15 PM	0	0	0	0	24	69	0	93	19	0	116	135	0	304	21	325	553
04:30 PM	0	0	0	0	27	45	0	72	30	0	112	142	0	307	48	355	569
04:45 PM	0	0	0	0	21	81	0	102	24	0	128	152	0	290	34	324	578
05:00 PM	0	0	0	0	20	88	0	108	24	0	138	162	0	282	35	317	587
Total Volume	0	0	0	0	92	283	0	375	97	0	494	591	0	1183	138	1321	2287
% App. Total	0	0	0		24.5	75.5	0		16.4	0	83.6		0	89.6	10.4		
PHF	.000	.000	.000	.000	.852	.804	.000	.868	.808	.000	.895	.912	.000	.963	.719	.930	.974



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File Name : Sepulveda\_Alameda\_onAlameda Site Code : 00000000

Start Date : 8/20/2014

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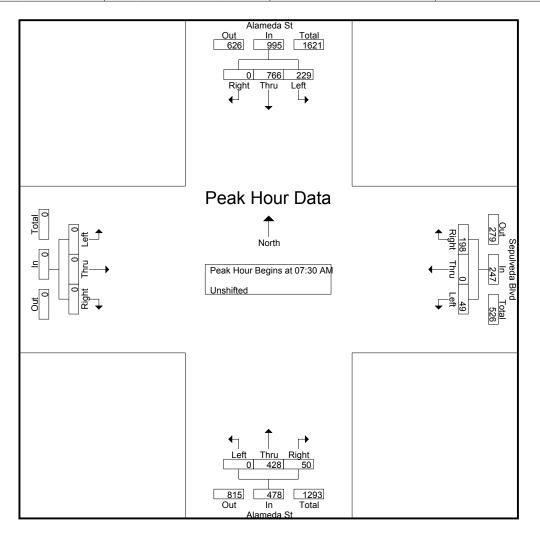
	Ala	ameda St		Sepul	lveda Blvd	Timeu- C		ameda St					
	Sou	ithbound			estbound		No	rthbound		Eas	stbound		
Start Time	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Int. Total
06:00 AM	49	174	0	2	0	20	0	68	16	0	0	0	329
06:15 AM	52	181	0	6	0	31	0	80	10	0	0	0	360
06:30 AM	74	210	0	13	0	36	0	87	12	0	0	0	432
06:45 AM	60	212	0	15	0	53	0	103	7	0	0	0	450_
Total	235	777	0	36	0	140	0	338	45	0	0	0	1571
			- 1			1			1			- 1	
07:00 AM	51	217	0	12	0	48	0	100	12	0	0	0	440
07:15 AM	50	184	0	11	0	46	0	86	15	0	0	0	392
07:30 AM	60	196	0	11	0	46	0	105	16	0	0	0	434
07:45 AM	62	196	0	14	0	49	0	117	11	0	0	0	449
Total	223	793	0	48	0	189	0	408	54	0	0	0	1715
08:00 AM	61	201	0	9	0	54	0	104	9	0	0	0	438
08:15 AM	46	173	0	15	0	49	0	102	14	0	0	0	399
08:30 AM	51	151	0	11	0	43	0	87	12	0	0	0	355
08:45 AM	50	142	0	13	0	39	0	92	13	0	0	0	349_
Total	208	667	0	48	0	185	0	385	48	0	0	0	1541
			- 1									- 1	
1												1	
04:00 PM	49	252	0	18	0	101	0	196	17	0	0	0	633
04:15 PM	59	218	0	27	0	98	0	144	14	0	0	0	560
04:30 PM	57	226	0	27	0	113	0	267	28	0	0	0	718
04:45 PM	54	211	0	26	0	112	0	240	21	0	0	0	664
Total	219	907	0	98	0	424	0	847	80	0	0	0	2575
05:00 PM	57	197	0	22	0	108	0	255	18	0	0	0	657
05:15 PM	82	222	0	18	0	74	0	226	16	0	0	0	638
05:30 PM	41	184	0	27	0	92	0	209	16	0	0	0	569
05:45 PM	59	177	0	18	0	58	0	147	20	0	0	0	479
Total	239	780	0	85	0	332	0	837	70	0	0	0	2343
10tai	237	700	0	0.5	Ü	332	0	037	70	· ·	Ü	0	2545
Grand Total	1124	3924	0	315	0	1270	0	2815	297	0	0	0	9745
Apprch %	22.3	77.7	0	19.9	0	80.1	0	90.5	9.5	0	0	0	
Total %	11.5	40.3	0	3.2	0	13	0	28.9	3	0	0	0	

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File Name: Sepulveda\_Alameda\_onAlameda

Site Code : 00000000 Start Date : 8/20/2014

		Alam	eda St			Sepulve	da Blvd			Alam	eda St						
		South	bound			Westl	ound			North	bound			Eastb	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 0	6:00 AM	to 11:45	AM - Peak	1 of 1		_				_				_		
Peak Hour for Ent	ire Interse	ection Be	gins at 07	:30 AM													
07:30 AM	60	196	0	256	11	0	46	57	0	105	16	121	0	0	0	0	434
07:45 AM	62	196	0	258	14	0	49	63	0	117	11	128	0	0	0	0	449
08:00 AM	61	201	0	262	9	0	54	63	0	104	9	113	0	0	0	0	438
08:15 AM	46	173	0	219	15	0	49	64	0	102	14	116	0	0	0	0	399
Total Volume	229	766	0	995	49	0	198	247	0	428	50	478	0	0	0	0	1720
% App. Total	23	77	0		19.8	0	80.2		0	89.5	10.5		0	0	0		
PHF	.923	.953	.000	.949	.817	.000	.917	.965	.000	.915	.781	.934	.000	.000	.000	.000	.958

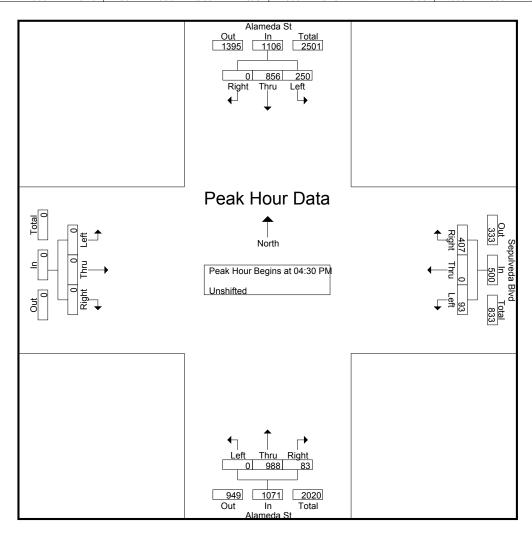


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File Name : Sepulveda\_Alameda\_onAlameda

Site Code : 00000000 Start Date : 8/20/2014

		Alamo	eda St			Sepulve	da Blvd			Alam	eda St						
		South	oound			Westl	oound			North	bound			Easth	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 1	2:00 PM	to 05:45	PM - Peak	1 of 1												
Peak Hour for Ent	ire Interse	ection Be	gins at 04	:30 PM													
04:30 PM	57	226	0	283	27	0	113	140	0	267	28	295	0	0	0	0	718
04:45 PM	54	211	0	265	26	0	112	138	0	240	21	261	0	0	0	0	664
05:00 PM	57	197	0	254	22	0	108	130	0	255	18	273	0	0	0	0	657
05:15 PM	82	222	0	304	18	0	74	92	0	226	16	242	0	0	0	0	638
Total Volume	250	856	0	1106	93	0	407	500	0	988	83	1071	0	0	0	0	2677
% App. Total	22.6	77.4	0		18.6	0	81.4		0	92.3	7.7		0	0	0		
PHF	.762	.947	.000	.910	.861	.000	.900	.893	.000	.925	.741	.908	.000	.000	.000	.000	.932



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File Name : Sepulveda\_Alameda\_onSepulveda Site Code : 00000000

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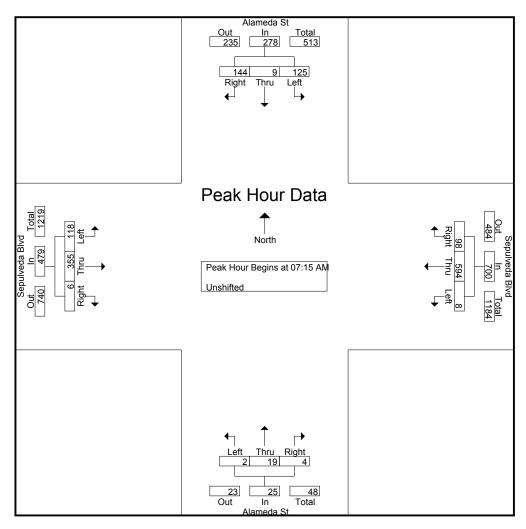
			lameda St uthbound			llveda Blvd estbound	l IIIIcu- C	Al	ameda St rthbound			lveda Blvd stbound		
Ctor	t Time	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Int. Total
	00 AM	21	8	34	Len	66	14	0	1	0	9	36	0	193
	15 AM	20	6	34	3	108	15	1	5	0	15	45	0	252
	30 AM	34	7	44	0	154	30	0	3	0	16	43 67	1	356
	45 AM	29	4	33	0	158	30	0	6	0	33	77	0	370
00.	Total	104	25	145	7	486	89	1	15	0	73	225	1	1171
	10tai	104	23	143	,	400	09	1	13	0	13	223	1	11/1
07:	00 AM	33	2	26	1	125	26	0	2	1	29	88	1	334
	15 AM	26	4	36	1	164	27	1	5	1	24	85	2	376
	30 AM	38	2	33	2	152	26	0	3	1	28	83	3	371
	45 AM	32	1	39	3	148	25	0	5	2	31	89	1	376
	Total	129	9	134	7	589	104	1	15	5	112	345	7	1457
00.	00 AM	29	2	36	2	130	20	1	6	0	35	98	0	359
	15 AM	29	3	28	2	119	20	_	6 6	4	30	83	0	328
	30 AM	39		28	1	103	30	2		0	30 24		0	
	45 AM	39 25	3 4	37	0	103	30	1	2	0	24 18	83 75	0	308 299
08.	Total	122	12	124	5	459	102	4	15	4	107	339	1	1294
	,						·			·			·	
04:	00 PM	32	4	28	1	101	68	2	5	2	46	186	1	476
04:	15 PM	46	4	23	0	112	71	1	4	4	52	213	0	530
	30 PM	44	1	39	1	103	69	1	6	5	64	247	0	580
04:	45 PM	34	5	33	1	120	70	1	6	3	62	219	0	554
	Total	156	14	123	3	436	278	5	21	14	224	865	1	2140
05:	00 PM	32	4	40	0	130	69	2	2	3	59	243	0	584
05:	15 PM	35	2	60	1	151	51	0	2	2	42	210	0	556
05:	30 PM	27	1	39	0	133	48	1	3	1	66	263	1	583
05:	45 PM	40	5	32	0	103	30	0	2	3	44	224	0	483
	Total	134	12	171	1	517	198	3	9	9	211	940	1	2206
Grand	l Total	645	72	697	23	2487	771	14	75	32	727	2714	11	8268
	orch %	45.6	5.1	49.3	0.7	75.8	23.5	11.6	62	26.4	21.1	78.6	0.3	
	otal %	7.8	0.9	8.4	0.3	30.1	9.3	0.2	0.9	0.4	8.8	32.8	0.1	

626.991.7522 www.ctcounters.com

File Name: Sepulveda\_Alameda\_onSepulveda

Site Code : 00000000 Start Date : 8/20/2014

		Alame	eda St			Sepulve	da Blvd			Alam	eda St			Sepulve	da Blvd		
		South	oound			Westl	oound			North	bound			Easth	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 0	6:00 AM	to 11:45	AM - Peak	1 of 1		_				-				-		
Peak Hour for Ent	ire Interse	ction Beg	gins at 07	7:15 AM													
07:15 AM	26	4	36	66	1	164	27	192	1	5	1	7	24	85	2	111	376
07:30 AM	38	2	33	73	2	152	26	180	0	3	1	4	28	83	3	114	371
07:45 AM	32	1	39	72	3	148	25	176	0	5	2	7	31	89	1	121	376
08:00 AM	29	2	36	67	2	130	20	152	1	6	0	7	35	98	0	133	359
Total Volume	125	9	144	278	8	594	98	700	2	19	4	25	118	355	6	479	1482
% App. Total	45	3.2	51.8		1.1	84.9	14		8	76	16		24.6	74.1	1.3		
PHF	.822	.563	.923	.952	.667	.905	.907	.911	.500	.792	.500	.893	.843	.906	.500	.900	.985

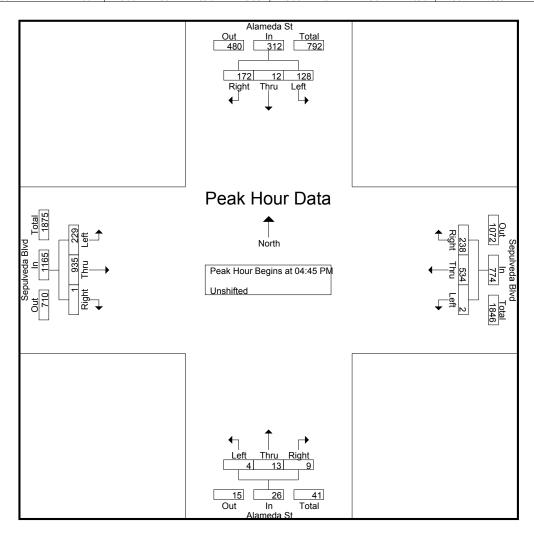


626.991.7522 Appendix E www.ctcounters.com

File Name: Sepulveda\_Alameda\_onSepulveda

Site Code : 00000000 Start Date : 8/20/2014

		Alame	eda St			Sepulve	da Blvd			Alam	eda St			Sepulve	da Blvd		
		South	ound			Westl	oound			North	bound			Eastl	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 1	2:00 PM	to 05:45	PM - Peak	1 of 1												
Peak Hour for Ent	ire Interse	ction Beg	gins at $04$	1:45 PM													
04:45 PM	34	5	33	72	1	120	70	191	1	6	3	10	62	219	0	281	554
05:00 PM	32	4	40	76	0	130	69	199	2	2	3	7	59	243	0	302	584
05:15 PM	35	2	60	97	1	151	51	203	0	2	2	4	42	210	0	252	556
05:30 PM	27	1	39	67	0	133	48	181	1	3	1	5	66	263	1	330	583
Total Volume	128	12	172	312	2	534	238	774	4	13	9	26	229	935	1	1165	2277
% App. Total	41	3.8	55.1		0.3	69	30.7		15.4	50	34.6		19.7	80.3	0.1		
PHF	.914	.600	.717	.804	.500	.884	.850	.953	.500	.542	.750	.650	.867	.889	.250	.883	.975



626.991.7522 www.ctcounters.com

File Name: Alameda\_405SBRamps

Site Code : 00000000 Start Date : 8/20/2014

Page No : 1

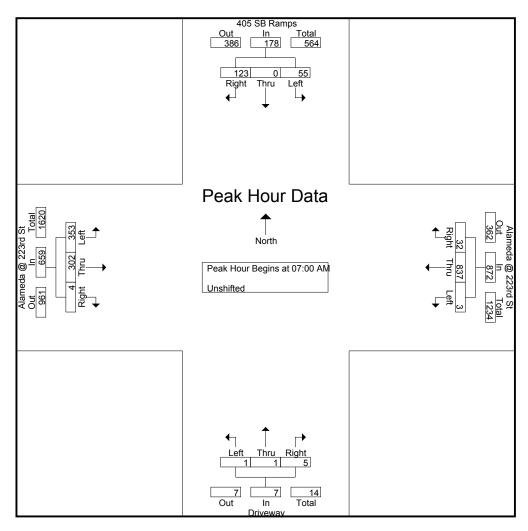
						rintea- U							
		SB Ramps			a @ 223rd	St		riveway			a @ 223rd	St	
		thbound			estbound			thbound			stbound		
Start Time	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Int. Total
06:00 AM	2	1	33	0	79	6	2	3	7	62	35	3	233
06:15 AM	8	0	35	6	101	6	4	4	4	67	37	1	273
06:30 AM	8	1	31	2	165	7	0	3	3	66	40	1	327
06:45 AM	3	2	35	0	173	4	1	0	1	71	57	1	348
Total	21	4	134	8	518	23	7	10	15	266	169	6	1181
1			1			1						1	
07:00 AM	6	0	27	0	202	7	1	0	2	79	56	0	380
07:15 AM	12	0	25	0	204	7	0	1	2	84	75	0	410
07:30 AM	22	0	37	2	231	15	0	0	0	95	83	2	487
07:45 AM	15	0	34	1	200	3	0	0	1	95	88	2	439
Total	55	0	123	3	837	32	1	1	5	353	302	4	1716
			1			. 1			- 1			. 1	
08:00 AM	12	0	28	2	162	4	3	0	0	86	70	4	371
08:15 AM	12	0	41	1	137	10	0	0	0	98	77	1	377
08:30 AM	7	0	31	0	109	4	1	1	0	78	63	2	296
08:45 AM	9	0	35	11	105	5	0	0	0	79	64	0	298
Total	40	0	135	4	513	23	4	1	0	341	274	7	1342
04.00 704	10	0	ا م	2				0	ا م	106	100	ا م	<b>7</b> 00
04:00 PM	13	0	8	3	74	14	1	0	2	186	199	0	500
04:15 PM	21	0	13	2	78	5	0	2	0	198	217	1	537
04:30 PM	26	1	8	0	65	19	1	0 2	1	210	204	14	549
04:45 PM	31	0		1	93	12	0		0	213	202	16	566
Total	91	1	40	6	310	50	2	4	3	807	822	16	2152
05:00 PM	26	1	ر ا	1	100	25	1	2	2	227	100	2	506
05:00 PM 05:15 PM	36 32	1	6 11	1	100	25 21	1	3	$\begin{bmatrix} 2 \\ 0 \end{bmatrix}$	227 190	192 200	2	596
		0	7	2	89		•	1				i	548
05:30 PM	24	0		4	77	18	0	1	2	185	208	0	526
05:45 PM	32 124	1	10 34	3 10	71	12	3	6	0	180	200	0	511
Total	124	2	34	10	337	76	3	6	4	782	800	3	2181
Constant	221	7	166	21	2515	204	17	22	27	25.40	2267	36	9573
Grand Total	331	7	466	31	2515	204	17	22	27	2549	2367		8572
Apprch %	41.2	0.9	58	1.1	91.5	7.4	25.8	33.3	40.9	51.5	47.8	0.7	
Total %	3.9	0.1	5.4	0.4	29.3	2.4	0.2	0.3	0.3	29.7	27.6	0.4	

626.991.7522 www.ctcounters.com

File Name: Alameda\_405SBRamps

Site Code : 00000000 Start Date : 8/20/2014

		405 SB	Ramps		Al	ameda @	223rd	St		Driv	eway		Al	ameda @	223rd	St	
		South	ound			Westl	oound			North	bound			Eastb	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 0	6:00 AM	to 11:45	AM - Peak	1 of 1		-				-				-		
Peak Hour for Ent	ire Interse	ction Beg	gins at $07$	7:00 AM													
07:00 AM	6	0	27	33	0	202	7	209	1	0	2	3	79	56	0	135	380
07:15 AM	12	0	25	37	0	204	7	211	0	1	2	3	84	75	0	159	410
07:30 AM	22	0	37	59	2	231	15	248	0	0	0	0	95	83	2	180	487
07:45 AM	15	0	34	49	1	200	3	204	0	0	1	1	95	88	2	185	439
Total Volume	55	0	123	178	3	837	32	872	1	1	5	7	353	302	4	659	1716
% App. Total	30.9	0	69.1		0.3	96	3.7		14.3	14.3	71.4		53.6	45.8	0.6		
PHF	.625	.000	.831	.754	.375	.906	.533	.879	.250	.250	.625	.583	.929	.858	.500	.891	.881

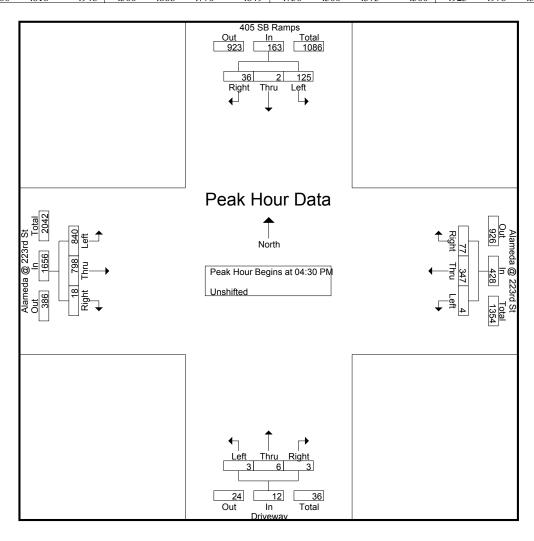


626.991.7522 www.ctcounters.com

File Name: Alameda\_405SBRamps

Site Code : 00000000 Start Date : 8/20/2014

																	_
		405 SB	Ramps		Al	ameda (	@ 223rd	St		Driv	eway		Al	ameda (	@ 223rd	St	
		South	bound			Westl	oound			North	bound			Eastl	oound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 1	2:00 PM	to 05:45	PM - Peak	1 of 1												
Peak Hour for Ent	ire Interse	ection Be	gins at 04	4:30 PM													
04:30 PM	26	1	8	35	0	65	19	84	1	0	1	2	210	204	14	428	549
04:45 PM	31	0	11	42	1	93	12	106	0	2	0	2	213	202	1	416	566
05:00 PM	36	1	6	43	1	100	25	126	1	3	2	6	227	192	2	421	596
05:15 PM	32	0	11	43	2	89	21	112	1	1	0	2	190	200	1	391	548
Total Volume	125	2	36	163	4	347	77	428	3	6	3	12	840	798	18	1656	2259
% App. Total	76.7	1.2	22.1		0.9	81.1	18		25	50	25		50.7	48.2	1.1		
PHF	.868	.500	.818	.948	.500	.868	.770	.849	.750	.500	.375	.500	.925	.978	.321	.967	.948



626.991.7522 www.ctcounters.com

File Name : Sepulveda\_TerminalIslandFrwy103 Site Code : 00000000

Start Date : 8/20/2014

Page No : 1

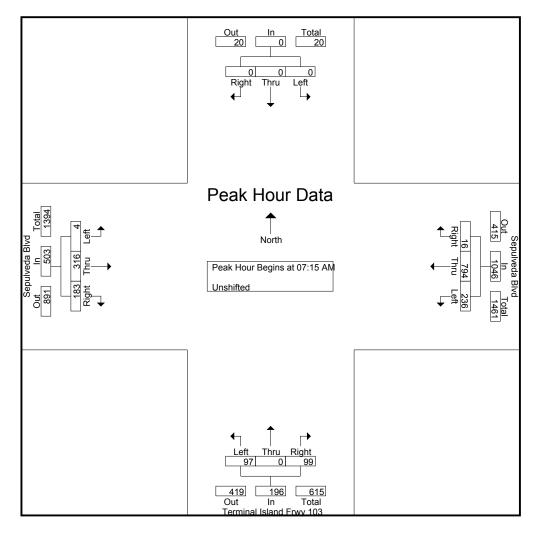
						rinted- U							
					ılveda Blvd			Island Frw	y 103		lveda Blvd		
		thbound		W	estbound			rthbound			stbound		
Start Time	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Int. Total
06:00 AM	0	0	0	42	99	0	6	0	18	0	28	13	206
06:15 AM	0	0	0	50	143	0	17	0	10	0	34	11	265
06:30 AM	0	0	0	67	197	0	21	0	23	0	35	25	368
06:45 AM	0	0	0	55	186	4	20	0	21	0	66	27	379
Total	0	0	0	214	625	4	64	0	72	0	163	76	1218
07:00 AM	0	0	0	47	147	3	27	0	19	1	61	34	339
07:15 AM	0	0	0	73	194	0	23	0	22	2	67	44	425
07:30 AM	0	0	0	59	230	8	22	0	24	0	78	55	476
07:45 AM	0	0	0	66	206	5	34	0	28	2	93	39	473
Total	0	0	0	245	777	16	106	0	93	5	299	172	1713
						i							
08:00 AM	0	0	0	38	164	3	18	0	25	0	78	45	371
08:15 AM	0	0	0	29	128	1	20	0	24	0	75	32	309
08:30 AM	0	0	0	33	117	2	35	0	18	1	75	46	327
08:45 AM	0	0	0	19	109	1	39	0	27	1	70	33	299
Total	0	0	0	119	518	7	112	0	94	2	298	156	1306
1													
04:00 PM	0	0	0	55	88	1	75	1	44	0	192	44	500
04:15 PM	0	0	0	45	96	1	88	1	59	0	232	56	578
04:30 PM	0	0	0	53	94	1	55	0	55	1	266	67	592
04:45 PM	0	0	0	55	103	1	102	0	55	0	248	63	627
Total	0	0	0	208	381	4	320	2	213	1	938	230	2297
1												1	
05:00 PM	0	0	0	38	105	0	60	0	67	0	245	80	595
05:15 PM	0	0	0	37	111	0	82	0	78	0	226	58	592
05:30 PM	0	0	0	37	106	0	67	0	48	0	281	55	594
05:45 PM	0	0	0	35	96	0	37	0	30	0	229	63	490
Total	0	0	0	147	418	0	246	0	223	0	981	256	2271
Grand Total	0	0	0	933	2719	31	848	2	695	8	2679	890	8805
Apprch %	0	0	0	25.3	73.8	0.8	54.9	0.1	45	0.2	74.9	24.9	
Total %	0	0	0	10.6	30.9	0.4	9.6	0	7.9	0.1	30.4	10.1	

626.991.7522 www.ctcounters.com

File Name: Sepulveda\_TerminalIslandFrwy103

Site Code : 00000000 Start Date : 8/20/2014

						Sepulve	da Blvd		Term	inal Isla	nd Frw	y 103		Sepulve	da Blvd		
		South	oound			Westl	oound			North	bound			Eastb	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 0	6:00 AM	to 11:45	AM - Peak	1 of 1		-				-				-		
Peak Hour for Ent	ire Interse	ction Beg	gins at 07	7:15 AM													
07:15 AM	0	0	0	0	73	194	0	267	23	0	22	45	2	67	44	113	425
07:30 AM	0	0	0	0	59	230	8	297	22	0	24	46	0	78	55	133	476
07:45 AM	0	0	0	0	66	206	5	277	34	0	28	62	2	93	39	134	473
08:00 AM	0	0	0	0	38	164	3	205	18	0	25	43	0	78	45	123	371
Total Volume	0	0	0	0	236	794	16	1046	97	0	99	196	4	316	183	503	1745
% App. Total	0	0	0		22.6	75.9	1.5		49.5	0	50.5		0.8	62.8	36.4		
PHF	.000	.000	.000	.000	.808	.863	.500	.880	.713	.000	.884	.790	.500	.849	.832	.938	.916

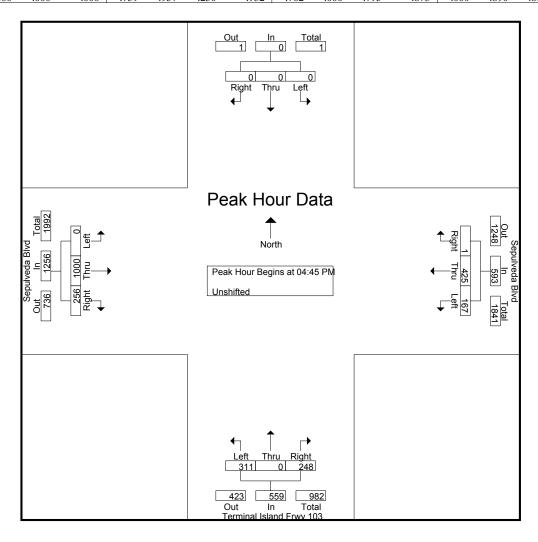


626.991.7522 Appendix E www.ctcounters.com

File Name : Sepulveda\_TerminalIslandFrwy103 Site Code : 00000000

Start Date : 8/20/2014

																	_
						Sepulve	da Blvd		Term	inal Isla	nd Frw	y 103	;	Sepulve	da Blvd		
		Southb	ound			West	oound			North	bound			Eastl	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 1:	2:00 PM	to 05:45	PM - Peak	1 of 1												
Peak Hour for Ent	ire Interse	ction Beg	gins at 04	1:45 PM													
04:45 PM	0	0	0	0	55	103	1	159	102	0	55	157	0	248	63	311	627
05:00 PM	0	0	0	0	38	105	0	143	60	0	67	127	0	245	80	325	595
05:15 PM	0	0	0	0	37	111	0	148	82	0	78	160	0	226	58	284	592
05:30 PM	0	0	0	0	37	106	0	143	67	0	48	115	0	281	55	336	594
Total Volume	0	0	0	0	167	425	1	593	311	0	248	559	0	1000	256	1256	2408
% App. Total	0	0	0		28.2	71.7	0.2		55.6	0	44.4		0	79.6	20.4		
PHF	.000	.000	.000	.000	.759	.957	.250	.932	.762	.000	.795	.873	.000	.890	.800	.935	.960



626.991.7522 www.ctcounters.com

File Name : Sepulveda\_SantaFe Site Code : 00000000 Start Date : 8/20/2014

Page No : 1

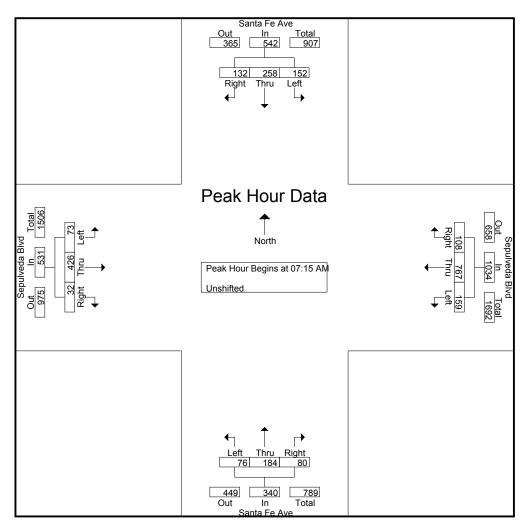
						rintea- U							
		ıta Fe Ave			lveda Blvd		San	ta Fe Ave			veda Blvd		
	Sor	uthbound		We	estbound		No	rthbound		Ea	stbound		
Start Time	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Int. Total
06:00 AM	14	24	14	9	114	15	11	22	10	6	55	4	298
06:15 AM	20	27	15	14	130	22	18	23	11	2	51	5	338
06:30 AM	28	37	27	9	194	17	18	35	15	4	68	6	458
06:45 AM	29	42	25	19	201	23	15	31	7	18	100	6	516
Total	91	130	81	51	639	77	62	111	43	30	274	21	1610
07:00 AM	24	38	26	15	184	24	23	36	8	12	84	2	476
07:15 AM	38	62	42	31	200	27	16	42	17	16	98	6	595
07:30 AM	30	56	38	45	201	21	22	40	23	27	106	4	613
07:45 AM	51	72	35	50	200	34	19	55	23	15	126	15	695
Total	143	228	141	141	785	106	80	173	71	70	414	27	2379
						1			1			1	
08:00 AM	33	68	17	33	166	26	19	47	17	15	96	7	544
08:15 AM	34	55	20	22	115	19	16	40	15	19	94	13	462
08:30 AM	34	47	16	19	120	36	20	37	31	10	97	8	475
08:45 AM	51	50	10	33	108	25	12	32	20	10	84	7	442
Total	152	220	63	107	509	106	67	156	83	54	371	35	1923
1						1			1			1	
04:00 PM	70	76	23	41	111	43	24	72	40	33	202	10	745
04:15 PM	59	81	21	39	118	38	15	77	47	34	242	7	778
04:30 PM	70	69	16	31	129	42	17	112	45	31	270	13	845
04:45 PM	85	91	17	29	133	34	18	122	61	40	247	8	885
Total	284	317	77	140	491	157	74	383	193	138	961	38	3253
0.5.00.77.5			ایما	•		- 1			ا مر	4.0	•••	ا م	
05:00 PM	82	71	21	30	90	34	21	98	49	40	228	9	773
05:15 PM	94	80	8	47	131	39	26	96	45	29	237	13	845
05:30 PM	81	71	15	45	116	31	21	85	41	29	238	6	779
05:45 PM	75	86	9	52	104	47	21	63	43	33	233	16	782
Total	332	308	53	174	441	151	89	342	178	131	936	44	3179
a .m . l	4000		اعبيا		• • • •				o I		• • • •		
Grand Total	1002	1203	415	613	2865	597	372	1165	568	423	2956	165	12344
Apprch %	38.2	45.9	15.8	15	70.3	14.7	17.7	55.3	27	11.9	83.4	4.7	
Total %	8.1	9.7	3.4	5	23.2	4.8	3	9.4	4.6	3.4	23.9	1.3	

626.991.7522 www.ctcounters.com

File Name: Sepulveda\_SantaFe

Site Code : 00000000 Start Date : 8/20/2014

		Santa l	Fe Ave			Sepulve	da Blvd			Santa	Fe Ave		i	Sepulve	da Blvd		
		South	oound			Westl	oound			North	bound			Eastb	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 0	6:00 AM	to 11:45	AM - Peak	1 of 1		_				_				_		
Peak Hour for Ent	ire Interse	ction Beg	gins at $07$	1:15 AM													
07:15 AM	38	62	42	142	31	200	27	258	16	42	17	75	16	98	6	120	595
07:30 AM	30	56	38	124	45	201	21	267	22	40	23	85	27	106	4	137	613
07:45 AM	51	72	35	158	50	200	34	284	19	55	23	97	15	126	15	156	695
08:00 AM	33	68	17	118	33	166	26	225	19	47	17	83	15	96	7	118	544
Total Volume	152	258	132	542	159	767	108	1034	76	184	80	340	73	426	32	531	2447
% App. Total	28	47.6	24.4		15.4	74.2	10.4		22.4	54.1	23.5		13.7	80.2	6		
PHF	.745	.896	.786	.858	.795	.954	.794	.910	.864	.836	.870	.876	.676	.845	.533	.851	.880

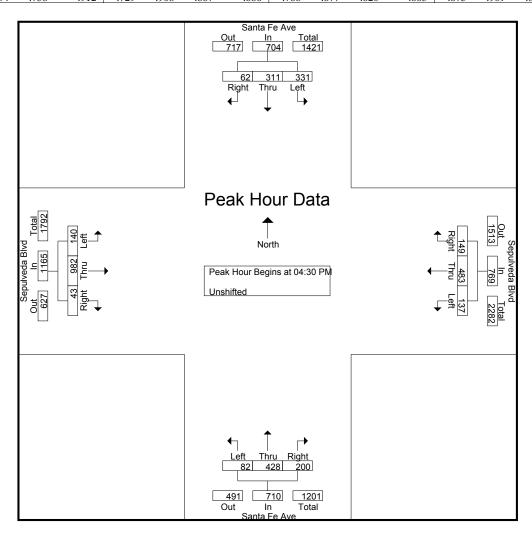


626.991.7522 Appendix E www.ctcounters.com

File Name: Sepulveda\_SantaFe

Site Code : 000000000 Start Date : 8/20/2014

																	_
		Santa I	Fe Ave			Sepulve	da Blvd			Santa	Fe Ave			Sepulve	da Blvd		
		South	ound			Westl	oound			North	bound			Eastl	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 1	2:00 PM	to 05:45	PM - Peak	1 of 1												
Peak Hour for Ent	ire Interse	ection Beg	gins at 04	:30 PM													
04:30 PM	70	69	16	155	31	129	42	202	17	112	45	174	31	270	13	314	845
04:45 PM	85	91	17	193	29	133	34	196	18	122	61	201	40	247	8	295	885
05:00 PM	82	71	21	174	30	90	34	154	21	98	49	168	40	228	9	277	773
05:15 PM	94	80	8	182	47	131	39	217	26	96	45	167	29	237	13	279	845
Total Volume	331	311	62	704	137	483	149	769	82	428	200	710	140	982	43	1165	3348
% App. Total	47	44.2	8.8		17.8	62.8	19.4		11.5	60.3	28.2		12	84.3	3.7		
PHF	.880	.854	.738	.912	.729	.908	.887	.886	.788	.877	.820	.883	.875	.909	.827	.928	.946



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File Name : Willow\_710SBRamps Site Code : 00000000

Start Date : 8/20/2014

Page No : 1

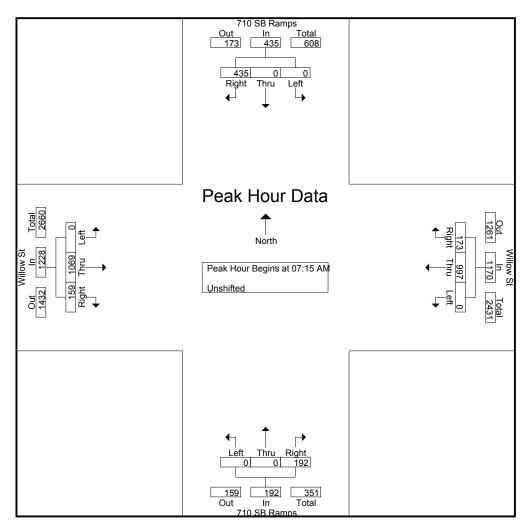
						Timicu- C							
		SB Ramps			/illow St			SB Ramps			illow St		
	Sou	thbound		We	estbound		No	rthbound		Ea	stbound		
Start Time	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Int. Total
06:00 AM	0	0	74	0	90	22	0	0	15	0	131	21	353
06:15 AM	0	0	81	0	134	18	0	0	30	0	184	28	475
06:30 AM	0	0	135	0	174	28	0	0	30	0	200	26	593
06:45 AM	0	0	112	0	193	23	0	0	34	0	221	39	622
Total	0	0	402	0	591	91	0	0	109	0	736	114	2043
07:00 AM	0	0	80	0	196	19	0	0	34	0	227	16	572
07:15 AM	0	0	137	0	215	42	0	0	50	0	242	39	725
07:30 AM	0	0	98	0	291	51	0	0	43	0	259	37	779
07:45 AM	0	0	111	0	261	48	0	0	47	0	323	42	832
Total	0	0	426	0	963	160	0	0	174	0	1051	134	2908
08:00 AM	0	0	89	0	230	32	0	0	52	0	245	41	689
08:15 AM	0	0	90	0	200	30	0	0	44	0	272	33	669
08:30 AM	0	0	68	0	179	29	0	0	54	0	269	51	650
08:45 AM	0	0	71	0	192	24	0	0	58	0	281	38	664_
Total	0	0	318	0	801	115	0	0	208	0	1067	163	2672
04:00 PM	0	0	131	0	262	18	0	0	95	0	409	53	968
04:15 PM	0	0	161	0	261	21	0	0	93	0	426	55	1017
04:30 PM	0	0	139	0	288	30	0	0	129	0	462	55	1103
04:45 PM	0	0	118	0	290	26	0	0	99	0	441	48	1022
Total	0	0	549	0	1101	95	0	0	416	0	1738	211	4110
05:00 PM	0	0	211	0	317	31	0	0	109	0	475	70	1213
05:15 PM	0	0	254	0	299	22	0	0	103	0	451	57	1186
05:30 PM	0	0	196	0	340	16	0	0	104	0	446	73	1175
05:45 PM	0	0	295	0	317	23	0	0	87	0	420	55	1197
Total	0	0	956	0	1273	92	0	0	403	0	1792	255	4771
Grand Total	0	0	2651	0	4729	553	0	0	1310	0	6384	877	16504
Apprch %	0	0	100	0	89.5	10.5	0	0	100	0	87.9	12.1	
Total %	0	0	16.1	0	28.7	3.4	0	0	7.9	0	38.7	5.3	

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File Name: Willow\_710SBRamps

Site Code : 00000000 Start Date : 8/20/2014

		710 SB	Ramps			Will	ow St			710 SB	Ramps			Will	ow St		
		South	ound			Westl	oound			North	bound			Eastb	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 0	6:00 AM	to 11:45	AM - Peak	1 of 1		-				-				-		
Peak Hour for Ent	ire Interse	ction Beg	gins at 07	1:15 AM													
07:15 AM	0	0	137	137	0	215	42	257	0	0	50	50	0	242	39	281	725
07:30 AM	0	0	98	98	0	291	51	342	0	0	43	43	0	259	37	296	779
07:45 AM	0	0	111	111	0	261	48	309	0	0	47	47	0	323	42	365	832
08:00 AM	0	0	89	89	0	230	32	262	0	0	52	52	0	245	41	286	689
Total Volume	0	0	435	435	0	997	173	1170	0	0	192	192	0	1069	159	1228	3025
% App. Total	0	0	100		0	85.2	14.8		0	0	100		0	87.1	12.9		
PHF	.000	.000	.794	.794	.000	.857	.848	.855	.000	.000	.923	.923	.000	.827	.946	.841	.909

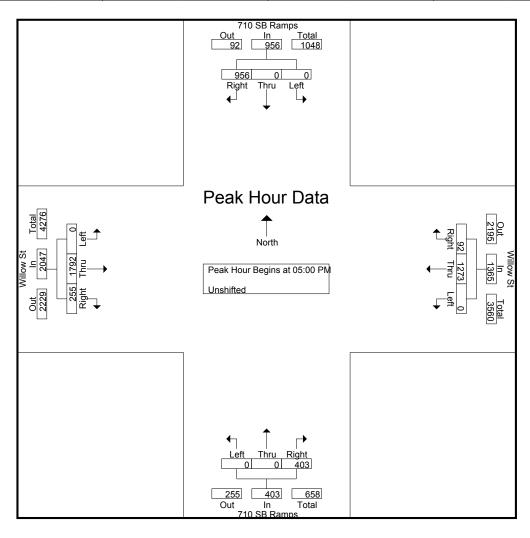


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File Name: Willow\_710SBRamps

Site Code : 00000000 Start Date : 8/20/2014

		710 SB	Ramps			Will	ow St			710 SB	Ramps			Will	ow St		
		Southb	ound			Westl	oound			North	bound			Eastb	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 12	2:00 PM 1	to 05:45	PM - Peak	1 of 1												
Peak Hour for Ent	ire Interse	ction Beg	gins at 05	5:00 PM													
05:00 PM	0	0	211	211	0	317	31	348	0	0	109	109	0	475	70	545	1213
05:15 PM	0	0	254	254	0	299	22	321	0	0	103	103	0	451	57	508	1186
05:30 PM	0	0	196	196	0	340	16	356	0	0	104	104	0	446	73	519	1175
05:45 PM	0	0	295	295	0	317	23	340	0	0	87	87	0	420	55	475	1197
Total Volume	0	0	956	956	0	1273	92	1365	0	0	403	403	0	1792	255	2047	4771
% App. Total	0	0	100		0	93.3	6.7		0	0	100		0	87.5	12.5		
PHF	.000	.000	.810	.810	.000	.936	.742	.959	.000	.000	.924	.924	.000	.943	.873	.939	.983



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File Name: Willow\_710NBRamps Site Code: 00000000

Start Date : 8/20/2014

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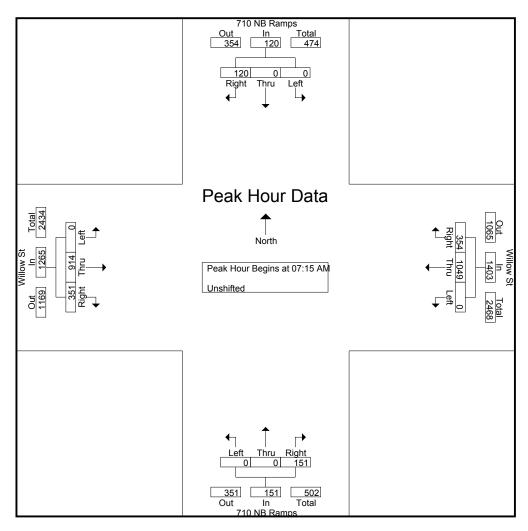
						rintea- U							
		<b>NB Ramps</b>			illow St			NB Ramps			illow St		
		thbound			estbound			rthbound			stbound		
Start Time	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Left	Thru	Right	Int. Total
06:00 AM	0	0	15	0	97	73	0	0	18	0	91	52	346
06:15 AM	0	0	22	0	127	78	0	0	18	0	129	88	462
06:30 AM	0	0	21	0	185	117	0	0	20	0	150	95	588
06:45 AM	0	0	21	0	191	110	0	0	31	0	172	81	606_
Total	0	0	79	0	600	378	0	0	87	0	542	316	2002
												1	
07:00 AM	0	0	22	0	196	105	0	0	25	0	172	89	609
07:15 AM	0	0	29	0	229	93	0	0	22	0	203	92	668
07:30 AM	0	0	35	0	304	92	0	0	44	0	215	87	777
07:45 AM	0	0	34	0	276	88	0	0	40	0	267	100	805
Total	0	0	120	0	1005	378	0	0	131	0	857	368	2859
1			1			1						i	
08:00 AM	0	0	22	0	240	81	0	0	45	0	229	72	689
08:15 AM	0	0	21	0	210	66	0	0	28	0	225	90	640
08:30 AM	0	0	23	0	186	50	0	0	31	0	221	97	608
08:45 AM	0	0	27	0	188	75	0	0	26	0	258	79	653
Total	0	0	93	0	824	272	0	0	130	0	933	338	2590
0.4.00 77.5			ا م						ا مما		400		0=0
04:00 PM	0	0	19	0	257	66	0	0	33	0	400	103	878
04:15 PM	0	0	24	0	260	54	0	0	29	0	409	112	888
04:30 PM	0	0	26	0	294	62	0	0	24	0	447	136	989
04:45 PM	0	0	21	0	297	63	0	0	26	0	460	81	948
Total	0	0	90	0	1108	245	0	0	112	0	1716	432	3703
05.00 DM	0	0	16	0	220	02	0	0	22	0	400	00	10.42
05:00 PM	0	0	16	0	330	93	0	0	23	0	492	89	1043
05:15 PM	0	0	19	0	304	71	0	0	21	0	454	99	968
05:30 PM	0	0	38	0	315	69	0	0	38	0	454	94	1008
05:45 PM	0	0	32	0	307	73	0	0	19	0	416	94	941
Total	0	0	105	0	1256	306	0	0	101	0	1816	376	3960
G 155 1	0	0	407	0	4702	1570	0	0	561	0	5064	1020	15114
Grand Total	0	0	487	0	4793	1579	0	0	561	0	5864	1830	15114
Apprch %	0	0	100	0	75.2	24.8	0	0	100	0	76.2	23.8	
Total %	0	0	3.2	0	31.7	10.4	0	0	3.7	0	38.8	12.1	

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File Name: Willow\_710NBRamps

Site Code : 00000000 Start Date : 8/20/2014

		710 NB	Ramps			Will	ow St			710 NB	Ramps			Will	ow St		
		Southb	ound			Westl	ound			North	bound			Eastb	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 0	6:00 AM	to 11:45	AM - Peak	1 of 1		_				_				_		
Peak Hour for Ent	ire Interse	ction Beg	gins at 07	:15 AM													
07:15 AM	0	0	29	29	0	229	93	322	0	0	22	22	0	203	92	295	668
07:30 AM	0	0	35	35	0	304	92	396	0	0	44	44	0	215	87	302	777
07:45 AM	0	0	34	34	0	276	88	364	0	0	40	40	0	267	100	367	805
08:00 AM	0	0	22	22	0	240	81	321	0	0	45	45	0	229	72	301	689
Total Volume	0	0	120	120	0	1049	354	1403	0	0	151	151	0	914	351	1265	2939
% App. Total	0	0	100		0	74.8	25.2		0	0	100		0	72.3	27.7		
PHF	.000	.000	.857	.857	.000	.863	.952	.886	.000	.000	.839	.839	.000	.856	.878	.862	.913

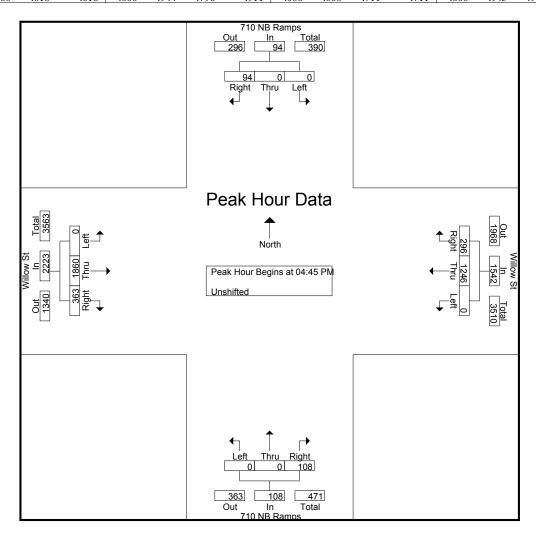


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File Name: Willow\_710NBRamps

Site Code : 00000000 Start Date : 8/20/2014

																	_
		710 NB	Ramps			Will	ow St			710 NB	Ramps			Will	ow St		
		South	oound			Westl	bound			North	bound			Eastl	ound		
Start Time	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Left	Thru	Right	App. Total	Int. Total
Peak Hour Analys	is From 1:	2:00 PM	to 05:45	PM - Peak	1 of 1												
Peak Hour for Ent	ire Interse	ection Be	gins at 04	4:45 PM													
04:45 PM	0	0	21	21	0	297	63	360	0	0	26	26	0	460	81	541	948
05:00 PM	0	0	16	16	0	330	93	423	0	0	23	23	0	492	89	581	1043
05:15 PM	0	0	19	19	0	304	71	375	0	0	21	21	0	454	99	553	968
05:30 PM	0	0	38	38	0	315	69	384	0	0	38	38	0	454	94	548	1008
Total Volume	0	0	94	94	0	1246	296	1542	0	0	108	108	0	1860	363	2223	3967
% App. Total	0	0	100		0	80.8	19.2		0	0	100		0	83.7	16.3		
PHF	.000	.000	.618	.618	.000	.944	.796	.911	.000	.000	.711	.711	.000	.945	.917	.957	.951



# **APPENDIX B: LOS CALCULATION SHEETS**



# **Traffic Impact Analysis**

**EXISTING CONDITIONS (BASELINE)** 



Project: Tesoro Los Angeles Refinery Traffic Study

Int #: 3

North/South Street: WILMINGTON AVENUE

LT

RT

ΤH

LT

RT

ΤH

LT

1.00

0.50

2.50

1.00

1.00

2.00

1.00

East/West Street: 223RD STREET

Scenario: Existing Conditions

Thru Lane:	1600 vph	N-S Split Phase :	N
Left-Turn Lane:	1600 vph	E-W Split Phase:	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	1.00	319	1,600	0.114	N-S(1):	0.160
	TH	2.00	647	3,200	0.202 *	N-S(2):	0.209 *
	LT	1.00	57	1,600	0.036	E-W(1):	0.295
Westbound	RT	1.00	53	1,600	0.000	E-W(2):	0.334 *
	TH	2.00	794	3,200	0.248 *		
	LT	1.00	200	1,600	0.125	V/C:	0.543
Northbound	RT	0.50	80	800	0.000	Lost Time:	0.100
	TH	2.50	494	4,000	0.124		
	LT	1.00	11	1,600	0.007 *		
Eastbound	RT	1.00	16	1,600	0.003	ICU:	0.643
	TH	2.00	545	3,200	0.170		
	LT	1.00	137	1,600	0.086 *	LOS:	В
Peak Period:	PM PEAK F	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	1.00	199	1,600	0.000	N-S(1):	0.138
	TH	2.00	724	3,200	0.226 *	N-S(2):	0.231 *
	LT	1.00	55	1,600	0.034	E-W(1):	0.359 *
Westbound	RT	1.00	143	1,600	0.055	E-W(2):	0.258
	TH	2.00	345	3,200	0.108		

177

124

416

8

10

792

240

1,600

800

4,000

1,600

1,600

3,200

1,600

0.111 \*

0.000

0.104

0.001

0.150

0.005 \*

0.248 \*

V/C:

ICU:

LOS:

Lost Time:

0.590

0.100

0.690

В

Northbound

Eastbound

<sup>\* =</sup> Critical Movement

Tesoro Los Angeles Refinery Traffic Study 5 Project: Int #:

North/South Street: 223rd Street Ramp (on Alameda Street)

East/West Street: **Alameda Street** 

**Existing Conditions** Scenario:

Thru Lane:	1600 vph	N-S Split Phase :	N
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK I	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.250 *
	TH	3.00	1,122	4,800	0.234	N-S(2):	0.234
	LT	1.00	159	1,600	0.099 *	E-W(1):	0.110 *
Westbound	RT	1.00	119	1,600	0.000	E-W(2):	0.000
	TH	0.00	0	0	0.000		
	LT	1.00	176	1,600	0.110 *	V/C:	0.360
Northbound	RT	0.00	242	1,600	0.151 *	Lost Time:	0.100
	TH	3.00	471	3,200	0.147		
	LT	0.00	0	0	0.000		
Eastbound	RT	0.00	0	0	0.000	ICU:	0.460
	TH	0.00	0	0	0.000 *		
	LT	0.00	0	0	0.000	LOS:	Α
Peak Period:	PM PEAK H	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.401 *
	TH	3.00	980	4,800	0.204	N-S(2):	0.204
	LT	1.00	164	1,600	0.103 *	E-W(1):	0.069 *
Martha L	D.T.	4 00	400	4 000	0.000	E 14/(0)	0.000

Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.401 *
	TH	3.00	980	4,800	0.204	N-S(2):	0.204
	LT	1.00	164	1,600	0.103 *	E-W(1):	0.069 *
Westbound	RT	1.00	122	1,600	0.000	E-W(2):	0.000
	TH	0.00	0	0	0.000		
	LT	1.00	111	1,600	0.069 *	V/C:	0.470
Northbound	RT	0.00	461	0	0.000	Lost Time:	0.100
	TH	3.00	968	4,800	0.298 *		
	LT	0.00	0	0	0.000		
Eastbound	RT	0.00	0	0	0.000	ICU:	0.570
	TH	0.00	0	0	0.000 *		
	LT	0.00	0	0	0.000	LOS:	Α

<sup>\* =</sup> Critical Movement

Project: Int #: **Tesoro Los Angeles Refinery Traffic Study** 

North/South Street: 223rd Street

Alameda Street Ramp East/West Street:

**Existing Conditions** Scenario:

Thru Lane:	1600 vph	N-S Split Phase :	N
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK H	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.088 *
	TH	0.00	0	0	0.000	N-S(2):	0.081
	LT	0.00	0	0	0.000 *	E-W(1):	0.161 *
Westbound	RT	0.00	0	0	0.000	E-W(2):	0.141
	TH	3.00	747	5,280	0.141		
	LT	2.00	223	3,168	0.070 *	V/C:	0.249
Northbound	RT	1.00	266	1,760	0.088 *	Lost Time:	0.100
	TH	0.00	0	0	0.000		
	LT	1.00	143	1,760	0.081		
Eastbound	RT	0.00	80	0	0.000	ICU:	0.349
	TH	3.00	398	5,280	0.091 *		
	LT	0.00	0	0	0.000	LOS:	Α
Peak Period:	PM PEAK F	IOUR					<del>-</del>

Peak Period:	PM PEAK F	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.255 *
	TH	0.00	0	0	0.000	N-S(2):	0.055
	LT	0.00	0	0	0.000 *	E-W(1):	0.279 *
Westbound	RT	0.00	0	0	0.000	E-W(2):	0.054
	TH	3.00	283	5,280	0.054		
	LT	2.00	92	3,168	0.029 *	V/C:	0.534
Northbound	RT	1.00	494	1,760	0.255 *	Lost Time:	0.100
	TH	0.00	0	0	0.000		
	LT	1.00	97	1,760	0.055		
Eastbound	RT	0.00	138	0	0.000	ICU:	0.634
	TH	3.00	1,183	5,280	0.250 *		
	LT	0.00	0	0	0.000	LOS:	В

<sup>\* =</sup> Critical Movement

**Tesoro Los Angeles Refinery Traffic Study** 

Project: Int #:

North/South Street: ALAMEDA STREET

East/West Street: SEPULVEDA BOULEVARD-ALAMEDA RAMF

**Existing Conditions** Scenario:

Thru Lane:	1600 vph	N-S Split Phase :	N
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.243 *
	TH	3.00	766	4,800	0.160	N-S(2):	0.160
	LT	1.00	229	1,600	0.143 *	E-W(1):	0.031 *
Westbound	RT	2.00	198	3,200	0.000	E-W(2):	0.000
	TH	0.00	0	0	0.000		
	LT	1.00	49	1,600	0.031 *	V/C:	0.274
Northbound	RT	0.00	50	0	0.000	Lost Time:	0.100
	TH	3.00	428	4,800	0.100 *		
	LT	0.00	0	0	0.000		
Eastbound	RT	0.00	0	0	0.000	ICU:	0.374
	TH	0.00	0	0	0.000 *		
	LT	0.00	0	0	0.000	LOS:	Α

Peak Period:	PM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.379 *
	TH	3.00	856	4,800	0.178	N-S(2):	0.178
	LT	1.00	250	1,600	0.156 *	E-W(1):	0.058 *
Westbound	RT	2.00	407	3,200	0.049	E-W(2):	0.049
	TH	0.00	0	0	0.000		
	LT	1.00	93	1,600	0.058 *	V/C:	0.437
Northbound	RT	0.00	83	0	0.000	Lost Time:	0.100
	TH	3.00	988	4,800	0.223 *		
	LT	0.00	0	0	0.000		
Eastbound	RT	0.00	0	0	0.000	ICU:	0.537
	TH	0.00	0	0	0.000 *		
	LT	0.00	0	0	0.000	LOS:	Α

<sup>\* =</sup> Critical Movement

Project: Int #: **Tesoro Los Angeles Refinery Traffic Study** 

North/South Street: SEPULVEDA BOULEVARD-ALAMEDA RAMF

East/West Street: **SEPULVEDA BOULEVARD** 

Scenario: **Existing Conditions** 

Thru Lane:	1600 vph	N-S Split Phase :	Υ
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	1.00	144	1,600	0.016	N-S(1):	0.055 *
	TH	0.13	9	215	0.042	N-S(2):	0.000
	LT	1.87	125	2,687	0.047 *	E-W(1):	0.227
Westbound	RT	1.00	98	1,600	0.019	E-W(2):	0.260 *
	TH	2.00	594	3,200	0.186 *		
	LT	1.00	8	1,600	0.005	V/C:	0.315
Northbound	RT	0.00	4	0	0.000	Lost Time:	0.100
	TH	2.00	19	3,200	0.008 *		
	LT	0.00	2	1,600	0.001		
Eastbound	RT	1.00	6	1,600	0.003	ICU:	0.415
	TH	1.00	355	1,600	0.222		
	LT	1.00	118	1,600	0.074 *	LOS:	Α
Peak Period:	PM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	1.00	172	1,600	0.000	N-S(1):	0.057 *
	TH	0.17	12	274	0.044	N-S(2):	0.000
	LT	1.83	128	2,633	0.049 *	E-W(1):	0.585 *
Westbound	RT	1.00	238	1,600	0.105	E-W(2):	0.310

Southbound	RT	1.00	172	1,600	0.000	N-S(1):	0.057 *
	TH	0.17	12	274	0.044	N-S(2):	0.000
	LT	1.83	128	2,633	0.049 *	E-W(1):	0.585 *
Westbound	RT	1.00	238	1,600	0.105	E-W(2):	0.310
	TH	2.00	534	3,200	0.167		
	LT	1.00	2	1,600	0.001 *	V/C:	0.642
Northbound	RT	0.00	9	0	0.000	Lost Time:	0.100
	TH	2.00	13	3,200	0.008 *		
	LT	0.00	4	1,600	0.003		
Eastbound	RT	1.00	1	1,600	0.000	ICU:	0.742
	TH	1.00	935	1,600	0.584 *		
	LT	1.00	229	1,600	0.143	LOS:	С

<sup>\* =</sup> Critical Movement

Project: Tesoro Los Angeles Refinery Traffic Study

Project: Te

North/South Street: TERMINAL ISLAND FREEWAY (SR-103)

East/West Street: WILLOW STREET

Scenario: Existing Conditions

Thru Lane:	1600 vph	N-S Split Phase :	Υ
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK I	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.034 *
	TH	1.00	0	1,600	0.000	N-S(2):	0.000
	LT	0.00	0	0	0.000 *	E-W(1):	0.181
Westbound	RT	0.00	16	0	0.000	E-W(2):	0.256 *
	TH	2.00	794	3,200	0.253 *		
	LT	2.00	236	2,880	0.082	V/C:	0.290
Northbound	RT	2.00	97	3,200	0.000	Lost Time:	0.100
	TH	0.00	0	0	0.000		
	LT	2.00	99	2,880	0.034 *		
Eastbound	RT	1.00	183	1,600	0.083	ICU:	0.390
	TH	2.00	316	3,200	0.099		
	LT	1.00	4	1,600	0.003 *	LOS:	Α
Peak Period:	PM PEAK F	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	DΤ	0.00	0	0	0.000	NLQ(1)·	U 1U8 *

Peak Period:	PM PEAK HOUR								
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS		
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.108 *		
	TH	1.00	0	1,600	0.000	N-S(2):	0.000		
	LT	0.00	0	0	0.000 *	E-W(1):	0.371 *		
Westbound	RT	0.00	1	0	0.000	E-W(2):	0.133		
	TH	2.00	425	3,200	0.133				
	LT	2.00	167	2,880	0.058 *	V/C:	0.479		
Northbound	RT	2.00	248	3,200	0.051	Lost Time:	0.100		
	TH	0.00	0	0	0.000				
	LT	2.00	311	2,880	0.108 *				
Eastbound	RT	1.00	256	1,600	0.063	ICU:	0.579		
	TH	2.00	1,000	3,200	0.313 *				
	LT	1.00	0	1,600	0.000	LOS:	Α		

<sup>\* =</sup> Critical Movement

Project: Tesoro Los Angeles Refinery Traffic Study

Project: Te

North/South Street: SANTA FE AVE

East/West Street: SEPULVEDA BOULEVARD

Scenario: Existing Conditions

Thru Lane:	1600 vph	N-S Split Phase :	Υ
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period: AM PEAK HOUR									
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS		
Southbound	RT	0.00	132	0	0.000	N-S(1):	0.205 *		
	TH	2.00	258	3,200	0.122 *	N-S(2):	0.000		
	LT	2.00	152	2,880	0.053	E-W(1):	0.198		
Westbound	RT	0.00	108	0	0.000	E-W(2):	0.319 *		
	TH	2.00	767	3,200	0.273 *	, ,			
	LT	2.00	159	2,880	0.055	V/C:	0.524		
Northbound	RT	0.00	80	0	0.000	Lost Time:	0.100		
	TH	2.00	184	3,200	0.083 *				
	LT	1.00	76	1,600	0.048				
Eastbound	RT	0.00	32	0	0.000	ICU:	0.624		
	TH	2.00	426	3,200	0.143				
	LT	1.00	73	1,600	0.046 *	LOS:	В		
Peak Period:	PM PEAK H	IOUR	•		-				
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA			
Southbound	RT	0.00	62	0	0.000	N-S(1):	0.313 *		
	TH	2.00	311	3,200	0.117 *	N-S(2):	0.000		
	LT	2.00	331	2,880	0.115	E-W(1):	0.368 *		
Westbound	RT	0.00	149	0	0.000	E-W(2):	0.286		
	TH	2.00	483	3,200	0.198				
	LT	2.00	137	2,880	0.048 *	V/C:	0.681		
Northbound	RT	0.00	200	0	0.000	Lost Time:	0.100		
	TH	2.00	428	3,200	0.196 *				
	LT	1.00	82	1,600	0.051				
Eastbound	RT	0.00	43	0	0.000	ICU:	0.781		
	TH	2.00	982	3,200	0.320 *				
	LT	1.00	140	1,600	0.088	LOS:	С		

<sup>\* =</sup> Critical Movement



# Appendix E Level of Service Workheet (Circular 212 Method)



Alameda Street Ramp

I/S #:

PROJECT TITLE: ICTF Modification and Expansion Project EIR

North-South Street: 223rd Street (on 223rd East-West Street:

Scenario: CEQA Baseline

Count Date: Analyst: hteris, Inc. Date: 7/22/2014

		AM PEAK HOUR			MD PE	EAK HO	UR	PM PEAK HOUR		
	No. of Phases			3			3			3
	Opposed Ø'ing: N/S-1, E/W-2 or Both-3?			2	4/5	0.0	2			2
1	Right Turns: FREE-1, NRTOR-2 or OLA-3?	NB 3 EB 0	SB WB	0	NB 3 EB 0	SB NB	0	NB 0 EB 3	SB WB	0
	ATSAC-1 or ATSAC+ATCS-2?	LD -	112	2			2		112	2
	Override Capacity			1500			1500			1500
	MOVEMENT		No. of	Lane		No. of	Lane		No. of	Lane
		Volume	Lanes	Volume	Volume	Lanes	Volume	Volume	Lanes	Volume
٥	Left	143	1	143	0	1	60	97	1	97
NORTHBOUND	← Left-Through		0	_	_	0	_		0	_
l ŏ	↑ Through	0	0	0	0	0	0	0	0	0
₩	↑ Through-Right		0			0			0	
F	Right	266	1	143	0	1	403	494	1	443
2	← Left-Through-Right		0			0			0	
	← Left-Right		0			0			0	
₽	Left	0	0	0	0	0	0	0	0	0
SOUTHBOUND	▶ Left-Through		0		_	0			0	_
9	Through	0	0	0	0	0	0	0	0	0
=	Through-Right		0		_	0			0	
15		0	0	0	0	0	0	0	0	0
so			0 0			0			0 0	
	↓ Left-Right		U			U				
	Left	0	0	0	1 0	0	0		0	0
Ω	→ Left  → Left-Through	0	0 0	U	0	0	0	0	0	0
EASTBOUND	→ Through	398	2	159	0	2	380	1,183	2	440
ğ	→ Through  Through-Right	390	1	159	U	1	300	1,103	1	440
l E	Right	80	0	80	0	0	45	138	0	138
AS	Left-Through-Right	00	0	00	0	0	40	130	0	130
ш	↓ Left-Right		0			0			0	
	1 Lott ragin		,		1	<u> </u>			. ,	
	√ Left	223	2	123	0	2	77	92	2	51
9	√ Left-Through		0	0		0			0	ŭ,
Į	← Through	747	3	249	0	3	82	283	3	94
BC	← Through-Right		0			0			0	
ST	Right	0	0	0	0	0	0	0	0	0
WESTBOUND	Left-Through-Right		0			0			0	
	├ Left-Right		0			0			0	
		٨	lorth-South:	143		-South:	403	^	lorth-South:	443
	CRITICAL VOLUMES		East-West:		3		462	East-West:		534
			SUM:	551		SUM:	865		SUM:	977
	VOLUME/CAPACITY (V/C) RATIO:			0.387			0.577			0.686
V/	C LESS ATSAC/ATCS ADJUSTMENT:			0.287			0.477			0.586
	LEVEL OF SERVICE (LOS):			A			A			Α
	22722 OF OZMITOL (200).									_

Version: 1i Beta; 8/4/2011

EX\_AM. out Fri Nov 14, 2014 09: 29: 31 EX AM

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Tesoro Los Angeles Refinery Integration & Compliance Project Traffic Study Existing AM Peak Hour

Scenario Report

Scenari o: EX AM

Command: Default Command

Vol ume:

Geometry:
Impact Fee:

Default Geometry
Default Impact Fee
Default Trip Generation
Default Trip Distribution
Default Path
Default Configuration Trip Generation: Trip Distribution:

Paths: Routes:

Configuration: Default Configuration

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Tesoro Los Angeles Refinery Page 1

### EX\_AM. out Integration & Compliance Project Traffic Study Existing AM Peak Hour

Impact	An	al y	si s	Report
				vi ce

Ιn	tersection		Base Del/ V/		Future Del/ V/	Change i n
#	1 Wilmington Ave / I-405 NB Ramp		S Veh C 20. 0 0. 478		S Veh C 20.0 0.478	+ 0.000 D/V
#	2 Wilmington Ave / I-405 SB Ramp	В	12. 4 0. 463	В	12. 4 0. 463	+ 0.000 D/V
#	4 Alameda Ave / I-405 NB Ramps	В	18. 3 0. 633	В	18. 3 0. 633	+ 0.000 D/V
#	9 I-405 SB Ramps / 223rd St	С	20. 4 0. 422	С	20. 4 0. 422	+ 0.000 D/V

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Tesoro Los Angeles Refinery Integration & Compliance Project Traffic Study Existing AM Peak Hour

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# EX\_AM.out Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative)

2000 HCM Operations Method (Future Volume Alternative)							
Intersection #1 Wilmington Ave / I-405 NB Ramps							
Cycle (sec): Loss Time (se	100	/+R=4.0 sec)	Criti Averaç	cal Vol./Cap ge Delay (se	o. (X): ec/veh):	0. 4 20	78 . 0
Approach: Movement:	North Bound L - T - I	South R L - T	Bound - R	East Bo L - T	ound - R	West Bo L - T	und - R
Control: Rights: Min. Green: Lanes:	Protected Include 0 0	Pern Ind 0 0 1 1 0 3	nitted clude 0 0 3 0 0	Inclu 0 0	ted ude 0	Permit Inclu 0 0 2 0 0	ted de 0
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:	0 362 1.00 1.00 1.00 0 362 0 0 0 362 1.00 1.00 1.00 0.90 0.90 0.90 0 404 0 0 0 404 1.00 1.00 1.00 1.00 1.00 1.00	33 21 37 30 1.00 1.0 33 21 37 0 0 0 0 33 21 37 00 1.00 1.0 00 0.90 0.9 37 23 47 0 0 37 23 47 0 1.00 1.0 00 1.00 1.0 00 1.00 1.0 00 1.00 1.0 00 1.00 1.0 00 1.00 1.0	71 0 00 1.00 71 0 0 0 0 0 71 0 00 1.00 00 0.90 14 0 00 1.00 00 1.00 14 0	0 0 1.00 1.00 0 0 0 0 0 0 1.00 1.00 0.90 0.90 0 0 0 0 1.00 1.00 1.00 1.00 0 0	0 1.00 0 0 0 0 1.00 0.90 0 0 1.00 1.00	693 0 1. 00 1. 00 693 0 0 0 693 0 1. 00 1. 00 0. 90 0. 90 773 0 773 0 1. 00 1. 00 1. 00 1. 00 773 0	484 1.00 484 0 0 484 1.00 0.90 540 1.00 1.00 540
Saturation FI Sat/Lane: Adjustment: Lanes: Final Sat.:		00 1900 190 35 0.28 0.9 00 1.00 3.0 15 536 518	00 1900 91 1.00 00 0.00 87 0	1900 1900 1.00 1.00 0.00 0.00 0 0	1900 1.00 0.00	1900 1900 0.59 1.00 2.00 0.00 2226 0	1900 0. 85 1. 00 1615
Capacity Anal Vol/Sat: Crit Moves:		1 1		0.00 0.00	0.00	0. 35   0. 00 ****	0. 33
Green/Cycle: Volume/Cap: Delay/Veh: User DelAdj: Adj Del/Veh: LOS by Move: HCM2kAvgQ:	0.00 0.34 0.3 0.00 0.33 0.0 0.0 24.7 22 1.00 1.00 1.0 0.0 24.7 22 A C 0 5	07 0.31 0.5 3 40.8 41. 00 1.00 1.0 3 40.8 41. C D [	66 0.00 0 0.0 00 1.00 0 0.0 0 A 5 0	A A O	0. 00 0. 0 1. 00 0. 0 A 0	B A 8 0	0. 62 0. 54 11. 5 1. 00 11. 5 B 10
Note: Queue reported is the number of cars per lane.							
Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CAF EX AM Fri Nov 14, 2014 09:29:32 Page 4-1							
Tesoro Los Angeles Refinery Integration & Compliance Project Traffic Study Existing AM Peak Hour							
Level Of Service Computation Report							
2000 HCM Operations Method (Future Volume Alternative) ************************************							

Page 3

EX_AM. out								
Cycle (sec): Loss Time (se	Loss Time (sec): 4 (Y+R=4.0 sec) Average Delay (sec/veh): 12.4							
Optimal Cycle *********** Approach: Movement:	e: 21 ***************** North Bound L - T - R	**************************************	Of Service: ******** East Bound L - T - R	**************************************				
Control: Rights: Min. Green: Lanes:	Permitted	Prot+Permi t	Permitted     Include     0     0     0     0     1     0     1     0	Permitted     Include     0     0     0     0     0     0				
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:	e:  0 304 359 1.00 1.00 1.00 0 304 359 0 0 0 0 0 0 0 304 359 1.00 1.00 1.00 0.95 0.95 0.95 0 321 379 0 0 0 0 321 379 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00	141 906 0 1.00 1.00 1.00 141 906 0 0 0 0 0 0 0 0 141 906 0 1.00 1.00 1.00 0.95 0.95 0.95 149 958 0 0 0 0 149 958 0 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00	123	0 0 0 1.00 1.00 1.00 0 0 0 0 0 0 0 0 0 0 0 0 1.00 1.00 1.00 0.95 0.95 0.95 0 0 0 0 0 0 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00				
Saturation Fl Sat/Lane: Adjustment: Lanes: Final Sat.:	I ow Modul e: 1900 1900 1900 1.00 0.95 0.85 0.00 2.00 1.00 0 3610 1615	1900 1900 1900 0.95 0.91 1.00 1.00 3.00 0.00 1805 5187 0	1900 1900 1900 0. 72 0. 95 0. 72 1. 00 0. 00 1. 00 1366 0 1366	1900 1900 1900 1.00 1.00 1.00 0.00 0.00 0.00 0 0 0				
Vol /Sat: Cri t Moves: Green/Cycl e: Vol ume/Cap: Del ay/Veh: User Del Adj: Adj Del /Veh: LOS by Move:	1. 00 1. 00 1. 00 0. 0 13. 4 16. 3 A B B		C A C	A A A				
HCM2kÅvgQ: 0 3 8 2 4 0 4 0 5 0 0 0 ***********************								
Tesoro Los Angeles Refinery Integration & Compliance Project Traffic Study Existing AM Peak Hour								
Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative)  ***********************************								

EX\_AM. out Loss Time (sec): 4 (Y+R=4.0 sec) Average Delay (sec/veh): 18.3 Optimal Cycle: 30 Level Of Service: B Final Volume: 0 599 51 Saturation Flow Module: Capacity Analysis Module: Vol /Sat: 0.00 0.17 0.03 0.00 0.27 0.27 0.00 0.00 0.00 0.34 0.00 0.21 Crit Moves: \*\*\*\* \* Note: Queue reported is the number of cars per lane. Tesoro Los Angeles Refinery Integration & Compliance Project Traffic Study Existing AM Peak Hour Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative) Intersection #9 I-405 SB Ramps / 223rd St 

movement:	North Bound L - T - R	South Bo L - T	- K	East Bo L - T		West Bo L - T	
Control: Rights: Min. Green: Lanes:	Permitted Include	Protect Inclu 0 0 0	ed de 0	Protect Inclu 0 0 2 0 2	ted lide 0	Protect Inclu 0 0 1 0 2	ed ide 0
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:	e:  1	5 55 0 0 1.00 1.00 5 55 0 0 0 0 0 0 0 5 55 0 0 1.00 1.00 8 0.88 0.88 6 62 0 0 0 0 6 62 0 0 1.00 1.00 0 1.00 1.00 0 1.00 1.00 6 62 0	123 1.00 123 0 0 123 1.00 0.88 140 0 140 1.00 1.00 140	353 302 1.00 1.00 353 302 0 0 0 0 353 302 1.00 1.00 0.88 0.88 401 343 0 0 401 343 1.00 1.00 1.00 1.00 401 343	1. 00 4 0 0 4 1. 00 0. 88 5 0 5 1. 00 1. 00	3 837 1.00 1.00 3 837 0 0 0 0 3 837 1.00 1.00 0.88 0.88 3 950 0 0 3 950 1.00 1.00 1.00 1.00 3 950	32 1. 00 32 0 0 32 1. 00 0. 88 36 0 36 1. 00 1. 00 36
Saturation Fl Sat/Lane: Adjustment: Lanes: Final Sat.:		0 1900 1900 0 0.95 1.00 2 1.00 0.00 7 1805 0	1900 0. 85 1. 00 1615	1900 1900 0. 92 0. 91 2. 00 2. 96 3502 5109	1900 0. 91 0. 04 68	1900 1900 0. 95 0. 90 1. 00 2. 89 1805 4966	1900 0. 90 0. 11 190
Capacity Anal Vol/Sat: Crit Moves: Green/Cycle: Volume/Cap: Delay/Veh: User DelAdj: Adj Del/Veh: LOS by Move: HCM2kAvgQ:	ysis Module: 0.00 0.00 0.0  ****  0.01 0.01 0.0  0.41 0.41 0.4  62.9 62.9 62.  1.00 1.00 1.0  62.9 62.9 62.  E E E  1 1  **************************	0 0.03 0.00 1 0.20 0.00 1 0.17 0.00 9 33.0 0.0 0 1.00 1.00 9 33.0 0.0 C A 1 2 0 *********	0. 09 **** 0. 22 0. 40 34. 4 1. 00 34. 4 C 4 *****	0. 11 0. 07  ****  0. 27 0. 70  0. 42 0. 10  30. 3 4. 7  1. 00 1. 00  30. 3 4. 7  C A  5 1  ***********	0. 07 0. 70 0. 10 4. 7 1. 00 4. 7 A	0.00 0.19 **** 0.02 0.45 0.10 0.42 49.3 18.6 1.00 1.00 49.3 18.6 D B 0 8	0. 19 0. 45 0. 42 18. 6 1. 00 18. 6 B
********	reported is the		12 hel	ıaııᠸ. *********	*****	******	*****

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EX\_PM. out Wed Nov 26, 2014 17: 31: 44 EX PM

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Tesoro Los Angeles Refinery Existing Conditionsq PM Peak Hour

Scenario Report

EX PM Scenari o:

Command: EX-PM Vol ume: PM

Geometry:
Impact Fee:

Existing
Default Impact Fee
Const-PM
Default Trip Distribution
Default Path

Trip Generation: Trip Distribution: Paths: Default Route Routes:

EX-PM Confi gurati on:

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Tesoro Los Angeles Refinery Page 1

#### EX\_PM. out Existing Conditionsq PM Peak Hour

#### Impact Analysis Report Level Of Service

Ιn	tersecti on		Base Del/V/		Future Del/ V/	Change i n
#	1 Wilmington Ave / I-405 NB Ramp		S Veh C 18. 5 0. 395		S Veh C 18. 5 0. 395	+ 0.000 D/V
#	2 Wilmington Ave / I-405 SB Ramp	В	15. 7 0. 629	В	15. 7 0. 629	+ 0.000 D/V
#	4 Alameda Ave / I-405 NB Ramps	С	23. 2 0. 665	С	23. 2 0. 665	+ 0.000 D/V
#	9 I-405 SB Ramps / 223rd St	В	19. 0 0. 502	В	19. 0 0. 502	+ 0.000 D/V

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Tesoro Los Angeles Refinery Existing Conditionsq PM Peak Hour

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## EX\_PM. out Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative)

*****	2000 HCM Op	eratio *****	ns Met	thod (	Future	Vol ur	ne Alt	ernati *****	ve)	***	****
Intersection	#1 Wilming	ton Av	e / I-	-405 N	IB Ramp	S					
Cycle (sec): Loss Time (sec) Optimal Cycle	10(ec): 8e: 2	0 8 (Y+R 7	=4.0 \$	sec)	Critic Averag Level	al Vol e Dela Of Sei	. /Cap ay (se rvi ce:	o. (X): ec/veh)	:	0. 3 18	95 . 5 B
Approach: Movement:	North Bo	- R	L -	- T		L .	ast Bo - T	- R	_	-	- R
Control: Rights: Min. Green: Lanes:	Protecto Include 0 0 0 0 2	ed ' de 0 0 1	, O 1 (	Permit Inclu	ted ide 0	0 0	Permit Inclu 0 0	ted	Pei	rmit nclu 0	ted
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:	0 282 1.00 1.00 0 282 0 0 0 0 0 282 1.00 1.00 0.95 0.95 0 297 0 0 0 297 1.00 1.00 1.00 1.00 0 297	151 1.00 151 0 0 151 1.00 0.95 159 0 159 1.00 1.00	71 1.00 71 0 0 71 1.00 0.95 75 0 75 1.00	794 1.00 794 0 0 794 1.00 0.95 837 0 837 1.00 1.00 837	0 1.00 0 0 0 0 1.00 0.95 0 0 1.00 1.00	1. 00 0 0 0 0 0 0 1. 00 0. 95 0 0 1. 00	1. 00 0 0 0 0 1. 00 0. 95 0 0 0 1. 00 1. 00	0 1.00 0 0 0 0 1.00 0.95 0 0 1.00 1.00	428 1. 00 1 428 0 0 428 1. 00 1 0. 95 0 451 0 451 1. 00 1 1. 00 1	0 0 0 0 . 00 . 95 0 0 0 . 00	302 1.00 302 0 0 302 1.00 0.95 318 1.00 1.00 318
Saturation FI Sat/Lane: Adjustment: Lanes: Final Sat.:	ow Modul e: 1900 1900 1.00 0.95 0.00 2.00 0 3610	1900 0. 85 1. 00 1615	0. 52 1. 00 979	3. 00 5187	1900 1. 00 0. 00	1900 1.00	1900 1.00 0.00 0	1900 1.00 0.00	1900 19 0. 59 1. 2. 00 0. 2234	900 . 00	1900 0. 85 1. 00 1615
User Del Adj : Adj Del /Veh: LOS by Move:	0.00 0.08 **** 0.00 0.41 0.00 0.20 0.0 19.1 1.00 1.00 0.0 19.1 A B	e: 0. 10 0. 41 0. 24 19. 6 1. 00 19. 6 B	0. 08 0. 41 0. 19 19. 2 1. 00 19. 2 B	0. 41 0. 39 21. 0 1. 00 21. 0	0. 00 0. 00 0. 00 0. 0 1. 00 0. 0 A	0.00	0. 00 0. 00 0. 00 0. 0 1. 00 0. 0 A	0. 00 0. 00 0. 00 0. 00 0. 0 1. 00 0. 0 A	1. 00 1. 15. 2 0 B_	. 00 . 00 0. 0	0. 20 0. 51 0. 39 15. 2 1. 00 15. 2 B
	0 3 ******* renorted is										
Note: Queue i											
Traffix 7.9 EX PM	9. 0415 (c) :	2007 D We	owling d Nov	g Asso 26, 2	oc. Lic 2014 17	ensed : 31: 44	to MN 4	MA, LON		, CA age	
	<b></b>		Existi	ng Co	jeles R onditio : Hour		^y			_ <b></b>	
	 L 2000 HCM Op				computa Future				ve)		
*****	*****	****	****	*****	***** Page 3	****	****	*****	*****	***	*****

Page 3

Intersection	#2 Wilmington Av	EX_PM. ve / I-405 SB Ra		
Cycle (sec):	100	Cri t	:*************************************	0. 629
Approach: Movement:	North Bound L - T - R	South Bound L - T - I	East Bound R L - T - R	West Bound L - T - R
Control: Rights: Min. Green: Lanes:	Permitted     Include     0    0    0     0    0    1	Protected Include 0 0 1 0 3 0 0	Permitted Include 0 0 0 0	Permitted Include 0 0 0
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:	0 406 479 1.00 1.00 1.00 0 406 479 0 0 0 0 0 0 0 406 479 1.00 1.00 1.00 0.98 0.98 0.98 0 415 490 0 0 0 0 415 490 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00	337 888 1.00 1.00 1.0 337 888 0 0 0 337 888 1.00 1.00 1.0 0.98 0.98 0.9 345 908 0 0 345 908 1.00 1.00 1.0 1.00 345 908	0 26 0 82 0 0 0 0 0 0 0 0 0 0 26 0 82 0 1.00 1.00 1.00 0 27 0 84 0 0 0 0 0 0 27 0 84 0 1.00 1.00 1.00 0 27 0 84 0 1.00 1.00 1.00 0 27 0 84	0 0 0 0 0 1.00 1.00 0 0 0 0 0 0 0 0 0 0
Saturation FI Sat/Lane: Adjustment: Lanes: Final Sat.:	ow Modul e: 1900 1900 1900 1.00 0.95 0.85 0.00 2.00 1.00 0 3610 1615	1900 1900 190 0. 95 0. 91 1.0 1. 00 3. 00 0.0 1805 5187	00 0.74 0.95 0.74 00 1.00 0.00 1.00 0 1415 0 1415	1900 1900 1900 1.00 1.00 1.00 0.00 0.00 0.00 0 0 0
Capacity Anal Vol/Sat: Crit Moves: Green/Cycle: Volume/Cap: Delay/Veh: User DelAdj: Adj Del/Veh: LOS by Move: HCM2kAvgQ:	ysis Module: 0.00 0.11 0.30  ****  0.00 0.48 0.48  0.00 0.24 0.63  0.0 15.2 20.9  1.00 1.00 1.00  0.0 15.2 20.9  A B C 0 4 12	C A /	**** 00 0.09 0.00 0.09 00 0.20 0.00 0.63 0 42.0 0.0 51.0 00 1.00 1.00 1.00	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00
	9.0415 (c) 2007 D		per lane. ************************************	
	Tes	soro Los Angeles Existing Condi PM Peak Hou	ti onsq	
******		Of Service Compu	utation Report ure Volume Alternati	 ve) *******
Intersection	#4 AI ameda Ave / ********* 100	′ I -405 NB Ramps	s ********************** :i cal Vol./Cap.(X):	

EX\_PM. out Loss Time (sec): 12 (Y+R=4.0 sec) Average Delay (sec/veh): 23.2 Optimal Cycle: 55 Level Of Service: C 

 Approach:
 North Bound
 South Bound
 East Bound
 West Bound

 Movement:
 L - T - R
 L - T - R
 L - T - R

 Control:
 Protected
 Protected
 Protected
 Permitted

 Rights:
 Include
 Include
 Include
 Include

 Min. Green:
 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
 0 0 0 0 0 0 0 0 0 0
 0 0 0 0 0 0 0 0 0 0 0 0 0

 Volume Module:
 Module:
 Module:
 Module:
 Module:
 Module:

 PHF Adj: PHF Volume: 0 959 0 0 0 959 Reduct Vol: Reduced Vol: PCE Adj : 1.00 1.00 MLF Adj : 1.00 1.00 Final Volume: 0 959 -----Saturation Flow Module: Capacity Analysis Module: Vol /Sat: 0.00 0.27 0.12 0.05 0.22 0.00 0.00 0.00 0.00 0.27 0.00 0.07 Crit Moves: \* Note: Queue reported is the number of cars per lane. Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CA<sup>2</sup> (PM Wed Nov 26, 2014 17:31:44 Page 6-1 Tesoro Los Angeles Refinery Existing Conditionsq PM Peak Hour Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative) Intersection #9 I-405 SB Ramps / 223rd St 

Page 5

Approach: Movement:	North Bound L - T - R	EX_PM.out South Bound L - T - R	East Bound L - T - R	West Bound L - T - R
Control: Rights: Min. Green: Lanes:	Split Phase Include 0 0 0 0 0 1! 0 0	Split Phase Include	Protected Include 0 0 0 2 0 2 1 0	Protected
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:	3 6 3 1.00 1.00 1.00 3 6 3 0 0 0 0 0 0 3 6 3 1.00 1.00 1.00 0.95 0.95 0.95 3 6 3 0 0 0 3 6 3 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00	125	840 798 18 1.00 1.00 1.00 840 798 18 0 0 0 0 0 0 840 798 18 1.00 1.00 1.00 0.95 0.95 0.95 886 842 19 0 0 0 886 842 19 1.00 1.00 1.00 1.00 1.00 1.00 886 842 19	4 347 77 1.00 1.00 1.00 4 347 77 0 0 0 0 0 0 0 4 347 77 1.00 1.00 1.00 0.95 0.95 0.95 4 366 81 0 0 0 4 366 81 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00
Saturation FI Sat/Lane: Adjustment: Lanes: Final Sat.:	l ow Modul e: 1900 1900 1900 0. 95 0. 95 0. 95 0. 25 0. 50 0. 25 453 907 453	1900 1900 1900 0. 95 0. 86 0. 86 1. 00 0. 05 0. 95 1805 86 1544	1900 1900 1900 0. 92 0. 91 0. 91 2. 00 2. 93 0. 07 3502 5057 114	1900 1900 1900 0. 95 0. 89 0. 89 1. 00 2. 46 0. 54 1805 4130 917
	0.01 0.01 0.01 0.01 0.01 0.01 0.50 0.50 0.50 64.0 64.0 64.0 1.00 1.00 1.00 64.0 64.0 64.0 E E E 1 1 1	0.07 0.02 0.02 ****  0.15 0.15 0.15  0.50 0.17 0.17  40.9 37.8 37.8  1.00 1.00 1.00  40.9 37.8 37.8  D D D  4 1 1  *******************************	_	0.00 0.09 0.09 
*******	*******	********	************	******

Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CA $\upphi$ 

#### **Traffic Impact Analysis**

**BASELINE PLUS PROJECT CONSTRUCTION** 



**AM PEAK HOUR** 

Movement Lanes

Int #: 3

Peak Period:

Approach

North/South Street: WILMINGTON AVENUE

East/West Street: 223RD STREET

Scenario: Existing Plus Construction

Thru Lane:	1600 vph	N-S Split Phase :	N
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Capacity

ICU ANALYSIS

Volume

трргоаоп	WOVCITICITE	3	VOIGITIC	Capacity	7	100 ANA	
Southbound	RT	1.00	319	1,600	0.114	N-S(1):	0.203
	TH	2.00	679	3,200	0.212 *	N-S(2):	0.219 *
	LT	1.00	125	1,600	0.078	E-W(1):	0.296
Westbound	RT	1.00	59	1,600	0.000	E-W(2):	0.334 *
	TH	2.00	794	3,200	0.248 *		
	LT	1.00	200	1,600	0.125	V/C:	0.553
Northbound	RT	0.50	84	800	0.000	Lost Time:	0.100
	TH	2.50	501	4,000	0.125		
	LT	1.00	11	1,600	0.007 *		
Eastbound	RT	1.00	17	1,600	0.004	ICU:	0.653
	TH	2.00	548	3,200	0.171		
	LT	1.00	137	1,600	0.086 *	LOS:	В
Peak Period:	PM PEAK F	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	1.00	199	1,600	0.000	N-S(1):	0.144
Southbound	RT TH	1.00 2.00	199 733	1,600 3,200	0.000 0.229 *	N-S(1): N-S(2):	0.144 0.234 *
Southbound						` '	
Southbound  Westbound	TH	2.00	733	3,200	0.229 *	N-S(2):	0.234 *
	TH LT	2.00 1.00	733 61	3,200 1,600	0.229 * 0.038	N-S(2): E-W(1):	0.234 * 0.362 *
	TH LT RT	2.00 1.00 1.00	733 61 215	3,200 1,600 1,600	0.229 * 0.038 0.096	N-S(2): E-W(1):	0.234 * 0.362 *
	TH LT RT TH	2.00 1.00 1.00 2.00	733 61 215 349	3,200 1,600 1,600 3,200	0.229 * 0.038 0.096 0.109	N-S(2): E-W(1): E-W(2):	0.234 * 0.362 * 0.259
Westbound	TH LT RT TH LT	2.00 1.00 1.00 2.00 1.00	733 61 215 349 182	3,200 1,600 1,600 3,200 1,600	0.229 * 0.038 0.096 0.109 0.114 *	N-S(2): E-W(1): E-W(2): V/C:	0.234 * 0.362 * 0.259
Westbound	TH LT RT TH LT	2.00 1.00 1.00 2.00 1.00 0.50	733 61 215 349 182 124	3,200 1,600 1,600 3,200 1,600 800	0.229 * 0.038 0.096 0.109 0.114 * 0.000	N-S(2): E-W(1): E-W(2): V/C:	0.234 * 0.362 * 0.259
Westbound	TH LT RT TH LT RT TH	2.00 1.00 1.00 2.00 1.00 0.50 2.50	733 61 215 349 182 124 424	3,200 1,600 1,600 3,200 1,600 800 4,000	0.229 * 0.038 0.096 0.109 0.114 * 0.000 0.106	N-S(2): E-W(1): E-W(2): V/C:	0.234 * 0.362 * 0.259
Westbound	TH LT RT TH LT RT TH LT	2.00 1.00 1.00 2.00 1.00 0.50 2.50 1.00	733 61 215 349 182 124 424 8	3,200 1,600 1,600 3,200 1,600 800 4,000 1,600	0.229 * 0.038 0.096 0.109 0.114 * 0.000 0.106 0.005 *	N-S(2): E-W(1): E-W(2): V/C: Lost Time:	0.234 * 0.362 * 0.259
Westbound	TH LT RT TH LT RT TH LT	2.00 1.00 1.00 2.00 1.00 0.50 2.50 1.00	733 61 215 349 182 124 424 8	3,200 1,600 1,600 3,200 1,600 800 4,000 1,600 1,600	0.229 * 0.038 0.096 0.109 0.114 * 0.000 0.106 0.005 * 0.001	N-S(2): E-W(1): E-W(2): V/C: Lost Time:	0.234 * 0.362 * 0.259

<sup>\* =</sup> Critical Movement

Int #:

North/South Street: 223rd Street Ramp (on Alameda Street)

East/West Street: Alameda Street

Thru Lane:	1600 vph	N-S Split Phase :	N
Left-Turn Lane:	1600 vph	E-W Split Phase:	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK I	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.257 *
	TH	3.00	1,145	4,800	0.239	N-S(2):	0.239
	LT	1.00	159	1,600	0.099 *	E-W(1):	0.127 *
Westbound	RT	1.00	119	1,600	0.000	E-W(2):	0.000
	TH	0.00	0	0	0.000		
	LT	1.00	203	1,600	0.127 *	V/C:	0.384
Northbound	RT	0.00	253	1,600	0.158 *	Lost Time:	0.100
	TH	3.00	489	3,200	0.153		
	LT	0.00	0	0	0.000		
Eastbound	RT	0.00	0	0	0.000	ICU:	0.484
	TH	0.00	0	0	0.000 *		
	LT	0.00	0	0	0.000	LOS:	Α
Daal- Dariada	DM DEAK I	IALIB				<u> </u>	

Peak Period:	PM PEAK H	HOUR				
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANALYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1): 0.433 *
	TH	3.00	1,001	4,800	0.209	N-S(2): 0.209
	LT	1.00	164	1,600	0.103 *	E-W(1): 0.071 *
Westbound	RT	1.00	122	1,600	0.000	E-W(2): 0.000
	TH	0.00	0	0	0.000	
	LT	1.00	114	1,600	0.071 *	V/C: 0.504
Northbound	RT	0.00	528	1,600	0.330 *	Lost Time: 0.100
	TH	3.00	1,025	3,200	0.320	
	LT	0.00	0	0	0.000	
Eastbound	RT	0.00	0	0	0.000	ICU: 0.604
	TH	0.00	0	0	0.000 *	
	LT	0.00	0	0	0.000	LOS: B

<sup>\* =</sup> Critical Movement

**AM PEAK HOUR** 

LT

0.00

0

0

0.000

Movement Lanes

Int #:

Peak Period:

Approach

North/South Street: 223rd Street

East/West Street: Alameda Street Ramp

Scenario: Existing Plus Construction

Thru Lane:	1600 vph	N-S Split Phase :	N
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Capacity

V/C

Volume

ICU ANALYSIS

LOS:

В

Southbound	RT	0.00	0	0	0.000	N-S(1):	0.086 *
	TH	0.00	0	0	0.000	N-S(2):	0.081
	LT	0.00	0	0	0.000 *	E-W(1):	0.172 *
Westbound	RT	0.00	0	0	0.000	E-W(2):	0.142
	TH	3.00	751	5,280	0.142		
	LT	2.00	250	3,168	0.079 *	V/C:	0.258
Northbound	RT	1.00	277	1,760	0.086 *	Lost Time:	0.100
	TH	0.00	0	0	0.000		
	LT	1.00	143	1,760	0.081		
Eastbound	RT	0.00	80	0	0.000	ICU:	0.358
	TH	3.00	409	5,280	0.093 *		
	LT	0.00	0	0	0.000	LOS:	Α
Peak Period:	PM PEAK H	IOUR					
Peak Period: Approach	PM PEAK H	HOUR Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
			Volume 0	Capacity 0	V/C 0.000	ICU ANA N-S(1):	LYSIS 0.291 *
Approach	Movement	Lanes		•			
Approach	Movement RT	Lanes 0.00	0	0	0.000	N-S(1):	0.291 *
Approach	Movement RT TH	0.00 0.00	0 0	0	0.000 0.000	N-S(1): N-S(2):	0.291 * 0.056
Approach Southbound	Movement RT TH LT	0.00 0.00 0.00	0 0 0	0 0 0	0.000 0.000 0.000 *	N-S(1): N-S(2): E-W(1):	0.291 * 0.056 0.305 *
Approach Southbound	Movement RT TH LT RT	0.00 0.00 0.00 0.00	0 0 0	0 0 0 0	0.000 0.000 0.000 * 0.000	N-S(1): N-S(2): E-W(1):	0.291 * 0.056 0.305 *
Approach Southbound	Movement RT TH LT RT TH	0.00 0.00 0.00 0.00 0.00 3.00	0 0 0 0 283	0 0 0 0 5,280	0.000 0.000 0.000 * 0.000 0.054	N-S(1): N-S(2): E-W(1): E-W(2):	0.291 * 0.056 0.305 * 0.054
Approach Southbound Westbound	Movement RT TH LT RT TH LT TH LT TH	Lanes 0.00 0.00 0.00 0.00 3.00 2.00	0 0 0 0 283 95	0 0 0 0 5,280 3,168	0.000 0.000 0.000 * 0.000 0.054 0.030 *	N-S(1): N-S(2): E-W(1): E-W(2): V/C:	0.291 * 0.056 0.305 * 0.054
Approach Southbound Westbound	Movement RT TH LT RT TH LT TH LT TH LT RT TH LT RT TH	Lanes 0.00 0.00 0.00 0.00 3.00 2.00 1.00	0 0 0 0 283 95 559 0	0 0 0 0 5,280 3,168 1,760	0.000 0.000 * 0.000 * 0.000 0.054 0.030 * 0.291 *	N-S(1): N-S(2): E-W(1): E-W(2): V/C: Lost Time:	0.291 * 0.056 0.305 * 0.054
Approach Southbound Westbound	Movement RT TH LT RT TH LT TH LT TH LT TH LT RT	Lanes 0.00 0.00 0.00 0.00 3.00 2.00 1.00 0.00	0 0 0 0 283 95 559 0	0 0 0 5,280 3,168 1,760	0.000 0.000 * 0.000 * 0.000 0.054 0.030 * 0.291 * 0.000	N-S(1): N-S(2): E-W(1): E-W(2): V/C:	0.291 * 0.056 0.305 * 0.054
Approach Southbound Westbound Northbound	Movement RT TH LT RT TH LT TH LT TH LT RT TH LT RT TH	Lanes 0.00 0.00 0.00 0.00 3.00 2.00 1.00 0.00 1.00	0 0 0 0 283 95 559 0	0 0 0 0 5,280 3,168 1,760 0	0.000 0.000 0.000 * 0.000 0.054 0.030 * 0.291 * 0.000 0.056	N-S(1): N-S(2): E-W(1): E-W(2): V/C: Lost Time:	0.291 * 0.056 0.305 * 0.054 0.596 0.100

<sup>\* =</sup> Critical Movement

Project: Int #:

North/South Street: ALAMEDA STREET

East/West Street: SEPULVEDA BOULEVARD-ALAMEDA RAMF

Thru Lane:	1600 vph	N-S Split Phase :	N
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK H	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.275 *
	TH	3.00	766	4,800	0.160	N-S(2):	0.160
	LT	1.00	279	1,600	0.174 *	E-W(1):	0.031 *
Westbound	RT	2.00	290	3,200	0.003	E-W(2):	0.003
	TH	0.00	0	0	0.000		
	LT	1.00	49	1,600	0.031 *	V/C:	0.306
Northbound	RT	0.00	52	0	0.000	Lost Time:	0.100
	TH	3.00	434	4,800	0.101 *		
	LT	0.00	0	0	0.000		
Eastbound	RT	0.00	0	0	0.000	ICU:	0.406
	TH	0.00	0	0	0.000 *		
	LT	0.00	0	0	0.000	LOS:	Α
Peak Period:	PM PFAK F	IOUR					

Peak Period:	PM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANALYSIS	
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.392 *
	TH	3.00	861	4,800	0.179	N-S(2):	0.179
	LT	1.00	270	1,600	0.169 *	E-W(1):	0.060 *
Westbound	RT	2.00	461	3,200	0.060 *	E-W(2):	0.060 *
	TH	0.00	0	0	0.000		
	LT	1.00	96	1,600	0.060 *	V/C:	0.452
Northbound	RT	0.00	83	0	0.000	Lost Time:	0.100
	TH	3.00	989	4,800	0.223 *		
	LT	0.00	0	0	0.000		
Eastbound	RT	0.00	0	0	0.000	ICU:	0.552
	TH	0.00	0	0	0.000 *		
* Oritical Massacrat	LT	0.00	0	0	0.000 *	LOS:	Α

<sup>\* =</sup> Critical Movement

Int #: 8

North/South Street: SEPULVEDA BOULEVARD-ALAMEDA RAMF

East/West Street: SEPULVEDA BOULEVARD

Thru Lane:	1600 vph	N-S Split Phase :	Υ
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK H	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANALYSIS	
Southbound	RT	1.00	151	1,600	0.000	N-S(1):	0.070 *
	TH	0.10	9	161	0.056	N-S(2):	0.000
	LT	1.90	170	2,735	0.062 *	E-W(1):	0.233
Westbound	RT	1.00	1.00 157 1,600 0.042 E-W(2):		0.282 *		
	TH	2.00	602	3,200	0.188 *		
	LT	1.00	8	1,600	0.005	V/C:	0.352
Northbound	RT	0.00	4	0	0.000	Lost Time:	0.100
	TH	2.00	19	3,200	0.008 *		
	LT	0.00	2	1,600	0.001		
Eastbound	RT	1.00	6	1,600	0.003	ICU:	0.452
	TH	1.00	365	1,600	0.228		
	LT	1.00	151	1,600	0.094 *	LOS:	Α
Peak Period:	PM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	1.00	179	1,600	0.000	N-S(1):	0.061 *
	TH	0.16	12	251	0.048	N-S(2):	0.000
	LT	1.84	141	2,654	0.053 *	E-W(1):	0.590 *
Westbound	RT	1.00	287	1,600	0.132	E-W(2):	0.320
	TH	2 00	546	3 200	0 171		

Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANALYSIS	
Southbound	RT	1.00	179	1,600	0.000	N-S(1):	0.061 *
	TH	0.16	12	251	0.048	N-S(2):	0.000
	LT	1.84	141	2,654	0.053 *	E-W(1):	0.590 *
Westbound	RT	1.00	287	1,600	0.132	E-W(2):	0.320
	TH	2.00	546	3,200	0.171		
	LT	1.00	2	1,600	0.001 *	V/C:	0.651
Northbound	RT	0.00	9	0	0.000	Lost Time:	0.100
	TH	2.00	13	3,200	0.008 *		
	LT	0.00	4	1,600	0.003		
Eastbound	RT	1.00	1	1,600	0.000	ICU:	0.751
	TH	1.00	943	1,600	0.589 *		
	LT	1.00	238	1,600	0.149	LOS:	С

<sup>\* =</sup> Critical Movement

Project: Te

North/South Street: TERMINAL ISLAND FREEWAY (SR-103)

East/West Street: WILLOW STREET

Thru Lane:	1600 vph	N-S Split Phase :	Υ
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK H	IOUR							
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS		
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.035 *		
	TH	1.00	0	1,600	0.000	N-S(2):	0.000		
	LT	0.00	0	0	0.000 *	E-W(1):	0.184		
Westbound	RT	0.00	16	0	0.000	E-W(2):	0.286 *		
	TH	2.00	890	3,200	0.283 *	I			
	LT	2.00	236	2,880	0.082	V/C:	0.321		
Northbound	RT	2.00	99	3,200	0.000	Lost Time:	0.100		
	TH	0.00	0	0	0.000				
	LT	2.00	101	2,880	0.035 *				
Eastbound	RT	1.00	184	1,600	0.083	ICU:	0.421		
	TH	2.00	327	3,200	0.102				
	LT	1.00	4	1,600	0.003 *	LOS:	Α		
Peak Period:	PM PEAK F	IOUR	·	·	•	•			
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANALYSIS			
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.108 *		

Peak Period:	PM PEAK F	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANALYSIS	
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.108 *
	TH	1.00	0	1,600	0.000	N-S(2):	0.000
	LT	0.00	0	0	0.000 *	E-W(1):	0.387 *
Westbound	RT	0.00	1	0	0.000	E-W(2):	0.138
	TH	2.00	440	3,200	0.138		
	LT	2.00	167	2,880	0.058 *	V/C:	0.495
Northbound	RT	2.00	248	3,200	0.051	Lost Time:	0.100
	TH	0.00	0	0	0.000		
	LT	2.00	312	2,880	0.108 *		
Eastbound	RT	1.00	260	1,600	0.065	ICU:	0.595
	TH	2.00	1,054	3,200	0.329 *		
	LT	1.00	0	1,600	0.000	LOS:	Α

<sup>\* =</sup> Critical Movement

Int #: 11

North/South Street: SANTA FE AVE

East/West Street: SEPULVEDA BOULEVARD

Scenario: Existing Plus Construction

Thru Lane:	1600 vph	N-S Split Phase :	Υ
Left-Turn Lane:	1600 vph	E-W Split Phase:	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK H	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANALYSIS	
Southbound	RT	0.00	132	0	0.000	N-S(1): 0.205	5 *
	TH	2.00	258	3,200	0.122 *	N-S(2): 0.000	)
	LT	2.00	152	2,880	0.053	E-W(1): 0.202	2
Westbound	RT	0.00	108	0	0.000	E-W(2): 0.349	<b>3</b> *
	TH	2.00	863	3,200	0.303 *		
	LT	2.00	159	2,880	0.055	V/C: 0.554	4
Northbound	RT	0.00	80	0	0.000	Lost Time: 0.100	)
	TH	2.00	184	3,200	0.083 *		
	LT	1.00	76	1,600	0.048		
Eastbound	RT	0.00	32	0	0.000	ICU: 0.654	4
	TH	2.00	437	3,200	0.147		
	LT	1.00	73	1,600	0.046 *	LOS: B	
Peak Period:	PM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANALYSIS	
Southbound	RT	0.00	62	0	0.000	N-S(1): 0.313	3 *
	TH	2.00	311	3,200	0.117 *	N-S(2): 0.000	)
	LT	2.00	331	2,880	0.115	E-W(1): 0.385	5 *
Westbound	RT	0.00	149	0	0.000	E-W(2): 0.290	)
	TH	2.00	498	3,200	0.202		

137

200

428

82

43

1,036

140

2,880

0

3,200

1,600

0

3,200

1,600

0.048 \*

0.000

0.051

0.000

0.088

0.337 \*

0.196 \*

V/C:

ICU:

LOS:

Lost Time:

0.698

0.100

0.798

С

2.00

0.00

2.00

1.00

0.00

2.00

1.00

LT

RT

ΤH

LT

RT

ΤH

LT

Northbound

Eastbound

<sup>\* =</sup> Critical Movement



# Appendix E Level of Service Workheet (Circular 212 Method)



Alameda Street Ramp

I/S #:

PROJECT TITLE: ICTF Modification and Expansion Project EIR

North-South Street: 223rd Street (on 223rd East-West Street:

Scenario: CEQA Baseline

Count Date: Analyst: hteris, Inc. Date: 7/22/2014

		Al	M PEAK HOU	IR	MD	PEAK HO	UR	l Pi	VI PEAK HOU	R
	No. of Phases			3			3			3
	Opposed Ø'ing: N/S-1, E/W-2 or Both-3?			2			2			2
١,	Right Turns: FREE-1, NRTOR-2 or OLA-3?	NB 3	SB	0	NB 3		0	NB 0	SB	0
		EB 0	WB	0	EB (	NB	0	EB 3	WB	0
	ATSAC-1 or ATSAC+ATCS-2?			2			2			2
	Override Capacity		No. of	1500 Lane		No. of	1500 Lane		No. of	1500 Lane
	MOVEMENT	Volume	Lanes	Volume	Volume	Lanes	Volume	Volume	Lanes	Volume
	↑ Left	143	1	143	C	_	60	97	1	97
9		140	0	143		0	00	37	0	57
Ď	↑ Through	0	0	0			0	0	0	0
BC	↑ Through-Right	v	0	ŭ		0	ŭ	· ·	0	ŭ
I 폰	→ Right	266	1	143			403	494	1	443
NORTHBOUND	← Left-Through-Right	200	0	170		0	700	454	0	440
Ž	Left-Hilough-Right		0			0			0	
	Leit-Right		U				Į.			
	Left	0	0	0		0	0	0	0	0
SOUTHBOUND	Left-Through	· ·	0	ŭ		0	ŭ		0	ĭ
00	Through	0	0	0		0	0	0	0	0
Ě	← Through-Right		0			0			0	
Ė	باً Right	0	0	0	C	0	0	0	0	0
õ	← Left-Through-Right		0			0			0	
S	↓ Left-Right		0			0			0	
	_ر Left	0	0	0	C		0	0	0	0
N	→ Left-Through		0			0			0	
EASTBOUND	→ Through	398	2	159	C		380	1,183	2	440
TB	→ Through-Right		1		_	1			1	
4S.	Right	80	0	80	C		45	138	0	138
E,	Left-Through-Right		0			0			0	
	- ✓ Left-Right		0			0			0	
	√ Left	223	2	123	I c	2	77	92	2	51
Q	τ Left Left-Through	223	0	123		0	11	92	0	31
WESTBOUND	← Through	747	3	249		E	82	283	3	94
BO	← Through-Right	171	0	243		0	02	200	0	5-7
ST	Right	0	0	0	C		0	0	0	0
ΛĒ	Left-Through-Right		0			0			0	Ů
	├ Left-Right		0			0			0	
		۸	lorth-South:	143	Nort	h-South:	403	<i>I</i>	lorth-South:	443
	CRITICAL VOLUMES		East-West:	408	Eá	st-West:	462		East-West:	534
			SUM:	551		SUM:	865		SUM:	977
	VOLUME/CAPACITY (V/C) RATIO:			0.387			0.577			0.686
V/	C LESS ATSAC/ATCS ADJUSTMENT:			0.287			0.477			0.586
	LEVEL OF SERVICE (LOS):			0.207 <b>A</b>			A			0.560 A
	LEVEL OF SERVICE (LOS):			Α			Α			Α

Version: 1i Beta; 8/4/2011

EX+Const-AM. out

EX + Const AM Mon Nov 24, 2014 13: 57: 52 Page 1-1 

> Tesoro Los Angeles Refinery Existing Plus Construction Conditions AM Peak Hour

Scenario Report

EX + Const AM Scenari o:

Command: EX+Const-AM

Vol ume: AM

Geometry:
Impact Fee:

Trip Generation: Trip Distribution:

Existing
Default Impact Fee
Const-AM
Default Trip Distribution
Default Path
Default Route Paths: Routes: Configuration: EX+Const-AM

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Tesoro Los Angeles Refinery Page 1

# EX+Const-AM. out Existing Plus Construction Conditions AM Peak Hour

Impact	An	al y	si s	Report	
				vi ce	

Ιn	tersecti on	Base Del/V/	Future Del/ V/	Change i n
#	1 Wilmington Ave / I-405 NB Ramp	LOS Veh C C 21.4 0.499	LOS Veh C C 21.5 0.500	+ 0.080 D/V
#	2 Wilmington Ave / I-405 SB Ramp	D 44.2 0.355	E 57. 9 0. 439	+13.706 D/V
#	4 Alameda Ave / I-405 NB Ramps	C 21.2 0.690	C 25.6 0.807	+ 4.446 D/V
#	9 I-405 SB Ramps / 223rd St	C 23.4 0.472	C 24.6 0.502	+ 1.194 D/V

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Tesoro Los Angeles Refinery Existing Plus Construction Conditions AM Peak Hour

### EX+Const-AM. out Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative)

*****	2000 HCM Opera			e Volume Alt		e) ******	*****
Intersection	#1 Wilmingtor	n Ave / I-	405 NB Rar	nos			
Cycle (sec): Loss Time (se Optimal Cycle	100 ec): 8 (	(Y+R=4.0 s	Criti sec) Avera Level	cal Vol./Cap age Delay (se Of Service:	o.(X): ec/veh):	0. 50 21.	00 . 5 C
Approach: Movement:	North Bound L - T -	R L -	ith Bound T - R	East Bo L - T -	- R	West Book	- R
Control: Rights: Min. Green: Lanes:	Protected Include 0 0 0 0 2 0	0 0 1 1 0	Permitted Include 0 (	Permit	ted ide 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	Permital Include 0 0 0	ted
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:	e:  0 362  1.00 1.00 1.  0 362  0 1  0 0  0 363  1.00 1.00 1.  0.90 0.90 0.  0 405  0 0  0 405  1.00 1.00 1.	33 21 00 1.00 33 21 13 0 0 0 46 21 00 1.00 90 0.90 51 23 0 0 51 23 00 1.00 00 1.00 51 23	371 (1.00 1.00 371 (1.00 1.00 1.00 1.00 1.00 1.00 1.00 419 (1.00 1	0 0 0 0 1.00 1.00 0 0 0 0 0 0 0 0 0 0 0 0 0 1.00 1.0	1.00 1 0 0 0 0 0 0 1.00 1 0.90 0 0 0 1.00 1	693 0 1. 00 1. 00 693 0 0 0 693 0 1. 00 1. 00 0. 90 0. 90 773 0 0 0 773 0 1. 00 1. 00 1. 00 1. 00 1. 00 1. 00 773 0	484 1.00 484 0 0 484 1.00 0.90 540 1.00 1.00 540
Saturation FI Sat/Lane: Adjustment: Lanes: Final Sat.:	ow Modul e: 1900 1900 19 1.00 0.95 0. 0.00 2.00 1. 0 3610 16	900 1900 85 0.30 00 1.00 615 574	1900 1900 0. 91 1. 00 3. 00 0. 00 5187 (	1900 1900 1.00 1.00 0.00 0.00	1900 1 1.00 0 0.00 2 0 2	1900 1900 0. 59 1. 00 2. 00 0. 00 2226 0	1900 0. 85 1. 00 1615
User Del Adj :	0.00 0.11 0. 0.00 0.33 0. 0.00 0.34 0. 0.0 25.6 23 1.00 1.00 1.	03 0.04 0 33 0.14 0 10 0.30 0 3.4 40.9 0 00 1.00	0.08 0.00 0.14 0.00 0.59 0.00 41.8 0.0 1.00 1.00	0.00 0.00 0.00 0.00 0.00 0.0 0.0 0.0 0.1.00 1.00	0.00 0 0.00 0 0.0 1 1.00 1	0. 35  0. 00 6 * * * * 0. 59  0. 00 0. 59  0. 00 13. 4  0. 0 1. 00  1. 00	0. 33 0. 59 0. 56 13. 3 1. 00
Adj Del /Veh: LOS by Move: HCM2kAvgQ: ******	0.0 25.6 23 A C 0 5 ******	C D 1	D A 5 (	A A O	A O	13. 4	13.3 B 10 ****
Note: Queue I	reported is th	ne number	of cars pe	er lane.	******	*****	*****
Traffix 7.9 EX + Const AN	9.0415 (c) 200 W	D7 Dowling Mon Nov	Assoc. Li 24, 2014	censed to MN  3:57:53	MA, LONG	BEACH, CA <sup>4</sup> Page	
	Exi st	ting Plus	s Angeles Constructi I Peak Hour	on Condition	ıs		
*****	Leve Leve 2000 HCM Opera			ation Report		· · · · · · · · · · · · · · · · · · ·	****
			Page 3				

Page 3

#### EX+Const-AM. out

Intersection	#2 Wilmington #	ve / I -405	SB Ramp	S *****	*****	*****	****
Cycle (sec): Loss Time (se	100 ec): 12 (Y+ e: 44 ********	R=4.0 sec)	Critic Averag	al Vol. e Delay	/Cap.(X): (sec/veh	0. 4	39 '. 9 E
Approach: Movement:	North Bound	South B L - T	ound - R	Eas L -	t Bound T - R	L - T	- R
	Permitted Include	Protec Incl 0 0 1 0 3	ted ude 0	Pe I 0 0 1	rmitted nclude 0 0	0 0 0	ted ide 0
Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj:	6:  0 304 359  1.00 1.00 1.00  0 304 359  0 13 0  0 0 0  0 317 359  1.00 1.00 1.00  0.95 0.95 0.95  0 335 379  0 0 0  0 335 379  1.00 1.00 1.00  1.00 1.00 1.00  0 335 379	141 906 1.00 1.00 141 906 0 4 0 0 141 910 1.00 1.00 0.95 0.95 149 962 0 0 149 962 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00	0 1.00 0 0 0 0 1.00 0.95 0 0 0 1.00 1.00	123 1.00 1 123 0 0 123 1.00 1 0.95 0 130 0 130 1.00 1 1.00 1	0 164 .00 1.00 0 164 0 96 0 0 0 260 .00 1.00 .95 0.95 0 275 0 0 0 275 .00 1.00 .00 1.00 .00 1.00	0 0 1.00 1.00 0 0 0 0 0 0 0 0 1.00 1.00 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0 1. 00 0 0 0 0 1. 00 0. 95 0 0 1. 00 1. 00
Saturation F Sat/Lane: Adjustment: Lanes: Final Sat.:		1900 1900 0. 95 0. 91 1. 00 3. 00 1805 5187	1900 1.00 0.00	1900 1 0.72 0 1.00 0 1368	0. 95 0. 72 0. 00 1. 00 0 1368	0 0	1900 1.00 0.00
Vol /Sat: Cri t Moves: Green/Cycl e: Vol ume/Cap: Del ay/Veh: User Del Adj: Adj Del /Veh: LOS by Move: HCM2kAvgQ:	ysis Module: 0.00 0.09 0.23 0.00 0.17 0.17 0.00 0.54 1.38 0.0 38.9 232.8	0. 08 0. 19  ****  0. 34 0. 51  0. 24 0. 36  23. 9 14. 8  1. 00 1. 00  23. 9 14. 8  C B  3 6	0. 00 0. 00 0. 00 0. 0 1. 00 0. 0 A	1.00 1 22.1 C 3	0.00 0.20 **** 0.00 0.37 0.00 0.54 0.0 25.8 0.00 1.00 0.0 25.8 A C	0.00 0.00 0.00 0.00 0.00 0.00 0.0 0.0 1.00 1.00 0.0 0.0 A A 0 0	0. 00 0. 00 0. 00 0. 0 1. 00 0. 0 A
Note: Queue ******	reported is the ******************** 9.0415 (c) 2007	number of c	ars per ***** oc. Lic	lane. ****** ensed t	*****	******	*****
	Te Existir	soro Los An g Plus Cons AM Pea	tructio	efinery n Condi	tions		
*****	 Level 2000 HCM Operati *******	Of Service ons Method	 Computa (Future *****	tion Re Volume	port	i ve) *******	
Intersection	#4 Alameda Ave	/ I -405 NB	Ramps				
Cycle (sec):	100				/Cap. (X):	0.8	

EX+Const-AM. out Loss Time (sec): 12 (Y+R=4.0 sec) Average Delay (sec/veh): 25.6 Optimal Cycle: 79 Level Of Service: C Final Volume: 0 601 55 0 916 54 Saturation Flow Module: Capacity Analysis Module: Vol /Sat: 0.00 0.17 0.03 0.00 0.27 0.27 0.00 0.00 0.00 0.44 0.00 0.21 Crit Moves: \*\*\*\* \* Note: Queue reported is the number of cars per lane. Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CAPEX + Const AM Mon Nov 24, 2014 13:57:53 Page 6-1 Tesoro Los Angeles Refinery Existing Plus Construction Conditions AM Peak Hour Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative) Intersection #9 I-405 SB Ramps / 223rd St 

Page 5

Approach: Movement:	North Bound L - T -	R	EX+( South L - T	- R	Eas L -	st Bour T -				
Control: Rights: Min. Green: Lanes:	Split Phase Include 0 0 0 0 1! 0	0	Split Inc 0 1 0 0	Phase Tude 0 0	Pro 1 0 2 0	ncl ude 0 2 1	0 0	Pr 0	otect Inclu 0 ) 2	ed de 0
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:	e: 1 1 1 1.00 1.00 1. 1 1 0 0 0 0 0 1 1 1.00 1.00 1. 0.88 0.88 0. 1 1 0 0 1 1 1.00 1.00 1. 1.00 1.00 1.	5 00 5 0 0 5 00 88 6 0 6 00 00 6	55 1.00 1.0 55 0 0 55 1.00 1.0 0.88 0.8 62 0 62 1.00 1.0	0 123 0 1.00 0 123 0 24 0 0 0 147 0 1.00 8 0.88 0 167 0 0 167 0 1.00 0 1.00 0 167	353 1.00 1 353 21 0 374 1.00 1 0.88 0 425 0 425 1.00 1 1.00 1	302 1.00 1 302 1 0 303 1.00 1 0.88 0 344 0 344 1.00 1 1.00 1	4 1. 00 4 0 0 4 1. 00 0. 88 5 0 5 1. 00	3 1. 00 3 0 0 3 1. 00 0. 88 3 1. 00 1. 00 3	837 8 0 845 1.00 0.88 959 0 959 1.00	32 1. 00 32 0 0 32 1. 00 0. 88 36 0 36 1. 00 1. 00 36
Saturation Fl Sat/Lane: Adjustment: Lanes: Final Sat.:	ow Module: 1900 1900 19 0.90 0.90 0. 0.14 0.14 0.	900 90 72 218	1900 190 0. 95 1. 0 1. 00 0. 0	0 1900 0 0.85 0 1.00 0 1615	1900 1 0. 92 0 2. 00 2 3502 5	1900 1 0. 91     0 2. 96     0 5109	1900 ). 91 ). 04 67	1900 0. 95 1. 00 1805	1900 0. 91 2. 89 4973	1900 0. 91 0. 11 188
Capacity Anal Vol/Sat: Crit Moves: Green/Cycle: Volume/Cap: Delay/Veh: User DelAdj: Adj Del/Veh: LOS by Move: HCM2kAvgQ:	ysis Module: 0.00 0.00 0.  0.01 0.01 0.  0.50 0.50 0.  72.6 72.6 72.6 72  1.00 1.00 1.  72.6 72.6 72.6 72  E E  1 1  ****************************	00 ( 50 ( 50 ( 2.6 ( 00 ( 2.6 ( E 1	0.03 0.0 0.21 0.0 0.17 0.0 32.9 0. 1.00 1.0 32.9 0. C A	0 0. 10 **** 0 0. 21 0 0. 50 0 36. 4 0 1. 00 0 36. 4 D 0 5 ****	0. 12 0 **** 0. 24 0 0. 50 0 33. 2 1. 00 1 33. 2 C	0. 07 0 0. 61 0 0. 11 0 8. 3 1. 00 1 8. 3 A	0. 07 0. 61 0. 11 8. 3 1. 00 8. 3 A	0. 00 0. 02 0. 11 50. 0 1. 00 50. 0	0. 19 **** 0. 38 0. 50 23. 7 1. 00 23. 7 C 9	0. 19 0. 38 0. 50 23. 7 1. 00 23. 7 C
	reported is th					*****	****	*****	*****	*****

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EX+Const-PM. out

EX + Const PM Mon Nov 24, 2014 13: 58: 17 Page 1-1 <del>-</del>

Tesoro Los Angeles Refinery Existing Plus Construction Conditions PM Peak Hour

Scenario Report

EX + Const PM Scenari o:

Command: EX+Const-PM

Vol ume: PM

Geometry: Impact Fee: Trip Generation: Trip Distribution: Existing
Default Impact Fee
Const-PM

Default Trip Distribution Default Path Default Route

Paths: Routes: Configuration: EX+Const-PM

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Tesoro Los Angeles Refinery Page 1

# EX+Const-PM. out Existing Plus Construction Conditions PM Peak Hour

Impact	An	al y	/si s	R	epor	t
· Leve						

Ιn	tersecti on	Base Del/V/	Future Del/ V/	Change i n
#	1 Wilmington Ave / I-405 NB Ramp	LOS Veh C B 18.5 0.395	LOS Veh C B 18.6 0.395	+ 0.176 D/V
#	2 Wilmington Ave / I-405 SB Ramp	B 15.7 0.629	B 16.5 0.641	+ 0.786 D/V
#	4 Alameda Ave / I-405 NB Ramps	C 23. 2 0. 665	C 23.8 0.683	+ 0.617 D/V
#	9 I-405 SB Ramps / 223rd St	C 24.3 0.327	C 23.7 0.395	-0.516 D/V

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Tesoro Los Angeles Refinery Existing Plus Construction Conditions PM Peak Hour

### EX+Const-PM. out Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative)

*****	2000 HCM Operatio	ons Method (Futur	e Volume Alternati	Ve) ******
Intersection	#1 Wilmington Av	/e / I-405 NB Ram	ps *******	*****
Cycle (sec): Loss Time (se Optimal Cycle	100 ec): 8 (Y+F e: 27	Criti R=4.0 sec) Avera Level	cal Vol./Cap.(X): ge Delay (sec/veh) Of Service: *******	0. 395 : 18. 6 B
Approach: Movement:	North Bound L - T - R	South Bound L - T - R	East Bound L - T - R	West Bound L - T - R
Control: Rights: Min. Green: Lanes:	 Protected Include 0 0 0 0 0 2 0 1	Permitted	I ncl ude 0 0 0	Permitted Include 0 0 0 2 0 0 0 1
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:	l l	71 794 0 1.00 1.00 1.00 71 794 0 0 1 0 0 0 0 71 795 0 1.00 1.00 1.00 0.95 0.95 0.95 75 838 0 0 0 0 75 838 0 1.00 1.00 1.00 1.00 1.00 1.00 75 838 0	0 0 0 1.00 1.00 1.00 0 0 0 0 0 0 0 0 0 0 0 0 1.00 1.00 1.00 0.95 0.95 0.95 0 0 0 0 0 0 1.00 1.00 1.00 1.00 1.00 1.00	428
Saturation FI Sat/Lane: Adjustment: Lanes: Final Sat.:		1900 1900 1900 0.51 0.91 1.00 1.00 3.00 0.00 973 5187 0	1900 1900 1900 1.00 1.00 1.00 0.00 0.00 0.00	1900 1900 1900 0.59 1.00 0.85 2.00 0.00 1.00 2234 0 1615
	ysis Module: 0.00 0.08 0.15  ****  0.00 0.41 0.41 0.00 0.20 0.36 0.0 19.1 20.8 1.00 1.00 1.00 0.0 19.1 20.8 A B C 0 3 5  **********************************		0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00	0. 20 0. 00 0. 20  ****  0. 51 0. 00 0. 51  0. 40 0. 00 0. 39  15. 2 0. 0 15. 2  1. 00 1. 00 1. 00  15. 2 0. 0 15. 2  B A B  5 0 6  **********************************
	9. 0415 (c) 2007 [		censed to MMA, LON	
	Tes Existing	soro Los Angeles g Plus Constructi PM Peak Hour	on Conditions	
****		Of Service Comput ons Method (Futur	ation Report e Volume Alternati	ve)
		Page 3		

Page 3

#### EX+Const-PM. out

Intersection	#2 Wilmington Av	/e / I -405 SB Ramp	S *******	*****
Cycle (sec): Loss Time (sec) Optimal Cycle	100 ec): 12 (Y+F e: 52 ********	R=4.0 sec) Averag	al Vol./Cap.(X): Delay (sec/veh) Of Service: ************************************	0.641 : 16.5 B
Approach: Movement:	North Bound L - T - R	South Bound L - T - R	East Bound L - T - R	West Bound L - T - R
Control: Rights: Min. Green: Lanes:		Protected Include 0 0 0 0 1 0 3 0 0	Permitted Include 0 0 0	Permitted Include 0 0 0
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:		337 888 0 1.00 1.00 1.00 337 888 0 0 1 0 0 0 0 337 889 0 1.00 1.00 1.00 0.98 0.98 0.98 345 909 0 0 0 0 345 909 0 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00	26 0 82 1.00 1.00 1.00 26 0 82 0 0 15 0 0 0 26 0 97 1.00 1.00 1.00 0.98 0.98 0.98 27 0 99 0 0 0 0 27 0 99 1.00 1.00 1.00 1.00 1.00 1.00 27 0 99	0 0 0 0 0 1.00 1.00 0 0 0 0 0 0 0 0 0 0
Saturation Fi Sat/Lane: Adjustment: Lanes: Final Sat.:	ow Modul e: 1900 1900 1900 1.00 0.95 0.85 0.00 2.00 1.00 0 3610 1615	1900 1900 1900 0. 95 0. 91 1. 00 1. 00 3. 00 0. 00 1805 5187 0	1900 1900 1900 0. 75 0. 95 0. 75 1. 00 0. 00 1. 00 1423 0 1423	1900 1900 1900 1.00 1.00 1.00 0.00 0.00 0.00 0 0 0
User Del Adj: Adj Del /Veh: LOS by Move: HCM2kAvgQ:	0. 00 0. 14 0. 30   ****  0. 00 0. 47 0. 47  0. 00 0. 29 0. 64  0. 0 16. 2 21. 7  1. 00 1. 00 1. 00  0. 0 16. 2 21. 7  A B C 0 5 12	0. 19 0. 18 0. 00  ****  0. 30 0. 77 0. 00  0. 64 0. 23 0. 00  33. 1 3. 2 0. 0  1. 00 1. 00 1. 00  33. 1 3. 2 0. 0  C A A  10 3 0	0. 02 0. 00 0. 07 ****  0. 11 0. 00 0. 11  0. 17 0. 00 0. 64  40. 6 0. 0 49. 9  1. 00 1. 00 1. 00  40. 6 0. 0 49. 9  D A D  1 0 4	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00
Note: Queue	reported is the r ************************* 9.0415 (c) 2007 D	number of cars per  **********  Dowling Assoc. Licon Nov 24, 2014 13	lane. ************************************	******
	Tes	 soro Los Angeles R	efi nery	
	Existing	g Plus Constructio PM Peak Hour		
	2000 HCM Operatic *******	Of Service Computations Method (Future	tion Report Volume Alternati	ve) *******
****		*****		
Cycle (sec):	100	Critic Page 4	al Vol./Cap.(X):	0. 683

EX+Const-PM. out Loss Time (sec): 12 (Y+R=4.0 sec) Average Delay (sec/veh): 23.8 Optimal Cycle: 57 Level Of Service: C Fi nal Vol ume: 0 973 250 83 788 0 0 0 417 0 109 Saturation Flow Module: Capacity Analysis Module: Vol /Sat: 0.00 0.27 0.15 0.05 0.22 0.00 0.00 0.00 0.00 0.29 0.00 0.07 Crit Moves: Note: Queue reported is the number of cars per lane. Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CAPEX + Const PM Mon Nov 24, 2014 13:58:18 Page 6-1 Tesoro Los Angeles Refinery Existing Plus Construction Conditions PM Peak Hour Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative) Intersection #9 I-405 SB Ramps / 223rd St 

Page 5

Approach: Movement:	North Bound L - T - R	L - I -	I East Bound R L - T -	West Bound R L - T - R 
Control: Rights: Min. Green: Lanes:	Split Phase Include	Split Phase Include O O	Protected Include 0 0 0 0 2 0 2 1	Protected
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:	e:  3 6  1.00 1.00 1.0  3 6  0 0  0 0  3 6  1.00 1.00 1.0  0.95 0.95 0.9  3 6  0 0  3 6  1.00 1.00 1.0  1.00 1.0	3 125 2 0 1.00 1.00 1. 3 125 2 0 0 0 0 0 0 3 125 2 0 1.00 1.00 1. 5 0.95 0.95 0. 3 132 2 0 0 0 3 132 2 0 1.00 1.00 1. 0 1.00 1.00 1.	36	4 4 347 77 00 1.00 1.00 1.00 4 4 347 77 0 0 1 0 0 0 0 0 0 0 4 4 348 77 00 1.00 1.00 1.00 95 0.95 0.95 0.95 4 4 367 81 0 0 0 0 4 4 367 81 0 1.00 1.00 1.00
Saturation F Sat/Lane: Adjustment: Lanes:		0 1900 1900 19 5 0. 95 0. 86 0. 5 1. 00 0. 05 0. 3 1805 82 15	900 1900 1900 19 86 0.92 0.91 0. 95 2.00 2.96 0.	00 1900 1900 1900 91 0.95 0.89 0.89 04 1.00 2.46 0.54 66 1805 4133 914
	ysis Module: 0.01 0.01 0.0  ****  0.02 0.02 0.0  0.39 0.39 0.3  56.4 56.4 56.  1.00 1.00 1.0  56.4 56.4 56.  E E E  1 1  **************************	1 0.07 0.03 0.  2 0.19 0.19 0.  9 0.39 0.14 0.  4 36.6 34.3 34  0 1.00 1.00 1.  4 36.6 34.3 34  D C  1 4 1  *******************************	03  0.16  0.06  0. 19  0.41  0.61  0. 14  0.39  0.10  0. 1.3  20.8  7.9  7. 00  1.00  1.00  1. 1.3  20.8  7.9  7. C  C  A  1  6  2.	06  0.00  0.09  0.09
		number of cars		******

Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CA?

#### **Traffic Impact Analysis**

YEAR 2021 WITHOUT PROJECT



**AM PEAK HOUR** 

LT

1.00

246

Movement Lanes

Int #: 3

Peak Period:

Approach

North/South Street: WILMINGTON AVENUE

East/West Street: 223RD STREET

Scenario: 2021 Base

Thru Lane:	1600 vph	N-S Split Phase :	Ν
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Capacity

1,600

0.154

ICU ANALYSIS

LOS:

С

Volume

Southbound	RT	1.00	327	1,600	0.117	N-S(1):	0.163
	TH	2.00	663	3,200	0.207 *	N-S(2):	0.214 *
	LT	1.00	58	1,600	0.036	E-W(1):	0.302
Westbound	RT	1.00	54	1,600	0.000	E-W(2):	0.342 *
	TH	2.00	813	3,200	0.254 *		
	LT	1.00	205	1,600	0.128	V/C:	0.556
Northbound	RT	0.50	82	800	0.000	Lost Time:	0.100
	TH	2.50	506	4,000	0.127		
	LT	1.00	11	1,600	0.007 *		
Eastbound	RT	1.00	16	1,600	0.003	ICU:	0.656
	TH	2.00	558	3,200	0.174		
	LT	1.00	140	1,600	0.088 *	LOS:	В
Peak Period:	PM PEAK H	HOUR					
Peak Period: Approach	PM PEAK I	HOUR Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
			Volume 204	Capacity 1,600	V/C 0.000	ICU ANA N-S(1):	LYSIS 0.142
Approach	Movement	Lanes					
Approach	Movement RT	Lanes 1.00	204	1,600	0.000	N-S(1):	0.142
Approach	Movement RT TH	1.00 2.00	204 742	1,600 3,200	0.000 0.232 *	N-S(1): N-S(2):	0.142 0.237 *
Approach Southbound	Movement RT TH LT	1.00 2.00 1.00	204 742 56	1,600 3,200 1,600	0.000 0.232 * 0.035	N-S(1): N-S(2): E-W(1):	0.142 0.237 * 0.366 *
Approach Southbound	Movement RT TH LT RT	1.00 2.00 1.00 1.00	204 742 56 146	1,600 3,200 1,600 1,600	0.000 0.232 * 0.035 0.056	N-S(1): N-S(2): E-W(1):	0.142 0.237 * 0.366 *
Approach Southbound	Movement RT TH LT RT TH	1.00 2.00 1.00 1.00 2.00	204 742 56 146 353	1,600 3,200 1,600 1,600 3,200	0.000 0.232 * 0.035 0.056 0.110	N-S(1): N-S(2): E-W(1): E-W(2):	0.142 0.237 * 0.366 * 0.264
Approach Southbound Westbound	Movement RT TH LT RT TH LT TH LT	Lanes 1.00 2.00 1.00 1.00 2.00 1.00	204 742 56 146 353 181	1,600 3,200 1,600 1,600 3,200 1,600	0.000 0.232 * 0.035 0.056 0.110 0.113 *	N-S(1): N-S(2): E-W(1): E-W(2): V/C:	0.142 0.237 * 0.366 * 0.264 0.603
Approach Southbound Westbound	Movement RT TH LT RT TH LT TH LT RT	Lanes 1.00 2.00 1.00 1.00 2.00 1.00 0.50	204 742 56 146 353 181 127	1,600 3,200 1,600 1,600 3,200 1,600 800	0.000 0.232 * 0.035 0.056 0.110 0.113 * 0.000	N-S(1): N-S(2): E-W(1): E-W(2): V/C: Lost Time:	0.142 0.237 * 0.366 * 0.264 0.603 0.100
Approach Southbound Westbound	Movement RT TH LT RT TH LT TH LT TH LT TH LT RT	Lanes 1.00 2.00 1.00 1.00 2.00 1.00 2.00 1.00 2.50	204 742 56 146 353 181 127 426	1,600 3,200 1,600 1,600 3,200 1,600 800 4,000	0.000 0.232 * 0.035 0.056 0.110 0.113 * 0.000 0.107	N-S(1): N-S(2): E-W(1): E-W(2): V/C:	0.142 0.237 * 0.366 * 0.264 0.603

<sup>\* =</sup> Critical Movement

Int #:

North/South Street: 223rd Street Ramp (on Alameda Street)

East/West Street: Alameda Street

Scenario: 2021 Base

Thru Lane:	1600 vph	N-S Split Phase :	N
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Dual ET T Cha	ity. 10	70			LOST TIME	(70 Or Oyolo).	10
Peak Period:	AM PEAK I	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.257 *
	TH	3.00	1,149	4,800	0.239	N-S(2):	0.239
	LT	1.00	163	1,600	0.102 *	E-W(1):	0.113 *
Westbound	RT	1.00	122	1,600	0.000	E-W(2):	0.000
	TH	0.00	0	0	0.000		
	LT	1.00	180	1,600	0.113 *	V/C:	0.370
Northbound	RT	0.00	248	1,600	0.155 *	Lost Time:	0.100
	TH	3.00	482	3,200	0.151		
	LT	0.00	0	0	0.000		
Eastbound	RT	0.00	0	0	0.000	ICU:	0.470
	TH	0.00	0	0	0.000 *		
	LT	0.00	0	0	0.000	LOS:	Α
Peak Period:	PM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.410 *
	TH	3.00	1,004	4,800	0.209	N-S(2):	0.209
	LT	1.00	168	1,600	0.105 *	E-W(1):	0.071 *
Westbound	RT	1.00	125	1,600	0.000	E-W(2):	0.000
	TH	0.00	0	0	0.000		
	LT	1.00	114	1,600	0.071 *	V/C:	0.481
Northbound	RT	0.00	472	0	0.000	Lost Time:	0.100
	TH	3.00	991	4,800	0.305 *		
	LT	0.00	0	0	0.000		

<sup>\* =</sup> Critical Movement

RT

TH

LT

0.00

0.00

0.00

0

0

0

0

0

0

0.000

0.000

0.000 \*

ICU:

LOS:

0.581

Α

Eastbound

Int #:

North/South Street: 223rd Street

East/West Street: Alameda Street Ramp

Scenario: 2021 Base

Thru Lane:	1600 vph	N-S Split Phase :	N
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Duai Li Feliai	ty. 10	/0			LUST TITLE	(70 OI CYCIE).	10
Peak Period:	AM PEAK I	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.090 *
	TH	0.00	0	0	0.000	N-S(2):	0.083
	LT	0.00	0	0	0.000 *	E-W(1):	0.165 *
Westbound	RT	0.00	0	0	0.000	E-W(2):	0.145
	TH	3.00	765	5,280	0.145		
	LT	2.00	228	3,168	0.072 *	V/C:	0.255
Northbound	RT	1.00	272	1,760	0.090 *	Lost Time:	0.100
	TH	0.00	0	0	0.000		
	LT	1.00	146	1,760	0.083		
Eastbound	RT	0.00	82	0	0.000	ICU:	0.355
	TH	3.00	408	5,280	0.093 *		
	LT	0.00	0	0	0.000	LOS:	Α
Peak Period:	PM PEAK I	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.261 *
	TH	0.00	0	0	0.000	N-S(2):	0.056
	LT	0.00	0	0	0.000 *	E-W(1):	0.286 *
Westbound	RT	0.00	0	0	0.000	E-W(2):	0.055
	TH	3.00	290	5,280	0.055		
	LT	2.00	94	3,168	0.030 *	V/C:	0.547
Northbound	RT	1.00	506	1,760	0.261 *	Lost Time:	0.100
	TH	0.00	0	0	0.000		
					i e	i	

99

141

1,212

0

1,760

0

5,280

0

0.056

0.000

0.000

0.256 \*

ICU:

LOS:

0.647

В

Eastbound

 $\mathsf{LT}$ 

RT

TH

LT

1.00

0.00

3.00

0.00

<sup>\* =</sup> Critical Movement

Project: Int #:

North/South Street: ALAMEDA STREET

East/West Street: SEPULVEDA BOULEVARD-ALAMEDA RAMF

Scenario: 2021 Base

Thru Lane:	1600 vph	N-S Split Phase :	N
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

	444 DE 417 I	10115					
Peak Period:	AM PEAK I	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.249 *
	TH	3.00	785	4,800	0.164	N-S(2):	0.164
	LT	1.00	235	1,600	0.147 *	E-W(1):	0.031 *
Westbound	RT	2.00	203	3,200	0.000	E-W(2):	0.000
	TH	0.00	0	0	0.000		
	LT	1.00	50	1,600	0.031 *	V/C:	0.280
Northbound	RT	0.00	51	0	0.000	Lost Time:	0.100
	TH	3.00	438	4,800	0.102 *		
	LT	0.00	0	0	0.000		
Eastbound	RT	0.00	0	0	0.000	ICU:	0.380
	TH	0.00	0	0	0.000 *		
	LT	0.00	0	0	0.000	LOS:	Α

Peak Period:	PM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.389 *
	TH	3.00	877	4,800	0.183	N-S(2):	0.183
	LT	1.00	256	1,600	0.160 *	E-W(1):	0.059 *
Westbound	RT	2.00	417	3,200	0.050	E-W(2):	0.050
	TH	0.00	0	0	0.000		
	LT	1.00	95	1,600	0.059 *	V/C:	0.448
Northbound	RT	0.00	85	0	0.000	Lost Time:	0.100
	TH	3.00	1,012	4,800	0.229 *		
	LT	0.00	0	0	0.000		
Eastbound	RT	0.00	0	0	0.000	ICU:	0.548
	TH	0.00	0	0	0.000 *		
	LT	0.00	0	0	0.000	LOS:	Α

<sup>\* =</sup> Critical Movement

Int #: 8

North/South Street: SEPULVEDA BOULEVARD-ALAMEDA RAMF

East/West Street: SEPULVEDA BOULEVARD

Scenario: 2021 Base

Thru Lane:	1600 vph	N-S Split Phase :	Y
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

						, ,	
Peak Period:	AM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	1.00	147	1,600	0.016	N-S(1):	0.056 *
	TH	0.13	9	210	0.043	N-S(2):	0.000
	LT	1.87	128	2,691	0.048 *	E-W(1):	0.233
Westbound	RT	1.00	100	1,600	0.020	E-W(2):	0.266 *
	TH	2.00	608	3,200	0.190 *		
	LT	1.00	8	1,600	0.005	V/C:	0.322
Northbound	RT	0.00	4	0	0.000	Lost Time:	0.100
	TH	2.00	19	3,200	0.008 *		
	LT	0.00	2	1,600	0.001		
Eastbound	RT	1.00	6	1,600	0.003	ICU:	0.422
	TH	1.00	364	1,600	0.228		
	LT	1.00	121	1,600	0.076 *	LOS:	Α
Peak Period:	PM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	1.00	176	1,600	0.000	N-S(1):	0.058 *
	TH	0.17	12	269	0.045	N-S(2):	0.000
	LT	1.83	131	2,638	0.050 *	E-W(1):	0.600 *
Westbound	RT	1.00	244	1,600	0.108	E-W(2):	0.318
	TH	2.00	547	3,200	0.171	, ,	
	LT	1.00	2	1,600	0.001 *	V/C:	0.658
Northbound	RT	0.00	9	0	0.000	Lost Time:	0.100

2.00

0.00

1.00

1.00

1.00

TH LT

RT

ΤH

LT

13

4

1

958

235

3,200

1,600

1,600

1,600

1,600

0.008 \*

0.003

0.000

0.147

0.599 \*

ICU:

LOS:

0.758

С

Eastbound

<sup>\* =</sup> Critical Movement

Project: Int #:

North/South Street: TERMINAL ISLAND FREEWAY (SR-103)

East/West Street: **WILLOW STREET** 

Scenario: 2021 Base

Thru Lane:	1600 vph	N-S Split Phase :	Y
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK I	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.034 *
	TH	1.00	0	1,600	0.000	N-S(2):	0.000
	LT	0.00	0	0	0.000 *	E-W(1):	0.185
Westbound	RT	0.00	16	0	0.000	E-W(2):	0.262 *
	TH	2.00	813	3,200	0.259 *		
	LT	2.00	242	2,880	0.084	V/C:	0.296
Northbound	RT	2.00	101	3,200	0.000	Lost Time:	0.100
	TH	0.00	0	0	0.000		
	LT	2.00	99	2,880	0.034 *		
Eastbound	RT	1.00	187	1,600	0.086	ICU:	0.396
	TH	2.00	324	3,200	0.101		
	LT	1.00	4	1,600	0.003 *	LOS:	Α
Peak Period:	PM PEAK I	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.111 *
	TH	1.00	0	1,600	0.000	N-S(2):	0.000
	LT	0.00	0	0	0.000 *	E-W(1):	0.379 *
Westbound	RT	0.00	1	0	0.000	E-W(2):	0.136
	TH	2.00	435	3,200	0.136		

1 out 1 official							
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.111 *
	TH	1.00	0	1,600	0.000	N-S(2):	0.000
	LT	0.00	0	0	0.000 *	E-W(1):	0.379 *
Westbound	RT	0.00	1	0	0.000	E-W(2):	0.136
	TH	2.00	435	3,200	0.136		
	LT	2.00	171	2,880	0.059 *	V/C:	0.490
Northbound	RT	2.00	254	3,200	0.053	Lost Time:	0.100
	TH	0.00	0	0	0.000		
	LT	2.00	319	2,880	0.111 *		
Eastbound	RT	1.00	262	1,600	0.064	ICU:	0.590
	TH	2.00	1,024	3,200	0.320 *		
	LT	1.00	0	1,600	0.000	LOS:	Α

<sup>\* =</sup> Critical Movement

Int #: 11

North/South Street: SANTA FE AVE

East/West Street: SEPULVEDA BOULEVARD

RT

ΤH

LT

RT

ΤH

LT

0.00

2.00

1.00

0.00

2.00

1.00

Scenario: 2021 Base

Thru Lane:	1600 vph	N-S Split Phase :	Υ
Left-Turn Lane:	1600 vph	E-W Split Phase :	N
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK I	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	135	0	0.000	N-S(1):	0.209 *
	TH	2.00	264	3,200	0.125 *	N-S(2):	0.000
	LT	2.00	156	2,880	0.054	E-W(1):	0.204
Westbound	RT	0.00	111	0	0.000	E-W(2):	0.327 *
	TH	2.00	786	3,200	0.280 *		
	LT	2.00	163	2,880	0.057	V/C:	0.536
Northbound	RT	0.00	82	0	0.000	Lost Time:	0.100
	TH	2.00	188	3,200	0.084 *		
	LT	1.00	78	1,600	0.049		
Eastbound	RT	0.00	33	0	0.000	ICU:	0.636
	TH	2.00	436	3,200	0.147		
	LT	1.00	75	1,600	0.047 *	LOS:	В
	•						
Peak Period:	PM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	64	0	0.000	N-S(1):	0.321 *
	TH	2.00	319	3,200	0.120 *	N-S(2):	0.000
	LT	2.00	339	2,880	0.118	E-W(1):	0.377 *
Westbound	RT	0.00	153	0	0.000	E-W(2):	0.292
	TH	2.00	495	3,200	0.203	, ,	
	LT	2.00	140	2,880	0.049 *	V/C:	0.698

205

438

84

44

1,006

143

0

3,200

1,600

0

3,200

1,600

0.000

0.053

0.000

0.089

0.328 \*

0.201 \*

Lost Time:

ICU:

LOS:

0.100

0.798

С

Northbound

Eastbound

<sup>\* =</sup> Critical Movement



# Appendix E Level of Service Workheet (Circular 212 Method)



Alameda Street Ramp

I/S #:

PROJECT TITLE: ICTF Modification and Expansion Project EIR

North-South Street: 223rd Street (on 223rd East-West Street:

Scenario: CEQA Baseline

Count Date: Analyst: keris, Inc. Date: 7/22/2014

	AM PEAK HOUR MD PEAK HOUR PM PEA							M PEAK HOU	IR	
	No. of Phases			3			3			3
	Opposed Ø'ing: N/S-1, E/W-2 or Both-3?			2			2			2
ı	Right Turns: FREE-1, NRTOR-2 or OLA-3?	NB 3 EB 0	SB WB	0	NB 3 EB 0	SB NB	0	NB 0 EB 3	SB WB	0
	ATSAC-1 or ATSAC+ATCS-2?	<i>EB</i> 0	WB	2	EB 0	ND	2	<i>LB</i> 3	WB	2
	Override Capacity			1500			1500			1500
	MOVEMENT		No. of	Lane		No. of	Lane		No. of	Lane
	MOVEMENT	Volume	Lanes	Volume	Volume	Lanes	Volume	Volume	Lanes	Volume
	↑ Left	146	1	146	0	1	60	99	1	99
NORTHBOUND	← Left-Through		0			0			0	
o	∱ Through	0	0	0	0	0	0	0	0	0
H	→ Through-Right		0			0			0	
RT	<mark> → Right</mark>	272	1	147	0	1	403	506	1	454
Q	← Left-Through-Right		0			0			0	
_	Left-Right		0			0			0	
		•		<del>-</del> '	•	-				
0	→ Left	0	0	0	0	0	0	0	0	0
SOUTHBOUND	├─ Left-Through		0			0			0	
o l	Through	0	0	0	0	0	0	0	0	0
甲	← Through-Right		0			0			0	
5	-√ Right	0	0	0	0	0	0	0	0	0
00	← Left-Through-Right		0			0			0	
0,	人, Left-Right		0			0			0	
					,					-
0	Left	0	0	0	0	0	0	0	0	0
ΙŽ	→ Left-Through		0			0			0	
EASTBOUND	→ Through	408	2	163	0	2	380	1,212	2	451
TB	→ Through-Right → Right	00	1 0	00	0	1	45		1 0	444
AS	Right  Left-Through-Right	82	0	82	0	0	45	141	0	141
ш	↓ Left-Through-Right		0			0			0	
	- Leit-Right	<u></u>	U			! U				
	√ Left	228	2	125	0	2	77	94	2	52
9	₹ Left-Through	220	0	123	I	0	"	34	0	32
WESTBOUND	← Through	765	3	255	0	3	82	290	3	97
BO	← Through-Right	. 55	0	200	Ĭ	0	02		0	- 01
ST	Right	0	0	0	0	0	0	0	0	0
ΛE	Left-Through-Right	Ĭ	0	ŭ		0	ŭ		0	Ů
_ >	├ Left-Right		0			0			0	
		٨	lorth-South:	147	North	-South:	403		Vorth-South:	454
	CRITICAL VOLUMES	ĺ	East-West:	418	Eas	t-West:	462	1	East-West:	
			SUM:	565		SUM:	865		SUM:	1002
	VOLUME/CAPACITY (V/C) RATIO:	ĺ		0.396			0.577			0.703
V/	C LESS ATSAC/ATCS ADJUSTMENT:	ĺ		0.296			0.477			0.603
	LEVEL OF SERVICE (LOS):	Î		A			A			В
	(200).			^			^			

Version: 1i Beta; 8/4/2011

2020NP-AM. out

2020 NP AM Tue Dec 2, 2014 11:59:34 Page 1-1 

> Tesoro Los Angeles Refinery Year 2020 No Project AM Peak Hour

Scenario Report

2020 NP AM Scenari o:

Command: 2020-AM Vol ume: 2020 AM Geometry:
Impact Fee: 2017

Default Impact Fee

Const-AM

Impact Fee: Trip Generation: Trip Distribution: Default Trip Distribution Default Path

Paths: Default Route Routes:

Configuration: 2020-AM

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> Tesoro Los Angeles Refinery Page 1

#### 2020NP-AM. out Year 2020 No Project AM Peak Hour

Impact Analysis Report Level Of Service

Ιn	tersection		Base Del/ V/		Future Del/ V/	Change i n
#	1 Wilmington Ave / I-405 NB Ramp		S Veh C 21.7 0.512		S Veh C 21.7 0.512	+ 0.000 D/V
#	2 Wilmington Ave / I-405 SB Ramp	С	21. 8 0. 364	С	21. 8 0. 364	+ 0.000 D/V
#	4 Alameda Ave / I-405 NB Ramps	С	23. 4 0. 687	С	23. 4 0. 687	+ 0.000 D/V
#	9 I-405 SB Ramps / 223rd St	С	23. 5 0. 484	С	23. 5 0. 484	+ 0.000 D/V

Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CA<sup>2</sup> 2020 NP AM Tue Dec 2, 2014 11:59:34 Page 3-1

Tesoro Los Angeles Refinery Year 2020 No Project AM Peak Hour

AW Peak Hour

### 2020NP-AM.out Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative)

Cycle (sec): 100 Critical Vol./Cap. (X): 0.512
Loss Time (sec): 8 (Y+R=4.0 sec) Average Delay (sec/veh): 21.7
Optimal Cycle: 39 Level Of Service: C Approach: North Bound South Bound East Bound West Bound Movement: L - T - R Volume Modul e: Saturation Flow Module: Capacity Analysis Module: Vol/Sat: 0.00 0.11 0.02 0.00 0.09 0.00 0.00 0.00 0.36 0.00 0.34 Crit Moves: Crit Moves: Green/Cycle: 0.00 0.33 0.33 0.00 0.14 0.00 0.00 0.00 0.00 0.59 0.00 0.59 Volume/Cap: 0.00 0.35 0.07 0.00 0.61 0.00 0.00 0.00 0.00 0.60 0.00 0.58 Delay/Veh: 0.0 25.4 22.9 0.0 41.7 0.0 0.0 0.0 0.0 14.0 0.0 13.8 Note: Queue reported is the number of cars per lane. Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CA $^\circ$  D20 NP AM Tue Dec 2, 2014 11:59:34 Page 4-1 Tesoro Los Angeles Refinery Year 2020 No Project AM Peak Hour \_\_\_\_\_ Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative)

Page 3

2020NP-AM. out Intersection #2 Wilmington Ave / I-405 SB Ramps ************************************								
Cycle (sec): Loss Time (se	ec): 100 ec): 12 (Y+	Critic R=4.0 sec) Averaç	cal Vol./Cap.(X): ge Delay (sec/veh)	0. 364 : 21. 8				
Approach: Movement:	North Bound L - T - R	South Bound L - T - R	East Bound L - T - R	West Bound L - T - R				
Control: Rights: Min. Green: Lanes:	Permitted     Include     0     0     0     0     2     1     1	Protected     Include     0     0     0     2     0     3     0	Permitted     Include     0    0    0     0    1    0	Permitted     Include     0    0    0				
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:	0 311 368 1.00 1.00 1.00 0 311 368 0 0 0 0 0 0 0 311 368 1.00 1.00 1.00 0.95 0.95 0.95 0 329 389 0 0 0 0 329 389 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00 329 389	144 928 0 1.00 1.00 1.00 144 928 0 0 0 0 0 0 0 144 928 0 1.00 1.00 1.00 0.95 0.95 0.95 152 981 0 0 0 0 152 981 0 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00	126	0 0 0 0 0 1.00 1.00 0 0 0 0 0 0 0 0 0 0				
Saturation F Sat/Lane: Adjustment: Lanes: Final Sat.:	I ow Modul e: 1900 1900 1900 1.00 0.84 0.84 0.00 2.00 2.00 0 3178 3178	1900 1900 1900 0. 92 0. 91 1. 00 2. 00 3. 00 0. 00 3502 5187 0	1900 1900 1900 0. 71 0. 95 0. 71 1. 00 0. 00 1. 00 1353 0 1353	1900 1900 1900 1.00 1.00 1.00 0.00 0.00 0.00 0 0 0				
Vol /Sat: Cri t Moves: Green/Cycl e: Vol ume/Cap: Del ay/Veh: User Del Adj: Adj Del /Veh: LOS by Move:	1.00 1.00 1.00 0.0 34.6 35.8 A C D	0.39 0.61 0.00 0.11 0.31 0.00 19.3 9.6 0.0 1.00 1.00 1.00 19.3 9.6 0.0 B A A	C A C	A A A				
HCM2kÁvgQ: 0 5 7 2 5 0 4 0 5 0 0 0								
Tesoro Los Angeles Refinery Year 2020 No Project AM Peak Hour								
Level Of Service Computation Report  2000 HCM Operations Method (Future Volume Alternative)  ***********************************								

2020NP-AM. out Loss Time (sec): 12 (Y+R=4.0 sec) Average Delay (sec/veh): 23.4 Optimal Cycle: 58 Level Of Service: C Approach: North Bound South Bound East Bound West Bound Movement: L - T - R L - T - R L - T - R L - T - R Control: Protected Protected Protected Protected Permitted Rights: Include I -----| Saturation Flow Module: Capacity Analysis Module: Vol /Sat: 0.00 0.17 0.03 0.03 0.26 0.00 0.00 0.00 0.00 0.35 0.00 0.21 Crit Moves: \*\*\*\* \* Note: Queue reported is the number of cars per lane. Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CA  $^\circ$  2020 NP AM Tue Dec 2, 2014 11:59:34 Page 6-1

	s Angeles Refinery 020 No Project Peak Hour	
Level Of Servi 2000 HCM Operations Meth	ice Computation Report nod (Future Volume Alternative) *****	****
Intersection #9 I-405 SB Ramps / 223	3rd St **************	*****
Cycle (sec): 100 Loss Time (sec): 16 (Y+R=4.0 sec) Optimal Cycle: 48 ************************************	Critical Vol./Cap.(X): ec) Average Delay (sec/veh):     Level Of Service: ************************************	0. 484 23. 5 C *****

Page 5

Approach: Movement:	North Bour L - T -	R L	2020N outh Bo - T	- R	Ea L -		- R	L -		- R
Control: Rights: Min. Green: Lanes:	Split Phas Include 0 0 0 0 1! 0	se ' S 0 0 0 1	olit Ph Inclu O O	ase de 0	Pr 0 2 0	otect Inclu 0 ) 2	ed de d	' Pro I 0	ncl u	ed ' de 0
	1 1 1 1 1 1 1 0 1 1 0 0 0 0 1 1 1 1 0 0 0 0 1	5 5. 1.00 1.00 5 5. 0 0 5 5. 1.00 1.00 5 88 0.80 6 6 0 6 1.00 1.00 6 6	6 0 0 1.00 6 0 0 0 0 0 6 0 0 1.00 8 0.88 4 0 0 0 1.00 0 1.00 0 1.00 0 1.00 0 1.00	126 1. 00 126 0 0 126 1. 00 0. 88 143 0 143 1. 00 1. 00 143	362 1.00 362 0 0 362 1.00 0.88 411 0 411 1.00 1.00 411	309 1.00 309 0 0 309 1.00 0.88 351 0 351 1.00	1. 00 4 0 0 4 1. 00 0. 88 5 0 5 1. 00 1. 00	3 1.00 1 3 0 0 3 1.00 1 0.88 0 3 1.00 1 1.00 1	857 0 0 857 1.00 0.88 973 0 973 1.00	33 1.00 33 0 0 33 1.00 0.88 37 0 37 1.00 1.00
Saturation Fl Sat/Lane: Adjustment: Lanes: Final Sat.:	ow Module: 1900 1900 1 0.90 0.90 0 0.14 0.14 0	1900 1900 0.90 0.90 0.72 1.00	0 1900 5 1.00 0 0.00	1900 0. 85 1. 00 1615	1900 0. 92 2. 00 3502	1900 0. 91 2. 96 5110	1900 0. 91 0. 04 66	1900 1 0. 95 0 1. 00 2 1805 4	0. 90 2. 89 4965	1900 0. 90 0. 11 191
Capacity Anal Vol/Sat: Crit Moves: Green/Cycle: Volume/Cap: Delay/Veh: User DelAdj: Adj Del/Veh: LOS by Move: HCM2kAvgQ:	ysis Module: 0.00 0.00 0  0.01 0.01 0  0.48 0.48 0  70.0 70.0 7  1.00 1.00 1  70.0 70.0 7  E E  1 1	0.00 0.00 0.01 0.1 0.48 0.1 70.0 34. 1.00 1.0 70.0 34. E C	4 0.00 8 0.00 9 0.00 9 0.0 0 1.00 9 0.0 A 2 0 ******	0. 09 **** 0. 18 0. 48 37. 9 1. 00 37. 9 D 4 *****	0. 12 **** 0. 24 0. 48 32. 9 1. 00 32. 9 C 6	0. 07 0. 63 0. 11 7. 4 1. 00 7. 4 A 2	0. 07 0. 63 0. 11 7. 4 1. 00 7. 4 A	0. 00 ( 0. 02 ( 0. 11 ( 49. 9 2 1. 00 1 49. 9 2	0. 20 * * * * 0. 40 0. 48 22. 2 1. 00 22. 2 C	0. 20 0. 40 0. 48 22. 2 1. 00 22. 2 C
*********	Note: Queue reported is the number of cars per lane.									

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2020NP-PM. out

2020 NP PM Tue Dec 2, 2014 12:05:06 Page 1-1 

Tesoro Los Angeles Refinery Year 2020 No Project PM Peak Hour

Scenario Report

2020 NP PM Scenari o:

Command: 2020-PM Vol ume: 2020 PM Geometry:
Impact Fee: 2017

Default Impact Fee Const-PM Default Trip Distribution Default Path Impact Fee: Trip Generation: Trip Distribution:

Paths: Default Route Routes: Configuration: 2020-PM

Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CAP 200 NP PM Tue Dec 2, 2014 12:05:07 Page 2-1 2020 NP PM

> Tesoro Los Angeles Refinery Page 1

#### 2020NP-PM. out Year 2020 No Project PM Peak Hour

Impact Analysis Report Level Of Service

Ιn	tersecti on		Base Del/V/		Future Del/ V/	Change i n
#	1 Wilmington Ave / I-405 NB Ramp		S Veh C 18. 4 0. 420		S Veh C 18. 4 0. 420	+ 0.000 D/V
#	2 Wilmington Ave / I-405 SB Ramp	В	15. 7 0. 362	В	15. 7 0. 362	+ 0.000 D/V
#	4 Alameda Ave / I-405 NB Ramps	С	23. 5 0. 681	С	23. 5 0. 681	+ 0.000 D/V
#	9 I-405 SB Ramps / 223rd St	В	19. 1 0. 514	В	19. 1 0. 514	+ 0.000 D/V

Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CA $^\circ$  2020 NP PM Tue Dec 2, 2014 12:05:07 Page 3-1

Tesoro Los Angeles Refinery Year 2020 No Project PM Peak Hour

PM Peak noul -----Page 2

### 2020NP-PM. out Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative)

*****	2000 HCM Operations Method (Future Volume Alternative)										
Intersection											
Cycle (sec): Loss Time (sec) Optimal Cycle	10 ec): e: 2	00 8 (Y+R 28	e=4.0 s	sec)	Critic Averag Level	al Vol e Dela Of Sei	./Cap ay (se rvi ce:	o. (X): ec/veh)	:	0. 4 18	20 . 4 B
Approach: Movement:	North Bo L - T	- R	L -	- T	ound - R	L.	ast Bo - T	- R	L -	est Bo · T	
Control: Rights: Min. Green: Lanes:	Protect Inclu 0 0 0 0 2	ed ( ide 0 0 1	, O (	Permit Inclu 0 3	tted	0 0	Permit Inclu O	ted de d		Permit Inclu 0 0	ted '
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj:	l	155 1.00 155 0 0 155 1.00 0.95 163 0 163 1.00 1.00	0 1.00 0 0 0 0 1.00 0.95 0 0	886 1.00 886 0 886 1.00 0.95 934 0	0 1.00 0 0 0 0 1.00 0.95 0 0 1.00 1.00	1. 00 0 0 0 0 0 0 1. 00 0. 95 0 0 1. 00	0 1.00 0 0 0 0 1.00 0.95 0 0 1.00 1.00	1. 00 0 0 0 0 0 1. 00 0. 95 0 0 1. 00 1. 00	438 1.00 438 0 0 438 1.00 0.95 462 1.00 462 1.00	1.00 0 0 0 0 0 1.00 0.95 0 0	309 1.00 309 0 309 1.00 0.95 326 0 326 1.00 1.00 326
Saturation FI Sat/Lane: Adjustment: Lanes: Final Sat.:	1900 1900 1.00 0.95 0.00 2.00 0 3610	1900 0. 85 1. 00 1615		0. 91 3. 00 5187	1900 1.00 0.00	1. 00	1900 1.00 0.00	1900 1.00 0.00 0	1900 0. 59 2. 00 2234	1.00	1900 0. 85 1. 00 1615
User Del Adj: Adj Del /Veh: LOS by Move: HCM2kAvgQ:	0. 00 0. 08 ****  0. 00 0. 43 0. 00 0. 20 0. 0 17. 9	e: 0. 10 0. 43 0. 24 18. 4 1. 00 18. 4 B 3	0. 00 0. 00 0. 00 0. 0 1. 00 0. 0 A	0. 18 **** 0. 43 0. 42 20. 1 1. 00 20. 1 C	0.00 0.00 0.00 0.0 1.00 0.0 A 0	0. 00 0. 00 0. 0 1. 00 0. 0 A	A O	A O	В 5	0. 00 0. 00 0. 0 1. 00 0. 0 A	0. 20 0. 49 0. 41 16. 5 1. 00 16. 5 B
Note: Queue r	reported is	the n	umber	of ca	ars per	l ane.	*****	****	*****	****	*****
Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CA9 2020 NP PM Tue Dec 2, 2014 12:05:07 Page 4-1											
Tesoro Los Angeles Refinery Year 2020 No Project PM Peak Hour											
Level Of Service Computation Report											
*****	2000 HCM Operations Method (Future Volume Alternative) ************************************										

Page 3

2020NP-PM. out Intersection #2 Wilmington Ave / I-405 SB Ramps ************************************								
Cycle (sec): Loss Time (se	100 ec): 12 (Y+R	C=4.0 sec) A	ri ti ca verage	al Vol./Cap.() e Delay (sec/\	(): 0.362 /eh): 15.7 B			
Approach: Movement:	North Bound L - T - R	South Bou L - T -	nd R	East Bound L - T -	d West Bound R L - T - R			
Control: Rights: Min. Green: Lanes:	Permitted     Include     0    0     0    0    1	Protecte Includ 0 0 2 0 3 0	d le 0	Permitted Include 0 0	Permitted Include 0 0 0 0			
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:	1	345 910 1.00 1.00 345 910 0 0 345 910 1.00 1.00 0.98 0.98 353 930 0 0 353 930 1.00 1.00	0 1. 00 0 0 0 0 1. 00 0 0. 98 0 0 0 1. 00 0	27 0 0 0 27 0 1.00 1.00 1. 0.98 0.98 0. 28 0 0 0 28 0 1.00 1.00 1.	84 0 0 0 00 1.00 1.00 1.00 84 0 0 0 0 0 0 0 0 0 0 0 0 0 84 0 0 0 84 0 0 0 00 1.00 1.00 1.00 98 0.98 0.98 0.98 86 0 0 0 0 0 0 0 86 0 0 0 00 1.00 1.00 1.00 00 1.00 1.00 1.00 86 0 0 0			
Saturation FI Sat/Lane: Adjustment: Lanes: Final Sat.:		0. 92 0. 91 2. 00 3. 00 3502 5187	1900 1. 00 0. 00	1900 1900 19 0. 75 0. 95 0. 1. 00 0. 00 1. 1430 0 14	900 1900 1900 1900 75 1.00 1.00 1.00 00 0.00 0.00 0.00 130 0 0			
Capacity Anal Vol/Sat: Crit Moves: Green/Cycle: Volume/Cap: Delay/Veh: User DelAdj: Adj Del/Veh: LOS by Move: HCM2kAvgQ:	ysis Module: 0.00 0.13 0.16  ****  0.00 0.44 0.44  0.00 0.31 0.36  0.0 18.4 19.0  1.00 1.00 1.00  0.0 18.4 19.0  A B B  0 5	0. 28 0. 71 0. 36 0. 25 29. 2 5. 0 1. 00 1. 00 29. 2 5. 0 C A 5 4	A O	0. 02 0. 00 0. 0. 17 0. 00 0. 0. 12 0. 00 0. 35. 5 0. 0 37 1. 00 1. 00 1. 35. 5 0. 0 37 D A	06 0.00 0.00 0.00 17 0.00 0.00 0.00 36 0.00 0.00 0.00 7.7 0.0 0.0 0.0 00 1.00 1.00 1.00 7.7 0.0 0.0 0.0 D A A A			
**************************************								
Tesoro Los Angeles Refinery Year 2020 No Project PM Peak Hour								
Level Of Service Computation Report  2000 HCM Operations Method (Future Volume Alternative)  ***********************************								
Intersection	Intersection #4 Alameda Ave / I-405 NB Ramps							

Lanes:	0 (	0 2	0 1	1 0 2	0 0	0 0 0	0 0	1 0 0	0 1
Volume Module	e:								
Base Vol:	1 00	944	195	82 773	1 00	0 0	1 00	393 0	108
Growth Adj: Initial Bse:	1.00	1. 00 944	1. 00 195	1. 00 1. 00 82 773	1. 00 0	1.00 1.00	1. 00 0	1. 00 1. 00 393 0	1. 00 108
Added Vol:	0	0	0	0 0	Ö	0 0	Ŏ	0 0	0
PasserByVol:	0	0	0	0 0	0	0 0	0	0 0	0
Initial Fut:	0 1. 00	944 1. 00	195 1. 00	82 773 1.00 1.00	0 1. 00	0 0 1.00	0 1. 00	393 0 1.00 1.00	108 1. 00
User Adj: PHF Adj:		0. 96	0. 96	0. 96 0. 96	0. 96	0. 96 0. 96	0. 96	0. 96 0. 96	0. 96
PHF Volume:	0	982	203	85 804	0	0 0	0	409 0	112
Reduct Vol:	0	0	0	0 0	0	0 0	0	0 0	0
Reduced Vol: PCE Adi:	1 00	982 1. 00	203 1. 00	85 804 1.00 1.00	0 1. 00	0 0 1.00 1.00	0 1. 00	409 0 1. 00 1. 00	112 1. 00
MLF Adj:		1.00	1.00	1.00 1.00	1. 00	1.00 1.00	1.00	1.00 1.00	1.00
Fi nal Vol ume:	0	982	203	85 804	0	0 0	0	409 0	112
Saturation F	· I ow Ma	odul e							
Sat/Lane:		1900	1900	1900 1900	1900	1900 1900	1900	1900 1900	1900
Adjustment:		0. 95	0.85	0. 95 0. 95	1.00	1.00 1.00	1.00	0. 77 1. 00	0.85
Lanes: Final Sat.:		2. 00 3610	1. 00 1615	1.00 2.00 1805 3610	0. 00 0	0.00 0.00	0. 00 0	1. 00 0. 00 1461 0	1. 00 1615
Capacity Anal					0.00		0.00		0 07
Vol/Sat: Crit Moves:	0.00	0. 27 ****	0. 13	0. 05	0. 00	0.00 0.00	0. 00	0. 28 0. 00	0. 07
Green/Cycl e:		0.40	0.40	0.07 0.47	0.00	0.00 0.00	0.00	0.41 0.00	0.82
Volume/Cap: Delay/Veh:		0. 68 26. 1	0. 31 20. 9	0. 68 0. 48 59. 7 18. 4	0. 00 0. 0	0.00 0.00	0. 00 0. 0	0. 68 0. 00 27. 3 0. 0	0. 08 1. 7
User Del Adj :			1.00	1.00 1.00	1. 00	1. 00 1. 00	1. 00	1.00 1.00	1.00
Adj Del /Veh:	0.0	26. 1	20. 9	59. 7 18. 4	0.0	0.0 0.0	0.0	27. 3 0. 0	1. 7
LOS by Move:	A O	C 14	C	E B 4 9	A O	A A O O	A O	C A 11 0	Α 1
HCM2kAvgQ:			<del>4</del> *****	4 7 ******	*****	*****	****	*******	1 *****

Note: Queue reported is the number of cars per lane.

Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CA $\S$  2020 NP PM Tue Dec 2, 2014 12:05:07 Page 6-1

Tesoro Los Angeles Refinery Year 2020 No Project PM Peak Hour

Intersection #9 I-405 SB Ramps / 223rd St

Cycle (sec): 100 Critical Vol./Cap.(X): 0.514
Loss Time (sec): 16 (Y+R=4.0 sec) Average Delay (sec/veh): 19.1
Optimal Cycle: 50 Level Of Service: B

Approach: Movement:	North Bound L - T - R	L - I - R	East Bound L - T - R	
Control: Ri ghts: Mi n. Green: Lanes:	Split Phase Include 0 0 0 0 0 1! 0 0	Split Phase Include	Protected Include 0 0 0 2 0 2 1 0	Protected     Include     0    0    0     1    0    2    1   0
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:		128 2 37 1.00 1.00 1.00 128 2 37 0 0 0 0 0 0 128 2 37 1.00 1.00 1.00 128 2 37 1.00 1.00 1.00 0.95 0.95 0.95 135 2 39 0 0 0 135 2 39 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00	860 817 18 1.00 1.00 1.00 860 817 18 0 0 0 0 0 0 860 817 18 1.00 1.00 1.00 0.95 0.95 0.95 907 862 19 0 0 0 907 862 19 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00	4 355 79 1.00 1.00 1.00 4 355 79 0 0 0 0 0 4 355 79 1.00 1.00 1.00 0.95 0.95 0.95 4 374 83 0 0 0 4 374 83 1.00 1.00 1.00 1.00 1.00 1.00 1.00 4 374 83
Saturation Fl Sat/Lane: Adjustment: Lanes:		1900 1900 1900 0.95 0.86 0.86 1.00 0.05 0.95 1805 84 1547	1900 1900 1900 0. 92 0. 91 0. 91 2. 00 2. 94 0. 06 3502 5060 111	1900 1900 1900 0. 95 0. 89 0. 89 1. 00 2. 45 0. 55 1805 4128 919
	ysis Module: 0.01 0.01 0.01 0.01 0.01 0.51 0.51 0.51 66.3 66.3 66.3 1.00 1.00 1.00 66.3 66.3 66.3 E E E 1 1 1	0.07 0.03 0.03  ****  0.15 0.15 0.15  0.51 0.17 0.17  41.2 37.8 37.8  1.00 1.00 1.00  41.2 37.8 37.8  D D D  ******************************	0. 26 0. 17 0. 17  ****  0. 50 0. 67 0. 67  0. 51 0. 25 0. 25  16. 8 6. 5 6. 5  1. 00 1. 00 1. 00  16. 8 6. 5 6. 5  B A A  10 4  ***********************************	0.00 0.09 0.09 ****  0.01 0.18 0.18 0.25 0.51 0.51 57.1 37.8 37.8 1.00 1.00 1.00 57.1 37.8 37.8 E D D 0 5
HCM2kAvgQ: ********** Note: Queue i	1 1 1 *************** reported is the	4 1 1	10 4 4 **********************************	0 5 5

Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CA?

### **Traffic Impact Analysis**

YEAR 2021 WITH PROJECT



Int #: 3

North/South Street: WILMINGTON AVENUE

East/West Street: 223RD STREET

Scenario: 2021 Plus Operations

TH

LT

RT

TH

 $\mathsf{LT}$ 

RT

TH

LT

2.00

1.00

0.50

2.50

1.00

1.00

2.00

1.00

Thru Lane:	1600 vph	N-S Split Phase :	N
Left-Turn Lane:	1600 vph	E-W Split Phase:	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK I	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	1.00	327	1,600	0.117	N-S(1):	0.163
	TH	2.00	664	3,200	0.208 *	N-S(2):	0.215 *
	LT	1.00	58	1,600	0.036	E-W(1):	0.302
Westbound	RT	1.00	54	1,600	0.000	E-W(2):	0.342 *
	TH	2.00	813	3,200	0.254 *		
	LT	1.00	205	1,600	0.128	V/C:	0.557
Northbound	RT	0.50	82	800	0.000	Lost Time:	0.100
	TH	2.50	507	4,000	0.127		
	LT	1.00	11	1,600	0.007 *		
Eastbound	RT	1.00	16	1,600	0.003	ICU:	0.657
	TH	2.00	558	3,200	0.174		
	LT	1.00	140	1,600	0.088 *	LOS:	В
Peak Period:	PM PEAK F	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	1.00	204	1,600	0.000	N-S(1):	0.142
	TH	2.00	743	3,200	0.232 *	N-S(2):	0.237 *
	LT	1.00	56	1,600	0.035	E-W(1):	0.366 *
Westbound	RT	1.00	146	1,600	0.056	E-W(2):	0.264
	1				l	` ′	

353

181

127

427

8

10

811

246

3,200

1,600

800

4,000

1,600

1,600

3,200

1,600

0.110

0.000

0.107

0.001

0.154

0.005 \*

0.253 \*

0.113 \*

V/C:

ICU:

LOS:

Lost Time:

0.603

0.100

0.703

С

Northbound

Eastbound

<sup>\* =</sup> Critical Movement

Int #:

North/South Street: 223rd Street Ramp (on Alameda Street)

East/West Street: Alameda Street

Scenario: 2021 Plus Operations

Thru Lane:	1600 vph	N-S Split Phase :	N
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK I	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.258 *
	TH	3.00	1,150	4,800	0.240	N-S(2):	0.240
	LT	1.00	163	1,600	0.102 *	E-W(1):	0.113 *
Westbound	RT	1.00	122	1,600	0.000	E-W(2):	0.000
	TH	0.00	0	0	0.000		
	LT	1.00	180	1,600	0.113 *	V/C:	0.371
Northbound	RT	0.00	249	1,600	0.156 *	Lost Time:	0.100
	TH	3.00	482	3,200	0.151		
	LT	0.00	0	0	0.000		
Eastbound	RT	0.00	0	0	0.000	ICU:	0.471
	TH	0.00	0	0	0.000 *		
	LT	0.00	0	0	0.000	LOS:	Α
Peak Period:	PM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.410 *
	TH	3.00	1,005	4,800	0.209	N-S(2):	0.209
	LT	1.00	168	1,600	0.105 *	E-W(1):	0.071 *
Westbound	RT	1.00	125	1,600	0.000	E-W(2):	0.000

Approacn	iviovement	Lanes	volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.410 *
	TH	3.00	1,005	4,800	0.209	N-S(2):	0.209
	LT	1.00	168	1,600	0.105 *	E-W(1):	0.071 *
Westbound	RT	1.00	125	1,600	0.000	E-W(2):	0.000
	TH	0.00	0	0	0.000		
	LT	1.00	114	1,600	0.071 *	V/C:	0.481
Northbound	RT	0.00	473	0	0.000	Lost Time:	0.100
	TH	3.00	991	4,800	0.305 *		
	LT	0.00	0	0	0.000		
Eastbound	RT	0.00	0	0	0.000	ICU:	0.581
	TH	0.00	0	0	0.000 *		
	LT	0.00	0	0	0.000	LOS:	Α
4 0 1 8 4							

<sup>\* =</sup> Critical Movement

Int #: 6

North/South Street: Alameda Street Ramp

East/West Street: 223rd Street

Scenario: 2021 Plus Operations

Thru Lane:	1600 vph	N-S Split Phase :	N
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK I	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.090 *
	TH	0.00	0	0	0.000	N-S(2):	0.083
	LT	0.00	0	0	0.000 *	E-W(1):	0.165 *
Westbound	RT	0.00	0	0	0.000	E-W(2):	0.145
	TH	3.00	765	5,280	0.145		
	LT	2.00	228	3,168	0.072 *	V/C:	0.255
Northbound	RT	1.00	273	1,760	0.090 *	Lost Time:	0.100
	TH	0.00	0	0	0.000		
	LT	1.00	146	1,760	0.083		
Eastbound	RT	0.00	82	0	0.000	ICU:	0.355
	TH	3.00	408	5,280	0.093 *		
	LT	0.00	0	0	0.000	LOS:	Α
Peak Period:	PM PEAK H	IOUR	<u> </u>				·
Annroach	Movement	Lange	Volume	Canacity	V/C	ΙΟΙΙ ΔΝΙΔ	I VSIS

Peak Period:	PM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.261 *
	TH	0.00	0	0	0.000	N-S(2):	0.056
	LT	0.00	0	0	0.000 *	E-W(1):	0.286 *
Westbound	RT	0.00	0	0	0.000	E-W(2):	0.055
	TH	3.00	290	5,280	0.055		
	LT	2.00	94	3,168	0.030 *	V/C:	0.547
Northbound	RT	1.00	507	1,760	0.261 *	Lost Time:	0.100
	TH	0.00	0	0	0.000		
	LT	1.00	99	1,760	0.056		
Eastbound	RT	0.00	141	0	0.000	ICU:	0.647
	TH	3.00	1,212	5,280	0.256 *		
* 0.00	LT	0.00	0	0	0.000	LOS:	В

<sup>\* =</sup> Critical Movement

North/South Street: ALAMEDA STREET

East/West Street: SEPULVEDA BOULEVARD-ALAMEDA RAMF

Scenario: **2021 Plus Operations** 

Thru Lane:	1600 vph	N-S Split Phase :	N
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.250 *
	TH	3.00	785	4,800	0.164	N-S(2):	0.164
	LT	1.00	236	1,600	0.148 *	E-W(1):	0.031 *
Westbound	RT	2.00	204	3,200	0.000	E-W(2):	0.000
	TH	0.00	0	0	0.000		
	LT	1.00	50	1,600	0.031 *	V/C:	0.281
Northbound	RT	0.00	51	0	0.000	Lost Time:	0.100
	TH	3.00	438	4,800	0.102 *		
	LT	0.00	0	0	0.000		
Eastbound	RT	0.00	0	0	0.000	ICU:	0.381
	TH	0.00	0	0	0.000 *		
	LT	0.00	0	0	0.000	LOS:	Α
							·

Peak Period:	PM PEAK H	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.390 *
	TH	3.00	877	4,800	0.183	N-S(2):	0.183
	LT	1.00	257	1,600	0.161 *	E-W(1):	0.059 *
Westbound	RT	2.00	418	3,200	0.050	E-W(2):	0.050
	TH	0.00	0	0	0.000		
	LT	1.00	95	1,600	0.059 *	V/C:	0.449
Northbound	RT	0.00	85	0	0.000	Lost Time:	0.100
	TH	3.00	1,012	4,800	0.229 *		
	LT	0.00	0	0	0.000		
Eastbound	RT	0.00	0	0	0.000	ICU:	0.549
	TH	0.00	0	0	0.000 *		
	LT	0.00	0	0	0.000	LOS:	Α

<sup>\* =</sup> Critical Movement

North/South Street: SEPULVEDA BOULEVARD-ALAMEDA RAMF

East/West Street: **SEPULVEDA BOULEVARD** 

Scenario: 2021 Plus Operations

Thru Lane:	1600 vph	N-S Split Phase :	Υ
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK I	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	1.00	148	1,600	0.016	N-S(1):	0.056 *
	TH	0.13	9	210	0.043	N-S(2):	0.000
	LT	1.87	128	2,691	0.048 *	E-W(1):	0.234
Westbound	RT	1.00	100	1,600	0.020	E-W(2):	0.267 *
	TH	2.00	610	3,200	0.191 *		
	LT	1.00	8	1,600	0.005	V/C:	0.323
Northbound	RT	0.00	4	0	0.000	Lost Time:	0.100
	TH	2.00	19	3,200	0.008 *		
	LT	0.00	2	1,600	0.001		
Eastbound	RT	1.00	6	1,600	0.003	ICU:	0.423
	TH	1.00	366	1,600	0.229		
	LT	1.00	122	1,600	0.076 *	LOS:	Α
Peak Period:	PM PEAK I	HOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	1.00	177	1,600	0.000	N-S(1):	0.058 *
	TH	0.17	12	269	0.045	N-S(2):	0.000
	1 17	4 00	101	2 620	0.050 *	E \\//4\.	0.604 *

Peak Period:	PM PEAK HOUR						
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	1.00	177	1,600	0.000	N-S(1):	0.058 *
	TH	0.17	12	269	0.045	N-S(2):	0.000
	LT	1.83	131	2,638	0.050 *	E-W(1):	0.601 *
Westbound	RT	1.00	244	1,600	0.108	E-W(2):	0.320
	TH	2.00	549	3,200	0.172		
	LT	1.00	2	1,600	0.001 *	V/C:	0.659
Northbound	RT	0.00	9	0	0.000	Lost Time:	0.100
	TH	2.00	13	3,200	0.008 *		
	LT	0.00	4	1,600	0.003		
Eastbound	RT	1.00	1	1,600	0.000	ICU:	0.759
	TH	1.00	960	1,600	0.600 *		
	LT	1.00	236	1,600	0.148	LOS:	С

<sup>\* =</sup> Critical Movement

Project: Te

North/South Street: TERMINAL ISLAND FREEWAY (SR-103)

East/West Street: WILLOW STREET

Scenario: 2021 Plus Operations

Thru Lane:	1600 vph	N-S Split Phase :	Υ
Left-Turn Lane:	1600 vph	E-W Split Phase :	Ν
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	Peak Period: AM PEAK HOUR							
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS	
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.034 *	
	TH	1.00	0	1,600	0.000	N-S(2):	0.000	
	LT	0.00	0	0	0.000 *	E-W(1):	0.186	
Westbound	RT	0.00	16	0	0.000	E-W(2):	0.263 *	
	TH	2.00	815	3,200	0.260 *			
	LT	2.00	242	2,880	0.084	V/C:	0.297	
Northbound	RT	2.00	101	3,200	0.000	Lost Time:	0.100	
	TH	0.00	0	0	0.000			
	LT	2.00	99	2,880	0.034 *			
Eastbound	RT	1.00	187	1,600	0.086	ICU:	0.397	
	TH	2.00	326	3,200	0.102			
	LT	1.00	4	1,600	0.003 *	LOS:	Α	
Peak Period:	PM PEAK H	IOUR						
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS	
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.111 *	

Peak Period:	PM PEAK F	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	0	0	0.000	N-S(1):	0.111 *
	TH	1.00	0	1,600	0.000	N-S(2):	0.000
	LT	0.00	0	0	0.000 *	E-W(1):	0.380 *
Westbound	RT	0.00	1	0	0.000	E-W(2):	0.137
	TH	2.00	437	3,200	0.137		
	LT	2.00	171	2,880	0.059 *	V/C:	0.491
Northbound	RT	2.00	254	3,200	0.053	Lost Time:	0.100
	TH	0.00	0	0	0.000		
	LT	2.00	319	2,880	0.111 *		
Eastbound	RT	1.00	262	1,600	0.064	ICU:	0.591
	TH	2.00	1,026	3,200	0.321 *		
	LT	1.00	0	1,600	0.000	LOS:	Α

<sup>\* =</sup> Critical Movement

Int #: 11

North/South Street: SANTA FE AVE

East/West Street: SEPULVEDA BOULEVARD

ΤH

LT

RT

ΤH

LT

2.00

1.00

0.00

2.00

1.00

Scenario: 2021 Plus Operations

Thru Lane:	1600 vph	N-S Split Phase :	Υ
Left-Turn Lane:	1600 vph	E-W Split Phase :	N
Dual LT Penalty:	10 %	Lost Time (% of cycle):	10

Peak Period:	AM PEAK H	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	135	0	0.000	N-S(1):	0.209 *
	TH	2.00	264	3,200	0.125 *	N-S(2):	0.000
	LT	2.00	156	2,880	0.054	E-W(1):	0.204
Westbound	RT	0.00	111	0	0.000	E-W(2):	0.328 *
	TH	2.00	788	3,200	0.281 *		
	LT	2.00	163	2,880	0.057	V/C:	0.537
Northbound	RT	0.00	82	0	0.000	Lost Time:	0.100
	TH	2.00	188	3,200	0.084 *		
	LT	1.00	78	1,600	0.049		
Eastbound	RT	0.00	33	0	0.000	ICU:	0.637
	TH	2.00	438	3,200	0.147		
	LT	1.00	75	1,600	0.047 *	LOS:	В
Peak Period:	PM PEAK F	IOUR					
Approach	Movement	Lanes	Volume	Capacity	V/C	ICU ANA	LYSIS
Southbound	RT	0.00	64	0	0.000	N-S(1):	0.321 *
	TH	2.00	319	3,200	0.120 *	N-S(2):	0.000
	LT	2.00	339	2,880	0.118	E-W(1):	0.378 *
Westbound	RT	0.00	153	0	0.000	E-W(2):	0.292
	TH	2.00	497	3,200	0.203		
	LT	2.00	140	2,880	0.049 *	V/C:	0.699
Northbound	RT	0.00	205	0	0.000	Lost Time:	0.100

438

84

44

1,008

143

3,200

1,600

0

3,200

1,600

0.201 \*

0.053

0.000

0.089

0.329 \*

ICU:

LOS:

0.799

С

Eastbound

<sup>\* =</sup> Critical Movement



# Appendix E Level of Service Workheet (Circular 212 Method)



Alameda Street Ramp

I/S #:

PROJECT TITLE: ICTF Modification and Expansion Project EIR

North-South Street: 223rd Street (on 223rd East-West Street:

Scenario: CEQA Baseline

Count Date: Analyst: keris, Inc. Date: 7/22/2014

AM PEAK HOUR MD PEAK HOUR PM PEAK HOUR								R		
	No. of Phases			3			3			3
	Opposed Ø'ing: N/S-1, E/W-2 or Both-3?			2			2			2
F	Right Turns: FREE-1, NRTOR-2 or OLA-3?	NB 3 EB 0	SB WB	0	NB 3 EB 0	SB NB	0	NB 0 EB 3	SB WB	0
	ATSAC-1 or ATSAC+ATCS-2?	LB == 0	WD	2	LB 0	,VD	2	LB 3	WB	2
	Override Capacity			1500			1500			1500
	MOVEMENT		No. of	Lane		No. of	Lane		No. of	Lane
	MOVEMENT	Volume	Lanes	Volume	Volume	Lanes	Volume	Volume	Lanes	Volume
	↑ Left	146	1	146	0	1	60	99	1	99
Ĭ	← Left-Through		0			0			0	
o	∱ Through	0	0	0	0	0	0	0	0	0
묖	→ Through-Right		0			0			0	
RT	<mark> → Right</mark>	273	1	148	0	1	403	507	1	455
NORTHBOUND	← Left-Through-Right		0			0			0	
_	Left-Right		0			0			0	
									_	
0	→ Left	0	0	0	0	0	0	0	0	0
Į	├─ Left-Through		0			0			0	
o l	Through	0	0	0	0	0	0	0	0	0
甲	← Through-Right		0			0			0	
5	-√ Right	0	0	0	0	0	0	0	0	0
SOUTHBOUND	← Left-Through-Right		0			0			0	
0,	人, Left-Right		0			0			0	
					,					
0	Left	0	0	0	0	0	0	0	0	0
ΙZ	→ Left-Through		0		_	0			0	
EASTBOUND	→ Through	408	2	163	0	2	380	1,212	2	451
TB	→ Through-Right → Right	00	1	00	•	1	4-		1	
AS	1 Kight	82	0	82	0	0	45	141	0	141
E,	Left-Through-Right		0 0			0			0 0	
	- ✓ Left-Right	I	U			0			U	
	√ Left	228	2	125	0	2	77	94	2	52
₽	γ Left	220	0	123		0	11	94	0	52
WESTBOUND	← Through	765	3	255	0	3	82	290	3	97
80	← Through-Right	, 00	0	233	I	0	02	230	0	31
ST	Right	0	0	0	0	0	0	0	0	0
VE	Left-Through-Right	Ĭ	0	· ·	Ĭ	0	ŭ		0	J
>	├ Left-Right		0			0			0	
	-	۸	lorth-South:	148	North-	-South:	403	٨	North-South:	455
	CRITICAL VOLUMES	ĺ	East-West:	418	Eas	t-West:	462	1	East-West:	548
			SUM:	566		SUM:	865		SUM:	1003
	VOLUME/CAPACITY (V/C) RATIO:	ĺ		0.397			0.577			0.704
V/	C LESS ATSAC/ATCS ADJUSTMENT:	ĺ		0.297			0.477			0.604
	LEVEL OF SERVICE (LOS):			A			A			В
		l								

Version: 1i Beta; 8/4/2011

2020+0ps\_AM. out Tue Dec 2, 2014 13: 55: 36

2020 Ops AM Page 1-1

Tesoro Los Angeles Refinery Year 2020 With Project Operations AM Peak Hour

Scenario Report

Scenari o: 2020 Ops AM

2020+0ps-AM 2020 AM Command: Vol ume: Geometry: Impact Fee: 2017

Default Impact Fee

Const-AM

Trip Generation: Trip Distribution: Default Trip Distribution Default Path

Paths: Default Route Routes: Configuration: 2020+0ps-AM

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> Tesoro Los Angeles Refinery Page 1

#### 2020+0ps\_AM.out Year 2020 With Project Operations AM Peak Hour

Impact Analysis Report Level Of Service

Ιn	tersecti on		Base Del/ V/		Future Del/ V/	Change i n
#	1 Wilmington Ave / I-405 NB Ramp		S Veh C 21.7 0.512		S Veh C 21.7 0.512	+ 0.001 D/V
#	2 Wilmington Ave / I-405 SB Ramp	С	21.8 0.364	С	21. 8 0. 365	+ 0.026 D/V
#	4 Alameda Ave / I-405 NB Ramps	С	23. 4 0. 687	С	23. 4 0. 687	+ 0.029 D/V
#	9 I-405 SB Ramps / 223rd St	С	23. 5 0. 484	С	23. 5 0. 484	+ 0.012 D/V

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Tesoro Los Angeles Refinery Year 2020 With Project Operations AM Peak Hour

AM Peak Hour

### 2020+Ops\_AM.out Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative)

Cycle (sec): 100 Critical Vol./Cap. (X): 0.512
Loss Time (sec): 8 (Y+R=4.0 sec) Average Delay (sec/veh): 21.7
Optimal Cycle: 39 Level Of Service: C Approach: North Bound South Bound East Bound West Bound Movement: L - T - R Volume Modul e: Saturation Flow Module: Vol/Sat: 0.00 0.11 0.02 0.00 0.09 0.00 0.00 0.00 0.36 0.00 0.34 Crit Moves: Green/Cycle: 0.00 0.33 0.33 0.00 0.14 0.00 0.00 0.00 0.00 0.59 0.00 0.59 Volume/Cap: 0.00 0.35 0.07 0.00 0.61 0.00 0.00 0.00 0.00 0.60 0.00 0.58 Delay/Veh: 0.0 25.4 23.0 0.0 41.7 0.0 0.0 0.0 0.0 0.0 14.0 0.0 13.8 Note: Queue reported is the number of cars per lane. Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CA $^\circ$ 2020 Ops AM Tue Dec 2, 2014 13:55:36 Page 4-1 Tesoro Los Angeles Refinery Year 2020 With Project Operations AM Peak Hour Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative)

Page 3

### 2020+0ps\_AM. out

Intersection #2 Wilmington Ave / I-405 SB Ramps					
Optimal Cycl	100 ec): 12 (Y+F e: 40	R=4.0 sec) Averag	cal Vol./Cap.(X): ge Delay (sec/veh) Of Service: ************************************	0. 365 : 21. 8 C	
Approach: Movement:	North Bound L - T - R	South Bound L - T - R	East Bound L - T - R	West Bound L - T - R	
Control: Rights: Min. Green: Lanes:	Permitted     Include     0    0    0     0    0    2    1   1	Protected Include 0 0 0 2 0 3 0 0	Permitted     Include     0     0     0     0     1     0     1     0	Permitted     Include     0    0    0	
Volume Modul Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:	1	144 928 0 1.00 1.00 1.00 144 928 0 0 0 0 0 0 144 928 0 1.00 1.00 1.00 0.95 0.95 0.95 152 981 0 0 0 0 152 981 0 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00	126	0 0 0 0 1.00 1.00 0 0 0 0 0 0 0 0 0 0 0	
Saturation F Sat/Lane: Adjustment: Lanes: Final Sat.:	1900 1900 1900 1.00 0.84 0.84 0.00 2.00 2.00 0 3178 3178	1900 1900 1900 0. 92 0. 91 1. 00 2. 00 3. 00 0. 00 3502 5187 0	1900 1900 1900 0. 71 0. 95 0. 71 1. 00 0. 00 1. 00 1353 0 1353	1900 1900 1900 1.00 1.00 1.00 0.00 0.00 0.00 0 0 0	
Vol /Sat: Cri t Moves: Green/Cycl e: Vol ume/Cap: Del ay/Veh: User Del Adj: Adj Del /Veh: LOS by Move: HCM2kAvgO:	0.00 0.48 0.57 0.0 34.7 35.8 1.00 1.00 1.00 0.0 34.7 35.8 A C D	0. 04 0. 19 0. 00  ****  0. 39 0. 61 0. 00  0. 11 0. 31 0. 00  19. 4 9. 6 0. 0  1. 00 1. 00 1. 00  19. 4 9. 6 0. 0  B A A  2 5 0	0. 10 0. 00 0. 13  ****  0. 27 0. 00 0. 27  0. 36 0. 00 0. 48  29. 5 0. 0 30. 9  1. 00 1. 00 1. 00  29. 5 0. 0 30. 9  C A C  4 0 5	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00	
Note: Queue reported is the number of cars per Iane. ************************************					
Tesoro Los Angeles Refinery Year 2020 With Project Operations AM Peak Hour					
Level Of Service Computation Report  2000 HCM Operations Method (Future Volume Alternative)  ***********************************					
Intersection	#4 Alameda Ave /	/ I -405 NB Ramps	******	*****	
Cycle (sec):	100	Critic Page 4	cal Vol./Cap.(X):	0. 687	

2020+0ps AM. out

Loss Time (sec): 12 (Y+R=4.0 sec) Average Delay (sec/veh): 23.4 Optimal Cycle: 58 Level Of Service: C Saturation Flow Module: Capacity Analysis Module: Vol /Sat: 0.00 0.17 0.03 0.03 0.26 0.00 0.00 0.00 0.00 0.35 0.00 0.21 Crit Moves: \*\*\*\* Note: Queue reported is the number of cars per lane. Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CA $\S$  2020 Ops AM Tue Dec 2, 2014 13:55:36 Page 6-1 Tesoro Los Angeles Refinery Year 2020 With Project Operations AM Peak Hour Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative) Intersection #9 I-405 SB Ramps / 223rd St \* 

Approach: Movement:	North Bound L - T - R	L - I - R		
Control: Rights: Min. Green: Lanes:	Split Phase Include 0 0 0 0 0 1! 0 0	Split Phase Include	Protected Include 0 0 0 2 0 2 1 0	Protected Include 0 0 0 1 0 2 1 0
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:	e:  1	56 0 126 1.00 1.00 1.00 56 0 126 0 0 0 0 0 0 56 0 126 1.00 1.00 1.00 0.88 0.88 0.88 64 0 143 0 0 0 64 0 143 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00	362 309 4 1.00 1.00 1.00 362 309 4 1 0 0 0 0 0 363 309 4 1.00 1.00 1.00 0.88 0.88 0.88 412 351 5 0 0 0 412 351 5 1.00 1.00 1.00 1.00 1.00 412 351 5	3 857 33 1.00 1.00 1.00 3 857 33 0 0 0 0 0 0 3 857 33 1.00 1.00 1.00 0.88 0.88 0.88 3 973 37 0 0 0 3 973 37 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00 3 973 37
Saturation F Sat/Lane: Adjustment: Lanes: Final Sat.:		1900 1900 1900 0.95 1.00 0.85 1.00 0.00 1.00 1805 0 1615	1900 1900 1900 0. 92 0. 91 0. 91 2. 00 2. 96 0. 04 3502 5110 66	1900 1900 1900 0. 95 0. 90 0. 90 1. 00 2. 89 0. 11 1805 4965 191
Capacity Anal Vol/Sat: Crit Moves: Green/Cycle: Volume/Cap: Delay/Veh: User DelAdj: Adj Del/Veh: LOS by Move: HCM2kAvgQ: *******	ysis Module: 0.00 0.00 0.00 ****  0.01 0.01 0.01 0.48 0.48 0.48 70.1 70.1 70.1 1.00 1.00 1.00 70.1 70.1 70.1 E E E 1 1 1 **************************	0.04 0.00 0.09  ****  0.18 0.00 0.18  0.19 0.00 0.48  34.9 0.0 37.9  1.00 1.00 1.00  34.9 0.0 37.9  C A D  2 0 4  **********************************	0. 12 0. 07 0. 07  ****  0. 24 0. 63 0. 63  0. 48 0. 11 0. 11  32. 9 7. 4 7. 4  1. 00 1. 00 1. 00  32. 9 7. 4 7. 4  C A A  6 2  *********************************	0. 00 0. 20 0. 20 0. 02 0. 40 0. 40 0. 11 0. 48 0. 48 49. 9 22. 2 22. 2 1. 00 1. 00 1. 00 49. 9 22. 2 22. 2 D C C
Sat/Lane: Adj ustment: Lanes: Final Sat.: Capacity Anal Vol/Sat: Crit Moves: Green/Cycle: Volume/Cap: Del ay/Veh: User Del Adj: Adj Del /Veh: LOS by Move: HCM2kAvgQ: *************** Note: Queue	1900 1900 1900 0.90 0.90 0.90 0.14 0.14 0.72 244 244 1218	0.95 1.00 0.85 1.00 0.00 1.00 1805 0 1615 	0. 92 0. 91 0. 91 2. 00 2. 96 0. 04 3502 5110 66     0. 12 0. 07 0. 07  **** 0. 24 0. 63 0. 63 0. 48 0. 11 0. 11 32. 9 7. 4 7. 4 1. 00 1. 00 1. 00 32. 9 7. 4 7. 4 C A A 6 2  **********************************	0. 95 0. 90 0. 90 1. 00 2. 89 0. 11 1805 4965 191    0. 00 0. 20 0. 20 0. 02 0. 40 0. 40 0. 11 0. 48 0. 48 49. 9 22. 2 22. 2 1. 00 1. 00 1. 00 49. 9 22. 2 22. 2 D C 0 9 9 *********************************

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2020+0ps\_PM. out

2020 Ops PM Tue Dec 2, 2014 13:55:46 Page 1-1

Tesoro Los Angeles Refinery Year 2020 With Project Operations PM Peak Hour

Scenario Report

2020 Ops PM Scenari o:

2020+0ps-PM 2020 PM Command: Vol ume: Geometry: Impact Fee: 2017

Default Impact Fee Const-PM

Trip Generation: Trip Distribution: Default Trip Distribution Default Path

Paths: Default Route Routes: Configuration: 2020+0ps-PM

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> Tesoro Los Angeles Refinery Page 1

#### 2020+0ps\_PM.out Year 2020 With Project Operations PM Peak Hour

Impact Analysis Report

Impact	Anal	ysi s	Report
	el Of		

Intersection			Base Del/V/		Future Del/ V/	Change i n	
#	1 Wilmington Ave / I-405 NB Ramp		S Veh C 18.4 0.420		S Veh C 18. 4 0. 420	+ 0.001 D/V	
#	2 Wilmington Ave / I-405 SB Ramp	В	15. 7 0. 362	В	15. 8 0. 363	+ 0.063 D/V	
#	4 Alameda Ave / I-405 NB Ramps	С	23. 5 0. 681	С	23. 6 0. 682	+ 0.038 D/V	
#	9 I-405 SB Ramps / 223rd St	В	19. 1 0. 514	В	19. 1 0. 514	-0.002 D/V	

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Tesoro Los Angeles Refinery Year 2020 With Project Operations PM Peak Hour

PM Peak Hou

## 2020+Ops\_PM.out Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative)

2000 HCM Operations Method (Future Volume Alternative)											
Intersection #1 Wilmington Ave / I-405 NB Ramps											
Cycle (sec): 100								20 . 4			
Approach: Movement:	North Bo L - T	ound - R	Sou L -	uth Bo - T	ound - R	Ea L -	ast Bo - T	ound - R	We L -	st Bo T	und
Control: Rights: Min. Green: Lanes:	Protect Inclu 0 0 0 0 2	ted ' ude 0	· F	Permit Inclu 0	tted ' ude 0	0 0	Permit Inclu 0 0	ted	' P	ermit Inclu 0	ted
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:	0 289 1. 00 1. 00 0 289 0 0 0 289 1. 00 1. 00 0. 95 0. 95 0 305 0 0 0 305 1. 00 1. 00 1. 00 1. 00 1. 00 1. 00 0 305	155 1.00 155 1 0 156 1.00 0.95 164 1.00 1.00	0 0 0 1.00 0.95 0 0 1.00 1.00		1. 00 0 0 0 0 1. 00 0. 95 0 0 0 1. 00 1. 00	1. 00 0 0 0 0 0 0 1. 00 0. 95 0 0 1. 00	1. 00 0 0 0 0 1. 00 0. 95 0 0 1. 00 1. 00	1. 00 0 0 0 0 0 1. 00 0. 95 0 0 0 1. 00 1. 00	438 1.00 438 0 0 438 1.00 0.95 462 1.00 1.00 462	0 0 0 0 1. 00 0. 95 0 0 0 1. 00 1. 00	309 1.00 309 0 0 309 1.00 0.95 326 1.00 1.00 326
Saturation FI Sat/Lane: Adjustment: Lanes: Final Sat.:	1	1900 0. 85 1. 00 1615	1900 1.00 0.00 0	0. 91 3. 00 5187	1900 1.00 0.00 0	1900 1.00	1900 1.00 0.00 0	1900 1. 00 0. 00 0	1900 0. 59 2. 00 2234	1900 1.00 0.00	1900 0. 85 1. 00 1615
Capacity Anal Vol/Sat: Crit Moves: Green/Cycle: Volume/Cap: Del ay/Veh: User Del Adj: Adj Del /Veh:	ysis Modul 0.00 0.08 ****	e: 0. 10 0. 43 0. 24 18. 4 1. 00	0. 00 0. 00 0. 00 0. 0 1. 00	0. 18 **** 0. 43 0. 42 20. 1	0. 00 0. 00 0. 00 0. 00 1. 00 0. 0	0. 00 0. 00 0. 00 0. 0 1. 00	0. 00 0. 00 0. 00 0. 0 1. 00 0. 0	0. 00 0. 00 0. 00 0. 0 1. 00	0. 21 **** 0. 49 0. 42	0. 00 0. 00 0. 00 0. 0 1. 00	0. 20 0. 49 0. 41 16. 5 1. 00 16. 5
LOS by Move: HCM2kAvgQ:	A B 0 3	В 3	A O	C 7	A O	A O	A O	A O	В 5	A O	В 6
Note: Queue reported is the number of cars per lane.											
Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CA♀         2020 Ops PM       Tue Dec 2, 2014 13:55:46       Page 4-1											
Tesoro Los Angeles Refinery Year 2020 With Project Operations PM Peak Hour											
Level Of Service Computation Report  2000 HCM Operations Method (Future Volume Alternative)  ***********************************											
Dago 2											

Page 3

### 2020+0ps\_PM. out

Intersection #2 Wilmington Ave / I-405 SB Ramps								
Cycle (sec): 100								
Approach: Movement:	Approach: North Bound		East Bound L - T - R	West Bound L - T - R				
Control: Rights: Min. Green: Lanes:	Permitted     Include     0    0    0     0    0    1	Protected Include 0 0 0 2 0 3 0 0	'' Permitted Include	Permitted Include 0 0 0 0 0 0 0				
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: MLF Adj: Final Volume:		345 910 0 1.00 1.00 1.00 345 910 0 0 0 0 0 0 0 345 910 0 345 910 0 1.00 1.00 1.00 0.98 0.98 0.98 353 930 0 0 0 0 353 930 0 1.00 1.00 1.00 1.00 1.00 1.00 353 930 0	27 0 84 1.00 1.00 1.00 27 0 84 0 0 1 0 0 0 27 0 85 1.00 1.00 1.00 0.98 0.98 0.98 28 0 87 0 0 0 28 0 87 1.00 1.00 1.00 1.00 1.00 1.00 1.00 387	0 0 0 1.00 1.00 1.00 0 0 0 0 0 0 0 0 0 0 0 0 1.00 1.00 1.00 0.98 0.98 0.98 0 0 0 0 0 0 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00				
Saturation F Sat/Lane: Adjustment: Lanes: Final Sat.:	I ow Modul e: 1900 1900 1900 1.00 0.84 0.84 0.00 2.00 2.00 0 3178 3178	1900 1900 1900 0. 92 0. 91 1. 00 2. 00 3. 00 0. 00 3502 5187 0	1900 1900 1900 0. 75 0. 95 0. 75 1. 00 0. 00 1. 00 1431 0 1431	1900 1900 1900 1.00 1.00 1.00 0.00 0.00 0.00 0 0 0				
Vol /Sat: Cri t Moves: Green/Cycl e: Vol ume/Cap: Del ay/Veh: User Del Adj: Adj Del /Veh: LOS by Move:	0.00 0.31 0.36 0.0 18.5 19.1 1.00 1.00 1.00 0.0 18.5 19.1 A B B			0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00				
HCM2kAvgQ: 0 5 6 5 4 0 1 0 3 0 0 0 *************************								
Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CA♀ 2020 Ops PM Tue Dec 2, 2014 13:55:46 Page 5-1								
Tesoro Los Angeles Refinery Year 2020 With Project Operations PM Peak Hour								
Level Of Service Computation Report  2000 HCM Operations Method (Future Volume Alternative)  ***********************************								
Intersection #4 Alameda Ave / I-405 NB Ramps								
Cycle (sec): 100 Critical Vol./Cap.(X): 0.682 Page 4								

2020+0ps\_PM. out

Loss Time (sec): 12 (Y+R=4.0 sec) Average Delay (sec/veh): 23.6 Optimal Cycle: 57 Level Of Service: C 

 Approach:
 North Bound
 South Bound
 East Bound
 West Bound

 Movement:
 L - T - R
 L - T - R
 L - T - R
 L - T - R

 Control:
 Protected
 Protected
 Protected
 Permitted

 Rights:
 Include
 Include
 Include

 Min. Green:
 0 0 0 0 0 0 0 0 0 0 0 0 0 0
 0 0 0 0 0 0 0

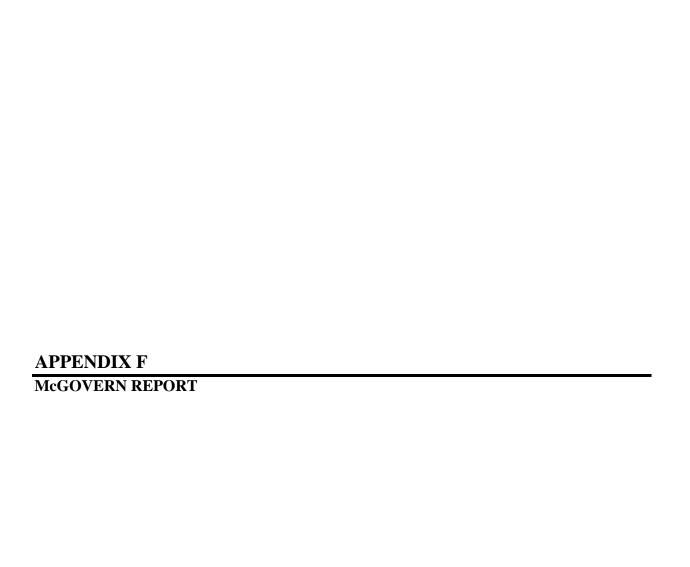
 Lanes:
 0 0 2 0 1 1 0 2 0 0 0 0 0 0 0 0 0 0
 1 0 0 0 1

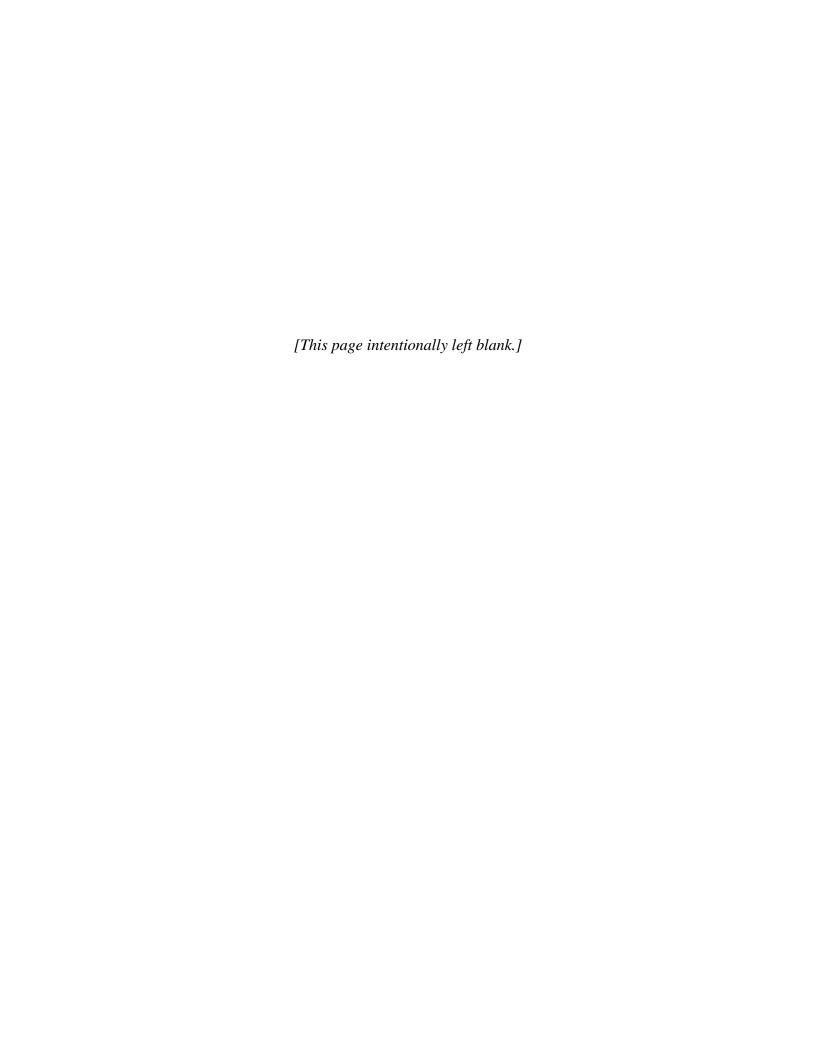
 Volume Module:

 -----||-----||-----||------| Saturation Flow Module: Capacity Analysis Module: Vol /Sat: 0.00 0.27 0.13 0.05 0.22 0.00 0.00 0.00 0.00 0.28 0.00 0.07 Crit Moves: \* Note: Queue reported is the number of cars per lane. Traffix 7.9.0415 (c) 2007 Dowling Assoc. Licensed to MMA, LONG BEACH, CA $\S$  2020 Ops PM Tue Dec 2, 2014 13:55:46 Page 6-1 Tesoro Los Angeles Refinery Year 2020 With Project Operations PM Peak Hour Level Of Service Computation Report 2000 HCM Operations Method (Future Volume Alternative) Intersection #9 I-405 SB Ramps / 223rd St Cycle (sec): 100 Critical Vol./Cap.(X): 0.514
Loss Time (sec): 16 (Y+R=4.0 sec) Average Delay (sec/veh): 19.1
Optimal Cycle: 50 Level Of Service: B

Approach:	North Bound		2020+0ps_PM.out South Bound East Bound				West Bound		
Movement:	L - T - I		L - T - R		- R	_ L - T - R			
Control: Rights: Min. Green: Lanes:	Split Phase Include 0 0	Split I Incl 0 0 ( ) 1 0 0	Phase Lude D 0	Protect Inclu 0 0 2 0 2	ed de 0	Protect Inclu 0 0 1 0 2	ed de 0		
Volume Module Base Vol: Growth Adj: Initial Bse: Added Vol: PasserByVol: Initial Fut: User Adj: PHF Adj: PHF Volume: Reduct Vol: Reduced Vol: PCE Adj: Final Volume:	1	3 128 2 00 1.00 1.00 3 128 2 0 0 0 0 0 0 3 128 2 00 1.00 1.00 25 0.95 0.95 3 135 2 0 0 0 3 135 2 0 1.00 1.00 1.00 1.00	2 37 0 0 0 0 2 37 0 1.00 5 0.95 2 39 0 0 2 39 0 1.00	860 817 1.00 1.00 860 817 1 0 0 0 861 817 1.00 1.00 0.95 0.95 908 862 0 0 908 862 1.00 1.00 1.00 1.00 908 862	18 1. 00 18 0 0 18 1. 00 0. 95 19 0 1. 00 1. 00	4 355 1.00 1.00 4 355 0 0 0 0 4 355 1.00 1.00 0.95 0.95 4 374 0 0 4 374 1.00 1.00 1.00 1.00 4 374	79 1. 00 79 0 0 79 1. 00 0. 95 83 0 1. 00 1. 00		
Saturation F Sat/Lane: Adjustment: Lanes: Final Sat.:	l ow Modul e: 1900 1900 190 0. 95 0. 95 0. 0 0. 25 0. 50 0. 2 453 907 4	00 1900 1900 95 0.95 0.86 25 1.00 0.05 33 1805 84	6 0.86 5 0.95 4 1547	1900 1900 0. 92 0. 91 2. 00 2. 94 3502 5060	1900 0. 91 0. 06 111	1900 1900 0. 95 0. 89 1. 00 2. 45 1805 4128	1900 0. 89 0. 55 919		
Capacity Anal Vol/Sat: Crit Moves: Green/Cycle: Volume/Cap: Delay/Veh: User DelAdj: Adj Del/Veh: LOS by Move: HCM2kAvqQ:	ysis Modul e: 0.01 0.01 0.0 **** 0.01 0.01 0.0 0.51 0.51 0.9 66.4 66.4 66 1.00 1.00 1.0 66.4 66.4 66	01 0. 07 0. 03 **** 01 0. 15 0. 19 05 0. 51 0. 17 04 41. 2 37. 8 00 1. 00 1. 00 04 41. 2 37. 8 05 0 0 0 0	3 0.03 5 0.15 7 0.17 8 37.8 0 1.00 8 37.8 D	0. 26 0. 17 **** 0. 50 0. 67 0. 51 0. 25 16. 8 6. 5 1. 00 1. 00 16. 8 6. 5 B A 10 4	0. 17 0. 67 0. 25 6. 5 1. 00 6. 5 A	0. 00 0. 09 **** 0. 01 0. 18 0. 25 0. 51 57. 1 37. 8 1. 00 1. 00 57. 1 37. 8 E D 0 5	0. 09 0. 18 0. 51 37. 8 1. 00 37. 8 D		
Note: Queue reported is the number of cars per lane.									

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# SJMcGovern Report for South Coast Air Quality Management District Tesoro Los Angeles Refinery Integration and Compliance Project

By: Dr. Stephen J McGovern, PE Date: October 12, 2015 [This page intentionally left blank.]

# Appendix F

# Contents

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l.		o What Extent Will the LARIC Project Change the Quality of Crudes Delivered to the efinery?	5
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	C.	What Crudes Will be Delivered to the Los Angeles Refinery as a Result of the LARIC Project?	14
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Ш	W	Vhat Information Must Tesoro Keep Confidential?	. 25

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I have been retained by the South Coast Air Quality Management District (SCAQMD) in connection with the SCAQMD's review of the Tesoro Los Angeles Refinery Integration and Compliance Project (the LARIC project) under the California Environmental Quality Act.

I have worked in and around the petroleum refining and/or renewable fuels industries for over 40 years. I have a Doctorate in Chemical Engineering from Princeton University and am a licensed Professional Engineer in New Jersey. I have recently served on two different National Research Council Committees regarding conventional and alternative fuels. I teach industry recognized courses on various aspects of refining technology. My Curriculum Vitae is attached as Appendix A.

The SCAQMD is preparing an Environmental Impact Report (EIR) for the proposed Tesoro Los Angeles Refinery Integration and Compliance (LARIC) Project at the Tesoro Los Angeles Refinery pursuant to the California Environmental Quality Act (CEQA) and has asked me to consider the following specific questions posed by SCAQMD as well as other issues as they may arise:

- 1. Does the proposed LARIC Project provide the ability to change the slate of crude oil that could be delivered and processed at the Tesoro Los Angeles Refinery?
- 2. If so, how would those qualities change and what effect could they have in the blending and crude processes (even if the permits for those processes are not changing)? Would the crudes be significantly heavier (have lower American Petroleum Institute (API) gravities) and/or contain more sulfur and be more acidic than the crudes they would replace? Would the crudes delivered to the Tesoro Los Angeles Refinery be significantly lighter and/or contain more volatile organic hydrocarbons than the crudes they would replace?
- 3. If the Tesoro Los Angeles Refinery modifications would facilitate refining a different slate of crude oil, would that change in slate cause an increase in criteria air pollutants, toxic air contaminants or GHG emissions from the Tesoro Los Angeles Refinery during the refining process?
- 4. If the Tesoro Los Angeles Refinery modifications would facilitate refining a different slate of crude oil, would that change in slate cause an increase in the risk of upset (increase in the potential for accidents that could lead to emergency events)?

Before answering these questions, we must define how the term "slate" as applied to crude oil input to a refinery is used in the petroleum industry. As used in this context "slate" can refer to a list of potential crude oils that the refiner can choose to purchase and be delivered as input to the refinery or it can refer to the blend of crude oils actually purchased and processed in a refinery. This report will address both definitions.

In short, my conclusions are summarized in the following numbered paragraphs. For detailed information that provides the basis for the following conclusions, the reader is referred to sections I, II, III, and IV.

- 1. The LARIC project will not change the modes by which Tesoro receives crude oil into the refinery complex. As such, the LARIC project will not allow Tesoro to access crudes that are not currently available to the refinery. The LARIC project will make minor changes to crude oil refining capabilities of the Tesoro Los Angeles Refinery, but will not increase the refinery's ability to process higher sulfur crudes or significantly change the refinery's ability to process lighter or heavier crudes. Therefore, the average quality of the crudes processed by the refinery will not change significantly as a result of the LARIC project. The quality of the crudes that Tesoro currently processes varies widely, from very heavy sour crudes to very light sweet crudes. Tesoro will continue to decide which crudes to purchase in the future at any given time based on a variety of factors, such as the quality and price of crudes on the market, the market demand for different products such as gasoline, jet fuel, or diesel fuel, the market prices for different products, and the refinery's configuration. It is difficult to predict with certainty what crudes Tesoro will purchase at any given time in the future because of changes in the world market forces. However, certain limitations applicable to the crudes currently received and processed will continue to apply in the future, as summarized in the following item and explained in more detail later in this report. Therefore, the LARIC project will not change the slate of crude oil that could be delivered to and processed at the Los Angeles refinery.
- 2. Certain aspects of the Tesoro Los Angeles Refinery's processing configuration limit the instantaneous quality of the crude mix that can be processed. These aspects of the refinery processing configuration will not be changed significantly by this project. Tesoro will continue to purchase crudes of varying quality to match the refinery's existing limitations in API gravity and sulfur content before processing them. Tesoro will continue to purchase crudes within the current range after implementation of the LARIC project, regardless of any change in the sources of crudes. Therefore, the air pollutant emissions from process equipment attributable to varying crude types will remain substantially the same.
- 3. Although some of the units in the Tesoro Los Angeles Refinery are being modified and new units are being added, the slate of crude oils available to the refinery will not change and the minor changes in average crude oil quality that might result would not cause an increase in operating emissions of criteria air pollutants, toxic air contaminants or GHG emissions after the mitigation methods that are part of the LARIC are applied.
- 4. The changes being made as a result of this project will not allow the refinery to

process a different slate of crude oil. As such, there will be no crude oil changes that make the refinery more prone to upset or potential leaks of hazardous or toxic substances. Although the LARIC project will not change the slate of crude oil processed in the refinery, some of the other changes proposed in this project will most likely reduce the probability of the release of toxic or hazardous substance within SCAQMD.

Information included in this document was provided both by Tesoro and through publically available sources. However, detailed information concerning the quality and potential sources of crude oil both processed in the past and contemplated to be processed in the future at Tesoro's Los Angeles Refinery are business confidential information and therefore are not included in the EIR or this report. Furthermore, detailed information describing the Tesoro Los Angeles Refinery's processing capabilities, other than information included in operating permits and other public documents is also confidential and not included in this report.

# I. To What Extent Will the LARIC Project Change the Quality of Crudes Delivered to the Refinery?

#### A. How Do Refiners Decide Which Crudes to Purchase?

Crude oil is a complex mixture of thousands of individual chemical compounds (molecules). An oil refinery separates and transforms these complex mixtures into the different, saleable, specification products that consumers demand such as gasoline, jet fuel, diesel fuel, asphalt and lubricating oils. Refineries also produce byproducts such as liquefied petroleum gas (LPG), petroleum coke, and sulfur.

The "oil industry" consists of producers of crude oil, refiners of crude oil and distributors, transporters and marketers of crude oil and finished products. Very few US oil companies perform all of these tasks. For example, Tesoro is an independent oil refiner, but does not drill for or produce crude oil. It purchases its crude oil through both short and long term contracts and on the spot market. As such, Tesoro must rely on other entities (oil producing companies and countries) to ensure that the quality of the crude oil it purchases meets specifications. Crude oils are produced and sold by various entities including governmental organizations such as member nations of the Organization of Petroleum Exporting Countries (OPEC), private companies under license to various governments and private companies producing oil from privately owned land.

Crude oils are generally categorized based on weight or "gravity" and sulfur content. Gravity (API gravity) is an indirect measure of the amount of gasoline and distillate (diesel fuel, jet fuel and home heating oil are collectively referred to as distillates) boiling range material that exist

in the crude as it is delivered to the refinery. Lower gravity crudes contain less gasoline and distillate and larger amounts of heavy tar-like components that require more complex refineries to convert these heavy molecules into gasoline and distillate. Current governmental regulations require gasoline and diesel fuel to be essentially sulfur free, so processing higher sulfur crudes also requires more complex refineries and additional costs to remove the sulfur from the final product. Since it requires less refinery equipment and operating expenses to convert light sweet crudes into gasoline and distillates than it does to convert heavy sour crudes, light sweet crudes are generally more valuable (higher priced) than heavy sour crudes. Crude traders generally price crude oils based on their relative weight and sulfur content. The Energy Information Administration of the US Department of Energy publishes monthly average costs of imported crude oils as a function of API gravity. Lower gravity crudes generally cost less for refineries to purchase than higher gravity crudes, but require more complex and expensive refineries to convert them into saleable products.

Gasoline typically has an API gravity of about 50, while diesel has an API gravity of about 35. Vacuum gas oil (VGO) and residue (the other major components of crude oil) have gravities of about 22 and 10 respectively. The gasoline that is naturally found in crude oil has a low octane and must be "reformed" in a naphtha catalytic reformer unit to increase its octane. The vacuum gas oil is "cracked" in a Fluid Catalytic Cracking (FCC) unit or hydrocracking unit to convert most of it to gasoline and diesel fuel. The residue is either sold as asphalt or heavy fuel oil or is cracked in a coker to produce additional gasoline and diesel fuel and pet coke. Lower gravity crudes with more VGO and residue require more processing in more complex and expensive refineries.

When a refinery is first built, the types and sizes of the various process units are chosen to match the characteristics of the specific "design" crude oil based on a detailed crude assay of the design oil or mix of oils. As new crude sources become available and sources of the design crude decline, refiners must purchase different crudes and blend them together to match refinery processing capabilities as closely as possible. Refiners also add new processing units or modify existing units to either handle the new crude oil mix, produce a different product mix or meet new product or emission specifications. Refiners evaluate these required configurational changes and crude oil purchases with computer programs know as LPs. (Linear Programing Optimization Routines).

Linear Programing is a complex mathematical tool that can be purchased from several different companies. Many refiners use the PIMS model offered by AspenTech. These models have mathematical representations of each refinery process unit and track essentially every major input, intermediate stream and product stream within the refinery. The basic model is licensed from AspenTech, but the refiner must then modify it to include all of the capabilities and constraints of the specific refinery being modeled. The constraints include operational, economic, logistical and environmental factors. The unit-specific information only changes

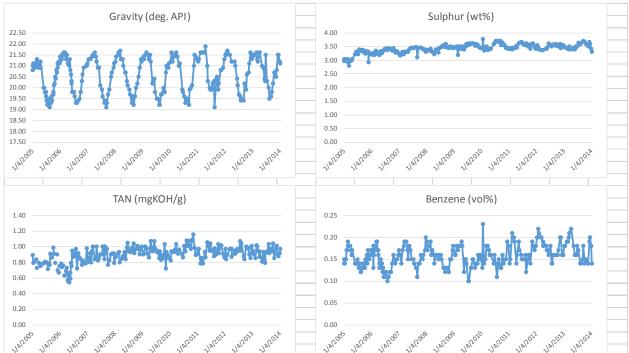
when hardware or environmental requirements change. Product demand and pricing, as well as crude oil price and availability can change every day.

The refinery and the corporate planning groups run these LP models every day. The models are used to determine the optimal crude mix the refinery should purchase from the crudes that are available to it. Once the crudes arrive at the refinery (this could be several weeks or months after the purchase decision is made), the model is run again to determine the most profitable product mix that can be made from the crudes "on-hand", given "today's" prices and product demands. The models are also used as longer term planning tools to determine if an investment such as the LARIC project will be beneficial to the refinery.

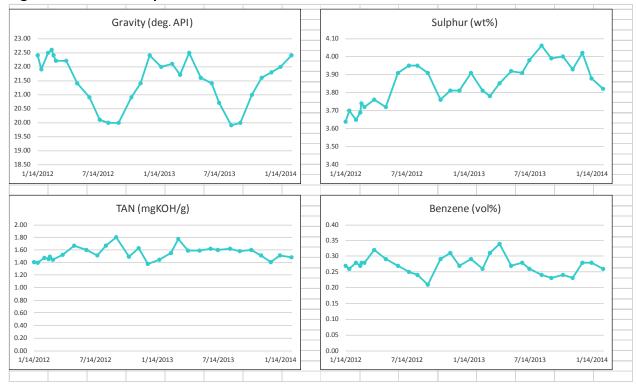
There are many different crude oils available on the world market. The "slate" of crude oils available to any refinery is a subset of the world market that is defined by transportation and delivery modes available to the refinery. In addition to gravity and sulfur, samples of each crude are analyzed in more detail by both producers and refiners. These detailed analyses are called crude assays. A crude assay on a single sample of crude oil can cost anywhere from \$5,000 to more than \$100,000. The cost of the crude assay increases with the level of detail desired. Refiners use these more detailed crude assays to determine the blends of various crudes that can be economically processed in their refinery.

LP models use available crude assay information to represent the crude oil input into the refinery. The refiners must either develop the crude assay information themselves or purchase the information from other sources. Some limited crude assay information is available from open sources, but the detailed information that is required to run a refinery LP is often copyrighted and cannot be distributed to the public without compensating the copyright owner. Detailed crude assays developed by refiners for use in their own LP modeling have competitive value and are therefore considered trade secret and business confidential information.

Although each crude oil has a specific name and generally accepted quality, every cargo is a blend of various oils produced from a number of individual wells, each well producing a slightly different quality oil. Therefore, a single crude assay is only an approximation of the actual quality of crude oil delivered to a refinery. For example, Crude Oil Quality, Inc. maintains a website (<a href="www.crudemonitor.ca">www.crudemonitor.ca</a>) that publishes limited analytical data on shipments of a number of Canadian crude oils. Figures 1 and 2 show the variability in Gravity, Sulfur, Total Acid Number (TAN) and Benzene of Western Canadian Select and Christina Dilbit. These are two, high volume, heavy, sour Canadian export crudes. The LARIC project will not change the availability of these crudes to the Tesoro Los Angeles refinery. This information is only included in this report to show typical crude oil quality variability. For example, the API gravity of Western Canadian Select has varied almost annually between about 19.5 and 21.5 API. Higher gravity occurs in the winter when more diluent is required to reduce viscosity.



**Figure 1: Selected Properties of Western Canadian Select** 



**Figure 2: Selected Properties of Christina Dilbit** 

LP modeling, which includes refinery configuration and economic considerations (crude price, relative product prices and operating costs), determines the actual crude mix and crude rates that the refinery will run to maximize profits. Each refinery has a different configuration and therefore is limited in the types of crude that can be economically processed in that particular refinery. The major processing units typically found in most refineries include: crude unit, vacuum tower, naphtha pretreater and reformer, jet fuel treating, distillate desulfurization units, fluid catalytic cracking unit, alkylation unit and a gas recovery/treating facility. Some refineries might also have a hydrocracker, a heavy gas oil (FCC feed) hydrotreater, a coker, a catalytic polymerization unit, a propane treating unit, a hydrogen plant, lube oil and/or asphalt production facilities as well as other specialty units such as an isomerization unit or benzene conversion unit. Each of these units operates on a different fraction of the crude oil. The exact refinery configuration and the processing capabilities of the individual units determine the crude oils that the refinery is capable of processing. For example, the lifting capabilities of

<sup>&</sup>lt;sup>1</sup> Both the US Department of Energy (DOE) and the Oil and Gas Journal publish annual listings of the processing capacities of every US refinery and the major processing units within each refinery. The DOE listing is available for download from the EIA website, free of charge. The Oil and Gas Journal survey is available for a nominal fee.

<sup>&</sup>lt;sup>2</sup> Refineries also have support facilities to generate steam and electricity, to produce boiler feed water, to recover and produce elemental sulfur. A refinery also includes units whose specific function is to minimize the release of potential contaminants into the environment. A schematic of a typical complex oil refinery can be found in AP-42 Figure 5.1.1 on the EPA website and is reproduced herein as Figure 3. A schematic of the existing Carson and Wilmington Operations of the Tesoro Refinery is shown in Figure 2-8 of the EIR for the proposed Project.

the crude unit and the size of the naphtha reformer limit the average naphtha content of the crude oil that the refinery can process. Most of the sulfur that enters a refinery with the crude oil is removed by the various processing units and converted to elemental sulfur by the sulfur plant. The size of the sulfur plant relative to the crude processing capacity of the refinery determines the maximum **average** crude sulfur content that the refinery can process. The size of the FCC unit, hydrocrackers and coker determine the amounts of VGO and residue that the refinery can process and therefore the heaviness of the crude that can be processed.

Based on the size of the various processing units in the Tesoro Los Angeles Refinery as reported in the U.S. DOE Energy Information Administration website, the maximum average crude oil sulfur content that the Tesoro Los Angeles Refinery complex can remove from its products at full capacity is about 1.5 wt%. Some sulfur also leaves the refinery with the various products, so the actual **average** crude sulfur content that can be processed is slightly higher than this value and is about 1.9 wt%. This is an average value. Individual crudes with sulfur contents above 3% can be processed in the refinery. Also, running the refinery at lower than maximum capacity allows a higher average sulfur crude slate to be processed.

The LARIC project will not increase the sulfur plant capacity nor the ability of the refinery to run a higher average crude sulfur content. A new jet fuel treating unit is being added to improve jet fuel quality but not increase jet fuel production or sulfur content. The coke drums are not being modified as part of this project, so the coke production capacity and hence the amount of sulfur that leaves the refinery with the coke is not expected to change significantly. Thus, the Tesoro Los Angeles refinery complex will not be able to process a significantly higher sulfur content crude slate following the LARIC project.

A refinery does not always run crude oils with sulfur contents that "fill" its sulfur removal/recovery capabilities. Crude oil sulfur content is one of many factors that impact the price and "processibility" of a crude oil. The yield structure and properties of the various fractions of the crude also impact its relative value to any given refinery. Thus, the sulfur content of the crude being run in the refinery on any given day is usually less than the maximum refinery capabilities. The scheduled or unscheduled shutdown of various refinery units can also change the maximum sulfur content of the crudes that can be processed on any given day.

The capacities of the Cokers, hydrocrackers and FCC units (the units that upgrade the heaviest portions of the crude) will be modified as a result of the LARIC project. The Wilmington FCC will be shut down. The Wilmington coker heater permit will be modified to allow an approximately 20% higher maximum heater firing rate. The Wilmington coker only processes a small fraction of the total input of the refinery and only processes heavy crudes. Since the coke drums are not increasing in capacity, this increase in furnace duty associated with the coker heater permit change is expected to provide at most a 2% (6,000 barrels per day) increase in crude oil

throughput capacity mostly in the distillate and VGO range boiling range.

The coker fractionator processes some of the Wilmington crude in addition to the coker products. The "worst case scenario" from an overall emissions perspective is to utilize this additional capability to process additional crude. This is the case that was evaluated in the EIR, so the emission increases associated with an increase in coker furnace permit will be relatively minor (see Table 4.2-4 in the EIR for the LARIC project).

The hydrocrackers and hydrotreating units are being modified to recover more ultra-low sulfur diesel (ULSD) and accept the lightest portions of the feeds that are currently processed in the Carson and Wilmington FCC units. These modifications allow the shutdown of the Wilmington FCC and the elimination of the emissions associated with the operation of the Wilmington FCC. Since the capacities of the cokers are not increasing and the FCC capacity is decreasing, the amount of heavy low gravity crude that the refinery can process will also not increase as a result of the LARIC project.

The average gravity of crude processed will also not increase because the LARIC project's refinery **product** slate would shift somewhat, producing less gasoline and more distillate. FCC units primarily produce gasoline, while hydrocracking units can be operated to produce primarily distillates. The production of more distillate and less gasoline requires less energy, resulting in a lower GHG footprint. Data in the California Air Resources Board (CARB) Low Carbon Fuel Standard (LCFS) lookup table lists the GHG footprint of CARBOB as 99.18 gram (g) CO2/megajoules (MJ) and that of ULSD as 98.03 g CO2/MJ. ULSD has a higher molecular weight than gasoline, so less "cracking" or molecular weight reduction is required to produce diesel from heavy crudes than to produce gasoline from heavy crudes. The modifications to the Tesoro hydrocrackers would allow this shift to less gasoline and more distillate.

Hydrocrackers that produce distillate rather than gasoline also consume less hydrogen in the cracking reactions because the molecular weight reduction is smaller.

The capacity of the naphtha reformers will not change as a result of the LARIC project. The "lifting" capabilities of the crude units will not increase, so the amount of light, high gravity crude that the refinery can process will also not increase as a result of the LARIC project.

#### B. What Crudes are Currently Delivered to the Tesoro Los Angeles Refinery?

The Wilmington and Carson refineries were originally designed to refine California crude oils. The Carson refinery was later expanded to also refine Alaskan North Slope Oil and other imported crude oils. Because of the declining production from the Alaska and California oil fields and the captive use of this production by the various producers, Tesoro currently buys

#### Appendix F

crude on the open market as a substitute for the original design crude oils in accordance with the information generated by the LP model. Some of this purchased crude is domestic production and some is imported from as far away as the Middle-East. According to U.S. DOE information, West Coast refineries processed 877 million barrels of oil in 2014. A little over half of this crude oil was imported into the U.S. and about 10% came from Canada.

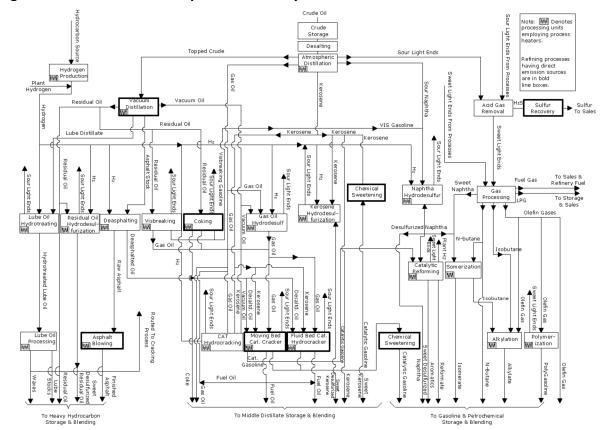


Figure 3: Schematic of a Complex Oil Refinery

Source: EPA AP-42, Chapter 5 Petroleum Refining

The Energy Information Administration of the US Department of Energy publishes much information concerning the types of crudes that are imported into the US, produced within the US and processed within US refineries. The information, however, is aggregated to avoid revealing the input to individual refineries. DOE recognizes that the crudes purchased and processed by individual refineries is valuable company confidential information and does not release this information.

Figure 4 shows the gravity and sulfur contents of crudes that have been delivered to West coast (PADD 5) refineries in the recent past, along with the same properties of various Canadian crudes that could be available as reported by Crude Oil Quality, Inc.

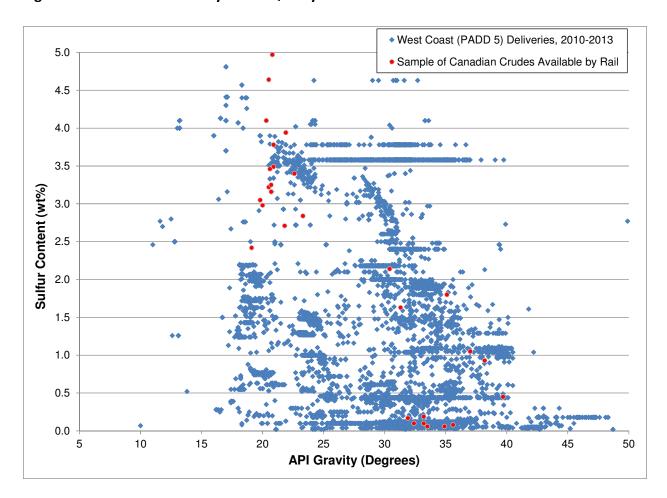


Figure 4: West Coast Refinery Crude Quality

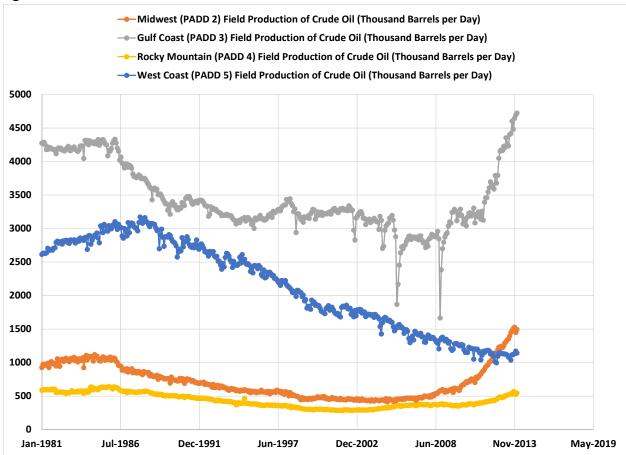
Tesoro Los Angeles currently receives some California and other crude oils via pipeline. It also receives both light sweet and heavy sour crudes via ship. The Tesoro Los Angeles Refinery does not have facilities to receive crude by rail and the LARIC project will not change modes of importing crude to the refinery so the slate of available crude oils will not change. The processing of these various crudes within the refinery is scheduled to match the operating constraints of the refinery.

# C. What Crudes Will Be Delivered to the Los Tesoro Angeles Refinery as a Result of the LARIC Project?

The major operating constraints of the refinery are not being changed by the LARIC project. The ability of the crude units to "lift" more light material is not being increased. The ability to convert heavier crude fractions into lighter products is not increasing. The sulfur removal capabilities of the refinery are not increasing, so the **limits** in the quality of the crude blends that can be processed within the refinery will not change. The sources of the crudes actually

purchased can change and the refinery will still have the ability to run "below the existing physical constraints". The actual **average** crude quality that the refining complex can run in the future will not change significantly.

In recent years, increasingly large volumes of crude oil have become available both domestically and from Canada. Processing more "local" crudes decreases the cost and carbon footprint associated with transporting crude oil to a refinery. Figure 5 shows historic crude oil production rates from various parts of the US. It is easy to see that West Coast crude production continues to decline while production from the mid-continent and gulf coast of the US is rapidly increasing. This increased production is mostly lighter crudes such as Bakken, WTI and WTS. This new production has upset the world crude oil market and resulted in a significant and unanticipated reduction in crude oil prices throughout the world, changing the relative values of different crudes.



**Figure 5: US Crude Oil Production** 

Through the mid-1990's PADD 5 was a net exporter of oil products to other parts of the US, Figure 6. Since then, the west coast and especially California has been a net importer of petroleum. Much of this oil has come from other countries.

#### Appendix F

The Tesoro Los Angeles Refinery currently receives crude oil by pipeline and by marine vessel at the Port of Long Beach. The LARIC project will not change the mode of transportation by which the Tesoro Los Angeles Refinery receives crude oil. The LARIC project does not include construction of new facilities to receive crude oil by rail. Tesoro will continue to receive crude oil by pipeline and waterborne cargoes. The size of the crude oil storage tanks that receive waterborne crude will increase, but as will be discussed in a subsequent section, this change in storage capacity will not impact the types of crudes that can be imported and processed and is expected to actually decrease VOC emissions associated with crude oil reception (during vessel hoteling in the port) and transfer. The sources of crude available by pipeline are currently and will continue to be determined by the pipeline operators. Tesoro's crude oil purchase decision mechanism based on LP modeling of the refinery will not change as a result of the LARIC project.

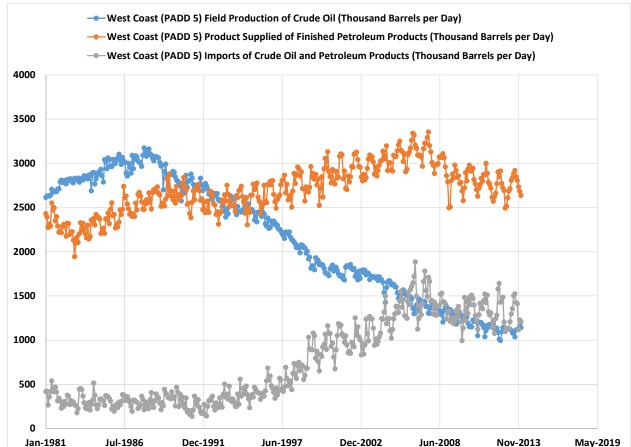


Figure 6: PADD 5 Petroleum Balance

#### II. Would Any Changes in Crude Sources Result in Increased Emissions?

There are several potential sources of emissions from an oil refinery:

- Point source emissions from furnaces and other process stacks. These point source emissions operate under and are limited by emission permits. Stack permits are being modified, which have the potential to increase emissions, but the shutdown of the Wilmington FCC more than offsets these minor increases. Although the processing capabilities of some of the other units are increasing, this is mostly being accomplished via energy efficiency improvements. As explained in the EIR, additional heat exchangers are being added to several units. These heat exchangers recover heat that is currently rejected and use it to provide additional capacity in some of the various conversion and separation processes in the refinery. These new heat exchangers will improve the overall energy efficiency of the complex.
- Fugitive emissions from pumps, valves, flanges, etc. The slight (~2% or up to 6,000 barrels per day) increase in potential crude processing rate will slightly increase the net

flow through much of the refinery piping and increase the potential for higher fugitive VOC emissions. The potential for fugitive VOC emission increases from higher flow rates is very small. New and modified VOC emission sources are subject to best available control technology (BACT) requirements, so fugitive VOC emissions from the LARIC project would be controlled via use of low leakage types of equipment, using welded connections in place of flanges and properly sealing flanges if weld joints are not possible. An active and effective leak detection and repair (LDAR) program pursuant to SCAQMD Rule 1173 – Control of Volatile Organic Compound Leaks and Releases from Components at Petroleum Facilities and Chemical Plants, also reduces VOC emissions from potential fugitive VOC sources. As discussed above, the type of crude oil processed is not expected to be lighter or have higher vapor pressure. Furthermore, the refinery will be producing less gasoline and more distillate, so the vapor pressure of the average product mix and the material moving through the piping system within the refinery will decrease, lessening the potential for VOC emissions.

- VOC emissions from crude storage tanks during filling and unloading. New or modified crude storage tanks would also be subject to BACT requirements, so fugitive VOC emissions would be minimized by use of closed tank vent systems, vapor recovery systems, floating roof tanks for medium volatility oils and pressurized tanks for high volatility material. Replacing several smaller fixed roof tanks with fewer, larger internal floating roof tanks will decrease VOC emissions from the transfer operations. However, the analysis in the EIR did not take credit for VOC emission reductions during crude transfer, so, overall the EIR shows an increase in fugitive VOC emissions from the new tanks (see EIR Table 4.2-4).
- VOC emission from LPG rail car unloading facilities. LPG rail car unloading facilities will be modified at Carson Operations to allow increased deliveries of approximately 4,000 bbl/day of Alkylation Unit feedstocks (LPG including propane, propylene, etc.). The increase in VOC emission caused by the increase in LPG imports and exports from the complex is addressed in the EIR (see EIR Table 4.2-4).

As already noted, the sources of crude oil currently received by the Tesoro Los Angeles Refinery constantly change based on a variety of factors and are expected to continue changing regardless of whether or not the LARIC project is implemented. However, the average gravity and sulfur contents of the future crude mix must still fall within Tesoro's existing feasible operating window. Figures 2-6 and 2-7 in the EIR (attached as Appendix B) show the blended crude API gravity and sulfur contents of the crude oil blends that have been processed in the Carson and Wilmington Operations of the Tesoro Los Angeles Refinery in the three years from 2012 to 2014. The Tesoro Los Angeles Refinery has 4 different crude units with different capabilities, three crude units in Carson and one in Wilmington. The Wilmington coker also processes some crude oil, so there are 5 different units that can each process crude oil directly. Each of the 5 units has different crude throughput and lifting capabilities as well as different

metallurgy to handle different levels of sulfur and acidity.

During the past three years, the Tesoro Los Angeles Refinery complex processed some crude oils with sulfur contents over 3 wt% and API gravities ranging from 10 to 35. Although this is a very wide range of properties, physical unit limitations and economic considerations resulted in average total crude oil properties for that period of slightly under 28 API and about 1.5 wt% sulfur. Based on U.S. DOE data, the average crude oil processed by west coast refineries during the same time period was about 28 API and 1.4 wt% sulfur. The average crude oil input quality to the Tesoro Los Angeles refinery is in line with other west coast refineries.

Tesoro Los Angeles's configuration of process units determines the range of crude oil qualities that can be processed in the facility. As discussed above, its ability to remove sulfur from the various refinery products and air pollutant emission streams limits the maximum sulfur content of the total crude oil blend that can be processed to about 1.8wt%. Processing blends with less than about 0.5 wt% sulfur although feasible causes inefficient operation of the refinery's equipment and is unlikely to occur.

The Tesoro Los Angeles Refinery must also operate within a relatively narrow range of blended crude gravities. At full crude rate, the Tesoro Las Angeles refinery must operate with an average crude API gravity between 23 and 32 API. Each of the 4 crude units can individually run crude outside this envelope, but the weighted average crude quality must stay within these bounds at full crude rate. The refinery can also run lighter or heavier crude mixes at a reduced rate.

The capacities of the coker and FCC, as determined by the physical constraints of the operating equipment, limit the amounts of heavy crude with high quantities of low gravity tar-like substances that can be run without producing excessive amounts of very low value heavy fuel oil. The capacities of these units determine the ability of the refinery to convert these tar-like crude fractions into specification gasoline and distillates. Excess low gravity material must be blended with distillate and exported as high sulfur heavy fuel oil. Not only is the world market for high sulfur heavy fuel oil continuing to decline, producing high sulfur heavy fuel oil reduces distillate production making the production and sale of high sulfur heavy fuel oil very unprofitable.

The rated capacities of the naphtha reformers at the Tesoro Los Angeles Refinery are not being increased. The lifting capabilities of the atmospheric distillation portions of the crude units are also not being increased. Therefore, additional light crudes cannot be processed effectively. Crude oils with higher API gravity will contain more naphtha and distillates that must be distilled (lifted) from the crude oil. Furthermore, the naphtha must be upgraded in a naphtha reformer. Since the LARIC project does not change the capacity of the refinery's naphtha

reformers, the refinery will not have the capacity to recover or upgrade additional naphtha. Furthermore, the impending Tier 3 gasoline sulfur regulations could require processing additional cracked naphtha in the light HDS units reducing their capacity to desulfurize naphtha recovered from crude oil. Crude blends with lighter gravities can exceed the capacity of the naphtha reformers and light stream hydrodesulfurization units at full refinery utilization. The refinery must then either export the excess intermediate streams to other refineries at distressed prices or reduce crude run to bring the refinery back into balance. Both of these options reduce refinery profitability and are highly unlikely.

Even though the "hard" operating limits are defined by physical equipment limitations, most of the actual crude blends that have been processed in the past three years at the Tesoro Los Angeles Refinery are well within these limits. The refinery requires some amount of operating "cushion" to ensure that it does not violate any true operating permit limits or other hard physical constraints such as tower flooding. Furthermore, operating at a minimum or maximum sulfur or gravity "limit" does not always produce the most profitable operation. The optimal crude mix, as determined by the LP model, is a function of the price and availability of various crudes as well as the price and demand for the various products.

Dilbits are a class of heavy crudes that have been available on the world market for more than 40 years, have been processed in many US refineries including some of the west coast refineries and are sold under a variety of names. They are one of many types of heavy, high sulfur crudes that are available throughout the world. They are produced as a blend of a high gravity, low viscosity diluent (dil) and a low gravity, high viscosity bitumen (bit). The diluents range from natural gas condensates to light sweet crudes such as Bakken. Dilbit are nothing more than pre-blended crudes to adjust overall properties to facilitate transport and refining. Most dilbits are shipped by pipeline, but some are also transferred to tankers for waterborne shipment. Of the approximately 1 billion barrels of Canadian crude imported into the US in 2014, only about 7% or just over 200 thousand barrels per day went to all of the west coast refineries combined, including those outside of California.

Large volumes of Bakken-type crude have recently become available from the north central United States and southern Canada. Unlike the heavy, high sulfur Canadian crudes, the Bakken crudes are light, sweet (low sulfur) crudes. Currently, most Bakken crude is shipped by rail. Since the Tesoro Los Angeles Refinery does not have facilities to receive crude oil by rail, it is unlikely that this refinery will process large volumes of Bakken crude. It must first be transferred to pipelines or ships or barges to be received by the refinery. Furthermore, as stated earlier in the report, the LARIC project will not allow the refinery to process a significantly lighter crude slate. Even if Bakken type crudes are available to the refinery, they could not be processed in volumes that would impact the average crude properties.

Neither Bakken, nor the heavy Canadian crudes could be profitably run by themselves at the

Tesoro Los Angeles Refinery. The refinery could not run at full capacity on either crude alone. When running pure Bakken, the refinery would be limited by its ability to lift and process the amount of naphtha contained in the crude and the units designed to process the heavy portion of the crude would be under-utilized. When running pure heavy Canadian crude, such as Christina Dilbit or Western Canadian Select, the refinery would be limited in its ability to handle the sulfur and residue in the crude and the units designed to process the lighter portions of the crude would be under-utilized. Information provided by the LP model is designed to avoid both of these scenarios.

All refinery units have minimum practical as well as maximum permitted operating limits. If a unit reaches its minimum operating limit it must be shut down. Thus, there are limits to how light or heavy a crude mix any refinery can run. Crudes like Bakken or heavy Canadian crudes, e.g., Western Canadian Select or Christina Dilbit, must be blended together with other crudes to optimize the refinery operation. By blending these crudes with other crudes, the refinery can run more efficiently and profitably at higher sustained rates than on either crude alone.

Table 1, extracted from a presentation given by John Auers of Turner, Mason & Co. at the Platts Crude Marketing Conference in Houston, TX on March 1, 2013 shows how two crude oils, with vastly different properties can be blended together to approximate the properties of a third crude oil. Table 1 shows how a blend of Western Canadian Select and Bakken crudes can give the same yields of the various refinery intermediate streams as Alaskan North Slope (ANS) crudes. Thus, refineries that were designed for ANS can substitute blends of WCS and Bakken for ANS. This table also shows that the light hydrocarbons (those contributing most to VOCs) in the blend are lower than those in ANS. Although the sulfur content of the blend is higher, this blend, if processed would only be a portion of the total crude fed to the refinery and the balance of the crude must be lower sulfur to remain within the appropriate limits.

Table 1: Crude oil comparison

Yield, vol%	Alaskan North Slope	WCS/Bakken Blend
API Gravity	32.1	32.1
Sulfur, wt%	0.9	1.4
TAN, mgKOH/g	0.6	0.1
Butanes and Lighter	4	3
Naphtha	26	26
Kero/Diesel	27	27
Gas Oil (FCC feed)	27	27
Residue (Coker feed or Asphalt)	16	16

Concerns have been raised for other refinery projects in California that any refinery project might allow an increase in the benzene content or the acidity of the crudes run in the refinery

or potentially increase the VOC emissions from lighter crudes. The benzene content of Alaskan North Slope, a high volume west coast crude, has been reported as 0.33% while two Canadian crudes suspected of having elevated benzene contents (Figures 1 and 2) on average actually have a lower benzene content than ANS. Crude Oil Quality, Inc. also reports the benzene content of Canadian light sweet crudes as less than 0.25%, again less than ANS, a high volume west coast crude. The benzene content of gasoline is limited by law. The Tesoro Los Angeles Refinery has a benzene saturation unit to reduce the benzene content of the finished gasoline. Like all refinery units, the benzene saturation unit has processing limits which are not being modified by the LARIC project. Thus, the refinery cannot substantially increase the amount of benzene it receives as input to the refinery.

The acidity of the Canadian crudes is also lower than that of typical California crudes and other heavy sour crudes. As noted earlier, the Carson and Wilmington Operations were originally designed to process California crudes. San Joaquin Valley crudes have acidities above 2 (as shown in the California Energy Commission report attached as Appendix C), while Figures 1 and 2 show values below 2 for heavy Canadian crudes. The acidity of the light sweet Canadian crudes is not reported because of its low value. Tesoro actively monitors and controls the acidity of the crudes it purchases and the blends it processes to stay within equipment capabilities. Tesoro also conducts an equipment inspection program that exceeds state and federal requirements. A more detailed explanation of the Tesoro corrosion monitoring program is included in Appendix D.

Crude oil volatility (vapor pressure or potential VOC emissions) has recently received increased scrutiny by various governmental agencies. Most of the focus has been on proper labeling/classification of crude oil shipped by rail from the Bakken formation and the use of proper rail cars for transport. Crude oil is a flammable liquid as defined by the Code of Federal Regulations (CFR) Title 46 (30.10) for Marine shipments and Title 49 (172.101) for land and air shipments. Both CFR sections define three subclasses of flammable liquids although the definitions are slightly different. Title 46 defines Grades A, B and C based on Reid Vapor Pressures (RVP, ASTM D323) of > or = to 14 pounds, under14 and over 8.5 pounds and less than or equal to 8.5 pounds, respectively. Title 49 defines three Packing Groups based on initial boiling point by ASTM D86 distillation and flash point. These are: Packing Groups I, II and III based on IBP<95 F (PG I), IBP >95F and Flash Point <73F (PG II) and Flash Point >73F and <149F and IBP>95F (PG III).

In addition to these shipping requirements, refiners also limit the volatility of crude they purchase. Most of the volatility or vapor pressure of crude oil is due to the small amounts of propane, butanes and pentanes (light paraffinic hydrocarbons) that are dissolved in the crude oil. Refineries are very limited in their ability to convert these light paraffinic hydrocarbons into gasoline. CARB gasoline has a Reid Vapor Pressure (RVP) limit of 7 pounds, so much of the light paraffinic hydrocarbons contained in the crude oil must be sold at a loss as LPG. Wholesale LPG

#### Appendix F

spot prices are typically much less than CARB gasoline prices, providing an economic incentive for Tesoro to control the vapor pressure of the crude it purchases.

Tesoro is expanding their facilities to unload additional quantities of higher value olefinic light hydrocarbons (propylene and butylenes). These olefinic light hydrocarbons can be upgraded to a high value CARB gasoline blending component in the alkylation unit. The shutdown of the Wilmington FCC unit reduces the amount of light olefins produced in the refinery. Both olefinic and paraffinic light hydrocarbons are often called LPG, although they have much different values.

There is no universal relationship between crude gravity and volatility or vapor pressure of the crude oil as shown in Figure 7 for 45 different crude oils. Based on the factors discussed above, there is no valid reason to believe that the crudes that arrive after the LARIC project will be higher volatility than those currently processed. Tesoro has financial incentives to minimize the volatility of crudes that it purchases.

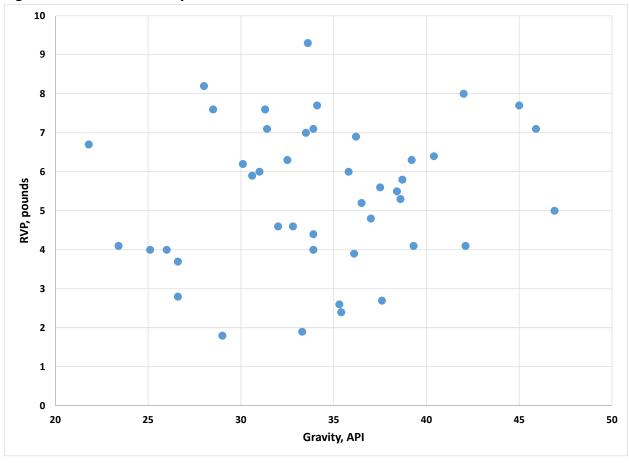


Figure 7: Crude oil volatility

As discussed in the EIR, the replacement of smaller crude oil storage tanks with new larger tanks will decrease the time required to unload a tanker and reduce hoteling emissions from the tanker during the overall unloading process. Of potential concern is whether or not these larger tanks will reduce the ability of the refinery to optimize crude purchases and therefore result in lighter or heavier average crude slates. It is my opinion that the larger tanks will not impact the ability of the refinery to blend various crudes to meet the refinery targets as explained below.

These new larger tanks only impact the waterborne crudes that arrive by tanker or barge. These are generally large cargoes that are purchased in advance, allowing the refinery adequate time to plan for their arrival and purchase complementary crudes. As explained in the EIR, the cargo size is set by the vessel size, not the tank size. The larger tanks will make the vessel unloading more efficient while not changing refinery operations.

The LARIC project will replace several fixed roof crude oil storage tanks that are currently connected to a vapor recovery system and are considered BACT with internal floating roof tanks. Although both tanks are considered BACT, the internal floating roof tanks generally

generate lower VOC emissions than fixed roof tanks. The lower emissions were not fully comprehended in the overall VOC emissions estimates in the EIR.

The proposed LARIC project is not expected to result in changes to the future crude slate processed in the Tesoro Los Angeles Refinery compared to what is currently processed at the refinery. Therefore, the average sulfur content and acidity of the crude is not expected to increase. These are the most corrosive elements of the crude, so there should be no increased risk of equipment failure due to corrosion.

The Wilmington FCC unit is a complex, circulating fluidized bed process unit. Although a typical FCC unit has few upsets, it has a relatively higher probability of upset than typical fixed bed units. Shutting down the Wilmington FCC unit will eliminate the overall risk of upset from this unit.

The operation of the hydrocracking units is being modified to decrease naphtha yield and increase distillate yield. It is well known to those in the industry that hydrocrackers that produce distillate are less at risk for upsets than those that produce naphtha. The analysis of risk of upset impacts from the modified hydrocracking units at both the Carson and Wilmington Operations concluded that hazards associated with the proposed modifications would result in a reduction in hazard impacts (see EIR Table 4.3-2).

The installation of the sulfuric acid regeneration unit will definitely reduce the risk of potential releases of fresh and spent sulfuric acid during the transport outside the refinery, because spent sulfuric acid would be regenerated and reused onsite, thus, eliminating fresh and spent sulfuric acid transport trips as explained in the EIR.

#### What Information Must Tesoro Keep Confidential?

Preparation of this report relied on information included in the EIR, as well as other publicly available information. Some additional information was provided to the author by Tesoro Los Angeles Refinery as business confidential information. Some information is copyrighted information with restrictive rights that limit its public dissemination without proper compensation. The following information is treated as business confidential:

- The specific North American crudes that Tesoro plans to purchase;
- The properties (weight, sulfur content, vapor pressure, and acidity) of specific crudes delivered to Tesoro in the past;
- The properties (weight, sulfur content, vapor pressure, and acidity) of specific crude blends processed at the refinery;
- Data purchased by Tesoro showing the weight and sulfur content of specific crudes, including North American crudes;

- Data generated by Tesoro showing the weight and sulfur content of specific crudes, including North American crudes;
- Detailed information regarding the weight and sulfur content of crude blends suitable for processing at the Tesoro Los Angeles Refinery based on the refinery's unique configuration; and
- Detailed daily measurements of the weight and sulfur content of crude blends processed at the Tesoro Los Angeles Refinery in the past.

Basic properties of most Canadian crudes such as gravity, sulfur, benzene and acidity are available on <a href="www.crudemonitor.ca">www.crudemonitor.ca</a>. Representative data have been included in this report. Detailed properties on Bakken crude could not be found in public documents. Crude assay compositional data can be purchased from companies such as AspenTech; however, this information is copyrighted and cannot be distributed to the general public. Other detailed information concerning the capabilities of the various refinery process units, the crudes that have been and will be run in the refinery and the planning tools that the refinery uses to make crude purchase decisions, is also considered to be confidential and, thus, not publicly available.

As discussed above, the U.S. DOE has determined that refineries do not have to release specific crude purchase information to the public nor do they have to release detailed information on the capabilities of the various processing units within the refinery. It is sufficient to release only unit capacities aggregated by unit type. This information is available on the DOE website and also by purchase through the Oil and Gas Journal. Although the refineries report more detailed information on crude purchases to the DOE and CARB, the agencies aggregate the data prior to publication to avoid revealing company confidential information.

Crude oils are a commodity that is heavily traded by oil companies as well as trading companies. Publishing what specific crudes Tesoro purchases or intends to purchase allows competitor refiners to bid on similar crudes and allows traders to purchase futures of these crudes. Both of these actions would increase the price Tesoro would then pay for future cargoes of these specific crudes. Releasing information on the specific crudes that Tesoro intends to purchase would put it at a disadvantage against it competitors.

The planning tools that a refinery uses can be purchased by anyone; however, they are copyrighted and cannot be redistributed without compensating the copyright owner. Furthermore, much of the value of these programs comes from configuring them and customizing them to closely match the capacities, capabilities, limitations and performance of the individual units in a particular refinery. This latter type of information would be of particular value to a competitor and is business confidential information.

# Appendix F

All of the conclusions and opinions set forth above are made to a reasonable degree of professional certainty.

Date

Stephen J. McGovern, P.E., PhD

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Appendix A

Curriclum Vitae

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# Stephen J. McGovern

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# **Transportation Fuels and Refining Technology Expert**

Over 40 years of experience in many aspects of petroleum refining technology and management, especially Hydroprocessing, Catalytic Cracking, Biofuels, Economics and Emissions. Outstanding record of fundamental research, process/project development and implementation as well as technical service and technical training.

# **Experience Summary:**

#### PetroTech Consultants 2000- present

Principal of consulting firm specializing in Petroleum and Biofuels Refining Technology **Mobil Corporation** 1973-2000

Senior Technical Expert in Refining Process Technology with special emphasis on Catalytic Cracking, Hydroprocessing and reactor design and emissions. Past Manager of Corporate Hydroprocessing Research and Technical Service group. Provided world-wide technical service and troubleshooting, technical input into laboratory experimental programs and the process design of new commercial units along with environmental and economic advice.

#### **Recent Accomplishments**

- Member of two US National Research Council committees evaluating the economic and environmental impacts of increasing biofuels production and alternate vehicle and fuels technologies
- Provided technology guidance to DARPA for the production of HEFA type bio based jet fuels
- Provided technical guidance to several commercial bio and alternative fuels companies
- Provided process designs for several Hydrocracking and ULSD units.
- Developed design for commercial biofuels hydrotreater
- Coordinated technology evaluation pilot unit studies for multiple clients
- Prepared a detailed assessment of the US refining industry's capabilities to produce ULSD.
- Prepared a detailed technical and economic assessment of solid acid alkylation technologies
- Evaluated technical and economic feasibility for producing 10 and 30ppm sulfur gasoline.
- Diagnosed performance problems of commercial hydroprocessing and FCC units.
- Assisted client in troubleshooting and improving novel fluid bed technology.
- Consulted on FCC emissions issues
- Provided expert testimony for FERC on refining economics
- Prepared expert reports on refinery environmental and technical issues
- Currently teach several refining technology courses for Refining Process Services.

# **Education**

Ph. D. Chemical Engineering, Princeton University, Princeton, New Jersey 1985

M. A. Chemical Engineering, Princeton University, Princeton, New Jersey 1982

M. S. Chemical Engineering, Drexel University, Philadelphia, Pennsylvania, 1976

B. S. Chemical Engineering, Drexel University, Philadelphia, Pennsylvania, 1973

New Jersey Professional Engineer, License No. 24GE26348

# **Other Accomplishments**

**Process Consultant, FCC and Clean Fuels Technology** – Senior technical expert in refining process technology.

- Initiated the development of Mobil's Cyclofine FCC third stage separator technology.
- Initiated the development of Mobil's improved FCC stripper technology.
- Designed and coordinated an extensive FCC pilot unit program to better understand the effects of feed quality on FCC yields and product properties.
- Provided guidance to various refineries regarding Air Emissions Compliance and Testing.
- Managed the rapid commercialization of Mobil's Octgain process for producing low sulfur gasoline.
- Provided technical and economic guidance for several major FCC and HDP revamps.
- Provided on-site FCC turnaround and troubleshooting support.
- Provided "cold eyes" and Value Engineering reviews of major projects.
- Participated in several refinery yield improvement surveys.
- Evaluated adsorption technology for removing sulfur from gasoline.
- Responsible for overseeing Mobil's FCC and Hydrocracking modeling efforts.
- Improved the FCC and HDP representations in refinery planning and operational LP's.
- Developed process for upgrading Sasol's Fischer-Tropsch liquids.
- Commercialized Mobil's Xylene Isomerization technology

3

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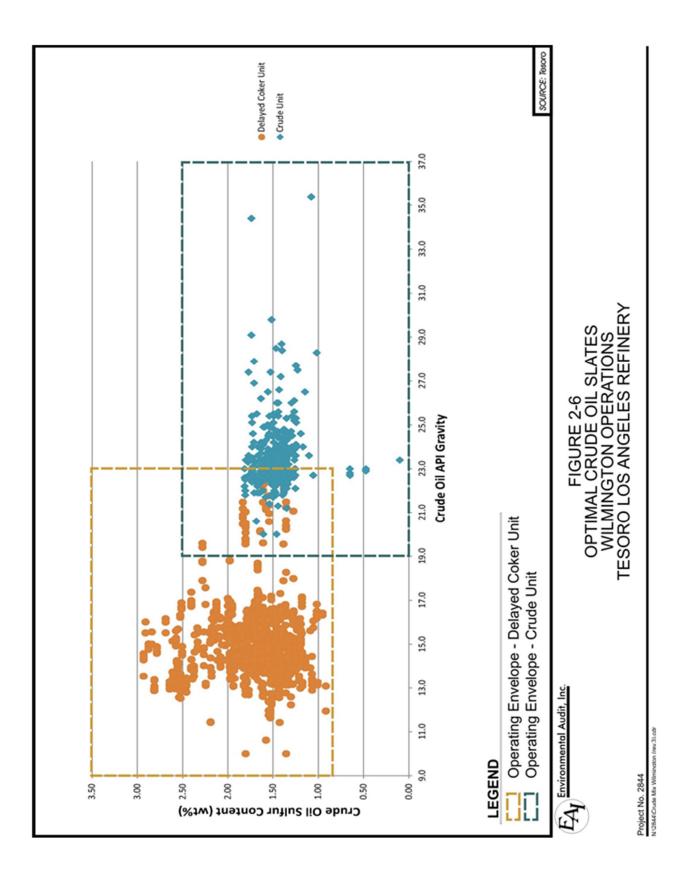
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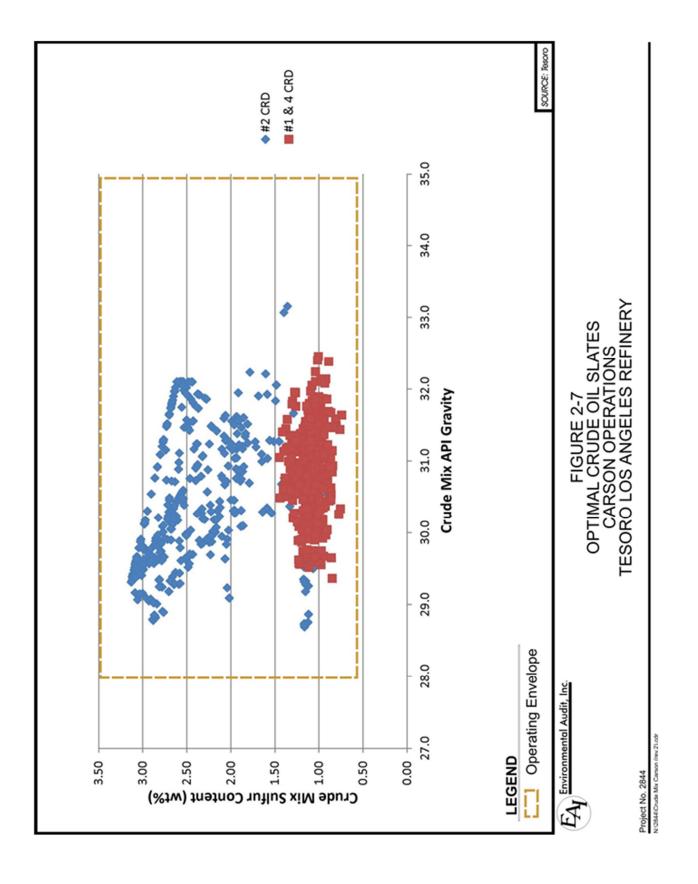
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#### Appendix B

Crude Oil API Gravity and Sulfur Content Graphs

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Appendix C

California Energy Commission Report

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# STAFF PAPER

## CALIFORNIA CRUDE OIL PRODUCTION AND IMPORTS

#### **Margaret Sheridan**

Fossil Fuels Office Fuels and Transportation Division California Energy Commission

#### **DISCLAIMER**

This paper was prepared by a member of the staff of the California Energy Commission. It does not necessarily represent the views of the Energy Commission, its employees, or the State of California. The Energy Commission, the State of California, its employees, contractors and subcontractors make no warrant, express or implied, and assume no legal liability for the information in this paper; nor does any party represent that the uses of this information will not infringe upon privately owned rights. This paper has not been approved or disapproved by the California Energy Commission nor has the California Energy Commission passed upon the accuracy or adequacy of the information in this paper.

APRIL 2006 CEC-600-2006-006

#### CALIFORNIA CRUDE OIL PRODUCTION AND **IMPORTS**

#### Introduction

Californians consume nearly 44 million gallons of gasoline and 10 million gallons of diesel every day. California refineries produce these fuels and other products from crude oil and blending components. Transportation fuel production in California depends on the availability and quality of the crude oils used by refineries in the state. Figure 1 shows the average annual refinery receipts of crude oil from 1986 to 2005. The supply of crude oil to California refineries has changed substantially in the last 10 years. Most notably, receipts of foreign crude oil have increased as production sources from California and Alaska have continued to decline.

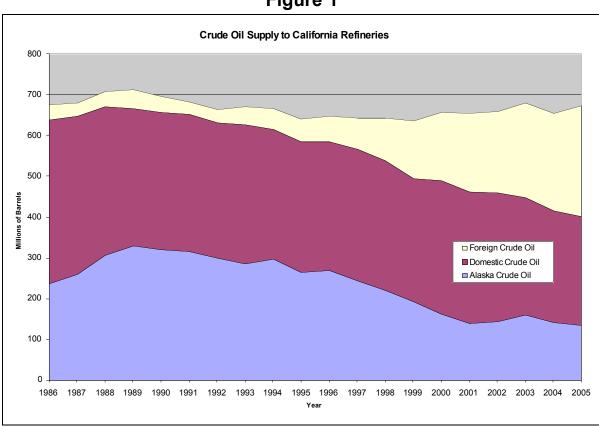


Figure 1

Source: Petroleum Industry Information Reporting Act

Historically, California has been relatively self-reliant in petroleum supplies. However, crude oil production in California has decreased by 23 percent since 1996.2 This decline of supply in the state has increased reliance on foreign and domestic imports. Starting in 1994, California refineries received more imported crude oil than in-state sources. In 2005, California crude oil accounted for approximately 37 percent of the total receipts.

The quality of the crude oil used by the refinery in conjunction with the complexity of processing units dictates the percentages of products produced. For example, lower quality crude oil is more difficult to refine into lighter products, such as motor and aviation gasoline. Refineries have minimum crude oil quality requirements that are determined by the processing units in the plant.

This paper presents information on crude oil characteristics, California crude oil production trends, and their possible impact on future transportation fuel production.

#### **Crude Oil Characteristics**

The quality of crude oil is determined by a number of characteristics that affect the proportions of transportation fuels and petroleum products produced when the oil is refined. The two most common measurements of crude oil quality are the specific gravity (which is measured in degrees) and the sulfur content of the oil. Acid content is also a factor in determining the corrosive properties of the crude oil entering the refinery.

#### Specific Gravity

The specific gravity is typically measured using the American Petroleum Institute (API) standard or the API gravity of the crude oil. The API gravity is the measure of the weight of crude oil in relation to the weight of water (water has an API gravity of 10 degrees). Crude oil is characterized as heavy, intermediate, or light with respect to its API gravity.

- Heavy Crude: Crude oils with API gravity of 18 degrees or less is characterized as heavy. The oil is viscous and resistant to flow, and tends to have a lower proportion of volatile components. Fifty one percent of California crude oil has an average API of 18 degrees or less.
- Intermediate Crude: Crude oils with an API greater than 18 and less than 36 degrees are referred to as intermediate. Forty eight percent of California crude oil has an average API between 18 and 36 degrees.
- Light Crude: Crude oils with an API gravity of 36 degrees or greater. Light crude oil produces a higher percentage of lighter, higher priced premium products.

#### Sulfur Content

Crude oil is defined as "sweet" if the sulfur content is 0.5 percent or less by weight and "sour" if the sulfur content is greater than 1.0 percent. Sulfur compounds in crude oil are chemically bonded to hydrocarbon molecules in the oil. Additional equipment in the refinery is required to remove the sulfur from crude oil, intermediate hydrocarbon feedstocks, and finished products. Transportation fuel specifications require extremely low sulfur contents, usually less than 80 parts per million (ppm).

#### Acid Content

Another characteristic of crude oil is the total acid number (TAN). The TAN represents a composite of acids present in the oil and is measured in milligrams (mg). A TAN number greater than 0.5 mg is considered high.<sup>3</sup> As an example, Wilmington and Kern crude oil have a TAN ranging from 2.2 to 3.2 mg, respectively.<sup>4</sup> However, some acids are relatively inert. Thus, the TAN number does not always represent the corrosive properties of the crude oil. Further, different acids will react at different temperatures – making it difficult to pinpoint the processing units within the refinery that will be affected by a particular high TAN crude oil. Nonetheless, high TAN crude oils contain naphthenic acids, a broad group of organic acids that are usually composed of carboxylic acid compounds. These acids corrode the distillation unit in the refinery and form sludge and gum which can block pipelines and pumps entering the refinery.<sup>5</sup>

The impact of corrosive, high TAN, crude oils can be overcome by blending higher and lower TAN oils, installing or retrofitting equipment with anticorrosive materials, or by developing low temperature catalytic decarboxylation processes using metal catalysts such as copper. Many California refineries already process high TAN crude. High TAN oils are sold on the market at a discount compared to higher quality crude oils.

High TAN oils account for an increasing percentage of the global crude oil market. Crude oil with a TAN greater than 1.0 mg increased in the world market from 7.5 percent in 1998 to 9.5 percent in 2003.<sup>6</sup>

#### **California Crude Oil Production**

The discovery of oil in Kern County in the late 19<sup>th</sup> century heralded a long history of oil production in California. At the turn of the 20<sup>th</sup> century, crude oil was valued primarily for the heavier products and refining was oriented towards the production of heating oil and lubricants. In the early 1900s, with growing automobile use, gasoline became a more important commodity.

California is currently ranked fourth in the nation among oil producing states, behind Louisiana, Texas, and Alaska, respectively. Crude oil production in California averaged 731,150 barrels per day in 2004, a decline of 4.7 percent from 2003. Statewide oil production has declined to levels not seen since 1943.<sup>7</sup>

Figure 2 shows California onshore and offshore crude oil production over the last 20 years. The production of heavy, intermediate, and light crude oil production are broken out for onshore and offshore (or Outer Continental Shelf [OCS]) areas.

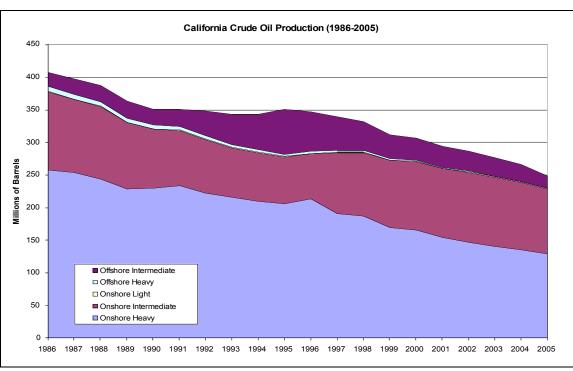


Figure 2

Sources: California Department of Conservation, Minerals Management Service

Production peaked in California in 1983. Production has declined at an average rate of 2.4 percent per year in the last 10 years.

Figure 2 shows a constant decline in onshore heavy crude oil production from 1986 through 2005 of 6.8 million barrels per year, or approximately 3.5 percent per year. Intermediate onshore oil production remained relatively flat. Offshore crude oil production peaked at 72 million barrels in 1995 and has declined by around 4.3 million barrels per year - or 10.2 percent per year - from 1995 through 2004.

The three major regions of California crude oil production are Kern County, the Los Angeles Basin, and the Outer Continental Shelf (OCS).

- Kern County: In 2004, oil from Kern County accounted for 77 percent of California's total onshore production and over 69 percent of the state's total oil production.<sup>8</sup> Approximately 58 percent of the crude oil has an API of 18 degrees or less. The Kern River oil field, located in the eastern San Joaquin Valley, accounts for approximately 24 percent of Kern County oil. Kern River oil is characteristically heavy and sour with an API of 13.4 degrees and a sulfur content of 1.2 percent.<sup>9</sup>
- Los Angeles Basin: The Los Angeles Basin is a sedimentary plain extending from central Los Angeles south through the Long Beach area. The two largest fields by area in this region are the Wilmington and the Huntington Beach fields with average APIs of 17.1 and 19.4 degrees, and average sulfur contents of 1.7 and 2.0 percent, respectively.
- Outer Continental Shelf:<sup>10</sup> The Federal Minerals Management Service oversees crude oil rigs located three nautical miles or greater from the coast. The OCS rigs accounted for 10.2 percent of the total California production in 2004. Many of these rigs are leased to commercial companies with pipelines extending to onshore processing facilities. The quality of OCS crude oil varies by field. Both sweet and sour OCS crude oils have API gravities ranging from 14 to 38 degrees.<sup>11</sup> Intermediate crude oil with an API gravity between 18 and 36 degrees accounted for 96.6 percent of the OCS production in 2004.

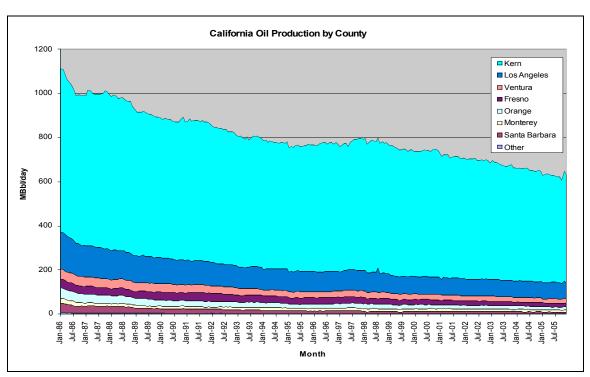
Table 1 shows an assay of selected California crude oils. The table provides the percentages of 2005 production to show the relative importance of the field. The distillation breakdown of each crude oil provides a general guideline of the refining product suite that would result after the initial crude distillation has been completed. The actual ratio of finished refined products will vary depending on the complexity of the refinery. Note that unrecoverable gas losses occur in the assay, resulting in distillation product summations of less than 100 percent.

Table 1

				Distillation breakdown (percent per volume)			
County	Field	Percent of 2005 Production	API Gravity & Sulfur	Total Gasoline & Naptha	Middle Distillates	Residuum	Lubes
Kern & San Luis Obispo	Midway Sunset	18.47%	12.6, 1.6%	0.00%	12.00%	50.30%	34.80%
Kern	Kern River	14.36%	13.3, 1.1%	0.00%	15.80%	56.10%	28.10%
Kern	Elk Hills	7.91%	34.6, 0.8%	34.30%	23.30%	25.00%	15.90%
Los Angeles	Wilmington	6.49%	17.1, 1.7%	9.50%	18.20%	52.80%	19.40%
Kern	Lost Hills	4.96%	18.4, 1.0%	7.60%	23.50%	42.70%	23.20%
Ventura	Ventura	1.75%	30.2, 1.0%	30.20%	20.80%	31.30%	16.30%
Kern	Belridge N. Lt.	1.63%	31.3, 0.3%	25.70%	25.70%	26.30%	20.90%
Monterey	San Ardo	1.52%	12.2, 2.3%	2.10%	14.50%	62.50%	20.50%
Los Angeles	Inglewood	1.24%	21.0, 1.8%	12.90%	27.60%	39.10%	19.40%
Orange	Huntington Beach	1.07%	19.4, 2.0%	12.00%	19.70%	48.90%	19.40%
Los Angeles	Long Beach	0.65%	25.0, 1.3%	18.90%	23.10%	40.60%	17.40%
Kern	Mount Poso	0.26%	16.0, 0.7%	0.00%	13.40%	52.00%	34.00%

Figure 3 shows the onshore production by county.

Figure 3



Source: Dept. of Conservation

California commonly uses Thermally Enhanced Oil Recovery (TEOR) techniques to help maintain crude oil production, because heavy, viscous crude oil requires heating to move the oil to the pump. Direct injection steaming and intermittent steaming are two types of TEOR. California crude oil production is also enhanced by injection of water (water flooding) and even carbon dioxide (CO<sub>2</sub>) to help maintain sufficient pressure in the crude oil field. In the absence of more aggressive use of TEOR, California's crude oil production is expected to continue to decline at a rate of 3.5 percent per year through 2019.<sup>13</sup>

Well activity provides an indication of potential production in the state. In 2004, drilling increased to 2,451 wells, a 6.7 percent increase from 2003. The number of plugged wells decreased to 2,039 from 2,501 in 2003. Drilling and plugging activities in the state have fluctuated by more than 900 wells from year to year; however, the general trend is relatively flat.

#### Alaska North Slope Crude Oil

In 2005, California imported 21 percent of its total crude oil supply from Alaska. Oil fields in Alaska's North Slope produce a wide range of crude oils. API gravities from different fields range from 22 to 40 degrees. Alaskan refineries located along the Trans Alaska Pipeline System (TAPS) "top" the crude oil to produce light petroleum products and return residual products to the line. The resulting blended crude oil stream is referred to as Alaska North Slope oil (ANS). The ANS is an intermediate sour crude with an average API gravity of 29-29.5 degrees and sulfur content of 1.1 percent.

Like California crude oils, ANS production has been declining in the last 10 years. The average annual rate of decline in ANS production is approximately 5 percent per year.

#### Foreign Crude Oil Imports

The majority of crude oil imports to California are from the Middle East, Central America, and South America. Figure 4 shows a six year history of imports by region.

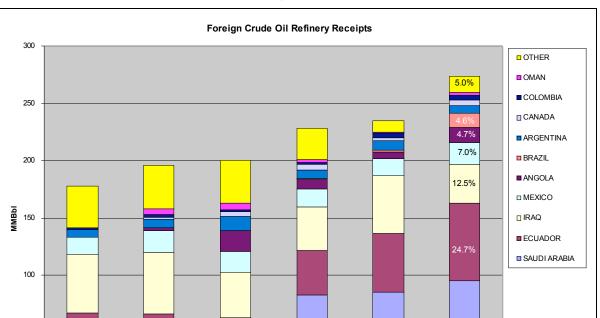


Figure 4

Source: Energy Information Administration

2004

2005

2002

50

2000

2001

Crude oil imported from countries with volatile political and social structures leaves California vulnerable to changing world events. For example, attacks on Nigerian oil industry personnel led to the recent shutdown of nearly 9 percent of Nigeria's total oil production, which could impact global oil availability and increase feedstock costs for California refineries. Also, the growing political tension between the U.S. and Iranian governments over Iran's nuclear program could impact California's crude oil supply if the U.S. decides to impose sanctions on Iran.

Table 2 shows approximate crude oil characteristics for several imported crude oils.<sup>14</sup>

Table 2

Crude source	Paraffins Percent Volume)	Aromatics (Percent Volume)	Naphthenes (Percent Volume)	Sulfur (Percent Weight)	API gravity (Approx.)	Napht. yield (Percent Volume)	Octane No.
Nigerian - Light	37	9	54	0.2	36	28	60
Saudi - Light	63	19	18	2	34	22	40
Saudi - Heavy	60	15	25	2.1	28	23	35
Venezuela - Light	35	12	53	2.3	30	2	60
Venezuela - Heavy	52	14	34	1.5	24	18	50
North Sea - Brent	50	16	34	0.4	37	31	50

Source: Office of Safety and Health Administration

The API gravity of refinery imports reported to the Energy Commission through the Petroleum Industry Information Reporting Act (PIIRA)<sup>15</sup> show an increase of 0.27 API per year from 1996 to 2005 for larger refineries. Smaller refineries show a relatively flat API during the same time period, predominantly because these smaller refineries solely use crude oil from California sources.<sup>16</sup>

#### **Crude Oil Supply and Distribution to California Refineries**

The distribution of domestic and imported crude oils is dependent on the port, pipeline, truck, and rail transport infrastructure within the state. All ANS and imported crude oils enter the state through ports in Los Angeles, Long Beach, and the Bay Area.

Water depth limits access to Bay Area ports. The water depth of these ports is typically between 32 to 45 feet, which is too shallow for large crude oil carriers. As an example, a carrier with a capacity of 1.3 million barrels will require a minimum water depth of at least 66 feet. For shallower ports, large vessels will anchor in a designated zone outside of the ports and smaller barges will transfer oil to the ports, a practice referred to as "lightering." This practice adds to the delivery cost of crude oil to the refinery and increases the risk of accidental release of crude oil into the environment.

Another complication for the Bay Area ports is silting in the bays. Dredging of the bays is controversial in that habitat is disturbed and dredged material must be disposed of in an environmentally sound manner. For example, approximately 4 million cubic yards of sediment are dredged from the Central and South Bay per year.<sup>17</sup>

Pipeline networks tie the San Joaquin Valley crude oil production with refineries in both the Los Angeles and the Bay Area. Figure 5 shows the major crude oil pipelines in California.

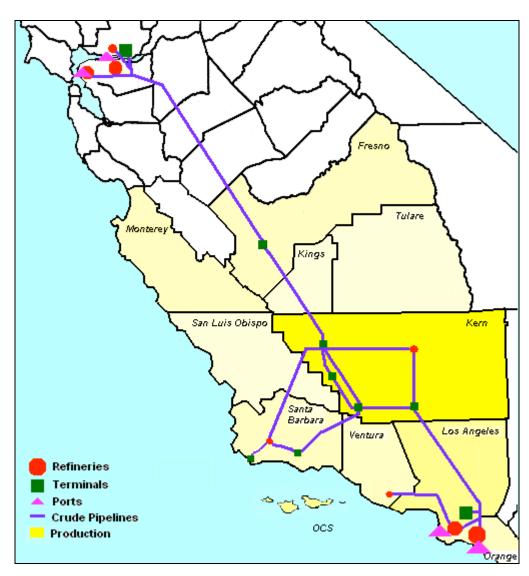


Figure 5

Source: California Energy Commission

In California, 51 percent of the crude oil produced in the state is heavy crude. The transport of heavy crude through pipelines is complicated by the viscosity and inertia of the oil. Thus, some of the crude oil pipeline systems throughout the state require external heating. Booster stations are placed at intervals on the line where heating and/or pumping units facilitate the flow of the crude through the line. The proximity of booster stations is determined by the viscosity of the crude and by the average heat loss from the pipes from ambient weather conditions. Heavier crude oils are also blended with lighter crude oils to reduce viscosity, allowing transportation through pipelines without any heating.

Inland California crude oils are typically first piped to local refineries (Bakersfield and Santa Maria) because they are nearby and do not have port access. The balance of inland crude oils are piped to Northern and Southern California refineries.

#### Refinery Operations

In the last two decades, California refineries have been running increasingly closer to capacity levels. Figure 6 shows the total crude oil throughput refining capacity and the throughput oil inputs to the refinery by area.

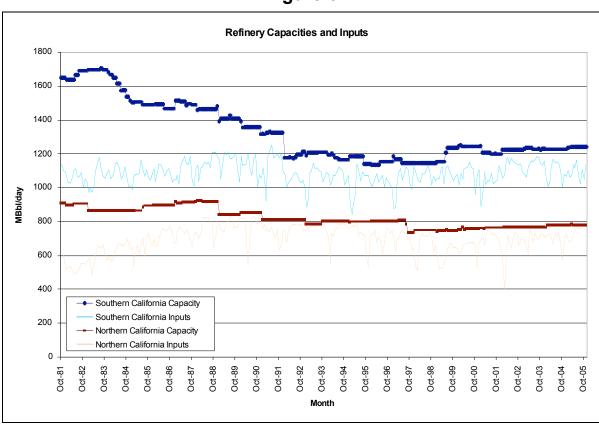


Figure 6

Source: Petroleum Industry Information Reporting Act

The steady decline in refinery capacity during the 1980s and early 1990s is followed by a noticeable creep upward in the late 1990s and early 2000s. With refinery creep and greater import capabilities in the Los Angeles area, southern refineries are less constrained than their Bay Area and Central California counterparts. Southern California refineries also show an increasing level of crude oil imports.

Refinery operations must also consider recent diesel regulations by the U.S. Environmental Protection Agency (EPA) and the California Air Resources

Board (ARB). The EPA regulation lowers the allowable amount of sulfur in on-road diesel fuel from less than 500 parts per million (ppm) to less than 15 ppm. This requirement will take effect on June 1, 2006. The sulfur content and API gravity of crude oil input to the refinery in conjunction with the complexity of process units will affect the quantity of ultra-low sulfur diesel produced by the facility.

The hydrocracking and hydrotreater units remove sulfur within the refinery. Hydrocracking units break hydrocarbon molecules into lighter compounds in the presence of hydrogen. Hydrotreatment involves the chemical reaction of hydrocarbon compounds with hydrogen in the presence of a catalyst such as cobalt or alumina.<sup>18</sup>

Refineries throughout the U.S. are currently upgrading their desulfurization processes in order to meet the new diesel sulfur standards. This upgrade typically involves techniques such as changing the catalyst in the hydrotreater or installing booster pumps to force more feedstock through the unit. Both hydrocrackers and hydrotreaters also remove heavy metals and aromatics from the feedstock. This is particularly important in California where lower aromatic standards will be required along with the new ultra low sulfur diesel standards.

#### **Findings**

- The declining crude oil production in South-Central California has resulted in higher crude oil costs because of reliance on higher priced imported crude oils.
- Pipeline utilization rates are decreasing and the procurement of crude oil to inland refineries is becoming increasingly difficult as local supplies decline.

#### **Current and Future Work**

Additional reporting requirements in the Energy Commission's new petroleum industry data collection regulations will greatly enhance the agency's understanding of crude oil and finished product movements within the state. The addition of port, terminal, and pipeline information will provide the details needed to track infrastructure use within the state. This additional information will be essential in: assessing near-term petroleum infrastructure demand shifts, reviewing project expansion plans, and completing contingency studies.

Research and analysis should focus, in particular, on the following areas:

 Crude oil quality: The growing dependence of California refineries on imported crude oils requires a more detailed look at the characteristics of overseas crude oils entering ports in the state. The general trend of

#### Appendix F

international crude oil production reflects an increase in low API, high sulfur content crude oil. However, overall API gravity in California refineries has increased primarily from the decline in heavy California crude oil production. The examination of supply information from secondary sources and from PIIRA reporting data will help to identify areas of constraint in the state.

- Total Acid Number (TAN): The increase in world production of heavy, sour, and high TAN crude oils will impact California refineries. An assessment of the crude oil processing capabilities of California refineries is needed to understand the potential implications of future changes in the global crude oil market.
- Crude oil pipelines: The decrease in crude oil production in the state has led
  to changes in the utilization rates of some crude oil pipelines. Modifying
  current pipeline systems and/or making new investments in distribution
  infrastructure may be necessary to provide more stable sources of crude oil
  for refineries without port access.

#### **Endnotes**

<sup>&</sup>lt;sup>1</sup> California State Board of Equalization data for 2004. Taxable gasoline figures amounted to an average of 43.5 million gallons per day, while taxable diesel fuel sales figures have been adjusted upward to reflect an estimated 22 percent distribution of exempt and refund diesel sales that are excluded from their taxable gallons.

<sup>&</sup>lt;sup>2</sup> Based on data compiled from the California Department of Conservation database production files, <a href="http://www.conservation.ca.gov/DOG/prod\_injection\_db/index.htm">http://www.conservation.ca.gov/DOG/prod\_injection\_db/index.htm</a> and MMS Offshore data, <a href="http://www.gomr.mms.gov/homepg/pubinfo/pacificfreeasci/product/pacificfreeprod.html">http://www.gomr.mms.gov/homepg/pubinfo/pacificfreeasci/product/pacificfreeprod.html</a>.

<sup>&</sup>lt;sup>3</sup> http://rru.worldbank.org/Documents/publicpolicyjournal/275-bacon-tordo.pdf.

<sup>&</sup>lt;sup>4</sup> http://www.pacificenergypier400.info/pdfs/CRUDESUP/PACIFICP.PDF.

<sup>&</sup>lt;sup>5</sup> http://www.ornl.gov/sci/fossil/Publications/RECENT%20PUBS/DDSum2003.pdf.

<sup>&</sup>lt;sup>6</sup> Anne Shafizadeh, Gregg McAteer, and John Sigmon, *High-Acid Crudes*, paper presented at Crude Oil Quality Group meeting, New Orleans, January 30, 2003, [http://www.coqq.org/20030130special.asp]

<sup>&</sup>lt;sup>7</sup> ftp://ftp.consrv.ca.gov/pub/oil/annual\_reports/2004/PR06\_Annual\_2004.pdf.

<sup>&</sup>lt;sup>8</sup> California Department of Conservation database production files, http://www.conservation.ca.gov/DOG/prod\_injection\_db/index.htm.

<sup>&</sup>lt;sup>9</sup> Van Vector, Samuel, *Pricing Royalty Crude Oil*, <a href="http://www.econ.com/apijan00.pdf">http://www.econ.com/apijan00.pdf</a>.

<sup>&</sup>lt;sup>10</sup> MMS data for 2004 is approximately 95 percent complete. December 2005 data not yet posted.

<sup>&</sup>lt;sup>11</sup> Jokuty, P.; Whiticar, S.; Wang, Z.; Fieldhouse, B.; and Fingas, M.; *A Catalogue of Crude Oil and Oil Product Properties for the Pacific Region*, 264p 1999.

<sup>12</sup> http://www.econ.com/apijan00.pdf.

<sup>&</sup>lt;sup>13</sup> <u>http://www.energy.ca.gov/2005\_energypolicy/documents/2005-0516\_workshop/presentations/</u>Baker%20&%20OBrien%20Presentation%205-16-05.pdf.

<sup>&</sup>lt;sup>14</sup> OSHA Technical Manual – Section IV: Chapter 2, <a href="http://www.osha-slc.gov/dts/osta/otm/otm\_iv/otm\_iv\_2.html">http://www.osha-slc.gov/dts/osta/otm/otm\_iv/otm\_iv\_2.html</a>.

<sup>&</sup>lt;sup>15</sup> PIIRA: the Petroleum Industry Information Reporting Act, Public Resources Code 25350 et seq.

<sup>&</sup>lt;sup>16</sup> Large and small refineries are defined here as refineries with crude oil receipts in 2005 greater than or less than 5 percent of the total for the state, respectively.

<sup>17</sup> http://www.spn.usace.army.mil/ltms/chapter2.pdf.

http://www.bp.com/genericarticle.do?categoryId=2013107&contentId=2019673.

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Appendix D

Tesoro Corrosion Monitoring Program

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### Appendix D: Brief Description of the Tesoro Corrosion Monitoring Program

The Los Angeles Refinery has an Inspection Manual that describes the minimum technical and administrative requirements for the inspection of all refinery equipment. It defines the authority and responsibility of individuals, and provides the system by which activities are conducted in accordance with regulations, codes and policies specified by the California Division of Occupational Safety and Health (Cal OSHA). Tesoro implements additional inspection programs, beyond regulatory requirements, to ensure the integrity of its refinery equipment. The Refinery's Inspection Supervisor is responsible for the administration and implementation of the Inspection Manual. To ensure the highest degree of reliability and integrity of refinery equipment, the Refinery uses a variety of inspection techniques and methods. These inspection practices meet or exceed applicable industry standards, such as the Recommended Practices of the American Petroleum Institute.

To ensure the continued integrity of equipment testing and inspection at its facilities, the Los Angeles Refinery follows company inspection standards which focus on the following core processes:

- Organizational Capability and Competency
- Inspection Documentation
- Inspection Planning and Execution
- Continuous Improvement
- Performance Management Assurance

Testing methods used for inspections include visual examination, non-destructive evaluation (e.g. ultrasonic thickness measurements), and performance evaluations (e.g. hydrostatic testing).

The inspection and testing program at the refinery is conducted on an established schedule. A database of required inspection dates is maintained. An inspection report is provided to Tesoro Refining leadership each month.

Managing inspection in crude distillation units includes focus on damage mechanisms such as Sulfidation, Wet H2S Damage, and Naphthenic Acid Corrosion. The Corrosion Engineer or knowledgeable person establishes predicted or historical damage mechanisms and predicted corrosion rate for each system or area of a process unit. These damage mechanisms are used by the Inspector to select the appropriate inspection method. Inspection plans are developed for all applicable damage mechanisms following company and industry standards for refinery inspection. Methods of establishing piping inspection criteria are described in industry and company standards in which the frequency and extent of inspections are based on a consequence of failure classification and established or predicted corrosion rates (likelihood of failure). The following industry standards are used to establish the inspection program:

- API 510 Pressure Vessel Inspection Code: In-Service Inspection, Rating, Repair, and Alteration
- API 570, Piping Inspection Code
- API 574 Recommended Practice, Inspection Practices for Piping Systems Components
- API RP 571, Damage Mechanisms Affecting Fixed Equipment in the Refining Industry
- API RP 580 Risk-Based Inspection API Publication
- 581, Risk-Based Inspection Resource Document
- API RP 939-C, Guidelines for Avoiding Sulfidation Corrosion Failures in Oil Refineries

NBI NB-23 National Board Inspection Code (NBIC)

In addition, implementation and monitoring of Integrity Operating Windows (IOW) is in progress and control of crude changes follows a rigorous management of change (MOC) process that has been a common practice for many years. Positive Material Identification and Low Silicon carbon steel surveys have been completed on the crude distillation units for piping in high temperature sulfidation service.

In addition to equipment integrity management programs, Tesoro employs operating practices to monitor and mitigate corrosion in these systems. These practices include obtaining routine laboratory analysis of hydrocarbon and water samples from the crude and vacuum units to monitor corrosive species or corrosion products and working with chemical vendors to provide corrosion inhibitors, passivators or chemical additives to reduce corrosion and fouling in the towers and associated feed and product piping and equipment. Operating envelopes or restrictions and alarms are used, for example on stream acid and sulfur content, to keep operations within boundaries and assure long term equipment reliability.