Guidelines for Calculating and Reporting Emissions from Bulk Loading Operations

May 2015

The purpose of this document is to provide operators with guidelines in estimating emissions from loading of volatile organic containing liquid materials in bulk. Loading losses are the primary source of evaporative emissions that occur as organic vapors in "empty" cargo tanks are displaced to the atmosphere by the liquid being loaded into the tanks. These vapors are a composite of: (1) vapors formed in the empty tank by evaporation of residual product from previous loads, (2) vapors transferred to the tank in vapor balance systems as product is being unloaded, and (3) vapors generated in the tank as the new product is being loaded.

In addition to VOC emissions from evaporative losses, other emissions (NOx, SOx, CO, PM, and toxic air contaminants), from controlling VOC emissions by means of thermal destruction are also expected.

The following guidelines should be used to calculate annual emissions from bulk loading operations. The methodologies assume certain default parameters. Site-specific information should be used, if it is available. There are three emission scenarios for bulk loading operations:

1. Simple Operation (No Control)
2. Equipped with a Vapor Collection and Recovery System
3. Equipped with a Balance System and Vapor Control System

CASE 1) SIMPLE OPERATION (NO VAPOR CONTROL)

$$E_1 = Q * L_L \qquad \text{Eq. 1}$$

Where,

E_1 = VOC Emission (un-captured vapor) from Loading Losses

Q = Throughput in 1,000 gallons loaded

L_L = Loading Loss Factor (lbs/1,000 Gallon Loaded) can be found in the Default Emission Factor tables or determined using information defined in US EPA AP-42, Section 5.2 as follows:

$$L_L = \frac{12.46 \times S \times P \times M}{T}$$

Where,

S = Saturation Factor (see AP-42, Table 5.2-1)

P = True Vapor Pressure, psia

M = Vapor Molecular Weight, lb/lb-mole

T = Temperature of the Liquid being Loaded, °R (°F + 460)

CASE 2) OPERATIONS EQUIPPED WITH VAPOR COLLECTION AND RECOVERY SYSTEMS

Loading emissions from this configuration consist of two parts: 1) uncollected vapor during loading; and 2) collected vapor that was further recovered by the system before exiting the recovery stack.

$E_2 = E_{uncollected} + E_{stack} = E_{uncollected} + E_{collected} * (1 - Eff_{VR})$

$E_2 = Q * L_L * (1 - Eff_{VC}) + Q * L_L * Eff_{VC} * (1 - Eff_{VR})$

$$E_2 = Q * L_L - Q * L_L * Eff_{VC} * Eff_{VR} \qquad Eq.\ 2$$

Where,

E_2 = VOC Emission from Loading Losses

Eff_{VC} = Vapor Collection Efficiency (fraction) as defined in US EPA AP-42, Section 5.2 as follows:

Eff_{VC} = 0.992 for tanker trucks passing MACT-level annual leak test; or

Eff_{VC} = 0.987 for tanker trucks passing the NSPS-level annual leak test; or

Eff_{VC} = 0.70 for tanker trucks not passing either of the above leak tests.

Eff_{VR} = Vapor Recovery Efficiency (fraction).
Without specific tests, Vapor Recovery Efficiency (Eff_{VR}) is assumed to be 0.95 and equation 2 becomes:

$$E_2 = Q * L_L * (1 - 0.95 * Eff_{VC}) \qquad Eq.\ 3$$

CASE 3) OPERATIONS EQUIPPED WITH A VAPOR BALANCE AND DESTRUCTION SYSTEM

Loading emissions from this configuration consisted of two parts: 1) uncollected vapor during loading; and 2) collected vapor that was further recovered by the system before exiting the recovery stack.

$E_3 = E_{uncollected} + E_{stack} = E_{uncollected} + E_{collected} * (1 - Eff_{VB}) * (1 - Eff_{VD})$

$E_3 = Q * L_L * (1 - Eff_{VC}) + Q * L_L * Eff_{VC} * (1 - Eff_{VB}) * (1 - Eff_{VD})$

$$E_3 = Q * L_L * [1 - Eff_{VC} (Eff_{VB} + Eff_{VD} - (Eff_{VB} * Eff_{VD}))] \qquad Eq.\ 4$$

Where,

E_3 = VOC Emission from Loading Losses

Eff_{VC} = Vapor Collection Efficiency (fraction) as defined in US EPA AP-42, Section 5.2

Eff_{VB} = Vapor Balance Efficiency (fraction)

Eff_{VD} = Vapor Destruction Efficiency (fraction)

A typical system is operating with Vapor Balance Efficiency (Eff_{VB}) of 50% (or 0.50). Without specific tests, Vapor Destruction Efficiency (Eff_{VD}) is assumed to be 99% (or 0.99) and equation 4 becomes:

$$E_3 = Q * L_L * (1 - 0.995 * Eff_{VC}) \qquad Eq.\ 5$$

THERMAL OXIDATION

If the operation is equipped with a VOC destruction system by means of thermal oxidation, other contaminants (NOx, SOx, CO, PM, and toxic air contaminants) resulted from burning off organic vapor are expected. AQMD encourages operators to use test results to calculate and report emissions. Since the organic vapor evaporates from loading of liquid organic materials, the captured for control vapor must be converted back into liquid form for consistency in emission calculations. The AQMD uses an equivalent method to determine the throughput of vapors directed to a thermal oxidizer (TO) as equivalent 1000 of gallons of liquid (Mgal).

$$TO_{Throughput} = \frac{E_{collected}}{1{,}000 * d_l} * (1 - Eff_{VB})$$

$$TO_{Throughput} = \frac{Q * L_L * Eff_{VC}}{1{,}000 * d_l} * (1 - Eff_{VB}) \qquad Eq.6$$

A typical system is operating with Vapor Balance Efficiency (Eff_{VB}) of 50% (or 0.50). Throughput for the TO become:

$$TO_{Throughput} = 0.0005 * Eff_{VC} * \frac{Q * L_L}{d_l} \qquad Eq.\ 7$$

Where, d_l is the liquid density.

EXAMPLES

The following examples will demonstrate how emissions are calculated for a typical bulk loading operation in all three cases. The examples also included images of screens for how to report emissions under the new reporting system.

CASE 1 - SIMPLE OPERATION (NO VAPOR CONTROL)

Company XYZ splash loaded 120,000 gallons of gasoline RVP 10 at the following conditions:

S = 1.45 (Saturation Factor from AP-42)

T = 70ºF = 530ºR (Temperature of Gasoline)

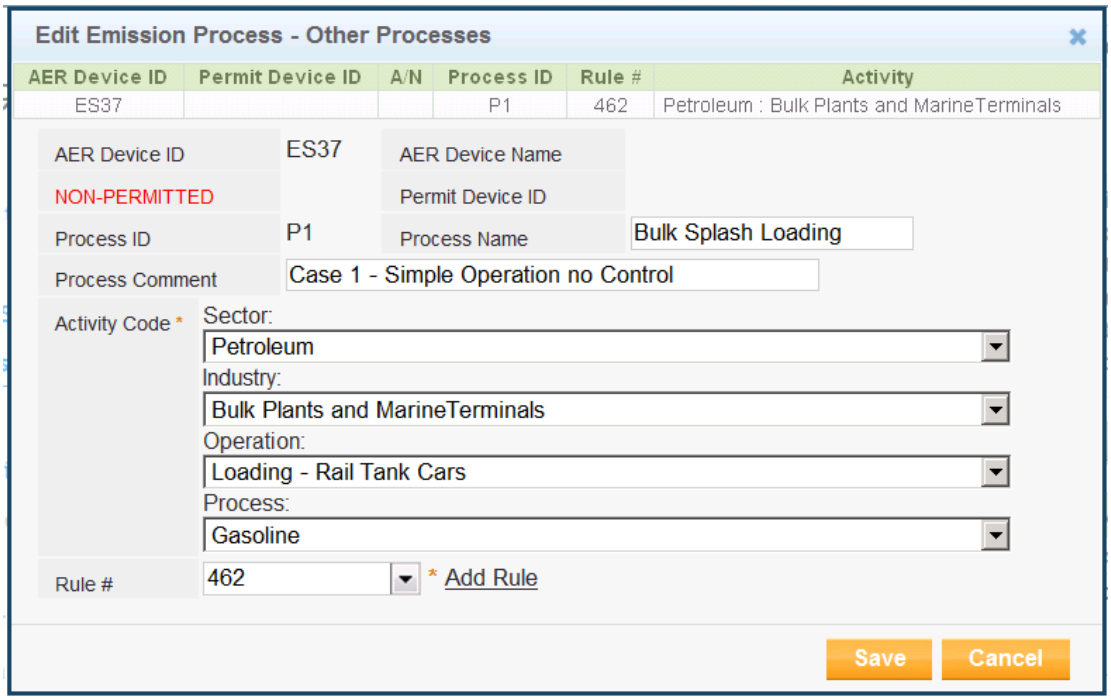
P = 6.2 psia (True Vapor Pressure)

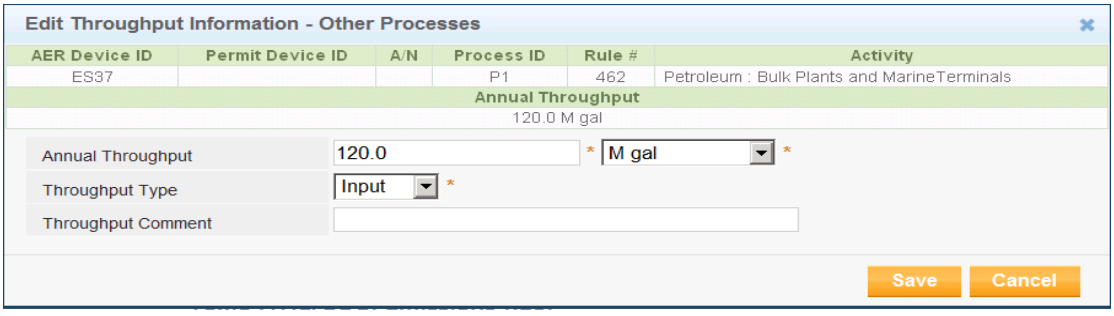
M = 66 lb/lb-mole (Vapor Molecular Weight)

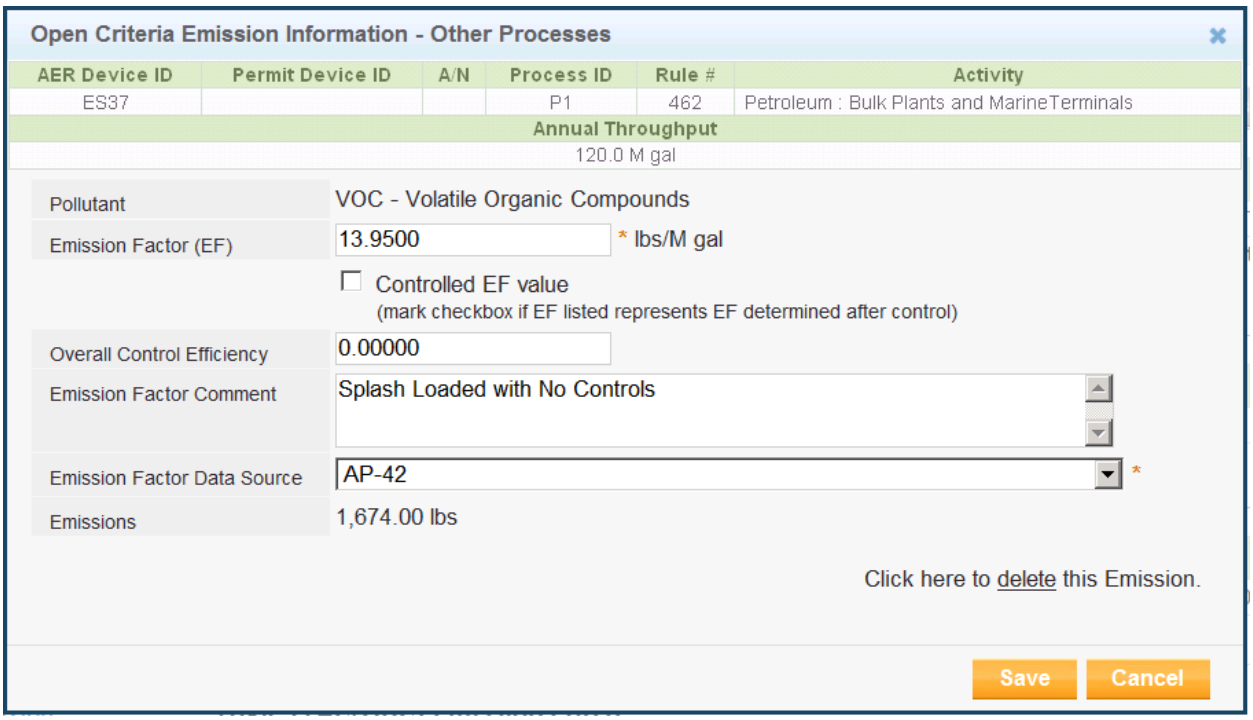
$$L_L = \frac{12.46 \times S \times P \times M}{T} = \frac{12.46 \times 1.45 \times 6.2 \times 66}{530} = 13.95\ lbs\ VOC/Mgal$$

Equation 1 yields the VOC emissions as follows:

$$E_1 = 120\ Mgals * 13.95\ \frac{lbs\ VOC}{Mgal} = 1{,}674\ lbs\ VOC$$



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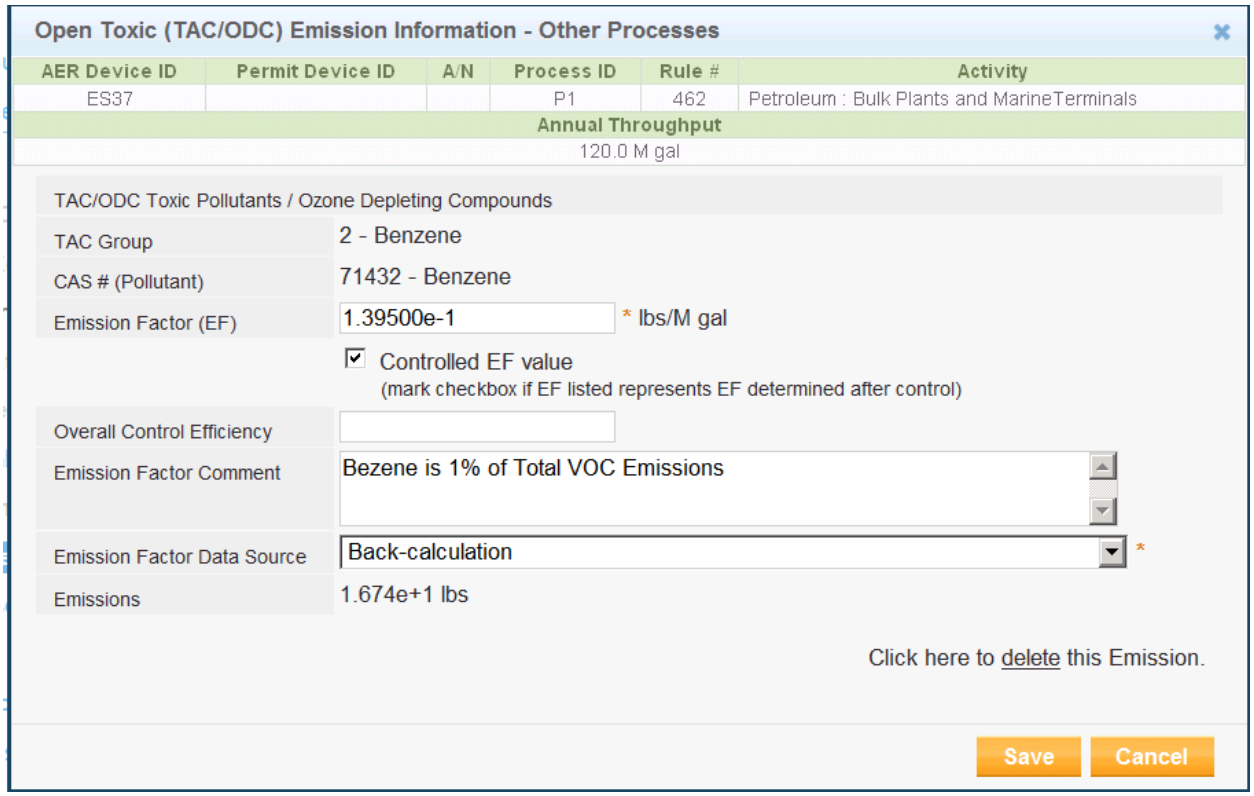
AER Device ID
Permit Device ID
A/N
Process ID
Rule #
Activity
ES37
P1
462
Petroleum : Bulk Plants and MarineTerminals
Annual Throughput
120.0 M gal
Pollutant
VOC - Volatile Organic Compounds
Emission Factor (EF)
13.9500
* lbs/M gal
Controlled EF value
(mark checkbox if EF listed represents EF determined after control)
Overall Control Efficiency
0.00000
Emission Factor Comment
Splash Loaded with No Controls
Emission Factor Data Source
AP-42
*
Emissions
1,674.00 lbs
Click here to delete this Emission.
Save
Cancel


Open Toxic (TAC/ODC) Emission Information - Other Processes
AER Device ID
Permit Device ID
A/N
Process ID
Rule #
Activity
ES37
P1
462
Petroleum : Bulk Plants and MarineTerminals
Annual Throughput
120.0 M gal
TAC/ODC Toxic Pollutants / Ozone Depleting Compounds
TAC Group
2 - Benzene
CAS # (Pollutant)
71432 - Benzene
Emission Factor (EF)
1.39500e-1
* lbs/M gal
Controlled EF value
(mark checkbox if EF listed represents EF determined after control)
Overall Control Efficiency
Emission Factor Comment
Bezene is 1% of Total VOC Emissions
Emission Factor Data Source
Back-calculation
*
Emissions
1.674e+1 lbs
Click here to delete this Emission.
Save
Cancel

CASE 2 - OPERATIONS EQUIPPED WITH VAPOR COLLECTION AND RECOVERY SYSTEMS

Company ABC operates a loading terminal with vapor balance service with submerged bottom filling technology into tanker trucks that have passed the MACT level leak test. The vapor vent line is connected to a refrigeration unit that recovers 95% of the vapor and returns it back as liquid to storage tank. ABC transferred 1,000,000 gallons of RVP 10 gasoline over the year at the following conditions:

S = 1.0 (Saturation Factor from AP-42)

T = 70ºF = 530ºR (Temperature of Gasoline)

P = 6.2 psia (True Vapor Pressure)

M = 66 lb/lb-mole (Vapor Molecular Weight)

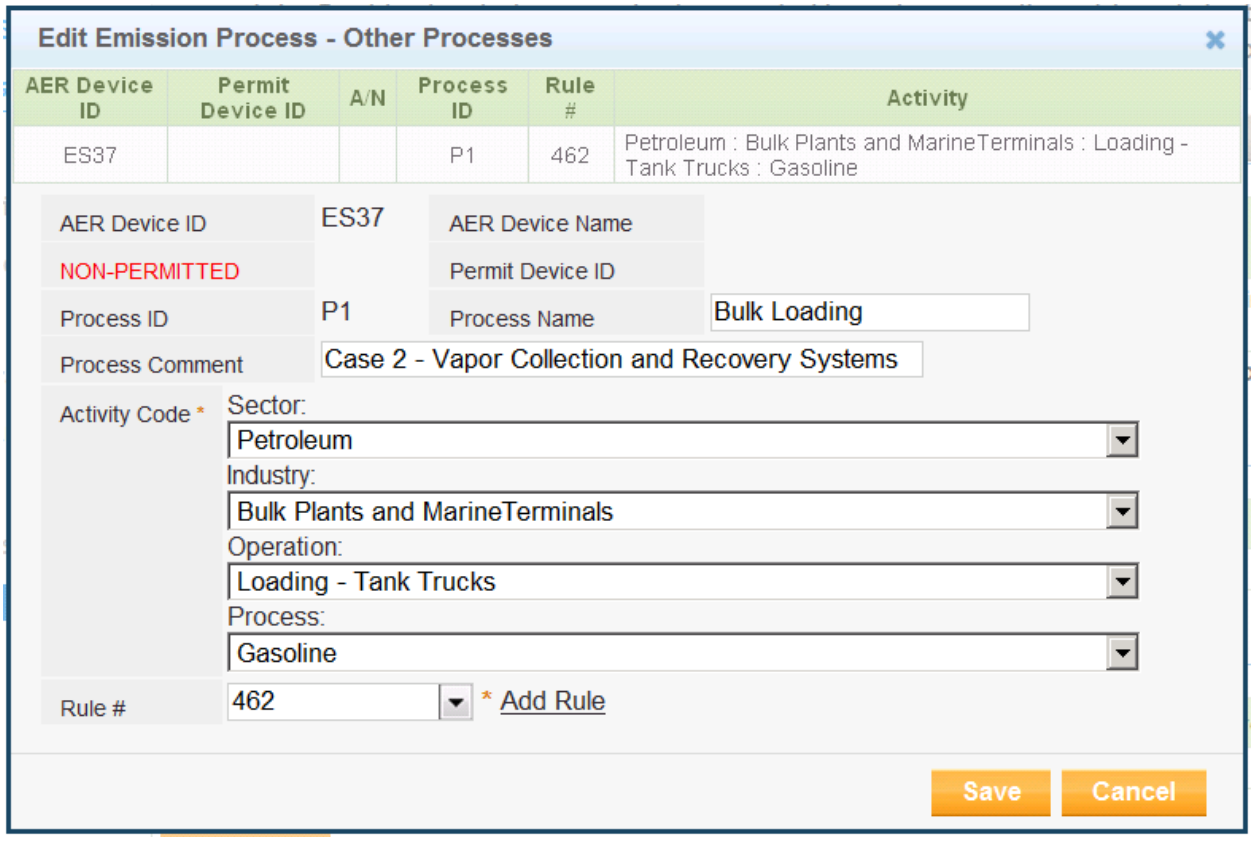
Eff_{VR} = 0.95 (Vapor Recovery Efficiency)

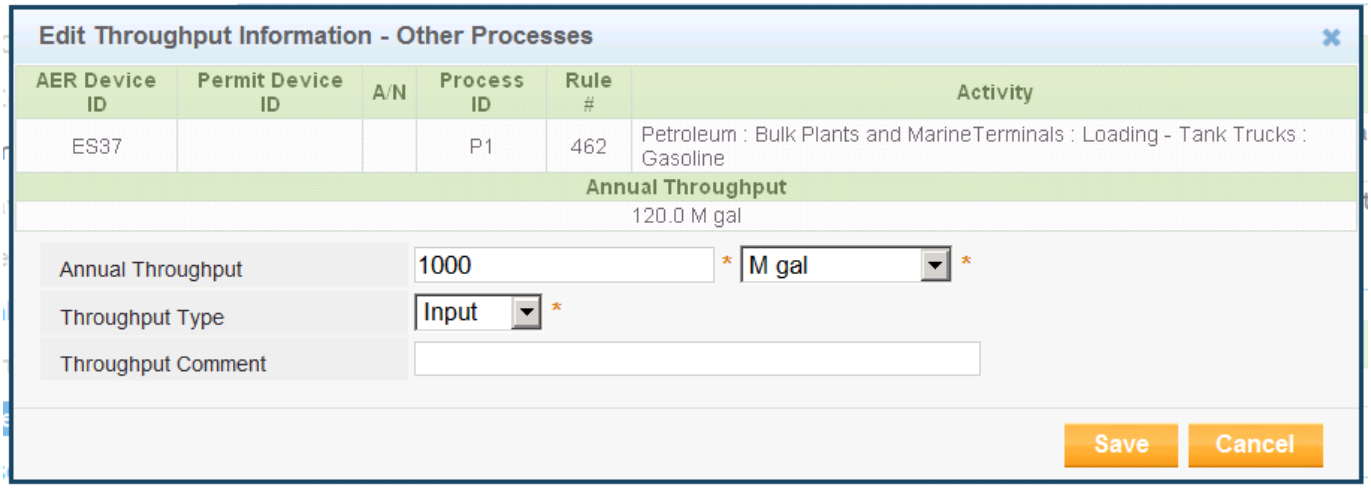
Eff_{VC} = 0.992 (Vapor Collection Efficiency)

$$L_L = \frac{12.46 \times S \times P \times M}{T} = \frac{12.46 \times 1 \times 6.2 \times 66}{530} = 9.62\ lb\ VOC/Mgal$$

Equation 3 yields the VOC emissions as follows:

$$E_2 = 1{,}000\ Mgals * 9.62\ \frac{lbs\ VOC}{Mgal} * (1 - 0.95 * 0.992) = 554\ lbs\ VOC$$

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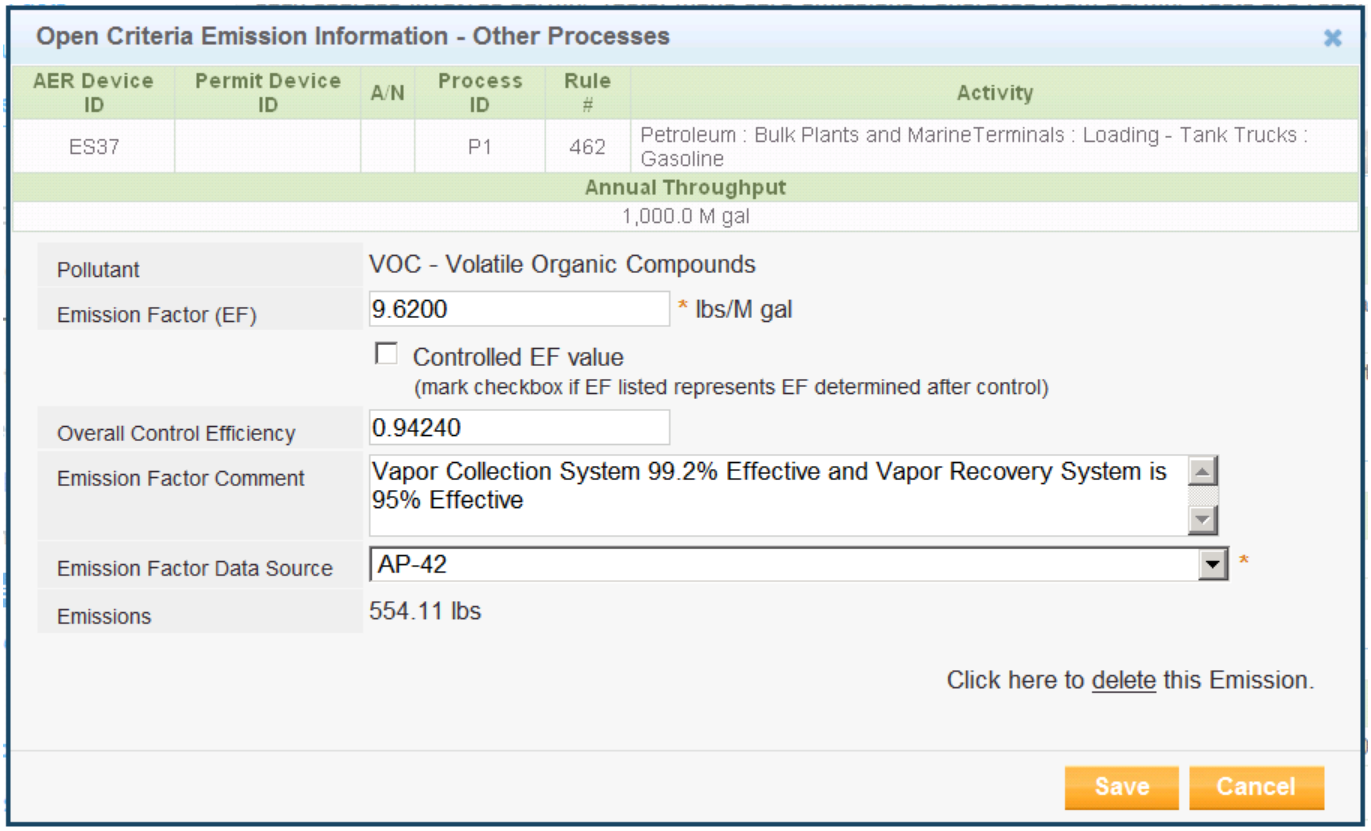
AER Device ID
Permit Device ID
A/N
Process ID
Rule #
Activity
ES37
P1
462
Petroleum : Bulk Plants and MarineTerminals : Loading - Tank Trucks : Gasoline
Annual Throughput
120.0 M gal
Annual Throughput
1000
M gal
Throughput Type
Input
Throughput Comment
Save
Cancel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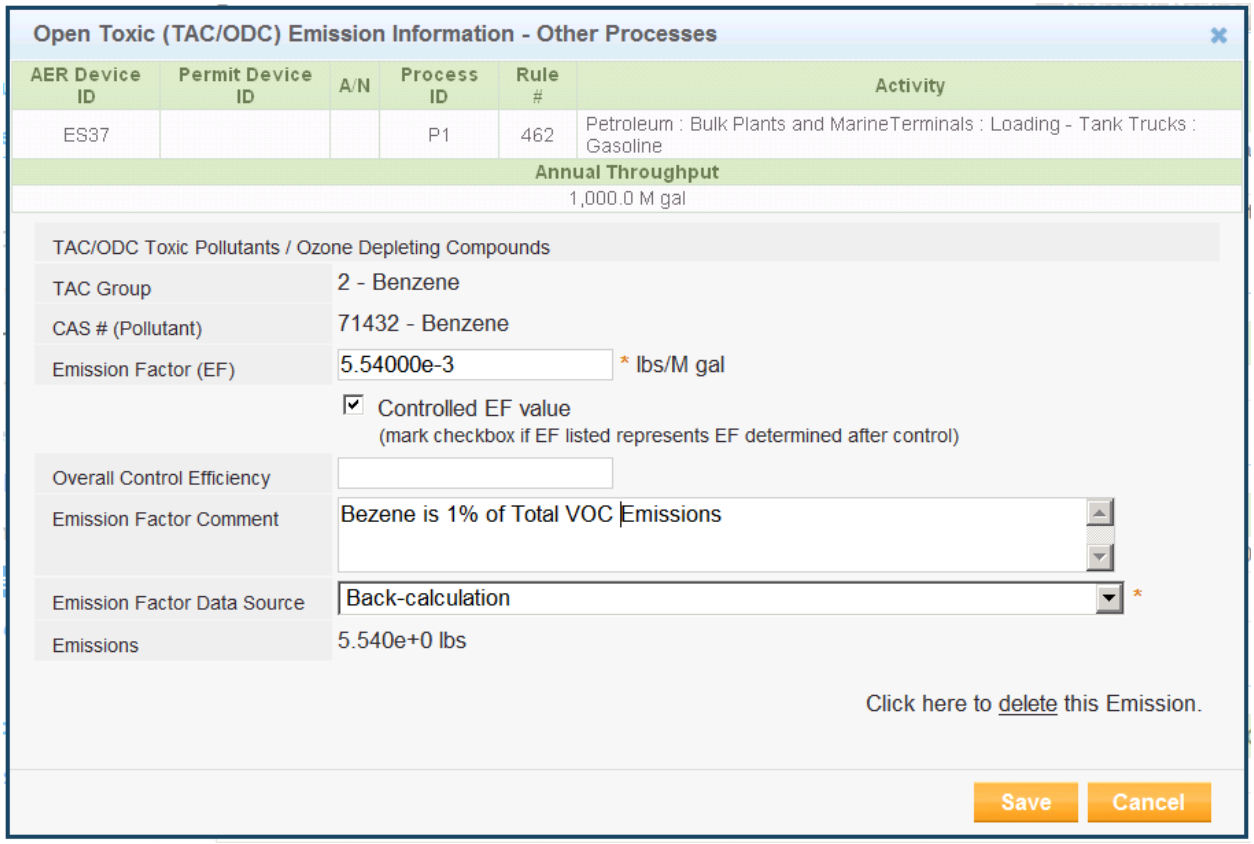
Permit Device ID
A/N
Process ID
Rule #
Activity
ES37
P1
462
Petroleum : Bulk Plants and MarineTerminals : Loading - Tank Trucks : Gasoline
Annual Throughput
1,000.0 M gal
Pollutant
VOC - Volatile Organic Compounds
Emission Factor (EF)
9.6200
lbs/M gal
Controlled EF value
(mark checkbox if EF listed represents EF determined after control)
Overall Control Efficiency
0.94240
Emission Factor Comment
Vapor Collection System 99.2% Effective and Vapor Recovery System is 95% Effective
Emission Factor Data Source
AP-42
Emissions
554.11 lbs
Click here to delete this Emission.
Save
Cancel



CASE 3 - OPERATIONS EQUIPPED WITH A VAPOR BALANCE AND DESTRUCTION SYSTEM

Over the year, company RST operates a loading terminal with submerged bottom filling 125,000,000 gallons of gasoline RVP 10 into tanker trucks that have passed the MACT level leak test at the same conditions as Case 2. The vapor vent line is connected to a system of vapor balance and then to an afterburner (thermal oxidizer -TO). The system of vapor balance achieves an overall efficiency of 49%. The oxidizer operates at 99.4% destruction efficiency.

L_L = 9.62 $lb\ VOC/Mgal$ (see Case 2 studies for loading loss factor calculation)

Q = 125,000 Mgals

Eff_{VC} = 0.992 (Vapor Collection Efficiency)

Eff_{VB} = 0.49 (Vapor Balance Efficiency)

Eff_{VD} = 0.994 (Vapor Destruction Efficiency)

Equation 4 yields the VOC emissions as follows:

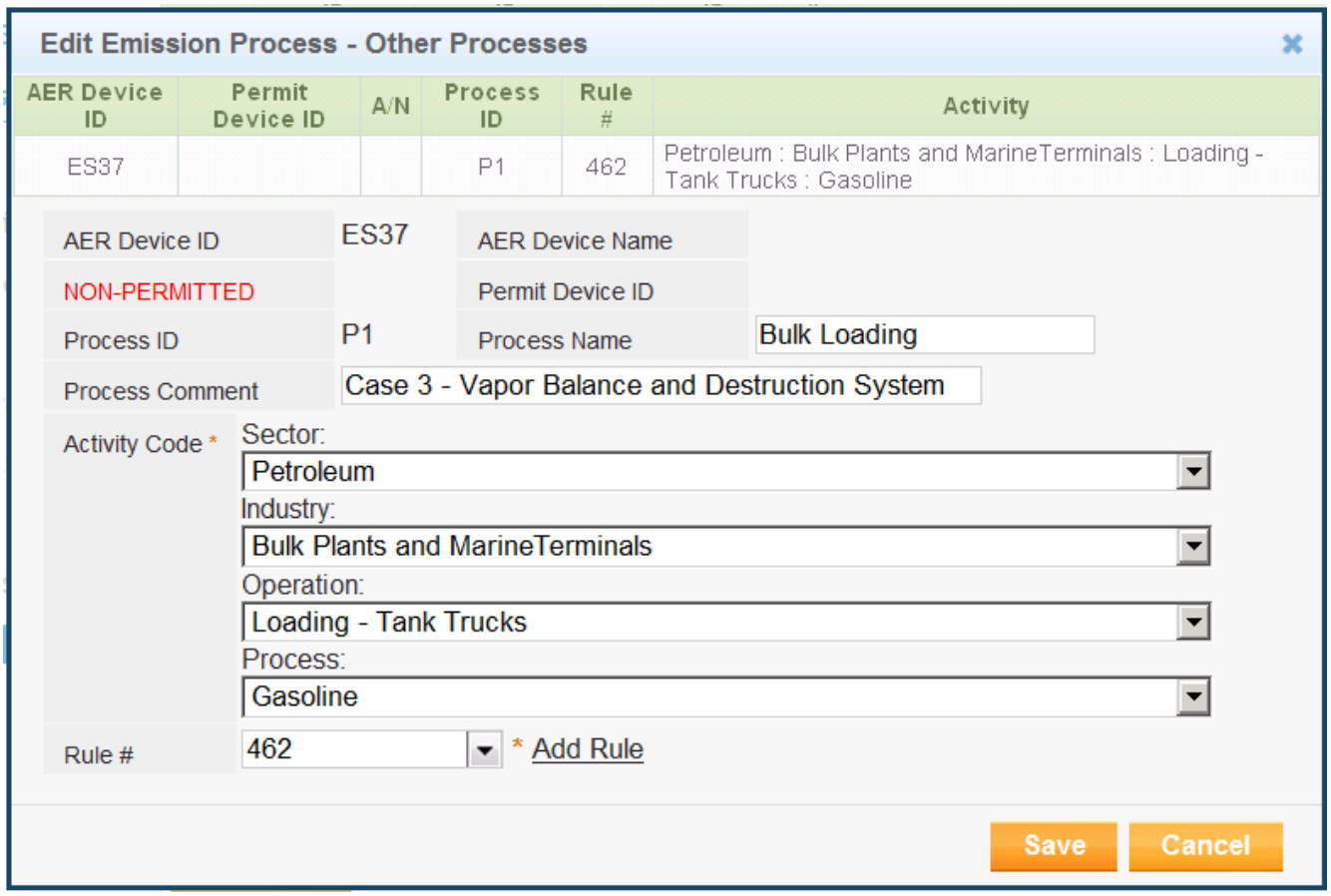
$$E_3 = 125{,}000\ Mgals * 9.62\ \frac{lbs\ VOC}{Mgal} * [1 - 0.992 * (0.49 + 0.994 - (0.49 * 0.994))] = 13{,}276\ lbs\ VOC$$

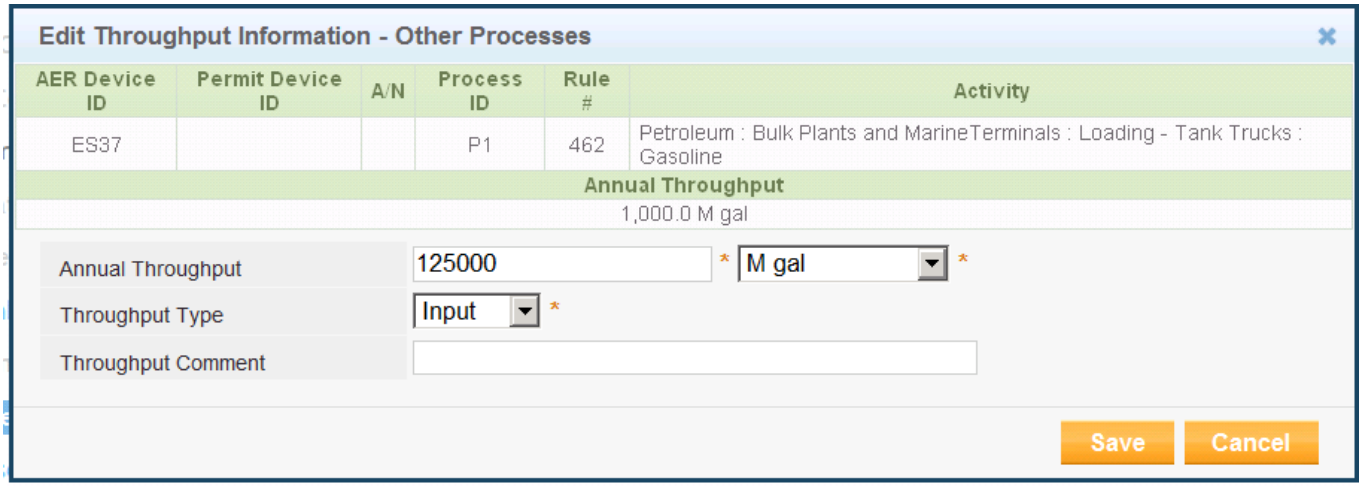
COMBUSTION EMISSIONS FROM THERMAL OXIDIZER (TO)

All thermal oxidizers used at bulk loading facilities are required to have a CARB Certification Test. In some cases, NOx, SOx, CO, and PM emission rates are tested and determined in terms of lbs of pollutant/Mgal material loaded. AQMD encourages operator to use the test results in calculating and reporting emissions.

In this example, other contaminants were not tested for the TO. Emissions for other air contaminants are calculated using the best available default factors published in AER Program Help & Support. Throughput for the TO is determined using Equation 5 as follows for gasoline RVP 10 with liquid density of 5.6 lbs/gallon:

$$TO_{Throughput} = \frac{125{,}000 * 9.62 * 0.992}{1{,}000 * 5.6} * (1 - 0.49) = 108.64\ Mgals\ of\ gasoline$$

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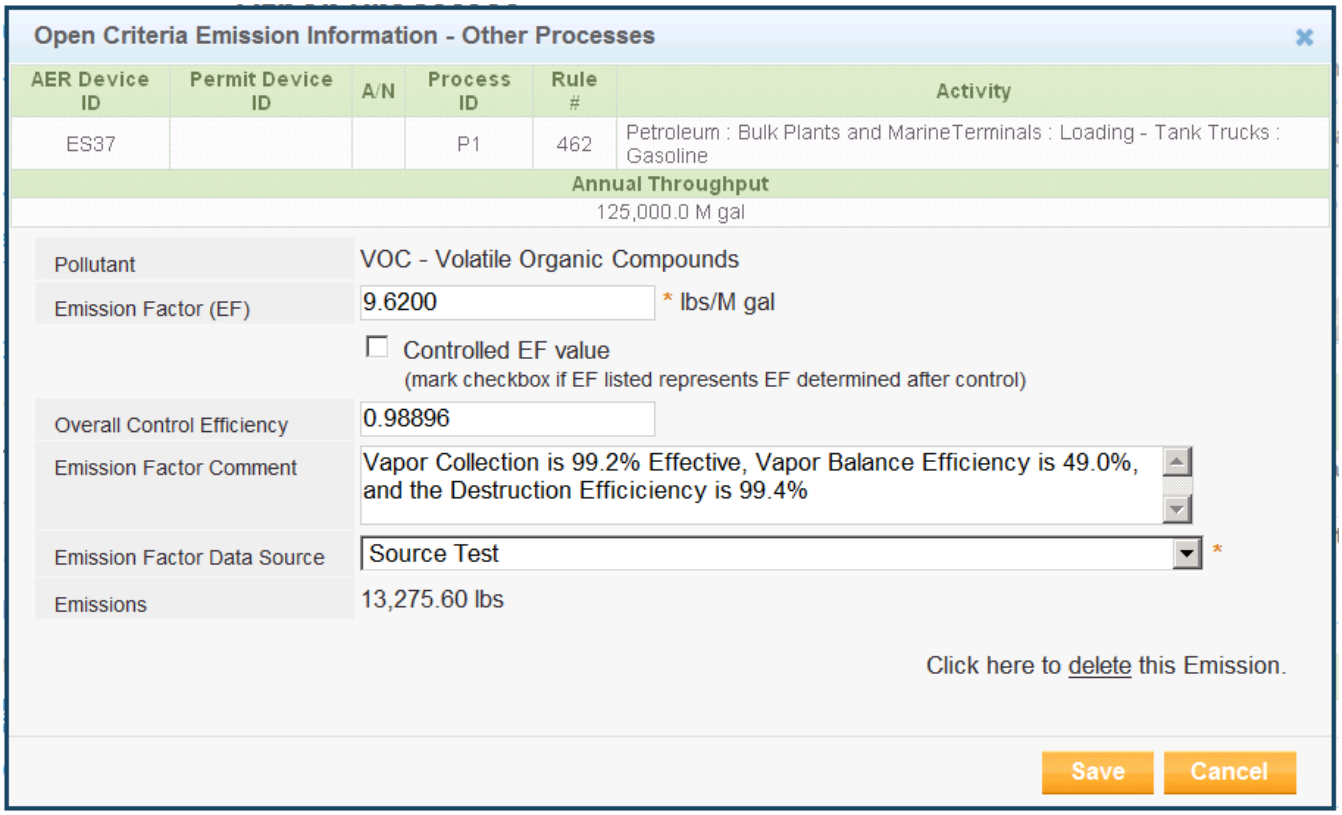
AER Device ID
Permit Device ID
A/N
Process ID
Rule #
Activity
ES37
P1
462
Petroleum : Bulk Plants and MarineTerminals : Loading - Tank Trucks : Gasoline
Annual Throughput
1,000.0 M gal
Annual Throughput
125000
M gal
Throughput Type
Input
Throughput Comment
Save
Cancel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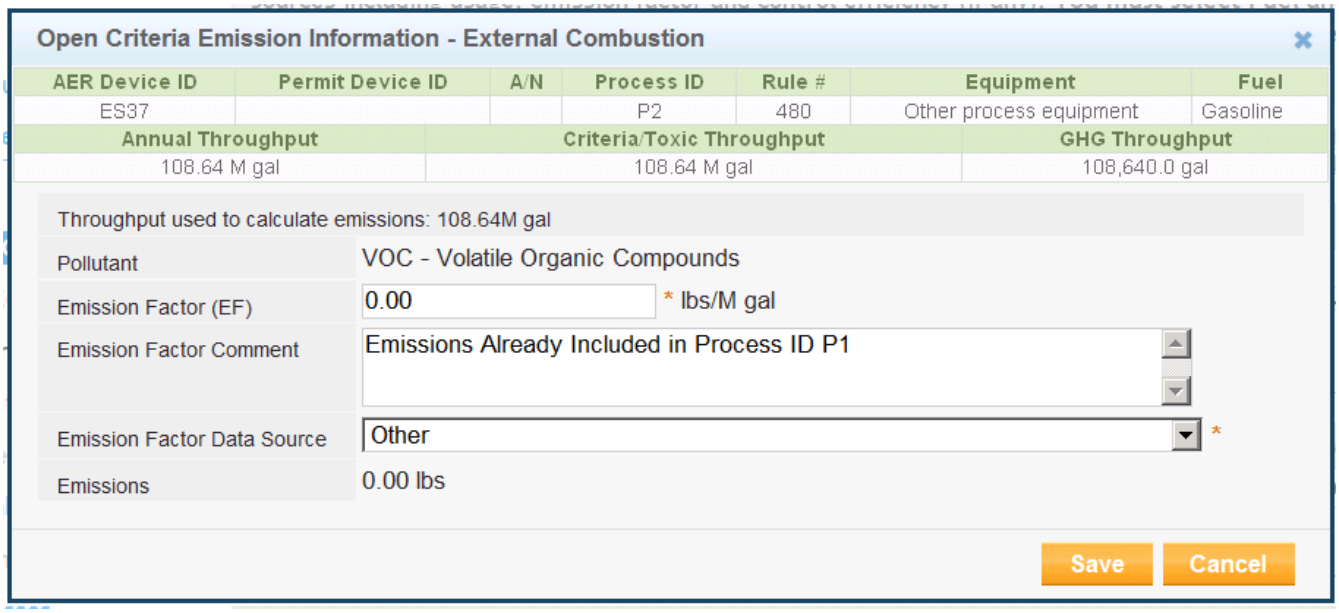
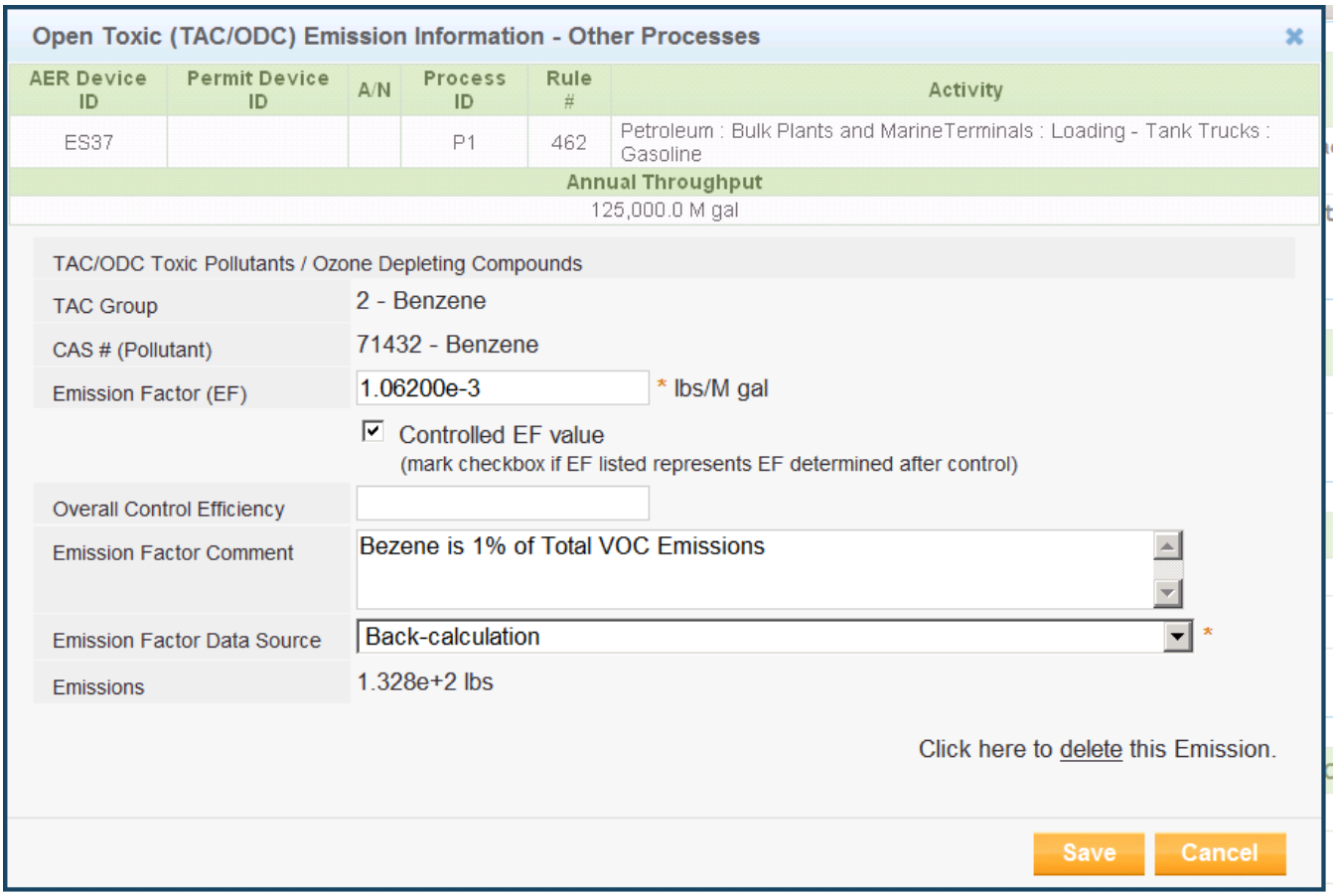
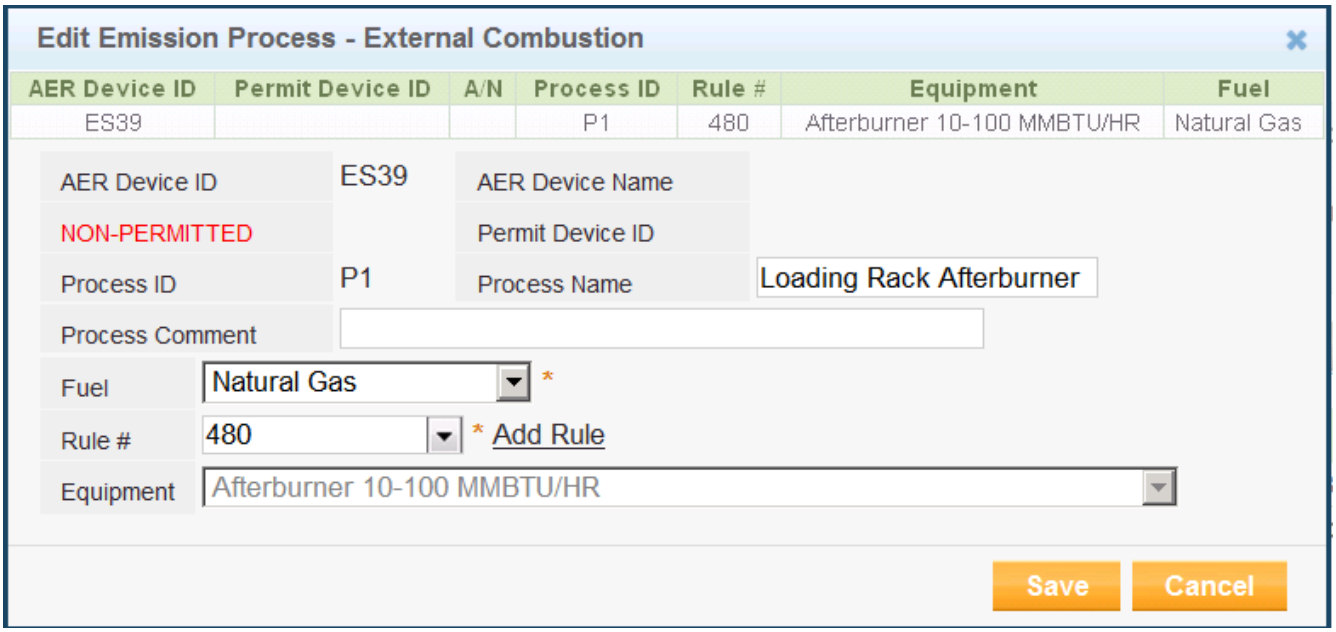
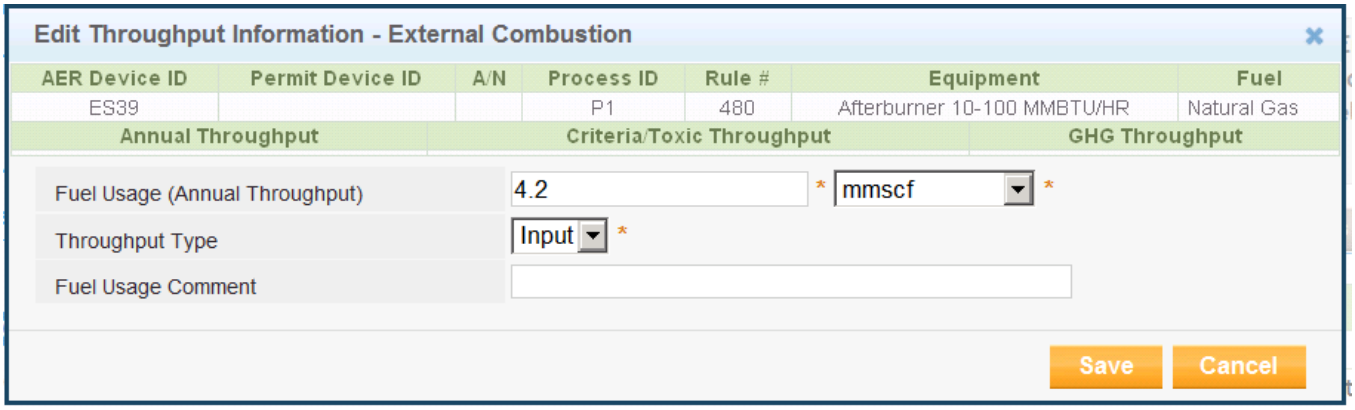
AER Device ID
Permit Device ID
A/N
Process ID
Rule #
Activity
ES37
P1
462
Petroleum : Bulk Plants and MarineTerminals : Loading - Tank Trucks : Gasoline
Annual Throughput
125,000.0 M gal
Pollutant
VOC - Volatile Organic Compounds
Emission Factor (EF)
9.6200
lbs/M gal
Controlled EF value
(mark checkbox if EF listed represents EF determined after control)
Overall Control Efficiency
0.98896
Emission Factor Comment
Vapor Collection is 99.2% Effective, Vapor Balance Efficiency is 49.0%, and the Destruction Efficiciency is 99.4%
Emission Factor Data Source
Source Test
Emissions
13,275.60 lbs
Click here to delete this Emission.
Save
Cancel


Open Criteria Emission Information - External Combustion
AER Device ID
Permit Device ID
A/N
Process ID
Rule #
Equipment
Fuel
ES37
P2
480
Other process equipment
Gasoline
Annual Throughput
Criteria/Toxic Throughput
GHG Throughput
108.64 M gal
108.64 M gal
108,640.0 gal
Throughput used to calculate emissions: 108.64M gal
Pollutant
VOC - Volatile Organic Compounds
Emission Factor (EF)
0.00
* lbs/M gal
Emission Factor Comment
Emissions Already Included in Process ID P1
Emission Factor Data Source
Other
*
Emissions
0.00 lbs
Save
Cancel


Open Toxic (TAC/ODC) Emission Information - Other Processes
AER Device ID
Permit Device ID
A/N
Process ID
Rule #
Activity
ES37
P1
462
Petroleum : Bulk Plants and MarineTerminals : Loading - Tank Trucks : Gasoline
Annual Throughput
125,000.0 M gal
TAC/ODC Toxic Pollutants / Ozone Depleting Compounds
TAC Group
2 - Benzene
CAS # (Pollutant)
71432 - Benzene
Emission Factor (EF)
1.06200e-3
* lbs/M gal
Controlled EF value
(mark checkbox if EF listed represents EF determined after control)
Overall Control Efficiency
Emission Factor Comment
Bezene is 1% of Total VOC Emissions
Emission Factor Data Source
Back-calculation
*
Emissions
1.328e+2 lbs
Click here to delete this Emission.
Save
Cancel





Report Criteria and toxic compounds using default factors as below:

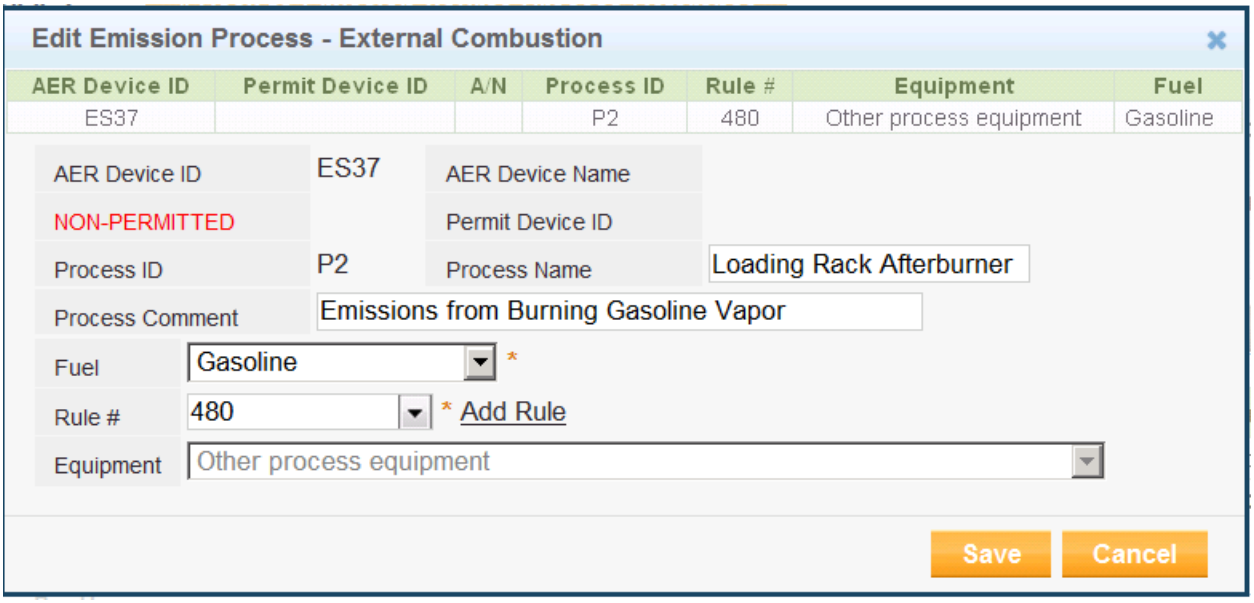
Criteria Emissions (lbs)

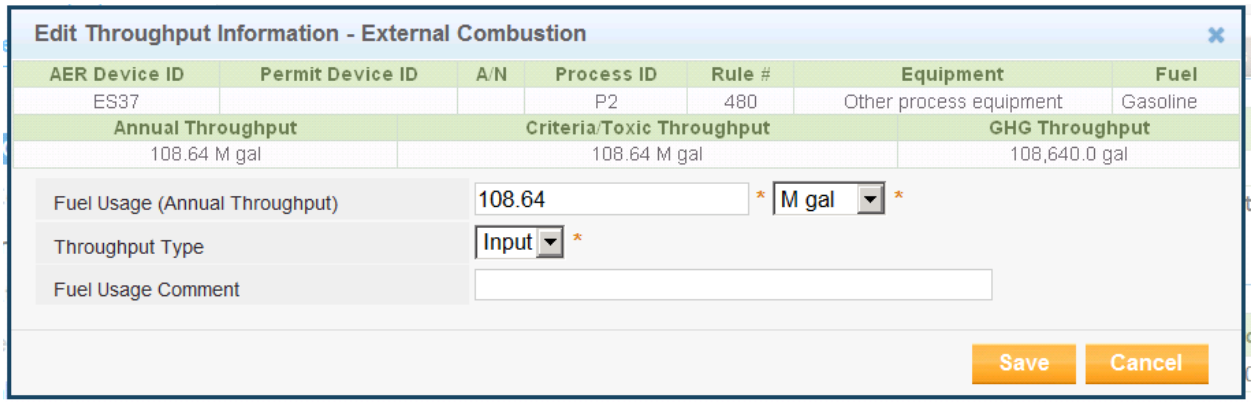
	Pollutant	EF	Unit	EF Data Source	Overall CE	Emissions
Open	VOC	7.00	lbs / mmscf	AQMD default		29.40
Open	NOx	130.00	lbs / mmscf	AQMD default		546.00
Open	SOx	0.60	lbs / mmscf	AQMD default		2.52
Open	CO	35.00	lbs / mmscf	AQMD default		147.00
Open	PM	7.50	lbs / mmscf	AQMD default		31.50

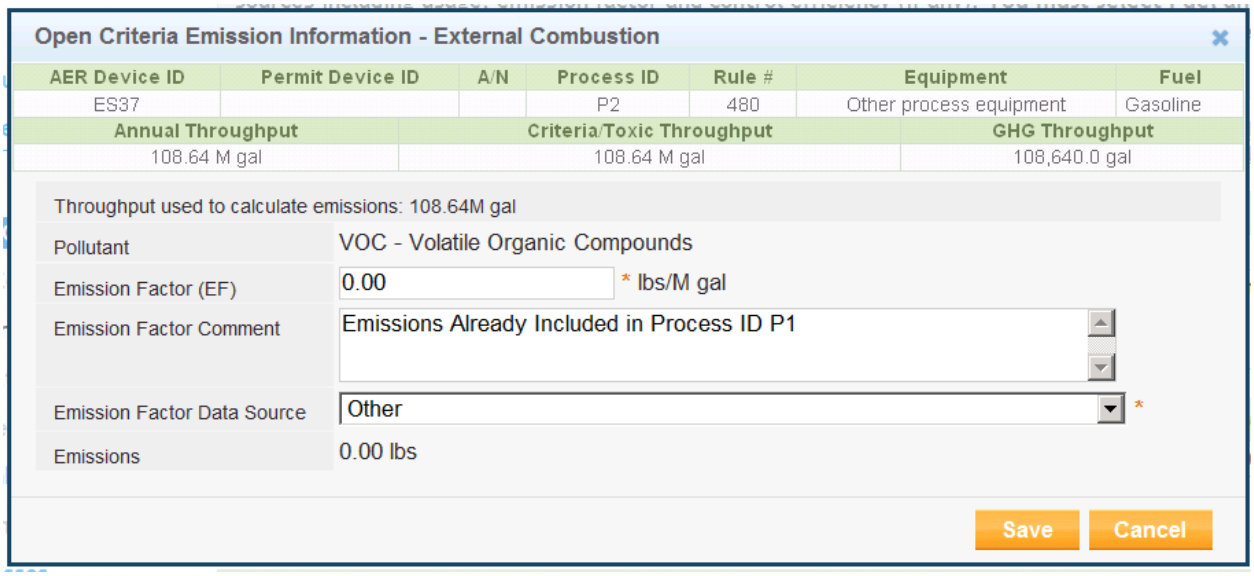
Toxic (TAC/ODC) Emissions (lbs)

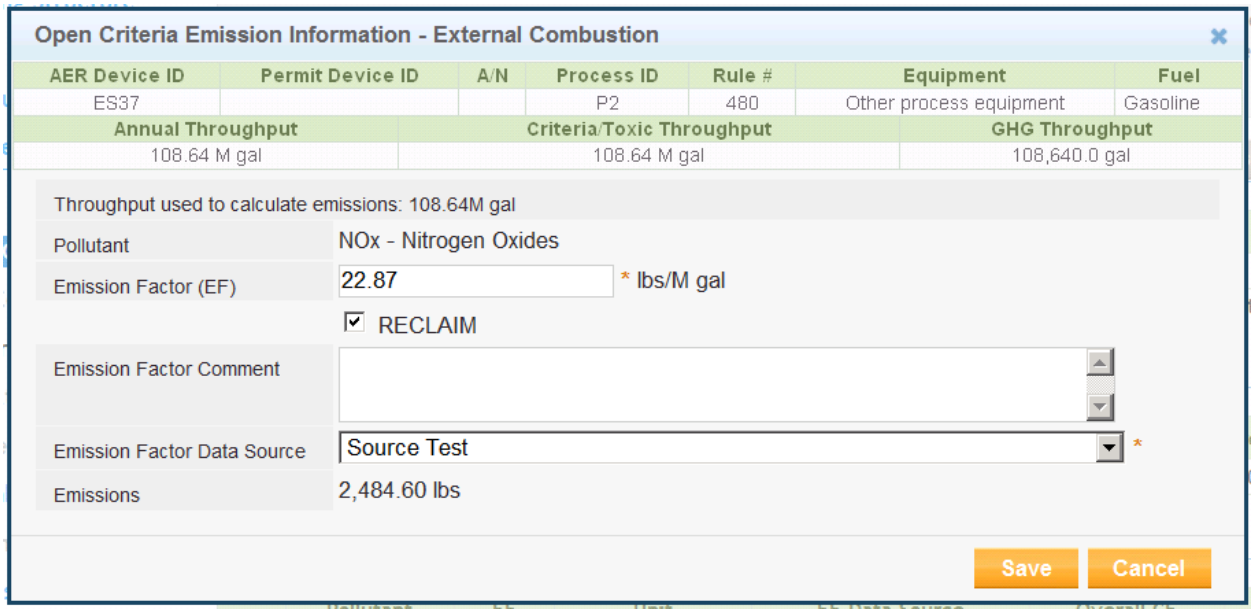
	TAC/ODC Group	CAS #	EF	Unit	EF Data Source	Overall CE	Emissions
Open	Benzene	71432	5.80000e-3	lbs / mmscf	AQMD default		2.436e-2
Open	Formaldehyde	50000	1.23000e-2	lbs / mmscf	AQMD default		5.166e-2
Open	PAHs [PAH, POM]	1151	1.00000e-4	lbs / mmscf	AQMD default		4.200e-4
Open	PAHs [PAH, POM]	91203	3.00000e-4	lbs / mmscf	AQMD default		1.260e-3
Open	Acetaldehyde	75070	3.10000e-3	lbs / mmscf	AQMD default		1.302e-2
Open	Acrolein	107028	2.70000e-3	lbs / mmscf	AQMD default		1.134e-2
Open	Ammonia	7664417	1.80000e+1	lbs / mmscf	AQMD default		7.560e+1
Open	Ethyl benzene	100414	6.90000e-3	lbs / mmscf	AQMD default		2.898e-2
Open	Hexane	110543	4.60000e-3	lbs / mmscf	AQMD default		1.932e-2
Open	Toluene	108883	2.65000e-2	lbs / mmscf	AQMD default		1.113e-1
Open	Xylenes	1330207	1.97000e-2	lbs / mmscf	AQMD default		8.274e-2

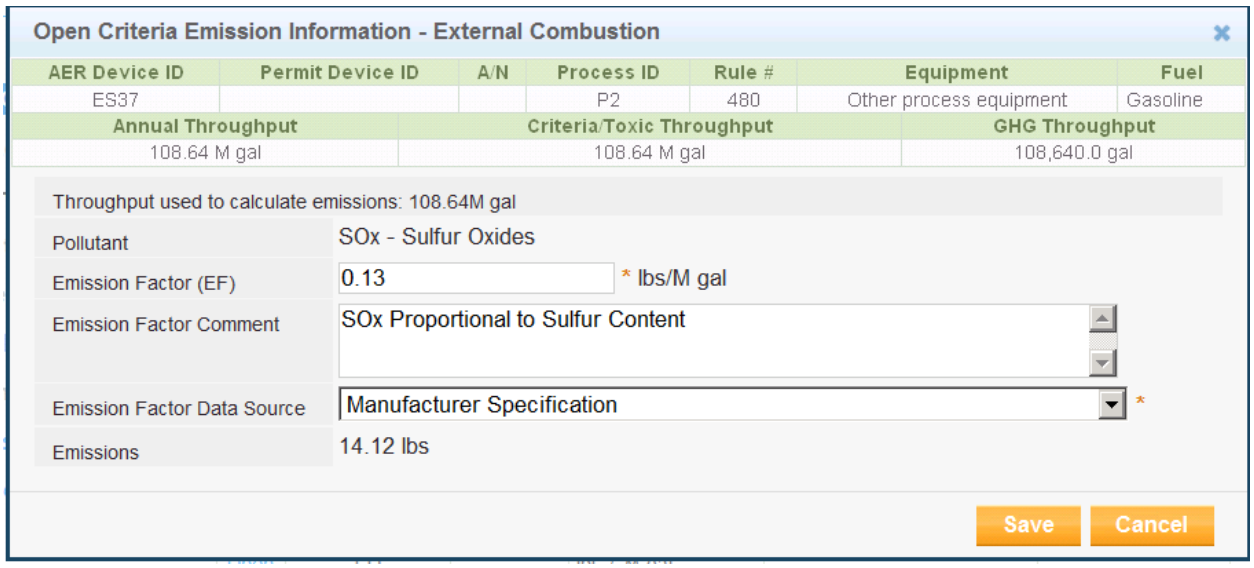
Add New




Edit Throughput Information - External Combustion
AER Device ID
Permit Device ID
A/N
Process ID
Rule #
Equipment
Fuel
ES37
P2
480
Other process equipment
Gasoline
Annual Throughput
Criteria/Toxic Throughput
GHG Throughput
108.64 M gal
108.64 M gal
108,640.0 gal
Fuel Usage (Annual Throughput)
108.64
M gal
Throughput Type
Input
Fuel Usage Comment
Save
Cancel


Open Criteria Emission Information - External Combustion
AER Device ID
Permit Device ID
A/N
Process ID
Rule #
Equipment
Fuel
ES37
P2
480
Other process equipment
Gasoline
Annual Throughput
Criteria/Toxic Throughput
GHG Throughput
108.64 M gal
108.64 M gal
108,640.0 gal
Throughput used to calculate emissions: 108.64M gal
Pollutant
VOC - Volatile Organic Compounds
Emission Factor (EF)
0.00
lbs/M gal
Emission Factor Comment
Emissions Already Included in Process ID P1
Emission Factor Data Source
Other
Emissions
0.00 lbs
Save
Cancel


Open Criteria Emission Information - External Combustion
AER Device ID
Permit Device ID
A/N
Process ID
Rule #
Equipment
Fuel
ES37
P2
480
Other process equipment
Gasoline
Annual Throughput
Criteria/Toxic Throughput
GHG Throughput
108.64 M gal
108.64 M gal
108,640.0 gal
Throughput used to calculate emissions: 108.64M gal
Pollutant
NOx - Nitrogen Oxides
Emission Factor (EF)
22.87
lbs/M gal
RECLAIM
Emission Factor Comment
Emission Factor Data Source
Source Test
Emissions
2,484.60 lbs
Save
Cancel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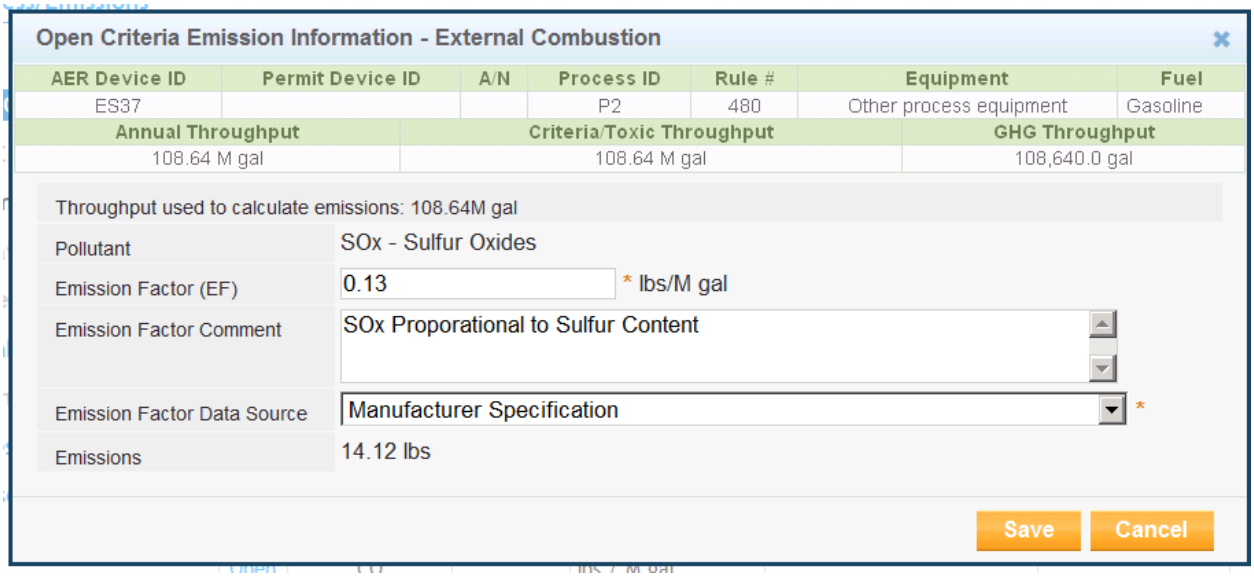
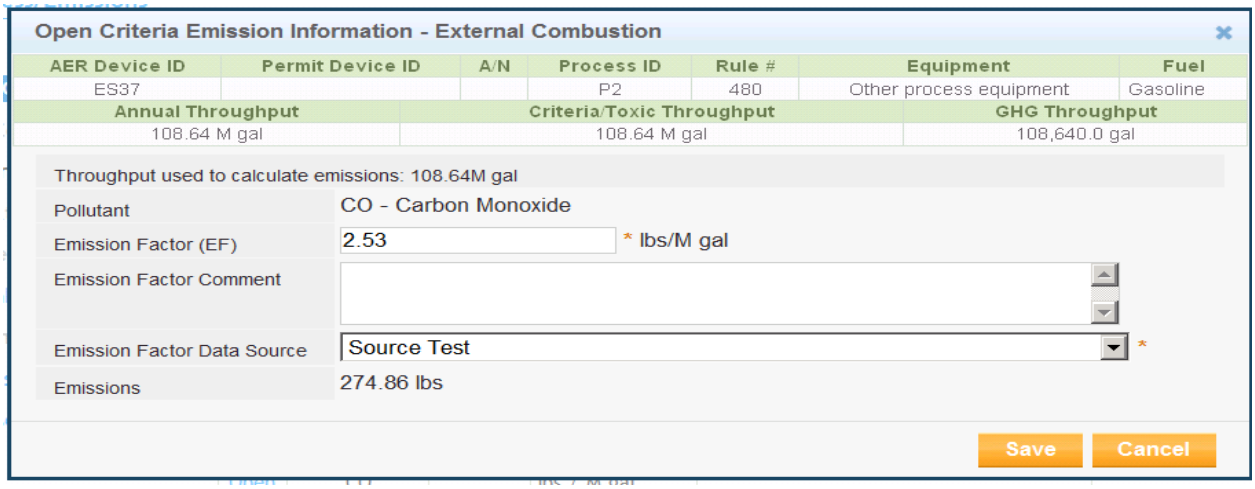
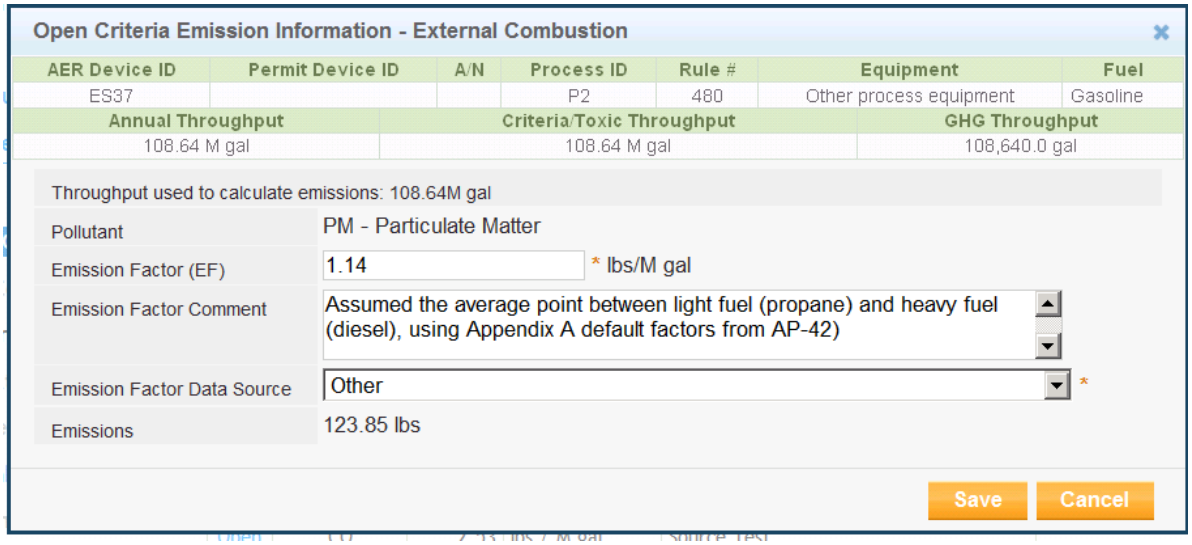
Permit Device ID
A/N
Process ID
Rule #
Equipment
Fuel
ES37
P2
480
Other process equipment
Gasoline
Annual Throughput
Criteria/Toxic Throughput
GHG Throughput
108.64 M gal
108.64 M gal
108,640.0 gal
Throughput used to calculate emissions: 108.64M gal
Pollutant
SOx - Sulfur Oxides
Emission Factor (EF)
0.13
* lbs/M gal
Emission Factor Comment
SOx Proportional to Sulfur Content
Emission Factor Data Source
Manufacturer Specification
*
Emissions
14.12 lbs
Save
Cancel


Open Criteria Emission Information - External Combustion
AER Device ID
Permit Device ID
A/N
Process ID
Rule #
Equipment
Fuel
ES37
P2
480
Other process equipment
Gasoline
Annual Throughput
Criteria/Toxic Throughput
GHG Throughput
108.64 M gal
108.64 M gal
108,640.0 gal
Throughput used to calculate emissions: 108.64M gal
Pollutant
SOx - Sulfur Oxides
Emission Factor (EF)
0.13
* lbs/M gal
Emission Factor Comment
SOx Proporational to Sulfur Content
Emission Factor Data Source
Manufacturer Specification
*
Emissions
14.12 lbs
Save
Cancel


Open Criteria Emission Information - External Combustion
AER Device ID
Permit Device ID
A/N
Process ID
Rule #
Equipment
Fuel
ES37
P2
480
Other process equipment
Gasoline
Annual Throughput
Criteria/Toxic Throughput
GHG Throughput
108.64 M gal
108.64 M gal
108,640.0 gal
Throughput used to calculate emissions: 108.64M gal
Pollutant
CO - Carbon Monoxide
Emission Factor (EF)
2.53
* lbs/M gal
Emission Factor Comment
Emission Factor Data Source
Source Test
*
Emissions
274.86 lbs
Save
Cancel



Facilities must report toxic emission as well for this process. If default emission factors are needed, use the following, in pounds/1000 gallons of equivalent gasoline burned.

POLLUTANT	CAS NO.	EMISSION FACTOR
Benzene	71432	3.8061
1,3-Butadiene	106990	0.9183
Formaldehyde	50000	3.4520
Nickel	7440020	0.0033
PAHs	1151	0.1438

Note that facilities that are subject to AB2588 Quadrennial reporting requirements must report emissions for toxic species listed in Table B-4 in the Supplemental Instructions for AB2588 Facilities – May 2015.