



# Proposed Rule (PR) 1147.2

NO<sub>x</sub> Reductions from Metal Processing Equipment

Working Group Meeting #3

November 6, 2019

Call-in Number / Passcode

866-705-2554 / 680785

# Agenda

- Summary of Working Group Meeting #2
- Process Temperatures, Furnace Types, and NO<sub>x</sub> Source Tests
- NO<sub>x</sub> Formation Pathways
- Continuation of BARCT Analysis
  - Technology Assessment
  - Establishing Proposed BARCT Emission Limit
- Next Steps

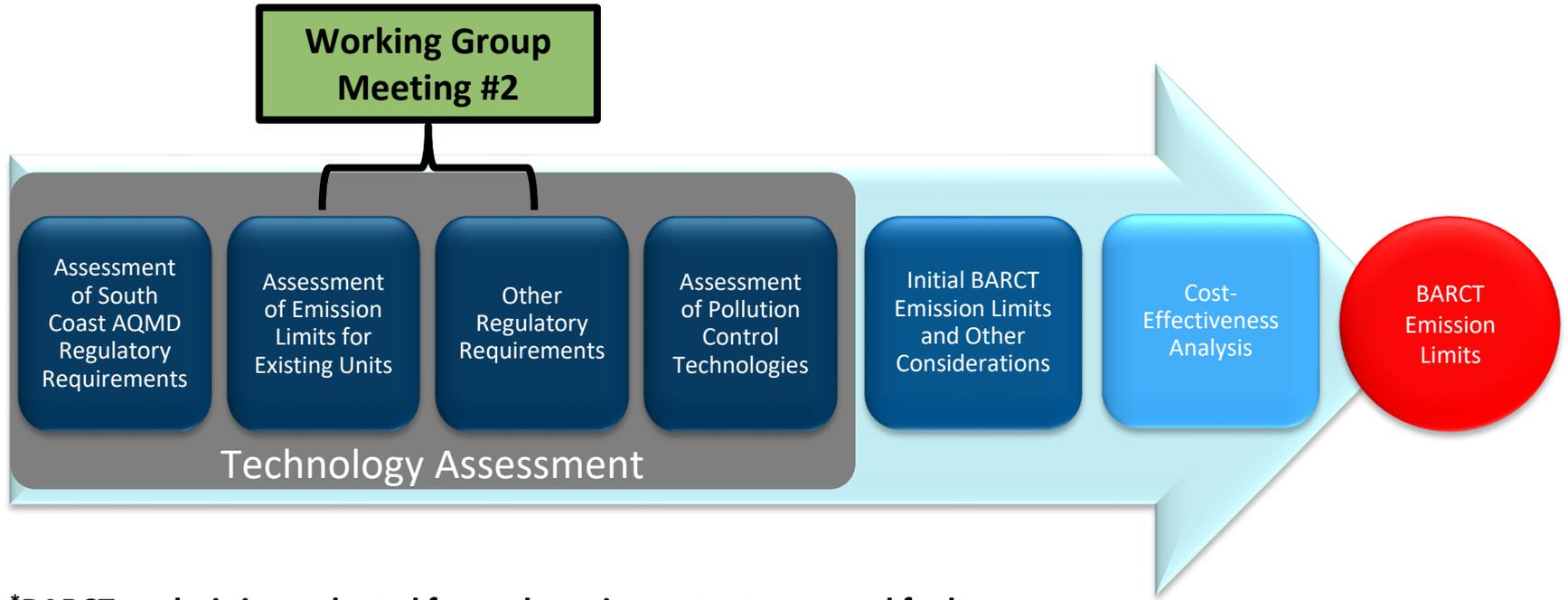


# Summary of Working Group Meeting #2

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- Rule 1147 Equipment Data Request
- BARCT Analysis
  - Assessment of Emission Limits for Existing Units
    - Metal Melting Furnaces
    - Metal Heat Treating Furnaces
  - Other Regulatory Requirements

# Working Group Meeting #2



**\*BARCT analysis is conducted for each equipment category and fuel type**



# Process Temperatures, Furnace Types, and NO<sub>x</sub> Source Tests

# Background & Approach

- Stakeholders commented about effects of differing temperatures and furnace types on NO<sub>x</sub> emissions
- Staff analyzed
  - Process temperature versus source test result
  - Process temperature and furnace type versus source test result
- Analyses of process temperatures and furnace types seek to answer two questions:

1. Is there a correlation between process temperatures and source test results?

2. Is there a correlation between process temperatures, furnace types, and source test results?

# Process Temperatures and Source Test Results – Methodology

- Evaluated metal melting and metal heat treating equipment categories separately for both RECLAIM and non-RECLAIM facilities
- For both equipment categories, graphed process temperatures and NO<sub>x</sub> source test results to assess any correlations
  - Process temperature obtained from permits
- For both equipment categories, grouped units into two temperature ranges
  - Focused on lowest NO<sub>x</sub> source test results in each temperature group

# Process Temperatures and Source Test Results – Assumptions

- Only furnaces that had both a process temperature and NO<sub>x</sub> source test result were included in this analysis
  - 228 of 250 units (87%) had both a source test result and listed a process temperature in its permit
  - Remaining units were not incorporated into this analysis
- Similar units processing the same materials at the same facility were given the same process temperature
- Average process temperature was used when a range of process temperatures was listed

# Process Temperatures & Furnace Types – Methodology and Assumptions

## ■ Methodology

- Evaluated metal melting and metal heat treating equipment categories separately for both RECLAIM and non-RECLAIM facilities
- For both equipment categories, graphed furnace type and process temperature with NO<sub>x</sub> source test result to assess any correlations
  - Process temperature and furnace type obtained from permits

## ■ Assumptions

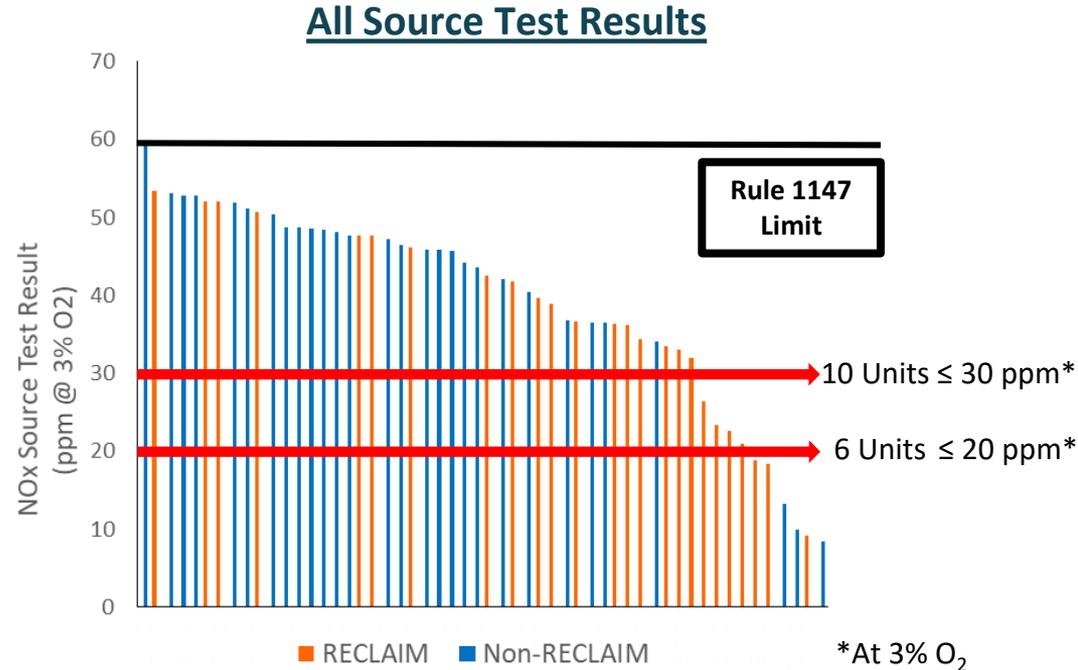
- Furnace type as identified by permit's equipment description may be categorized differently over time and across facilities
- Only furnaces that had both a process temperature and a NO<sub>x</sub> source test result were included in this analysis



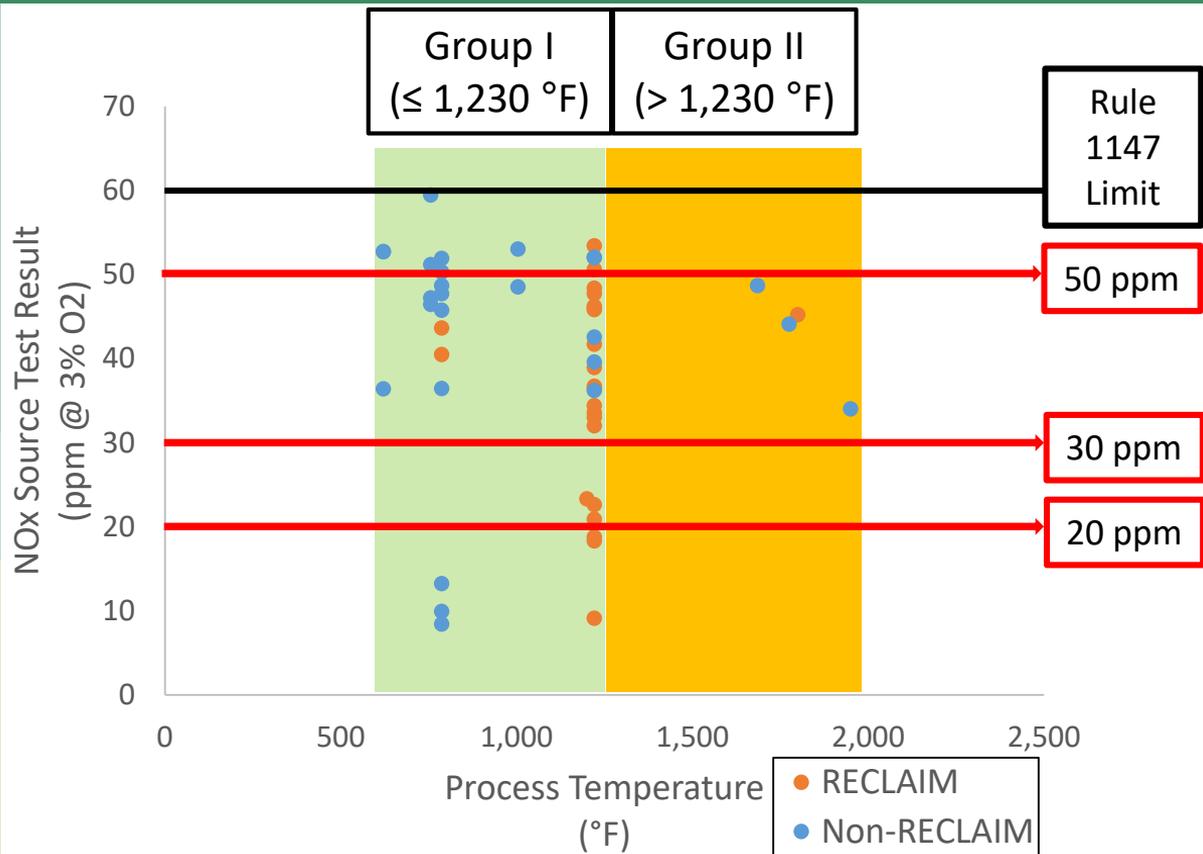
# Metal Melting Furnaces

# Metal Melting – Source Test Results from Working Group #2 Summary

- 54 NO<sub>x</sub> source test results
- 50 of the 54 units with source tests also listed a process temperature
- Source test results range from 8.4 to 59.6 ppm NO<sub>x</sub> from RECLAIM and non-RECLAIM facilities
  - 10 units ≤ 30 ppm
  - 6 units ≤ 20 ppm



# Metal Melting – Process Temperatures and Source Test Results



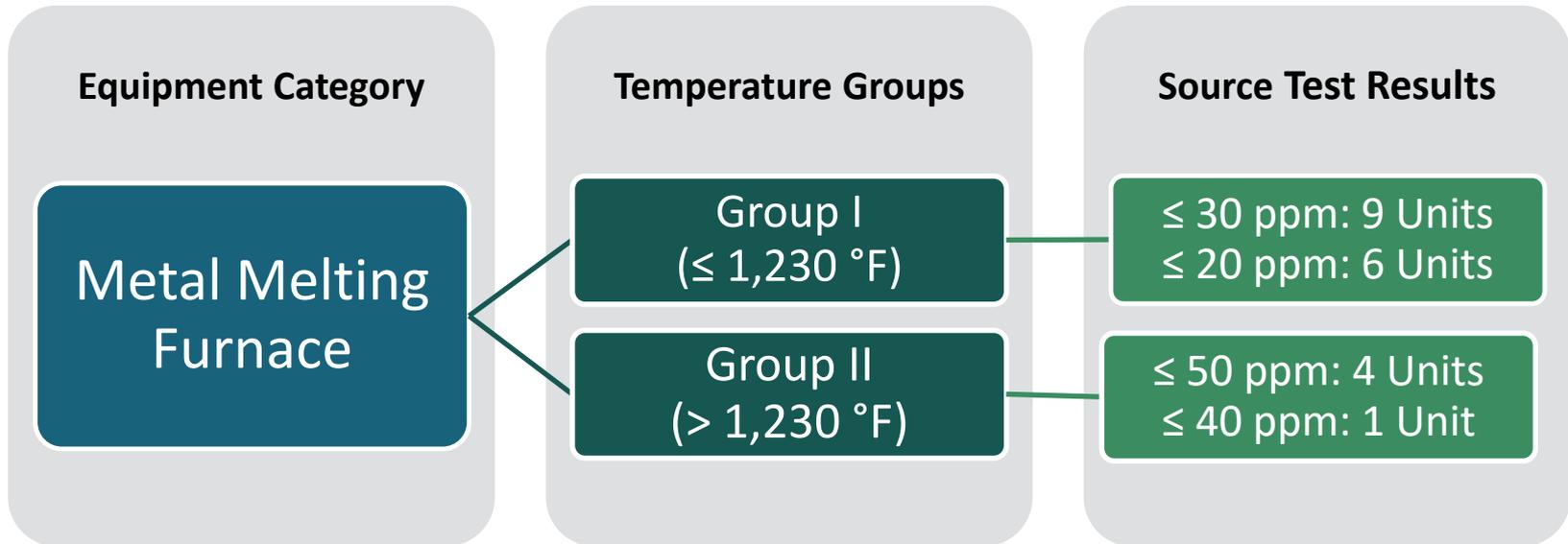
## Observations

Unit Count	≤ 1,230 °F	> 1,230 °F
≤ 50 ppm*	35	4
≤ 30 ppm*	9	No Units
≤ 20 ppm*	6	

\*At 3% O<sub>2</sub>

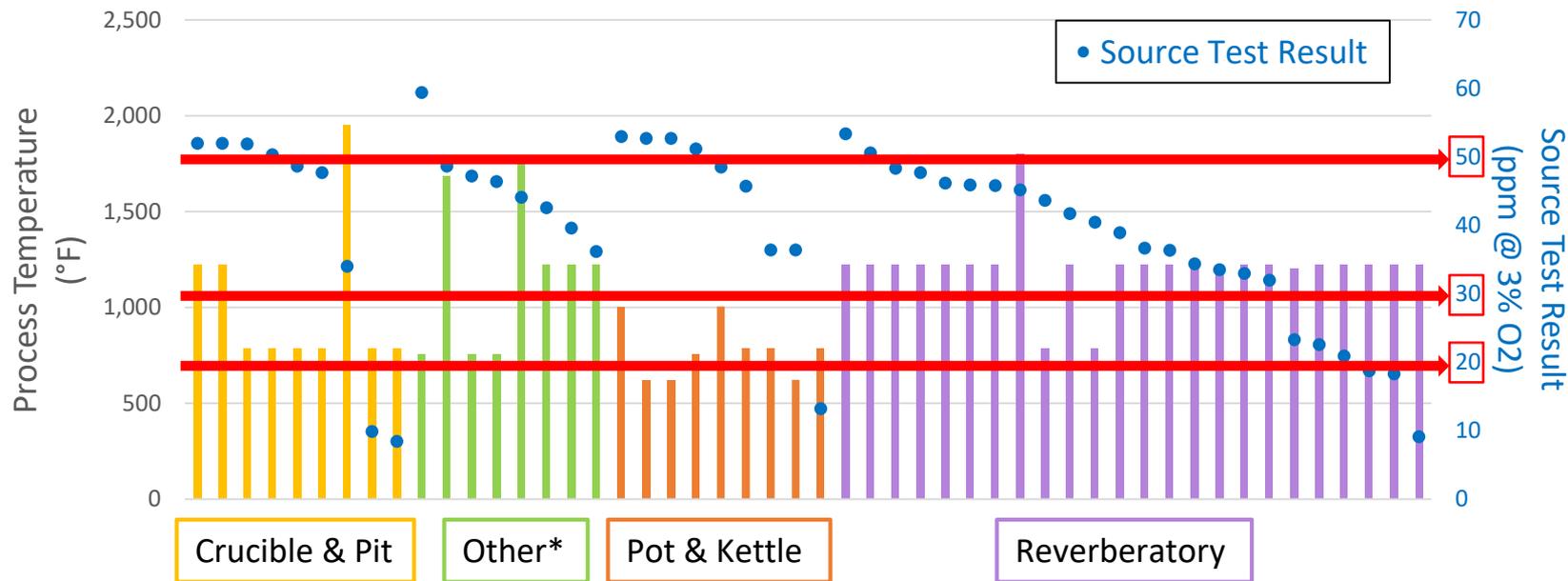
# Metal Melting – Process Temperatures and Source Test Results

1. Is there a correlation between process temperatures and source test results\*?



\*At 3% O<sub>2</sub>

# Metal Melting – Process Temperatures and Furnace Types



\* Other: Box, Furnace, Rotary (Non-Sweating), and Stack

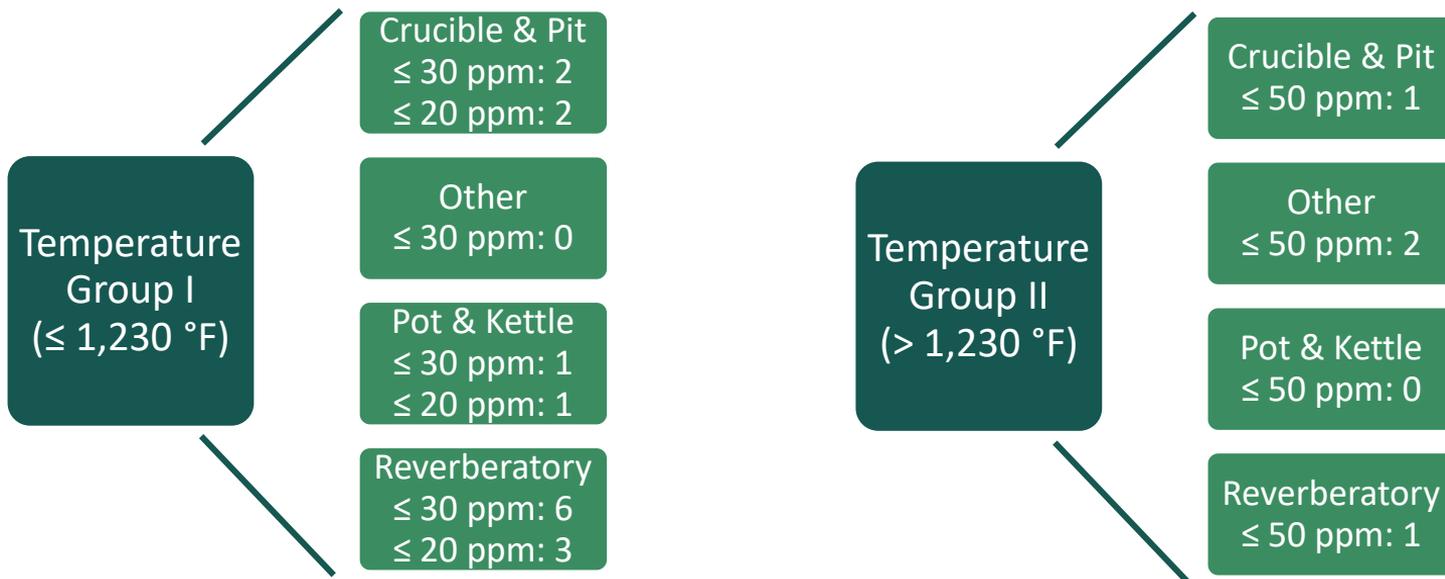
Unit Count	Crucible & Pit	Other	Pot & Kettle	Reverberatory	Total
≤ 50 ppm†	5	7	5	22	39
≤ 30 ppm†	2	0	1	6	9
≤ 20 ppm†	2	0	1	3	6

†At 3% O<sub>2</sub>

# Metal Melting – Process Temperatures and Furnace Types

2. Is there a correlation between process temperatures, furnace types, and source test results\*?

\*At 3% O<sub>2</sub>



All furnace types except Other exhibit a wide range of NOx source test results

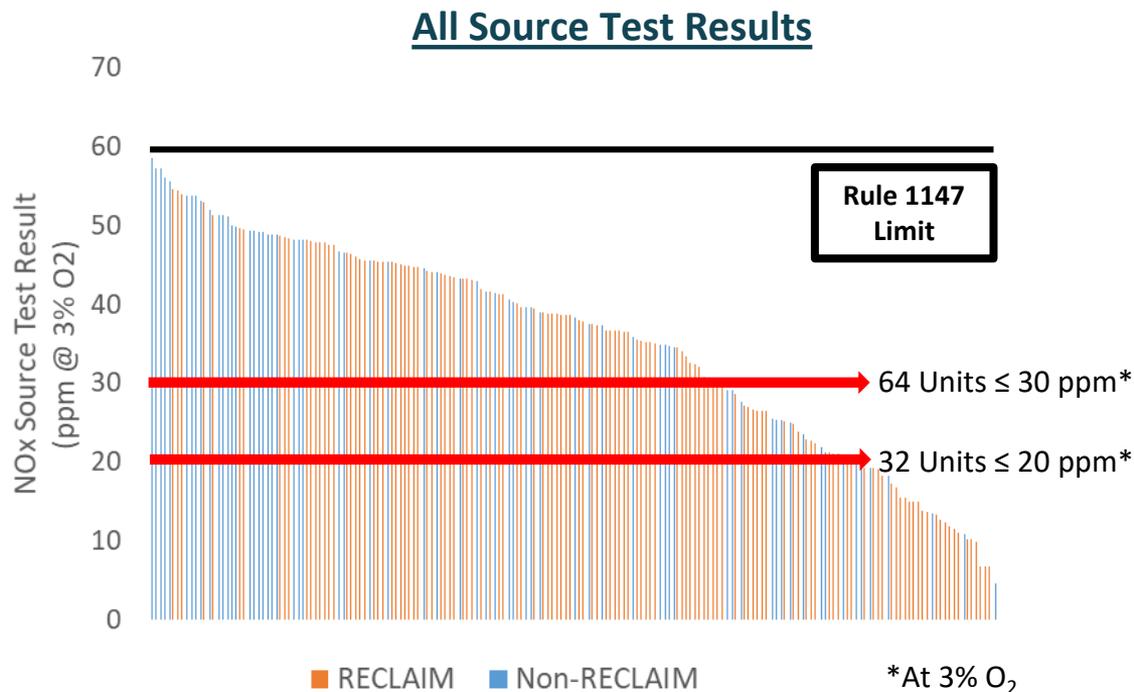


# **Metal Heat Treating Furnaces**

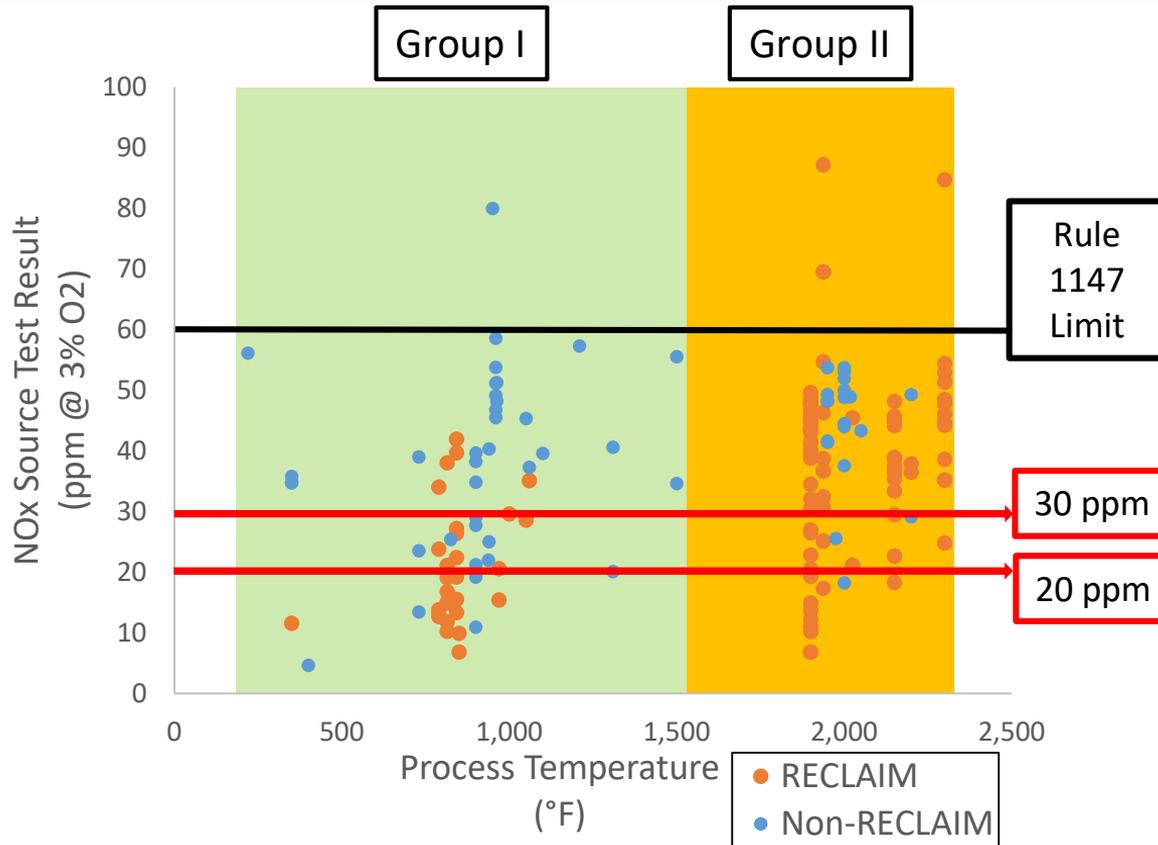
# Metal Heat Treating – Source Test Results from Working Group #2 Summary

Slide Updated

- 196 NOx source tests
- Results range from 4.6 to 115 ppm NOx from RECLAIM and non-RECLAIM facilities
  - 64 units  $\leq$  30 ppm
  - 32 units  $\leq$  20 ppm
- 178 of the 196 units with source tests also listed a process temperature

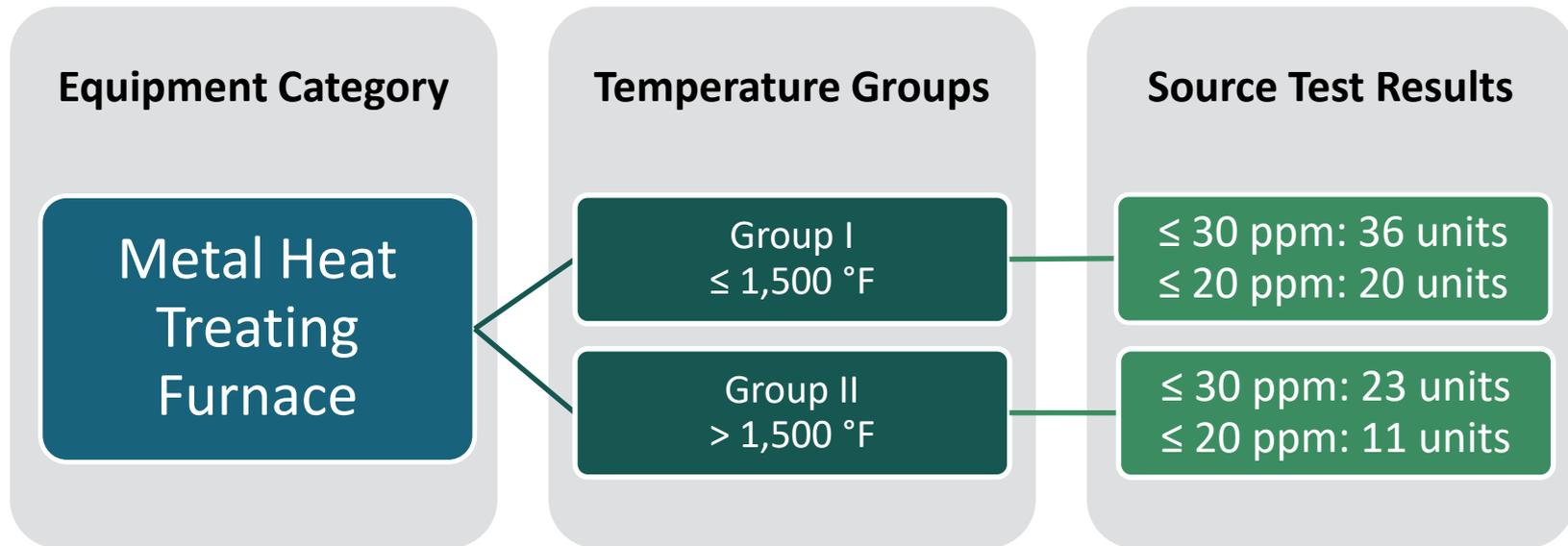


# Metal Heat Treating – Process Temperatures and Source Test Results



# Metal Heat Treating – Process Temperatures and Source Test Results

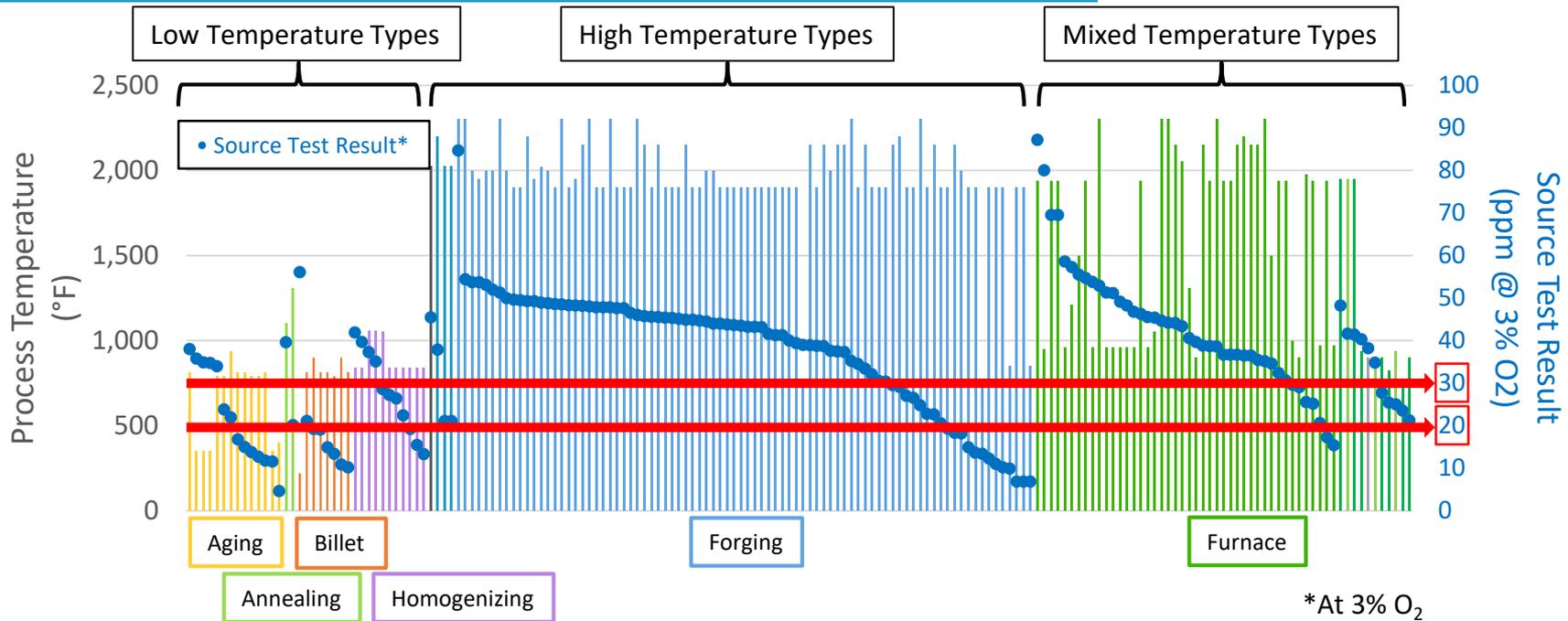
1. Is there a correlation between process temperatures and source test results\*?



- No correlation observed across temperatures
- $\text{NO}_x$  concentrations  $\leq 20$  ppm exist across temperatures

\*At 3%  $\text{O}_2$

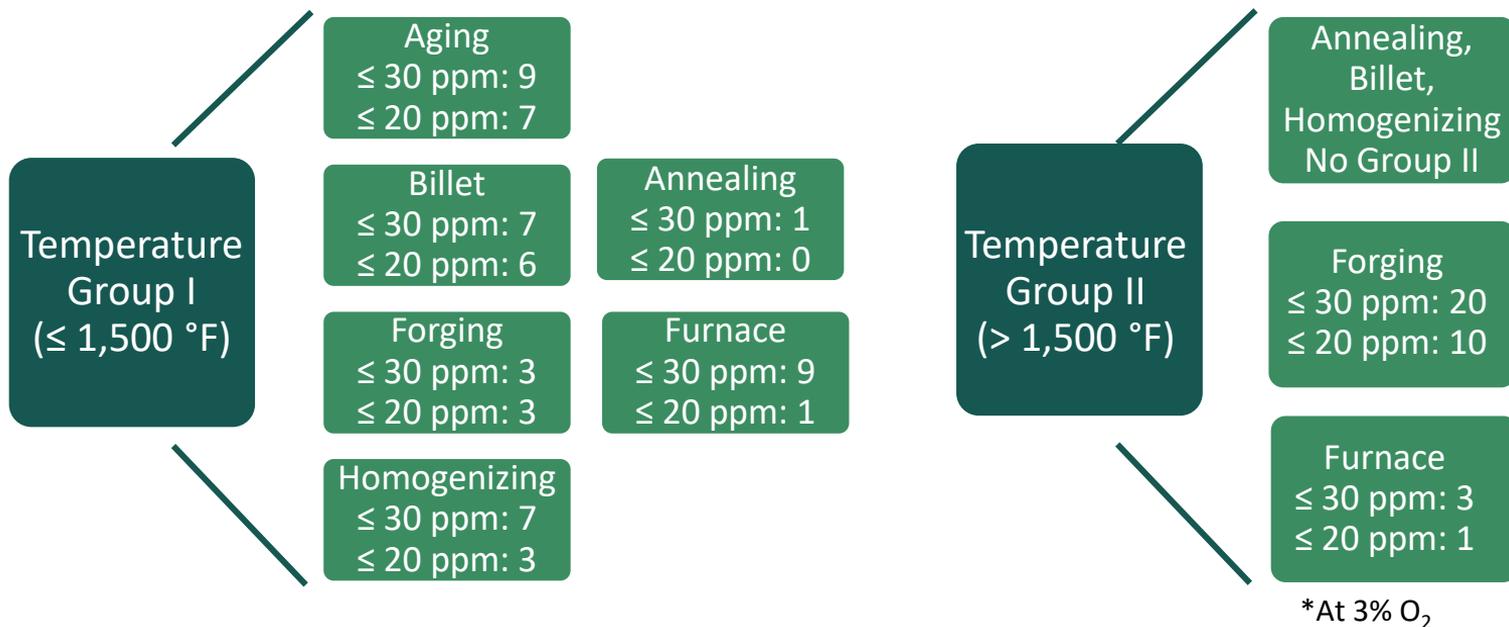
# Metal Heat Treating – Process Temperatures and Source Test Results



Unit Count	Aging	Annealing	Billet	Forging	Furnace	Homogenizing	Total
≤ 30 ppm	9	1	7	23	12	7	59
≤ 20 ppm	7	0	6	13	2	3	31

# Metal Heat Treating – Process Temperatures and Furnace Types

2. Is there a correlation between process temperatures, furnace types, and source test results\*?



- Forging-related units majority of applications > 1,500 °F
- NO<sub>x</sub> concentrations ≤ 20 ppm exist for all types across all temperatures



# $\text{NO}_x$ Formation Pathways

# Thermal & Process NO<sub>x</sub>

- Thermal NO<sub>x</sub> is formed from dissociation of N<sub>2</sub> from elevated temperatures, namely flame temperature
- Other sources of NO<sub>x</sub>, although minor for natural gas, are captured in source test results
- Electric furnaces not required to source test for NO<sub>x</sub>
  - EPA AP-42\* provides a 0.22 lb NO<sub>x</sub>/ton material processed emission factor for use in electric arc furnaces processing steel
    - 682 tons/month processed = 5 lb NO<sub>x</sub>/day

\*EPA. Emission Factor Documentation for AP-42 Section 12.5.1 – Iron and Steel Production – Steel Minimills Final Report. Apr 2009.  
<https://www3.epa.gov/ttn/chief/ap42/ch12/final/c12s0501.pdf>

# Electric Furnaces & Process NO<sub>x</sub>

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- Approximately 150 electric furnaces identified
- Largest electric furnaces have low NO<sub>x</sub> emissions relative to natural gas-fired furnaces
  - Majority of electric furnaces emit < 1 lb/day NO<sub>x</sub>
- Staff will continue to investigate cost-effectiveness of SCR control for process NO<sub>x</sub>

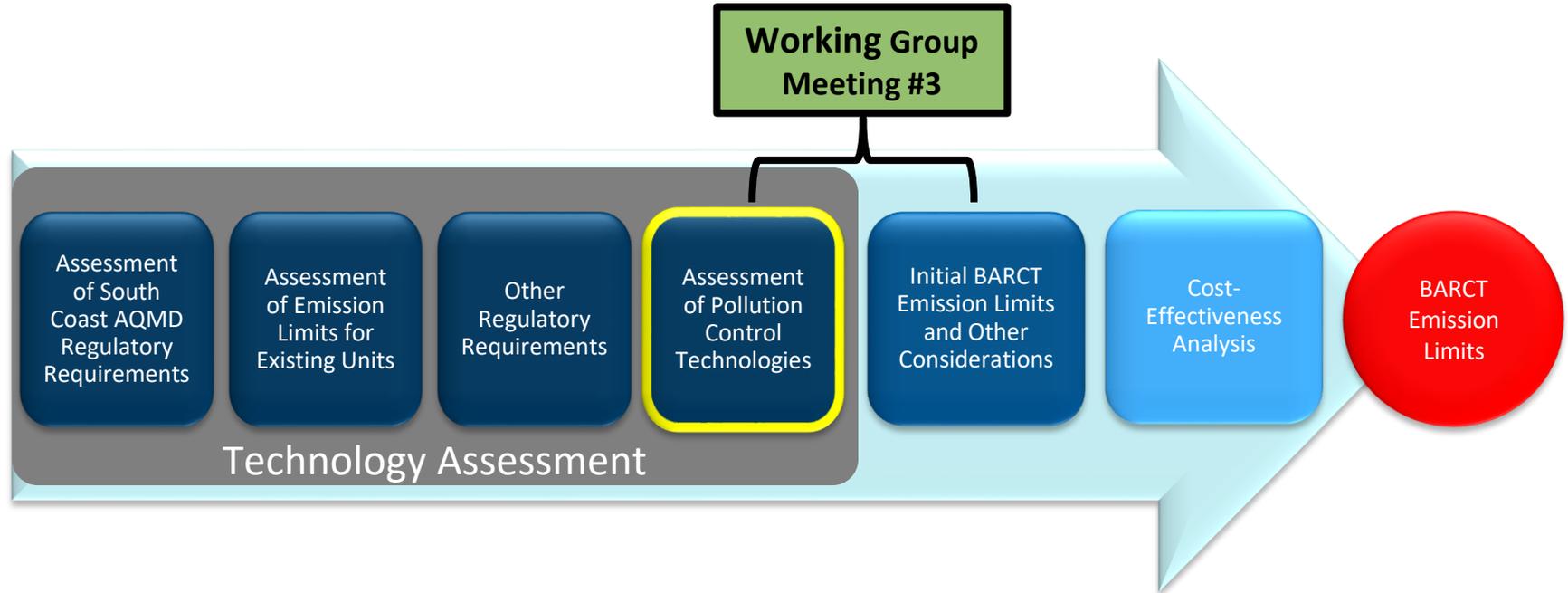
## Largest Electric Furnaces

Electric Rating (KW)	Material Process Rate (ton/day equivalent)	NO <sub>x</sub> Emissions (lbs/day)
2,500	83.2	18.3
1,250	39.9	8.8
1,250	39.9	8.8
1,250	39.9	8.8
1,250	39.9	8.8
1,500	31.7	7.0



# Continuation of BARCT Analysis

# Working Group Meeting #3: Current Progress



**\*BARCT analysis is conducted for each equipment category and fuel type**

# Working Group

## Meeting #2 Findings

- Previous Work Group Meetings established initial categories, analyzed permit limits and source test results, and reviewed existing regulations of other agencies
- Average NO<sub>x</sub> concentration in proposed universe
  - Metal Melting: 44 ppm
  - Metal Heat Treating: 42 ppm
- Other California air district BARCT limit
  - Metal Melting: 60 ppm
  - Metal Heat Treating: 60 ppm
- U.S. EPA BACT limit
  - Metal Melting: 33 ppm
  - Metal Heat Treating: 39 ppm

# Assessment of Pollution Control Technologies – Methodology & Approach

Researched multiple sources for available NO<sub>x</sub> control technologies

- Scientific Literature
- Vendor meetings
- Consultant meetings
- Facility site visits



Analyzed Sources to:

- Identify relevant burner technologies
- Identify post-combustion control technologies
- Understand capability and limitations of each technology

# Background

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Updated

- Purpose of technology assessment is to assess current NO<sub>x</sub> control technologies for metal melting and metal heat treating furnaces
- Two strategies utilized to reduce NO<sub>x</sub> emissions for metal melting and metal heat treating furnaces
  - Combustion Control
    - Low NO<sub>x</sub> Burners
    - Flue Gas Recirculation
    - Recuperative & Regenerative Burners
  - Post-Combustion Control
    - Selective Catalytic Reduction
    - Selective Non-catalytic Reduction

# Low NO<sub>x</sub> Burners

- Low NO<sub>x</sub> burners implement a variety of combustion optimization techniques to lower NO<sub>x</sub> emissions:
  - Combustion Staging: Performing partial combustion
  - Low Excess Air: Lowers excess air to < 2% and is obtained through feedback control systems to minimize flame temperature
  - Flame Enlargement: Lowers peak flame temperature but may overlap with adjacent burner flames or impinge parts
  - Radiant Burning: Firing mechanism to produce lower NO<sub>x</sub> emissions with higher excess air; more suited for new installations than retrofits

# Low NO<sub>x</sub> Burners (Cont.)

- Emissions Performance & Applicability
  - Product literature for two manufacturers<sup>1,2,3</sup> claim that both low and high temperature burners can meet 30 ppm @ 3% O<sub>2</sub>
  - Excess air and combustion air temperature identified as key metrics in burner applicability
- Other Findings
  - Of the units with control technology, 86% of the technologies are listed as Low NO<sub>x</sub> or Ultra-low NO<sub>x</sub> Burners on the unit permit
    - Use of Low and Ultra-low NO<sub>x</sub> language may not necessarily correlate to NO<sub>x</sub> concentration
    - 64% of units with Low and Ultra-low NO<sub>x</sub> Burners are > 30 ppm

<sup>1</sup> [http://digital.bnpmmedia.com/publication/?i=169784&article\\_id=1471463&view=articleBrowser&ver=html5#{"issue\\_id":169784,"view":"articleBrowser","article\\_id":"1471463"}](http://digital.bnpmmedia.com/publication/?i=169784&article_id=1471463&view=articleBrowser&ver=html5#{)

<sup>2</sup> <https://www.eclipsenet.com/products/furnnox/>

<sup>3</sup> <https://www.asminternational.org/c/portal/pdf/download?articleId=HTP00801P033&groupId=10192>

# Flue Gas Recirculation (FGR)

- Recirculation of exhaust gas via dampers, fans, and ductwork to the burners to dilute the combustion air
- Emissions Performance & Applicability
  - In the steel mill industry, FGR alone has shown to reduce  $\text{NO}_x$  by an additional 10%
  - Can be retrofitted onto furnaces but may require ductwork and additional fan capacity
  - Is often combined with Low  $\text{NO}_x$  Burners
- Mechanism
  - Flue gas contains combustion products that dilute oxygen content and lower the peak flame temperature
  - Typically 10 – 15%\* of combustion air is replaced with recirculated flue gas

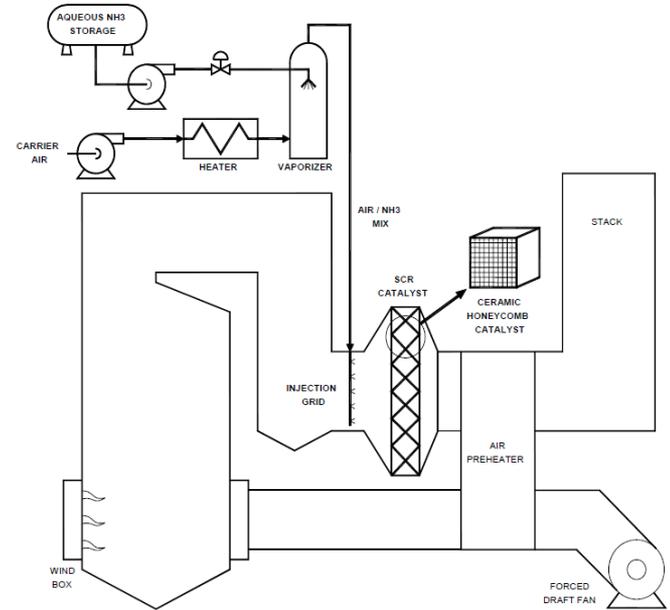
\* In the boiler industry

# Recuperative & Regenerative Burners

- Specific burner types utilizing heat exchange methods between exhaust gas and combustion air
- Due to elevated pre-heat temperatures, unit efficiency increases but NO<sub>x</sub> concentrations may increase
- Emissions Performance & Applicability
  - NO<sub>x</sub> concentration may not decrease due to elevated air pre-heat temperatures
  - Primary mechanism of NO<sub>x</sub> mass emission reductions is by reducing fuel use by 30 – 50%
  - Regenerative burners are better suited for new installs rather than retrofits
  - Recuperative burner units demonstrated to have ≤ 30 ppm NO<sub>x</sub> concentration

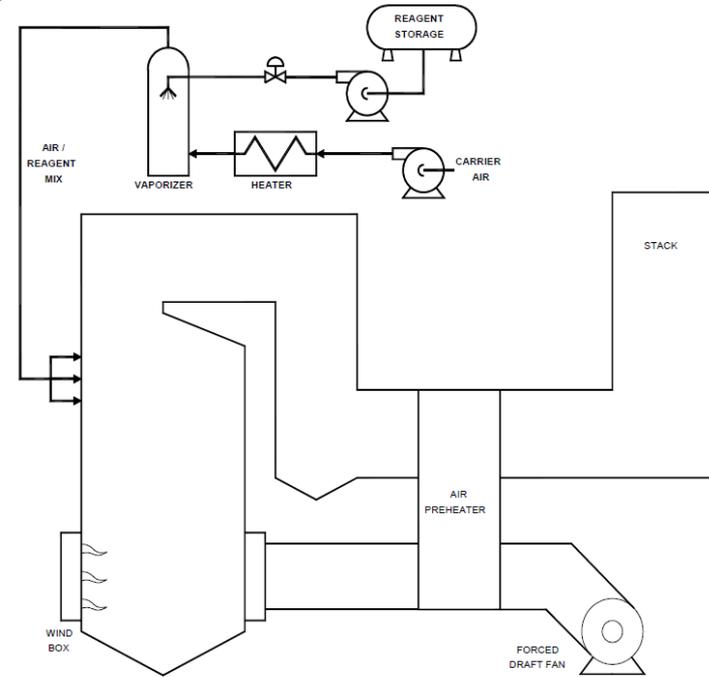
# Selective Catalytic Reduction (SCR)

- Injection of ammonia or urea into flue gas stream to reduce  $\text{NO}_x$  to  $\text{N}_2$  and  $\text{H}_2\text{O}$  with the use of catalysts
- Optimal Settings
  - Optimal temperature: 500 – 1,000 °F
  - Requires a 0.9:1 – 1:1 molar ratio of  $\text{NH}_3:\text{NO}_x$
- Emissions Performance & Applicability
  - $\text{NO}_x$  Reduction Efficiency: 80 – 85%+
  - One active furnace installation utilizes SCR to achieve an 80%  $\text{NO}_x$  reduction
  - Additional operating costs will be incurred over combustion control technologies (e.g. approximately \$26,000/yr for a 44 MMBtu/hr furnace)
  - Regeneration of catalyst 40% less expensive than catalyst replacement



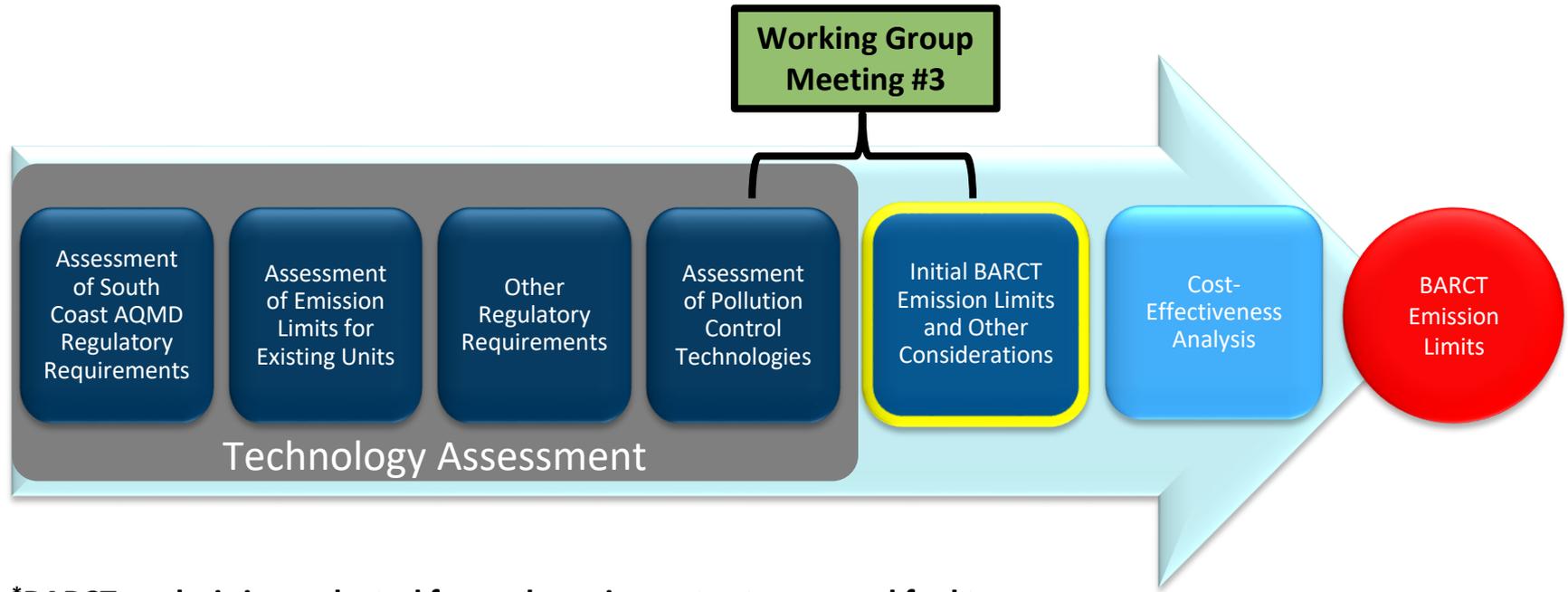
# Selective Non-catalytic Reduction (SNCR)

- Injection of ammonia or urea into flue gas stream to reduce  $\text{NO}_x$  to  $\text{N}_2$  and  $\text{H}_2\text{O}$  without the use of catalysts
- Optimal Settings
  - Optimal temperature: 1,500 – 2,200 °F
  - Requires a > 1 s residence time and a 2:1 – 4:1 molar ratio of  $\text{NH}_3:\text{NO}_x$ , leading to higher ammonia slip than SCR
- Emissions Performance & Applicability
  - $\text{NO}_x$  Reduction Efficiency: 60%\*
  - When combined with Low  $\text{NO}_x$  Burners, can achieve greater  $\text{NO}_x$  reductions than SCR alone (95%+ reductions)
  - Approximately 20% lower operating costs than SCR due to lack of catalyst
  - Optimal temperature difficult to maintain
    - No active installations in the proposed universe



\*60% is typical in the boiler industry

# Working Group Meeting #3: Current Progress



**\*BARCT analysis is conducted for each equipment category and fuel type**

# BARCT Limit Guidelines

- California Health and Safety Code Section 40406 defines BARCT as
  - “...an emission limitation that is based on the maximum degree of reduction achievable, taking into account environmental, energy, and economic impacts by each class or category of source.”*
- BARCT limit will adhere to Health and Safety Code Section 40920.6, which establishes requirements prior to adopting rules or regulations regarding retrofit control technologies
- In addition to the overall cost-effectiveness, additional considerations for:
  - Outliers
  - Stranded assets
  - Incremental cost-effectiveness
  - Accounting for recent installations – implementation of previous requirements (BARCT or BACT)

# Metal Melting – Initial BARCT Emission Limit

Slide Updated



60 ppm	9 – 59 ppm 13 (26%) ≤ 30 ppm 7 (14%) ≤ 20 ppm	60 ppm	SCR Installation: 11 ppm Burner Replacement: 20 – 30 ppm	11 ppm 20 – 30 ppm
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# Heat Treating – Initial BARCT Emission Limit

Slide Updated



60 ppm	5 – 115 ppm 59 (33%) ≤ 30 ppm 31 (17%) ≤ 20 ppm	60 ppm	SCR Installation: 11 ppm Burner Replacement: 20 – 30 ppm	11 ppm 20 – 30 ppm
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# Next Steps

- Continue site visits
- Conduct Cost-effectiveness Analysis
- Continue meetings with burner manufacturers
- Draft Proposed Rule Language initial concepts

<b>Rule Development Activity</b>	<b>Tentative Schedule</b>
Next Working Group Meeting	December 2019
Public Workshop	January 2020
Set Hearing	February 2020
Public Hearing	March 2020

# Contacts

PR 1147.2	PAR 1147	RECLAIM Questions	General Questions
<p><b>James McCreary</b> Assistant Air Quality Specialist <a href="mailto:jmccreary@aqmd.gov">jmccreary@aqmd.gov</a> 909-396-2451</p> <p><b>Uyen-Uyen Vo</b> Program Supervisor <a href="mailto:uvo@aqmd.gov">uvo@aqmd.gov</a> 909-396-2238</p> <p><b>Mike Morris</b> Planning and Rules Manager <a href="mailto:mmorris@aqmd.gov">mmorris@aqmd.gov</a> 909-396-3282</p>	<p><b>Shawn Wang</b> Air Quality Specialist <a href="mailto:swang@aqmd.gov">swang@aqmd.gov</a> 909-396-3319</p> <p><b>Gary Quinn, P.E.</b> Program Supervisor <a href="mailto:gquinn@aqmd.gov">gquinn@aqmd.gov</a> 909-396-3121</p> <p><b>Michael Krause</b> Planning and Rules Manager <a href="mailto:mkrause@aqmd.gov">mkrause@aqmd.gov</a> 909-396-2706</p>	<p><b>Kevin Orellana</b> Program Supervisor <a href="mailto:korellana@aqmd.gov">korellana@aqmd.gov</a> 909-396-3492</p> <p><b>Gary Quinn, P.E.</b> Program Supervisor <a href="mailto:gquinn@aqmd.gov">gquinn@aqmd.gov</a> 909-396-3121</p>	<p><b>Susan Nakamura</b> Assistant Deputy Executive Officer <a href="mailto:snakamura@aqmd.gov">snakamura@aqmd.gov</a> 909-396-3105</p>