SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT

CHAPTER II

SOURCE TEST PROGRAM OVERVIEW

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CHAPTER II

SOURCE TEST PROGRAM OVERVIEW

INTRODUCTION

For source test results to have value they must meet several objectives:

- 1. Completeness
- 2. Precision
- 3. Accuracy
- 4. Representativeness
- 5. Comparability

This chapter describes how a source test should be planned and executed to meet these objectives. Source testers must maintain records to show the level of attainment.

PLANNING THE SOURCE TEST

Intelligent planning of a source requires an understanding of the purposes and ultimate uses of the test data, and adequate information on the nature of the source to be tested.

Establishing Purpose of the Test

Source tests generally are conducted either to determine compliance with District, State or Federal regulations, or to obtain data for engineering purposes. Compliance testing requires that the source be tested as it normally operates. This means the source tester cannot request the company to change its operation to conduct the test under more "representative" conditions, such as worst case. In contrast, tests for engineering purposes often require the source to be tested under specific operating conditions. It is important to clearly establish the purpose of the test and the use of the data before conducting the test.

Proper coordination with the source operator often makes it possible to conduct a source test to obtain the data required for both compliance and engineering purposes.

A major problem in combining a compliance test with an engineering test is achieving completeness. While the data obtained may be sufficient to determine proper equipment operation and compliance with emission limits, it may be insufficient to establish representativeness of process operation. Information on representative operation is useful in enforcement proceedings if the test indicates noncompliance. Therefore, all equipment operating

parameters that have any effect on process emissions or control device efficiencies should be documented. Parameters to be monitored must be established before the test is conducted.

The requestor can usually provide information on the purpose of the test, but may not be aware of the capabilities and limitations of source testing. The request may need modification. The source tester may need to contact the company or others familiar with the operation to fully establish exactly what tests should be conducted and what parameters should be monitored.

Establishing Applicable Rules

Different rules have different testing requirements. For instance, rules for sulfur compounds, sulfur oxides, and sulfur dioxide each require different testing techniques. Some rules limit emissions as a function of process parameters. Therefore, the accurate determination of process rates (e.g. fuel usage, process weight) is just as important as accurate measurement of emission rates.

The applicability of a rule often depends on compliance dates or specific definitions of an operation. This information can be obtained from the equipment owner or operator, the engineer processing the company permits, or

the inspector responsible for enforcing the rules. In cases where some doubt exists as to the applicability, the appropriate District staff must be consulted.

Performing a Pretest Inspection

Depending on the complexity of the test or familiarity with the facility, the source tester may need to inspect the plant. Figure II-1 is a guide to determine the need for an on-site inspection. Figures II-2 and II-3 indicate typical items to be checked during the inspection. Important considerations include the following:

- Type of process or operation. (Obtain a flow diagram if available.)
- 2. Type of emissions.
- 3. Effect of plant operating conditions on emissions.
- 4. Location and condition of process instrumentation.

5. Duct size.

 Temperature, pressure, velocity, and moisture content of the effluent gas stream.

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II-4
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- 7. Location and accessibility of the sampling points.
- Adequacy of platforms, sampling ports, and power supply outlets.
- 9. Safety hazards and special equipment needs. (Obtain approval from appropriate safety officials, if necessary.)

Establishing Sampling Strategy and Data Requirements

The process being tested may be steady state or cyclic. If the process is cyclic, the sampling period should be planned to include at least one complete cycle. If the cycle is short it may be necessary to sample over several cycles to obtain an adequate sample. If the cycle is long it may be preferable to sample the cycle in separate but definable parts. Data obtained during each part may often be more useful than an average over the entire cycle.

Where process data are used in source test calculations, the accurate measurement of that data should be given as much importance as the accurate measurement of emission data. Therefore, the tester should plan to check calibrations of process instrumentation (using NBS traceability, as the highest standard of accuracy). Confirm that calculation techniques are appropriate and result in accurate

information, and verify that all data used in calculations are accurate. Methods of cross-checking process data should be used wherever possible.

Assuring Proper Sampling Facilities

Adequate sampling facilities are necessary for obtaining representative samples in a safe manner. This is required by District Rules and Regulations as follows:

"RULE 217. PROVISION FOR SAMPLING AND TESTING FACILITIES (Adopted January 9, 1976)

The Air Pollution Control Officer may require the applicant or permittee to provide and maintain such facilities as are necessary for sampling and testing. In the event of such requirements, the Air Pollution Control Officer shall notify the applicant in writing of the required size, number and location of sampling ports; the size and location of the sampling platform; the access to the sampling platform; and the utilities for operating the sampling and testing equipment. The platform and access shall be constructed in accordance with the General Industry Safety Orders of the State of California."

<u>Guidelines for Construction of Sampling</u> <u>and Testing Facilities</u>

The selection of the proper sampling site is important to assure obtaining a representative measurement of the pollutant emissions and the volumetric flow rate from a stationary source. Accessibility and safety also are essential considerations. The tester must consider clearance for sampling equipment, access to electrical power, exposure of personnel to weather and process heat, presence of hazardous gases, and any other pertinent safety factors.

Minimum construction requirements for permanent, safe, and accessible sampling facilities at a stack or duct are as follows:

Sampling Ports

<u>Port Location</u> - Ports should be located at least eight stack or duct diameters downstream and two diameters upstream from any bend, inlet, outlet, expansion, contraction, or other flow disturbance, or from a visible flame. To determine upstream and downstream disturbances for a rectangular stack or duct, calculate the equivalent diameter as follows:

If necessary, an alternative location at least two diameters downstream and one-half diameter upstream from any flow disturbance may be used, subject to approval by the Executive Officer or a designated representative. For any location selected, the gas should flow in a linear pattern parallel to the axis of the stack or duct, have a uniform velocity profile and not flow in a cyclonic pattern.

<u>Port Type</u> - A sampling port should be a 3-inch inside diameter welded nipple with a screw cap or a pipe with flange. A gate valve should be used for stacks handling hazardous gases or gases over 200°F under positive pressure.

<u>Port Installation</u> - Ports should be flush with the interior stack wall and extend outward from the exterior wall at least 2 inches and not more than 6 inches. Ports should be located at least 4 feet and not more than 5 feet above the work platform floor and meet clearance zone requirements described below. The ports should be located parallel and perpendicular to the centerline of the upstream disturbances. A 1-inch eyehook should be installed 24 inches above each port.

Monorails should be permanently installed at the stack for the equipment which is under Regulation IX (NSPS).

<u>Number of Ports</u> - If the sum of the stack inside diameter plus the port length is 5 1/2 feet or less, two ports should be installed 90 degrees apart. If this sum is over 5 1/2 feet, four ports should be installed 90 degrees apart. In case of rectangular stack or duct locate the ports on the widest of the two sides. Number of ports will depend on the grid configuration. (Follow Method 1.1, Section 2.3.)

Work Platform

<u>Size</u> - The work platform should be at least 4 feet wide. For two-port installation the platform should serve that quarter of the stack and extended at least 3 feet beyond each port. For a four-port installation the platform should serve the full circumference of the stack. The platform should be at least 5 feet wide.

<u>Construction</u> - Safe and easy access to the work platform should be provided by stairway, caged ladder, or other suitable means approved by the Executive Officer. The platform should have a safe guardrail and toeboard and be able to support 1000 pounds live load.

All construction must conform to the General Industry Safety Orders of the State of California.

For platforms over 30 feet high a pulley stand with a 3 feet swinging arm equipped with 10-12 inch pulley wheel with a 1/2 inch continuous manila rope should be provided.

<u>Clearances</u> - There should be no obstructions within a 3-foot radius on the platform beneath each port. There should be a clearance zone around each port extending one foot above, two feet below, and two feet on each side of the port. The zone should extend outward from the end of the port at least one stack diameter plus three feet.

Power Supply

Four electrical outlets, each capable of supplying 115-volt, 20-ampere, 60-cycle AC should be provided, preferably at each sampling site; or, alternatively, they may be located within 50 feet of each sampling site.

Additional Requirements

These guidelines cover situations requiring permanent sampling facility installations. Additional requirements

may be specified for situations with special needs such as flow pattern adjustment, hoist equipment, or variations in the number and location of sampling ports.

Sampling Methods

Selection of the most appropriate sampling method for a specific test operation must consider the chemical and physical properties of the sample to be collected and the types and limitations of analytical methods available for specific contaminants. Sampling methods available are integrated sampling, grab sampling, continuous sampling, or a combination of these. A description of these methods and the potential problems associated with each of them are presented below.

Integrated Sampling

Integrated sampling involves passing exhaust gases through a filter, a chemical absorbing solution, water, or any combination of these throughout the test period. The filter, solution, and/or container contents are then analyzed in the laboratory. This method determines average emissions but cannot discern variations in emissions during the test. Most sampling for particulate matter is done by the integrated method.

Integrated sampling normally requires more handling of test equipment than other methods, and the sample analysis techniques offer more possibilities for error. Therefore, careful quality control must be exercised during both the sampling and analytical procedures. Using a checklist will help reduce errors.

Grab Sampling

A grab sample is a gaseous sample taken during a short time period. These samples can be collected in several ways: by drawing directly into an evacuated container, by inflating a flexible bag, in a syringe, or by running several volumes of the gas through a container to purge the air contents and leave pure sample. After collection, samples are submitted for laboratory analysis.

Problems associated with grab sampling are:

• <u>Contamination by container or baq</u>. The material of the container or sample train should not react with either the sample being collected or the sampling medium. Containers to be reused must be properly passivated for the contaminant gas. A record of sample collections and the passivation process should be kept for each container.

- Loss of concentration of sample due to condensation on container walls. In some cases use of an extracting solution or a heated container can eliminate this loss.
- <u>Non-representative sample due to cyclic processes</u>. Integrated sample is preferred in this case.

Continuous Sampling

Continuous sampling techniques can be categorized as either extractive or in-situ (in-stack). A description of these techniques and the potential problems associated with each of them are presented below.

Extractive

Extractive sampling is the primary continuous sampling technique used by air pollution control agencies. It is accomplished by drawing a sample from the stack through a probe and into electronic instruments that analyze the gases. Both variations in real time emissions and average emissions can be determined by this method. Problems associated with this technique include the following:

• <u>Conditioning of the gases before passing through the</u> <u>measuring device</u>. The conditioning must not change the concentration of the specific pollutant to be measured.

- Interference from components of the gas stream other than the specific pollutant to be measured. False responses from other than the pollutant of interest and species interactions during measurement, may cause inaccurate results. Information on such interferences may be obtained from the instrument manufacturer or by guality control testing.
- Accuracy of calibration gases and possible influence of the carrier gas (balance or make-up gas) on the response of the analyzer. For periodic calibration of the analyzer NBS traceable calibration gas must be used. When inert carrier gas is required its influence on the response of the analyzer must be determined prior to its use.

In-situ

In-situ sampling instruments analyze the flue gases as they flow by sensors located in the stack. These instruments are usually permanent installations used for continuous stack monitoring purposes. Quality control of this equipment can be accomplished by periodic comparison testing with other approved sampling methods.

CONDUCTING THE SOURCE TEST

<u>General Test Requirements</u>

To meet the test objectives the source test must be performed by qualified personnel using proper test methods and equipment. The source test team leader must be properly trained in source sampling and experienced in using field test procedures under field conditions. Adequate staff must be available at each test station to perform the required sampling.

To assure the validity of a test, appropriate and properly calibrated sampling equipment must be used. Since calibration and maintenance of test equipment are subject to legal review, test personnel should keep a written record of each calibration. Standardized practices and complete documentation are emphasized as means of ensuring the validity and legal soundness of results. Calibration requirements are described in detail in Chapter III.

Standard source test procedures should be used, and modified only when they are necessary to obtain representative samples. Changes in methodology must be based on sound engineering and scientific judgment. Modifications must be documented and approved by the Executive Officer before use.

During the test it is essential that the process operates at normal conditions. For new source performance tests several operational conditions may be stipulated. For compliance tests no such conditions are stipulated to the operator. Test equipment should be functioning properly and operated to ensure the collection of a representative sample.

Changes in the normal operation of the process must be documented. Variations in the quantity or quality of the effluent gas, such as opacity, stack gas velocity, or temperature, should be investigated and the reasons documented.

Since source test results are frequently used as proof of compliance, the tester must pay close attention to quality control checks and documentation. Performance and documentation of pretest preparation and post-test checks are important. For reagents, containers, or filters, a record should include the date, the person who prepared them, and the location of these items from preparation until actual use for sampling. Because these items become an integral part of the sampling process, their integrity must be maintained from preparation through analysis. Each test method includes field data forms for record keeping purposes.

Recording Data

Since test data is physical evidence in legal proceedings, standardized field data forms manual should be used to gather all required information. Typical forms are shown in

Each field data form identifies the process tested, date and time, test location, testing and recording person. Data should be recorded in indelible ink. Erroneous values should be crossed out and corrections entered above them with tester's initials.

Sample Handling

Once the sample is collected it should be handled carefully to ensure that the sample submitted to the laboratory for analysis represents the actual sample taken at the reported test conditions.

Contamination and deterioration of the sample must be avoided. Security measures should be documented in a written record signed by the handlers of the samples. Sample identification should be verified throughout the test and analytical procedures.

One member of the source testing team should serve as sample custodian and be responsible for receiving equipment items

from the laboratory and entering the information on the field data forms. A label form to identify samples is shown in Figure II-4.

Chain of Custody

Legal rules of evidence require systematic sample identification at all processing points. Samples must be marked to ensure positive identification. Samples should be transported with precautions taken to eliminate the possibility of tampering, accidental destruction, and physical or chemical damage. Testing personnel must thoroughly understand the characteristic of the samples and deliver them to the laboratory on the same day as the sampling. When this delivery is impractical, the samples should be placed in a location secure from tampering, breakage, contamination, deterioration, and loss.

The sample custodian of the source test team must ensure and document that the samples have been transported to the laboratory custodian according to the precautions described in the test method. The chain of custody form shown in Figure II-5 establishes the identity of the sample. Such documentation ensures that the sample analyzed was the sample taken at a particular condition. Samples should be handled only by persons associated with the test. Ideally, all samples are transported from the test site to the

vehicle and from the vehicle to the laboratory by the same person.

- If no one is available to receive the samples, indicate where the samples are stored. Notify the Chem Lab Custodian as soon as possible.
- If no sample is collected, state in the I.D. Nos. column that analysis is not required.

To help each person remember from whom the sample was received and to whom, it was delivered, it is recommended that each recipient signs the receipt form for the sample. The chain-of-custody procedures should not delay the sample analysis. If the sample must be kept for future reference, store it in a secure area. To comply with legal rules all test reports should be filed in a secure place by a custodian. Although the field notes and calculations are generally included in the source test report, the original materials must be kept in the secure file. Do not take the original file to the field.

Sample Recovery and Analysis

Special care must be used in recovery and analysis of samples by personnel qualified to perform the specified laboratory procedures. Analytical procedures are included

in the test methods. Any deviation from these procedures requires prior approval of the Executive Officer.

Field Calculations

Field calculations must be checked for possible calculation errors due to procedural or mathematical mistakes, preferably by a team member other than the person who performed the original calculations. If a difference greater than typical round-off error is detected, the source of error must be found and corrected. If a standardized computer program is used, check the original data entry. If differences are observed, make a new computer run.

Experienced persons are able to recognize unusual test results which are due to entry errors.

Calculations should be carried out to at least one significant digit beyond that of the acquired data and then should be rounded off after final calculation to two significant digits for each run. All rounding off of numbers should be in accordance with the ASTM E380-82 procedures.

Test Report

A complete and clearly written report is a vital part of the source test, since the information will be used by a wide audience with varied needs and backgrounds. Some users will be highly skilled and need the most technical portions of the data, but will have little use for a discussion of standard, well-known test techniques. Others may need a detailed discussion of test methods. In legal proceedings the report serves as the official record of the testing process. Because of many uses of a source test report all test data should be included in each report. To assure that reports are complete it is advisable to prepare them in a standardized format. The general format for a source test report is outlined below. A complete example report is in the Appendix.

SOURCE TEST REPORT - GENERAL FORMAT

TITLE PAGE

- 1. Source test report number
- 2. Company name and address
- 3. Test report title
- 4. Test date, issue date, report author
- 5. Report reviewer

SUMMARY

<u>Introduction</u>

- 1. Firm tested and location
- 2. Basic equipment and control equipment tested
- 3. Person requesting test and reason
- 4. Date of test
- 5. Source test team members
- 6. Firm contact for test arrangements
- 7. Test observers

<u>Results</u>

- 1. Flow Rate.
- 2. Process Weight.
- 3. Contaminants measured
 - A. Emissions measured
 - B Emissions allowed
 - C. Applicable rules

GENERAL INTRODUCTION

The general introduction is a brief narrative listing the test date and location, basic and control equipment, applicable rules, and purpose of the test.

EQUIPMENT AND PROCESS DESCRIPTION

This section includes a brief description of the process and its basic equipment and control equipment, a schematic of the process, and the location of the test sampling port. It also includes process data or parameters that were monitored.

SAMPLING AND ANALYTICAL PROCEDURES

This section describes the sampling and analytical procedures, sampling apparatus with a schematic diagram, deviations from standard procedures, and the calculations performed with the sample components.

TEST CRITIQUE

The critique reports problems encountered in the test operations and abnormal conditions in the process operations. Deviations from standard procedures are described in detail. The section concludes with a discussion of the validity of the results.

ATTACHMENTS

- 1. Process diagrams
- 2. Sampling equipment diagrams
- 3. Meter data tables
- 4. Velocity data tables
- 5. Calculation sheets
- 6. Analytical laboratory reports

All original field report material should be filed with other documentation regarding checks and calibrations, chain of custody, process data, original recording, memos, inspection reports, test request, and lab request.

OTHER PROGRAM CONSIDERATIONS

Test Equipment

The specifications, criteria, and design features of the source testing equipment must meet the acceptable standards shown in Chapter III. A procurement log should be maintained to record the description of equipment, identification number, and acceptance check results. When an acceptance check includes calibration, the results are entered in a calibration log book. Repair and maintenance

logs also should be maintained. Figures II-6 and II-7 show procurement log and maintenance and repair record forms.

Equipment Preventive Maintenance

Systematic errors arise from deficiencies inherent in the equipment or from inaccurate calibration. To minimize systematic errors, effective preventive maintenance and calibration programs must be implemented. The calibration program is described in Chapter III.

Preventive maintenance is intended to reduce equipment downtime, improve reliability of source test results, and increase confidence in results. The program involves cleaning, lubricating, rebuilding, and adjusting equipment at predetermined intervals. A spare parts inventory should be maintained to help reduce equipment downtime. A recommended spare part list can usually be obtained from the equipment manufacturer.

Preventive maintenance should be performed on the following equipment:

- 1. Sampling pumps
- 2. Flow meters
- 3. Pressure gauges
- 4. Sampling instruments

- 5. Integrated sampling tanks
- 6. Mobile van sampling systems
- 7. Laboratory equipment
- 8. Other designated equipment

Maintenance service frequency is based on experience and manufacturer recommendations. Equipment maintenance should be performed on a scheduled basis or when indicated by performance deterioration or excessive wear. An equipment identification and service record should be kept on a maintenance log sheet. Figure II-8 lists acceptance limits and frequencies of maintenance for the equipment listed above.

One qualified individual should be responsible for:

- Planning and implementing an equipment maintenance program.
- Ensuring that all maintenance and calibration work is performed on schedule.
- Maintaining current equipment logs service records.

Instructions for periodic maintenance, calibration, and special care of instruments and equipment are frequently updated. Abstracts from manufacturer's service and maintenance manuals are primary information sources for

these updates. The accuracy and life of test equipment can be increased by employing the assistance of factory representatives in initial installation and performance testing and following manufacturer's operating instructions.

Initial Examination of Data

Test data should be examined for obvious abnormal values. These values should be corrected whenever possible and changes recorded and initialed. The presence of an error does not automatically require that an entire test be rejected.

Generally, determinate errors can be resolved and corrected. If the error is indeterminate, it still may be possible to calculate its significance and judge the acceptability of the final results. Test values judged to be invalid or suspicious should still be recorded and identified as such.

Data Reduction

Data reduction requires a standard calculation form or computer. The form should include step wise procedures to obtain accurate results. Computers are useful for handling large amounts of data and simplifying complex calculations. All calculations and computer inputs must be checked by at least two people. Then the supervisor must review the data to judge its validity.

Data from continuous emission analyzers are recorded on strip charts. Strip chart data should be integrated with a planimeter or similar device unless the recording is relatively constant with time. Data strip charts must be checked by a supervisor.

All reviewers must initial the calculation sheets and printouts.

Data Validation

When test results have been calculated, with precautions taken to assure accuracy, they are evaluated for representativeness of actual emissions. Variability in results of multiple tests on the same source at different times may be due to the following:

- 1. Variations in source operating parameters
- 2. Equipment and personnel variations in the field and the laboratory
- 3. Uncertainties or randomness of test method

Variation in source operation often is the most significant factor in the variation of the results. Knowledge of source operation and monitoring of key parameters will help identify these variations.

A good training program can reduce variations caused by personnel and a good preventive maintenance program can minimize variations in equipment performance..

Uncertainty of results is an important aspect in determining test reliability. Uncertainty may be measured by statistical methods or with control charts to compare test results with historical control limits. Several points should be considered when test results fall outside the control limits:

- Was the test method appropriate for the source tested?
- 2. Was the source operation varying?
- 3. Were equipment problem, or probable human error encountered during the test?
- 4. Was test data recorded and reduced properly?

If the cause of variations in results can be determined it should be noted in the test report. Another test should be conducted, if necessary. When possible, test results for each run should include the confidence interval (for example, 120 ppm \pm 10 ppm). The confidence interval is obtained from the uncertainty analysis or from other statistically sound methods.

Quality Assurance Audits

A quality assurance audit should be conducted by someone not a regular member of the source test team. This person conducts periodic performance audits and checks source test results. There are three types of performance audits:

- 1. Sampling audits
- 2. Analysis audits
- 3. Data processing audits

Sampling Audit

A complete sampling audit involves simultaneous testing with different equipment and operators, though it often is impractical from a cost and personnel standpoint. In most cases, an acceptable sampling audit consists of a qualitative appraisal of the test procedures and test equipment used during the test. The auditor verifies that all equipment was functioning properly during the test and that personnel performed all pre-test and post-test performance and calibration checks.

Analysis Audit

An analysis audit consists of separate analyses of commonly collected integrated samples. Samples of known concentration can be submitted to two or more independent laboratories. Samples may also be evaluated by separate chemists in the same laboratory.

Data Processing Audit

Data processing audits involve spot checks of data reduction and calculation procedures. Computation methods are checked by inserting "dummy" data sets into computer programs and calculation sheets.

Audit Checklist

Checklists are helpful in conducting most parts of an audit but an auditor must rely on good judgment. The auditor should attempt to resolve problems found and also record them for later review. See Figures II-9 through II-12 for audit checklists.

A periodic review of the preventive maintenance program, based on monitoring equipment downtime, should be part of the audit process.

Training

Errors by test personnel are due to carelessness, insufficient knowledge, or inadequate training and can be reduced by establishing a training program covering the following areas:

- 1. Operation and maintenance of equipment.
- 2. Detection of electronic problems.
- 3. Detection of sensor problems.
- 4. Detection of mechanical problems.
- 5. Performance of routine field repairs.
- 6. Calibration of instruments.
- 7. Limitations of instruments (range, responses, interference, functions, temperature, and moisture limits).
- 8. Quality assurance.
- 9. Technical writing.
- 10. Legal requirements of evidence.

A safety training program is mandatory. Personnel involved in field inspection and source testing must be adequately trained in using self-contained breathing apparatus, emergency life support apparatus, and personal monitors. Safety rules and guidelines must be given to the employees and strictly enforced. Periodic refresher training must be provided for the use of all safety equipment.

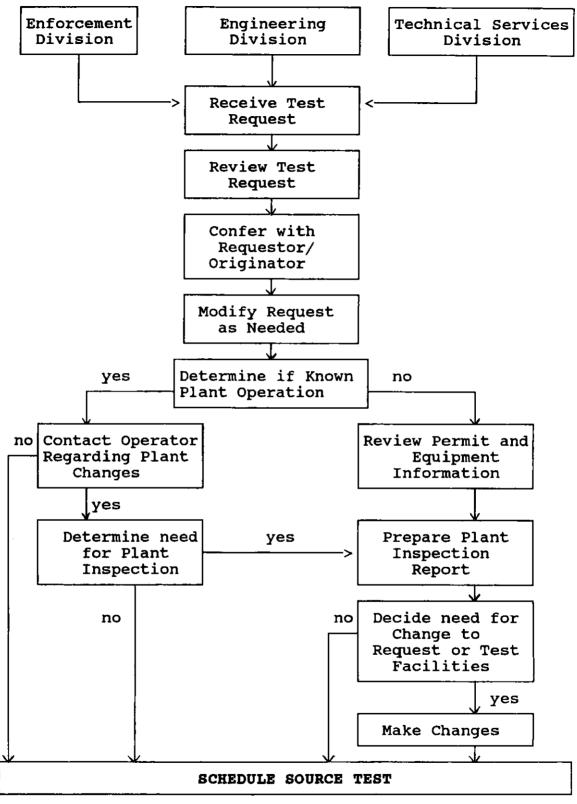


Figure II-1

PROCEDURE FOR PLANNING A SOURCE TEST

PLANT INSPECTION REPORT

DATE OF INSPECTION:

COMPANY AND UNIT:

COMPANY ADDRESS:

COMPANY PERSONNEL CONTACTED:

TELEPHONE NUMBER:

INSPECTED BY:

- I. Process and Equipment
 - 1. Basic and Control Equipment.
 - 2. Manufacturing Process and Schedule and Level of Plant Operation.
 - 3. Process Flow Sheet of Basic and Control Equipment.

II. Emissions

- 1. Location(s) of Emissions.
- 2. Temperature of the flue gases.
- 3. Types of Contaminants.
- 4. Estimated Contaminant Concentration.

Figure II-2

TYPICAL PLANT INSPECTION REPORT

- III. Test Method and Sampling Equipment
 - 1. Contaminants to be tested.
 - 2. Test Equipment Needed.
 - 3. Modification of Test Method and/or Equipment.
- IV. Request for Test Facility and Estimated Installation Date
- V. Safety Precautions for Hazardous Conditions
- VI. Recommendation for Modification of Source Test Request
- VII. Test Schedule
- VIII. Test Fee Applicability

Figure II-2 (Cont.)

STACK AND GAS STREAM DATA REQUIREMENTS

| Date of Inspection |
|--|
| Company |
| Equipment Basic |
| Control |
| Stack (Vent) Number |
| Process Parameter |
| Comments |
| Process Vented |
| Platform Height, ft |
| Platform Width, ft |
| Platform Length, ft |
| Stack Inside Diameter, in. at Port |
| Stack Wall Thickness, in. at Port |
| Stack Material of Construction |
| Sampling Ports: |
| Existing |
| Size opening |
| Distance from platform |
| Straight Distance before Ports, ft |
| Type of Restriction before Ports |
| Environment at Sampling Site |
| Work Space Area |
| Ambient Temperature at Sampling Site, ^O F |
| Average Pitot Reading, in. H ₂ O and Range of AP |
| Figure II-3 |

FORM FOR RECORD OF STACK AND GAS STREAM DATA

| Date of Inspection |
|--|
| Company |
| Equipment Basic Control |
| Stack Gas Velocity, ft/min |
| Stack Gas Flow Rate, ft/min |
| Stack (Vent) Number |
| Moisture, Percent by Volume |
| Stack Gas Temperature , ^o F |
| Particulate Loading, gr/scf |
| Particle Size |
| Gases Present |
| Stack Static Pressure, in H ₂ 0 |
| Water Spray Prior to Site |
| Dilution Air Prior to Site |
| Elevator to Site |
| Available Electricity and Distance, ft |
| Number of OutletsType of Plug |
| Comments |

Figure II-3 (Cont.)

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT TECHICAL SERVICES DIVISION

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| Source | |
|----------------|----------------|
| Item No | Method |
| Source Test No | Sampling Point |
| Preparation No | Run No |
| Analysis No | Date |

Figure II-4 Sample Label

| Source Name | | | Source | Test No. | |
|--------------------------------|------------|----------------|-----------------|----------------------------|------|
| | | | | Date | |
| N | | - | Control E | quipment | |
| | | | Bos Compliance | | |
| Requested by ream No. | | | For Compliance | , Rule(s) (specify) | |
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| | | | IPMENT REQUEST | | |
| | | 970 | | atory No | |
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| | | BQUIPMENT | CHAIN OF CUSTOD | Y | |
| From | To | | Por | Date | Time |
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| Source Test H Sample Descr | No | | | ratory No ysis Requeste | |
| Source Test I Sample Descri | No | | Labo | | |
| Sample No | | SAMPLE (| Labo. Anal; | ysis Requeste | |
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| Sample Descr: | | SAMPLE (| Labo. Anal; | ysis Requeste | |
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| Sample Descr: | Prom | SAMPLE (To | Labo. Anal | ysis Requeste | |
| Sample Descr: | Prom | SAMPLE (To | Labo. Anal | ysis Requeste | |



Form for Equipment and Analysis Requests and Chain of Custody

PROCUREMENT LOG

| Item De- | | Purchase | | | D | ate | _ | Dispo- | |
|-----------|----------|----------|---|--------------|----------|-----------------|------|--------|----------|
| scription | Quality | Order | # | Vendor | Ordered | ate Received | Cost | sition | Comments |
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Figure II-6

FORM FOR RECORD OF EQUIPMENT PROCUREMENT AND ACCEPTANCE CHECK

11-41

24 (1

| Equip. I.D. # | Date Inact. | Reason for Inactivation | Date To Shop | Date From Shop | Date Calib. | Date Re-Activ. | Remark |
|------------------|----------------|----------------------------|-----------------|-------------------|----------------|---------------------------------------|------------|
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SOURCE TESTING EQUIPMENT - RECORDS OF MAINTENANCE AND REPAIR

Figure II-7

FORM FOR RECORD OF TEST EQUIPMENT MAINTENANCE AND REPAIR

II·42

| Equipment | Acceptance Limits | Frequency of Service | Methods of <u>Service</u> |
|------------------------|--|-----------------------------------|---|
| Pump | Absence of leaks | Every 500 hrs. or operation or | 1. Visual insp. |
| | 2. Ability to draw manuf. reg. vacuum | 6 months, which- ever is less | 2. Clean 3. Replace parts |
| | and flow | | 4. Leak check |
| Flow Meter | Free mechan- ical move- | Every 500 hrs. of operation | 1. Visual insp. |
| | ment | or 6 months, whichever is | 2. Clean |
| | 2. Absence of malfunction | less | 3. Calibrate |
| Sampling Instrument | Absence of malfunction | As recommended by manufacturer | As recommended by manufacturer |
| | 2. Proper response to zero, span gas | | |
| Integrated Sampling | Absence of leaks | Depends on nature of use | 1. Steam clean |
| Tank | | | 2. Leak check |
| Mobile Van Sampling | Absence of leaks | Depends on nature of use | 1. Change Filters |
| System | | | 2. Change gas dryer |
| | | | 3. Leak check |
| | | | 4. Check for system contamination |
| Sampling | Sampling degradation test Lines less that of test series | | Flush with solvent. Blow air through line until dry. |

Figure II-8

TEST EQUIPMENT MAINTENANCE SCHEDULE

| Yes No | o | Operation |
|--------|-------|--|
| | | Presampling Preparation |
| | 1. | Knowledge of process conditions. |
| | 2. | Calibration of pertinent equipment prior to each field test, including date. |
| | | <u>On-Site Measurements</u> |
| | 3. | Pitot tube meets geometry requirements. |
| | 4. | Differential pressure gauge (DPG)is level and the liquid column set exactly on zero. |
| | 5. | DPG has the correct sensitivity. |
| | 6. | Traverse points adequately located. |
| | 7. | Check for absence of cyclonic flow. |
| | 8. | Leak check before and after sample run. (Both sampling train and Pitot tube). |
| | 9. | Sampling port adequately plugged. |
| | 10. | Process at correct operating conditions. |
| | 11. | Pitot tube properly aligned along its roll and pitch axes throughout the traverse. |
| | 12. | Pitot tube frequently cleared when measuring in a dust-laden gas. |
| | 13. | System stabilized at each traverse point during sampling. |
| | 14. | Stack gas static pressure, temperature and barometric pressure measurements taken. |
| | 15. | Velocity at the reference point being monitored. |
| | | Figure II-9 |

METHOD 1.1 AND 2.1 AUDIT CHECKLIST

II-44

| Yes | No | Operation |
|-----|----------|---|
| | | Postsampling |
| | | 16. All information recorded on data form as obtained. |
| | | 17. Any unusual conditions recorded. |
| | | 18. Independent check of calculations. |
| | | 19. Temperature sensor calibrated. |
| | | COMMENTS |
| | <u> </u> | |
| | | |
| | | Figure II-9 (Cont.) |

CHECKLIST FOR METHOD 3.1 AUDIT CHECKLIST

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| Yes | No | | Operations |
|-----|----|-----|---|
| | | 1. | Availability of theoretical values. |
| | | 2. | Use of O ₂ and/or CO ₂ analyzer. |
| | | 3. | Adequately sensitive range used. |
| | | | <u>On-Site Measurements</u> |
| | | 4. | Sampling train setup and leak tested. |
| | | 5. | Sampling train purged with stack gas prior to collecting the sample. |
| | | 6. | Constant rate sampling. |
| | | 7. | Transfer of sample from collapsible bag to gas analyzers. |
| | | 8. | Analyzer operation. |
| | | 9. | Sample transfer to evacuated flasks. |
| | | 10. | Perform independent calculations using data from audit. |
| | | 11. | Compare the audit value with the field team's test value. |
| | | 12. | Minimize volumetric reading error. |
| | | 13. | Check/verify applicable records of equipment calibration. |
| | | | Comments |

Figure II-10

METHOD 4.1 AUDIT CHECKLIST

| Yes | No | | Operations |
|-----|----|-----|--|
| | | | Presampling Preparation |
| | | 1. | Knowledge of process conditions. |
| | | 2. | Calibration of pertinent equipment; in particular, the dry gas meter before each test. |
| | | | <u>On-Site Measurements</u> |
| | | 3. | Leak testing of sample train before and after sample run. |
| | | 4. | Addition of water and silica gel to impingers, and correct location of impingers. |
| | | 5. | Constant sampling rate not exceeding specified limits. |
| | | 6. | Measurement of condensed water to within specified limits. |
| | | 7. | Pertinent process condition during sample collection. |
| | | 8. | Probe maintained at given temperature. |
| | | | Postsampling |
| | | 9. | Calculation procedure check. |
| | | 10. | Calibration checks. |
| | | | Comments |
| | | | |

Figure II-11

| <u>Yes</u> | No | | Operation |
|------------|----------|----------|---|
| | | | Presampling Preparation |
| | | 1. | Knowledge of process conditions. |
| | | 2. | Calibration of pertinent equipment In particular, the dry gas meter, orifice meter, and Pitot tube. |
| | | | <u>On-Site Measurements</u> |
| | | 3. | Sample train assembly. |
| | | 4. | Pre-test and post test leak check of train. |
| | | 5. | Isokinetic sampling rate. |
| | | 6. | Post-test check for the setup. |
| | | 7. | Sample recovery and integrity. |
| | | 8. | Recording of pertinent process information during sample collection. |
| | | | Postsampling |
| | | 9. | Check of analytical balance. |
| | | 10. | Use of acceptable detection blanks in correcting field sample results |
| | | 11. | Check of calculation procedure. |
| | <u> </u> | <u> </u> | Comments |

Figure II-12

APPENDIX

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SOURCE TEST REPORT

99-0000

CONDUCTED AT

Alpha Specific Resources Champion Petroleum Company 999 E. Street El Monte, CA

PARTICULATE MATTER, SULFUR OXIDES AND CARBON MONOXIDE EMISSIONS FROM AN FCCU REGENERATOR CONTROLLED BY AN ELECTROSTATIC PRECIPITATOR, PLUS DETERMINATION OF CONTINUOUS MONITOR ACCURACY

TESTED: November 9, 1999 ISSUED:

REPORT BY: Assistant A.Q. Engineer

REVIEWED BY:

Senior A.Q. Engineer

Manager

Supervising A.Q. Engineer

SOURCE TESTING AND MONITORING BRANCH

DIRECTOR, TECHNICAL SERVICES DIVISION

 Test No. 99-0000
 -2 Date 11/9/99

INTRODUCTION

1

| a. | Firm Tested |
|----|--|
| b. | Test LocationChampion Petroleum Company |
| c. | Unit Tested |
| d. | Test Requested by <u>Source Testing</u> |
| e. | Reason for Test RequestRule Compliance |
| f. | Date of Test |
| g. | Source Test Performed by <u>AA, BB, CC</u> |
| h. | Test Arrangements Made Through |
| i. | Source Test Observed by <u>FF</u> |
| j. | Company I.D. Number |
| k. | Permit Number |
| 1. | Application Number |

Test No. <u>99-0000</u>

Date <u>11/9/99</u>

Flow Rate 2,188 dscmm (77,260 dscfm) Process Weight 1.808 kg/hr (3.986×10^6 lb/hr)

| | Emiss | sions | Applicable |
|--|--|---|--|
| <u>Contaminant</u> | Measured | Allowed | Rule |
| Particulate Matter | | | |
| -Concentration | 27.5 mg/dscm (0.012 gr/dscf) | 84.3 mg/dscm (0.037 gr/dscf) | 404 (a) |
| -Solid Mass Rate | 2.82 kg/hr (6.22 lb/hr) | 23.6 kg/hr (30.0 lb/hr) | 405 (a) |
| Carbon Monoxide | Non e Detected | 2000 ppm | 407 (a)(l) |
| SO _x as SO ₂ from FCCU Regenerator | 17.5 kg/1000 bbl (38.5 lb/1000 bbl) | 60 kg/1000 bbl (132 lb/1000 bbl) | 1105 (a)(2) |
| -Particulate Mass Rate -Per 1000 lbs Coke Burn off | 0.23 kg/1000 kg (0.23 lb/1000 lb) | 1.0 kg/1000 kg (2.0 lb/1000 lb) | Reg. IX Subpart J 40 CFR60.102 (a)(1) |
| Relative Accuracy of SO ₂ CEM Expressed as percent of: | | | |
| Actual Conc. Allowed | + 6.3% | <u>+</u> 20 % | 218 (C)(2)(A) (viii)* |
| Conc. | + 1.8% | <u>+</u> 10% | |

* See Test Critique

Test No. <u>99-0000</u> -4- Date <u>11/9/</u>99

INTRODUCTION

On November 9, 1999, personnel from the South Coast Air Quality Management District (SCAQMD) conducted a source test on the Electrostatic Precipitator (ESP) serving a Fluid Catalytic Cracking Unit (FCCU) operated by Alpha Specific Resources Champion Petroleum Company, Utopia, CA.

The purpose of the test was to verify compliance with District rules for emissions of particulate matter (Rules 404, 405), carbon monoxide (Rule 407), sulfur oxides (Rule 1105), New Source Performance Standards for Petroleum Refineries (Regulation IX), and relative accuracy of CEM (Rule 218). This test was a part of the District program to conduct quarterly tests on all FCCUs.

EQUIPMENT AND PROCESS DESCRIPTION

The FCCU catalytically converts gas oil into lighter petroleum products, mainly gasoline.

Test No. <u>99-0000</u> -5- Date <u>11/9/99</u>

Oil feed from the Hydrodesulfurization Unit is combined with Slurry Settler Bottoms from the FCCU gas plant and regenerated catalyst, and fed to the FCCU reactor. The hydrocarbon vapors from the reactor are further processed in the FCCU gas plant. Spent catalyst from the reactor, flows to the regenerator for burn off of carbon deposits. The regenerated catalyst is recycled to the reactor.

The regenerator gases exhaust to cyclone separators and electrostatic precipitators for removal of particulate matter before venting to the atmosphere as shown in Figure 1.

The operating parameters during the test were:

Test No. <u>99-0000</u> -6- Date <u>11/9/99</u>

Process Weight:

FCCU Feed Rate

34,950 Bbl/day x 1 day/24 hr x 286 lb/Bbl = 416,000 lb/hr

Total Process Weight 3,570,000 lb/hr + 416,000 lb/hr = 3,986,000 lb/hr

SAMPLING AND ANALYTICAL PROCEDURES

Flow Rate

The gas velocity in the outlet stack was measured simultaneously with particulate sampling (traverse sampling). This was done using an S-type Pitot tube strapped to the particulate sampling probe, a differential pressure gauge, and a type "K" thermocouple with a digital reading device. The gas flow rate was calculated from the temperature, pressure, density, stack area, and moisture content of the sampled gases. See Figures 1 and 2 for sampling point and equipment schematic.

Test No. <u>99-0000</u>

-7-

Date <u>11/9/99</u>

Particulate Sampling

A particulate sample was collected using the District Method 5.2 (Draft) sampling train consisting of a stainless steel nozzle, a stainless steel probe with a heated glass liner, a heated fiberglass filter, two impingers each filled with 100 ml of deionized water, an empty bubbler, and a bubbler filled with tared silica gel. The system was connected to a leak-free vacuum pump, a temperature compensated dry gas meter and a calibrated orifice, as shown in Figure 2. The temperature of the probe and filter was maintained above the dew point (180-200°F) of the sample gases to prevent condensation of moisture but sufficiently low to catch sulfuric acid mist. The two impingers and two bubblers were contained in an ice bath to condense water vapor and other condensable matter contained in the sample stream.

The particulate sample was collected for a period of one hour using a 24 point traverse through two portholes 90 degrees apart, two and one-half minutes per point.

Test No. <u>99-0000</u> -8- Date <u>11/9/99</u>

Particulate matter deposited in the probe liner and impinger solutions, and caught on the filter was determined by gravimetric techniques.

Sulfuric acid dihydrate $(H_2SO_4.2H_2O)$ in the impinger, filter and probe wash solutions was determined by both the Sodium Hydroxide Titration Method and the Barium Chloride Precipitation Method.

Moisture content was determined by volumetric and gravimetric techniques.

For Rule 404 compliance, total particulate was calculated by adding the weights of: Particulate matter deposited in the nozzle, probe liner, and filter; adjusted impinger residue (aqueous residue minus sulfuric acid dihydrate and neutral sulfates as ammonium sulfate); and organic extraction from the impinger solutions.

For Rule 405 compliance, the solid particulate was calculated by adding the weights of: Particulate matter deposited in the nozzle, probe liner, and filter; and

Test No. <u>99-0000</u> -9- Date <u>11/9/99</u>

adjusted impinger residue (aqueous residue minus sulfuric acid dihydrate and neutral sulfates as ammonium sulfate); and subtracting the lesser of the two weights of sulfuric acid dihydrate, as determined by the Sodium Hydroxide Titration Method and the Barium Chloride Precipitation Method, from the probe liner and filter.

Sulfur Oxides Sampling

The exhaust from the ESP stack was sampled continuously for 72 minutes using the District Method 6.1 (Draft) sulfur oxide (SO_x) sampling train. The train consisted of a glass probe, a Whatman paper thimble, one impinger filled with 200 ml of 2-propanol, an empty bubbler, two impingers filled with 100 ml of hydrogen peroxide (3 percent), an empty bubbler, a bubbler filled with tared silica gel, a vacuum pump, and a temperature-compensated dry gas meter, as shown in Figure 3.

At the conclusion of the sampling the SO_X train was purged with ambient air for fifteen minutes at an average flow rate of 0.5 cfm.

Test No. <u>99-0000</u> -10- Date <u>11/9/99</u>

For Rule 1105 compliance the weight of total sulfur oxides, calculated as sulfur dioxide (SO_2) from the regenerator, was determined by adding the weights of: Sulfur trioxide (SO_3) in the 2-propanol, calculated as SO_2 ; and the SO_2 in the hydrogen peroxide.

Integrated Gas Sample

An integrated gas sample was collected in a Tedlar bag for 28 minutes at the stack using a peristaltic pump as shown in Figure 4. The sample was transferred into three, two-liter evacuated glass bulbs and analyzed for CO, CO_2 , and O_2 in the District laboratory using District Method 10.1 (Draft). The gases were separated by gas chromatography. Carbon dioxide was analyzed by nondispersive infrared spectrometry. Carbon monoxide was combusted to produce carbon dioxide and also was analyzed by nondispersive infrared spectrometry. Oxygen was analyzed by thermal conductivity.

Test No. <u>99-0000</u> -11- Date <u>11/9/99</u>

TEST CRITIQUE

The test was conducted under normal operating conditions, during daylight hours of operation on a pre arranged basis. Neutral sulfates, as ammonium sulfate were subtracted from the particulate catch since Alpha Specific Resources (Champion) injects ammonia into the electrostatic precipitator.

Exposure to high stack temperatures $(498^{\circ}F)$, high stack pressures (+4.1 inches H₂0) and high SO₂ concentrations (71 ppm) made source testing dangerous. In addition, particulate sampling was difficult because of the narrow platform, the lack of four available portholes, and the length limitation of the sample probe. Point number 12 on sample porthole number 1 could not be sampled, because of the tight fit of the sample probe/Pitot tube boot used to minimize escape of the stack gases into the work area. Therefore, a five minute particulate sample was collected at point number 11.

```
Test No. <u>99-0000</u> -12- Date <u>11/9/99</u>
```

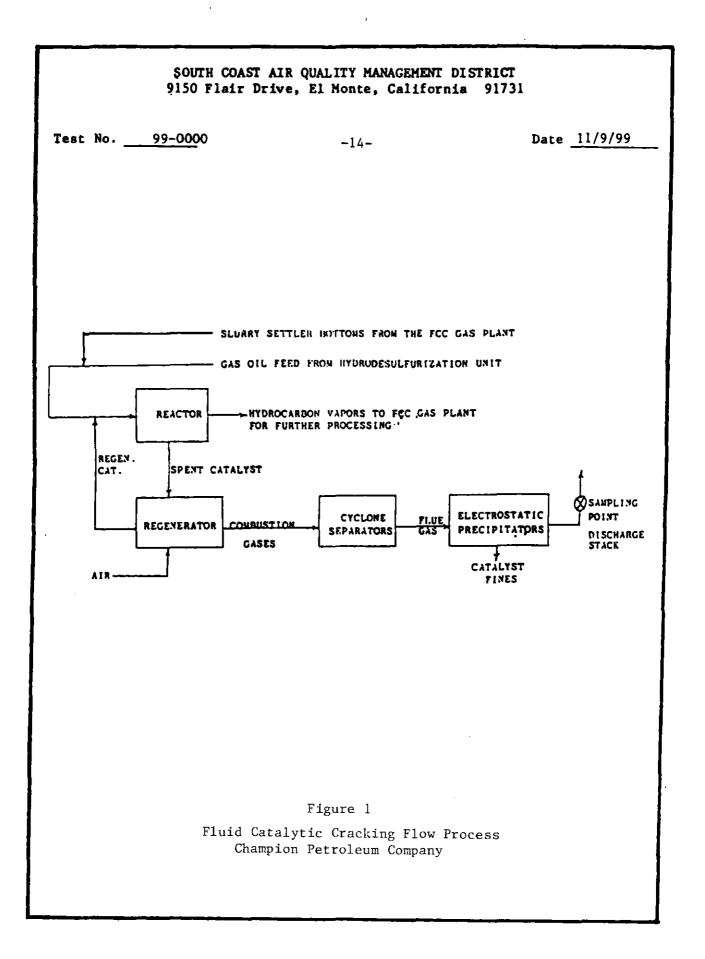
The test results indicate compliance with Rules 404, 405, 407 and 1105.

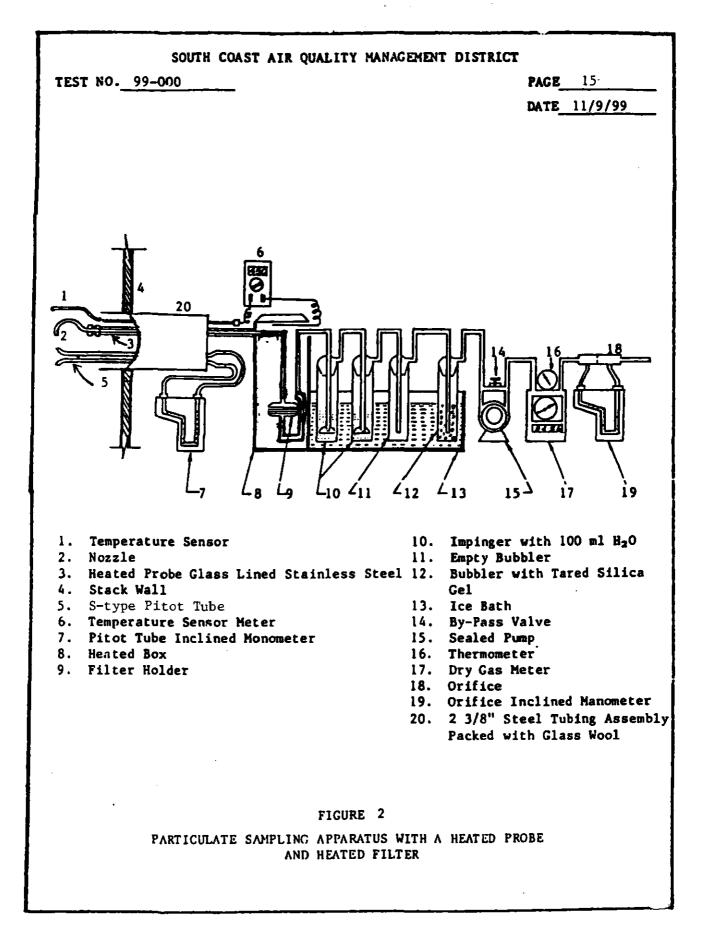
The Continuous Emission Monitor for sulfur dioxide was not certified at the time the test was conducted. However, the test results show compliance with Rule 218.

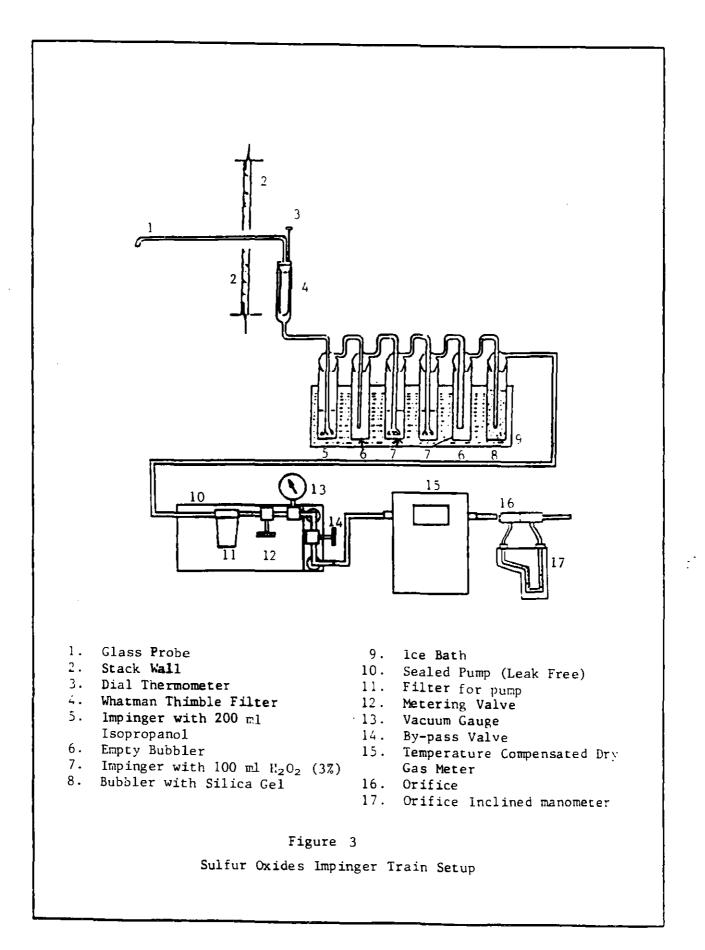
The particulate filter temperature exceeded the recommended limit of 200° F. Therefore, the correction for $H_2SO_4.2H_2O$ was obtained, by (1) subtracting the combined weight of the $H_2SO_4.2H_2O$ obtained on the particulate filter (< 1 mg) and the pre-filter residue (1 mg), from the combined weight of the pre-filter residue, the filter catch and the organic residue and (2) adding the prorated weight of $H_2SO_4.2H_2O$ (< 1 mg) obtained from the SO_X train thimble. For this test the corrections are negligible. Since the EPA sampling method was not strictly followed, compliance with Regulation IX cannot be confirmed. Since the particulate filter was maintained below $248^{\circ}F \pm 25^{\circ}F$ during the test, the

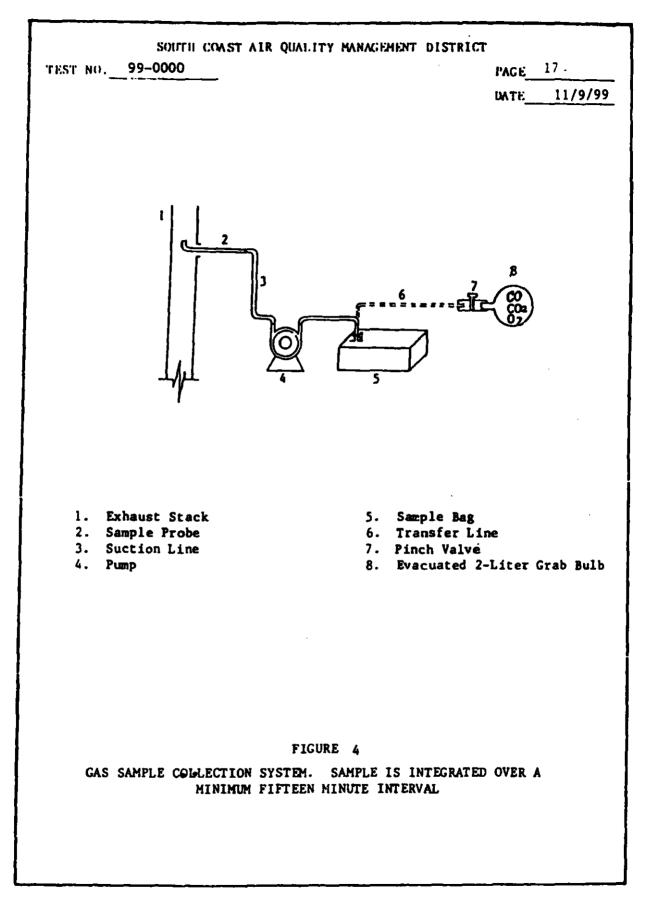
Test No. <u>99-0000</u> -13- Date <u>11/9/99</u>

weight of particulate obtained from the pre-filter and filter residue would be overstated for Reg. IX compliance purposes. However, under the conditions of the test the results did show compliance with Reg. IX limits.









| E | OUTH COAST AIR | -18- QUALI | TY MANAGEMENT | DISTRICT | |
|--|---|-----------------------------|--|---|---|
| Test No. <u>99-0000</u> Cajculated By | Samplin Train C.S. | <u>7</u> | Checked By | Bate | 11/9/99 |
| | SOURCE | E TEST | CALCULATION | 5 | |
| BURMARY | · · · · · · · · · · · · · · · · · · · | | · · · | | ····· |
| A. Average Traverse B. Average Reference C. Average Traverse D. Gas Meter Temper E. Gas Meter Correc | e Point Velocit Velocity (Dur) ature (Use 60 [°] f | ty (Pr ing Te F, for | e-Test) st) Temp. Comp. | (Computer) Meters) | <u>94</u> •F |
| F. Average Stack Te G. Stack Cross-Sect H. Barometric Press I. Gas Meter Pressu J. Total Stack Pres K. Pitot Correction | . Area <u>25,22</u> Jure <u>30.4</u> Jre <u>30.4</u> Jure <u>30.7</u> | ft" "HgA "HgA "HgA | M. Nozzle C N. Net Samp D. Net Soli P. Water Va | Time Toss-Sect. Area le Collection . d Collection por Condensed . me Metered | a <u>0,000/[5]</u> ft <u>23</u> m; <u>18</u> m; <u>73</u> m1 |
| R. Corrected Gas Vo | lume Metered [| (0 × I | /29.92) x | <u>520</u> × ε]. | <u>Z 9.55</u> dsc |
| PERCENT MOISTURE / | | | | | |
| 6. Percent Water Va T. Average Molecula | | | 4.64 x P 0.0464 x P) 4 |] | <u>12.74</u> x |
| (Component) | (Volume % / 1 | 1000) <u>x</u> | (1 - 5/100) | x (Molec, Wt.) | |
| <u>Water</u> | 0.1274 0.1427 Dry Ba | | 1.00 | <u> 18.0</u> 44.0 | <u>2.29</u> <u>5,48</u> |
| <u>Carbon Dioxide</u> Carbon Monoxide | 0.0 Dry Ba | | <u>0.8725</u> 0.8726 | 28.0 | 0,0 |
| | 0.0333 Dry Ba | sis | P. BTES | 32.0 | 0 93 |
| Nitrogen/Inerts | 0.824 Dry Ba | sis | 0.872.6 | 28.2 | 20,28 |
| | | | | <u> </u> | _ |
| <u></u> | <u> </u> | | | (Sum) | 28.83 |
| ELQW RATE | | | ·. | | |
| U. Gas Density Corr V. Flue Correction W. Velocity Pressur X. Corrected Veloci Y. Flow Rate (X x G Z. Flow Rate Y x AA.Flow Rate Z x (| Factor (A/B) e Correction Fa ty (C × K × U × × 60) <u>J</u> × <u>520</u> 9.92 (46 <u>0</u> + F | v x I | (| | |
| SAMPLE CONCENTRATIO | N/EMISSION RATE | Ē | | 0012 | • |
| BB.Sample Concentra CC.Sample Concentra DD.Sample Emission EE.Solid Emission R FF.Isokinetic Sampl | tion (54,143 x Rate (0.00857 x ate (<u>0.0001322</u> R | BB/ AA x x 0.) | Molec.Wt.) BB) (AA) | <u> </u> | gr/dscf ppm (dry lb/hr lb/hr % |
| FF.Isokinetic Sampl | | · • | ^^) II-67 | | <u> </u> |

DRAFT - Do not cite or quote

| SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT | PAGES | PAGE 19 |
|---|----------------------|----------------|
| ENFORCEMENT DIVISION | TEST NO. | DATE |
| SOURCE TESTING AND MONITORING BRANCH | | 11/9/99 |
| CALCULATION SHEET | PROCESSED BY C.S. | CHECKED BY |

LAB ANALYSIS

| ٨. | Filter Catch | 4 | ag |
|----|---|-------|---------------------------------|
| В. | (1) Filter Acid | | BR # 50 . 2H.D |
| | (2) Filter Total Sulfate | 2 | BB #1 50+ 2H2D B H2 50+ 2H2D |
| с. | Probe Catch | 14 | |
| D. | (1) Probe Acid | | Bg 46.504.21/20 |
| | (2) Probe Total Sulfate | 8 | mg Ar 50+ Zhid |
| Ε. | Impinger Catch | 130 | 118 |
| F. | (1) Impinger Acid | 12 | as He soy elle |
| | (2) Impinger Total Sulfate | 131 | mg H254. 2He |
| G. | Organic Extract | 4 | ng |
| Н. | H ₂ SO4.2H ₂ O from SO _X Train Thimble | <1 | ag |
| I. | Particulate Train Corrected Gas Volume Metered | 29.55 | dscf |
| J. | SO _x Train Corrected Gas Volume Metered | 33.60 | dscf |
| ĸ. | Prorated $H_2SO_4.2H_2O$ Mass $(\frac{H \times I}{J})$ | 0 | Eg |

FILTER (PARTICULATE) TEMPERATURE GREATER THAN 200°F

| L. | Total Particulate (A-B*+C-D*+E-F*+G+K) | mg |
|----|--|----|
| Μ. | Solid Particulate (L-G-K) | mg |
| N. | Total Particulate (Corrected for Ammonium Sulfate) | |
| 0 | (A-B*+C-D×+2-F(1)+G+K-[F(2)-(1)]. <u>132</u>) Solid Particulate (Corrected for Ammonium Sulfate) | ®g |
| 0. | (N-C-J) | œg |

FILTER TEMPERATURE LESS THAN 200°F

| P. | Total Particulate (A+C+E-F*+G) | | mg |
|----|--|----|------------|
| | Solid Particulate (P-B*-D*-G) | | mg |
| R. | Total Particulate (Corrected for Ammonium Sulfate) | | |
| | $(A+C+E-F(1)+G-[F(2)-F(1)],\frac{132}{114})$ $A+14+130-12+4-[131-12)ff_4 =$ | 23 | ng |
| s. | $(A+C+E-F(1)+G-[F(2)-F(1)], \frac{132}{134}), A+/4+130-12+4-5(131-12), \frac{152}{134}) =$ Solid Particulate (Corrected for Ammonium Sulfate) (R-B*-D*-G), 23-41-1-4 | 18 | n f |

* USE LOWER OF (1) AND (2)

| SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT | PAGES | PAGE 20 |
|---|----------------------|-----------------|
| TECHNICAL SERVICES DIVISION SOURCE TESTING AND MONITORING BRANCH | TEST NO. 99-0000 | DATE 11/9/99 |
| CALCULATION SHEET | PROCESSED BY C.S. | CHECKED BY |

Particulate Matter EPA Reg. IX

(Particulate from front part of train x $1.322 \times 10^{-4} \times AA/R$) =

 $18x1.322x10^{-4}x77260/29.55 = 6.22$ lbs/hr

*Coke Burn-off Rate = 26,794 lbs/hr

Particulate/1,000 lb coke burn-off = $6.22/26.794 \times 1000 = 0.23$ lb/1000 lb coke burn-off

| SOURCE | TEST PROOM | SUMMARY PREPA | RED ON 12-17 | 7-99 AT 13:30: | 34 |
|--|--|---|--|--|---|
| | | | | | |
| | | sure | | | |
| ·2) S | itack Static Pr | essure | (''H2O) | = 4.1 | |
| | | | | | |
| | | Time | | | |
| | | n Factor | | | |
| · - | | bration Factor | | | |
| | | ration Factor | | | |
| | | | | - 10 e- Tit | 1 Pert. (corrected for amm. 6 |
| | | ion Residue | | - Antion Hol | (Tot. Part Solit Ret.) Corr. (23 - 18) |
| | | | | | (23 - JB) |
| | | oluble Residue | | - 0 | |
| | | | | | |
| | |):68 Le | - | | |
| - | | ocity Head | | | |
| | | ocity | | | |
| | | ature | | | |
| | | sure | | | |
| | • | in Gas Sample. | | | |
| | | | | | |
| RULE 4 | 04: Particulat | e Concentratio | m (gr/dscf) | = 0.012 | |
| | | | (mg/dscm) | = 27.5 | |
| RULE 40 | 05: Solid Emis | sion Rate | (1b/hr) | = 3.22 | |
| | | | (kg/hr) | = 2.82 | |
| RULE 4 | 07: Average pp | m Carbon Monox | ide(CO) | = (A | |
| | | | | | |
| Isokin | etic Sampling H | Rate | | = 97 | |
| | | | | | |
| | | 04(a) | - | | |
| | | | | | |
| - JII E A1 | Dowahle40 | 25(a) | (1b/br) | = 30,0 0 | |
| | | | | | |
| | | | (kg/hr) | = 13.61 | |
| RULE A | lowable4 | 07(a) | (kg/hr) (ppm) | = 13.61 = 2000 | |
| RULE A1 | llowable46 | 07(a) | (kg/hr) (ppm) ********* | = 13.61 = 2000 | **** |
| RULE AL | llowable40 ********************************* | 07(a) ********************************* | (kg/hr) (ppm) *********** Velocity | = 13.61 = 2000 Drifice Press. | Meter Temp. |
| RULE AI | llowabie40 | 07(a) **************** Stack Temp. | (kg/hr) (ppm) *********** Velocity | = 13.61 = 2000 Drifice Press. | Meter Temp. |
| RULE AL | llowabie40 | 07(a) ********************************* | (kg/hr) (ppm) *********** Velocity | = 13.61 = 2000 Drifice Press. | Meter Temp. |
| RULE A) | llowable40 Veloc. Head (''H2D) | 07(a) Stack Temp. (DEG F) | (kg/hr) (ppm) ********** Velocity (ft/sec) | = 13.61 = 2000 Drifice Press. (''H2D) | Meter Temp. (Deg F) |
| RULE A1 4***** Point (#) | llowable40 Veloc. Head (''H2D) 2.90 | 07(a) Stack Temp. (DEG F) 499 | (kg/hr) (ppm) ********** Velocity | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 | Meter Temp. (Deg F) 82.0 |
| RULE A1 4***** Point (#) | llowable40 ********************************* | 07(a) Stack Temp. (DEG F) 499 501 | (kg/hr) (ppm) ********** Velocity (ft/sec) 150.27 150.43 | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 | Meter Temp. (Dey F) 82.0 84.0 |
| RULE A) | llowable40 Veloc. Head (''H2D) 2.80 2.80 2.80 2.70 | 07(a) Stack Temp. (DEG F) 499 501 500 | (kg/hr) (ppm) ********** Velocity (ft/sec) 150.27 150.43 147.64 | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.84 | Meter Temp. (Dey F) 82.0 84.0 86.0 |
| RULE A) | llowable40 Veloc. Head (''H2D) 2.90 2.80 2.80 2.70 2.90 | 07(a) Stack Temp. (DEG F) 499 501 500 498 | (kg/hr) (ppm) *********** Velocity (ft/sec) 150.27 150.43 147.64 150.2 | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.88 | Meter Temp. (Dey F) 82.0 84.0 86.0 88.0 |
| RULE A1 ****** Point (#) 1 2 3 4 5 | llowable40 Veloc. Head (''H2D) 2.90 2.80 2.70 2.80 2.70 | 07(a) ************************************ | (kg/hr) (ppm) ********** Velocity | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.88 0.85 | Meter Temp. (Dey F) 82.0 84.0 86.0 88.0 88.0 89.5 |
| RULE A1 ****** Point (#) 1 2 3 4 5 6 | llowable40 Veloc. Head (''H2D) 2.90 2.80 2.70 2.90 2.70 2.90 2.60 | 07(a) Stack Temp. (DEG F) 499 501 500 498 498 498 498 | (kg/hr) (ppm) ********** Velocity | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.84 0.88 0.85 0.32 | Meter Temp. (Dey F) 82.0 84.0 86.0 88.0 89.5 92.0 |
| RULE A ****** Point (#) 1 2 3 4 5 6 7 | llowable40 Veloc. Head (''H2D) 2.90 2.80 2.70 2.90 2.70 2.60 2.10 | 07 (a) Stack Temp. (DEG F) 499 501 500 498 498 498 498 497 497 | (kg/hr) (ppm) ********** Velocity | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.88 0.85 0.32 0.66 | Meter Temp. (Dey F) 82.0 84.0 86.0 88.0 89.5 72.0 72.3 |
| RULE A ****** Point (#) 1 2 3 4 5 6 7 8 | Veloc. Head (''H2D) 2.80 2.80 2.70 2.70 2.60 2.10 1.70 | 07 (a) Stack Temp. (DEG F) 499 501 500 498 498 498 498 497 500 | (kg/hr) (ppm) ********** Velocity | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.85 0.32 0.66 0.53 | Meter Temp. (Deg F) 82.0 84.0 86.0 88.0 89.5 92.0 92.5 93.5 |
| RULE A ****** Point (#) 1 2 3 4 5 4 5 6 7 8 9 | Veloc. Head (''H2D) 2.90 2.80 2.70 2.70 2.60 2.10 1.70 1.70 | 07 (a) Stack Temp. (DEG F) 499 501 500 498 498 498 498 497 500 500 500 500 500 | (kg/hr) (ppm) ********** Velocity | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.85 0.32 0.66 0.53 0.53 | Meter Temp. (Deg F) 82.0 84.0 86.0 88.0 87.5 72.0 72.5 73.5 73.5 74.5 |
| RULE A ****** Point (#) 1 2 3 4 5 6 7 8 9 10 | Veloc. Head (''H2D) 2.90 2.80 2.70 2.70 2.60 2.10 1.70 1.70 1.30 | 07 (a) Stack Temp. (DEG F) 499 501 500 498 498 498 498 497 500 500 500 500 500 500 500 50 | (kg/hr) (ppm) ********** Velocity | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.85 0.85 0.32 0.66 0.53 0.53 0.53 0.41 | Meter Temp. (Deg F) 82.0 84.0 86.0 88.0 89.5 92.0 92.5 93.5 93.5 94.5 96.0 |
| RULE A) ****** Point (#) 1 2 3 4 5 6 7 8 9 10 11 | Veloc. Head (''H2D) 2.80 2.80 2.70 2.80 2.70 2.60 2.10 1.70 1.70 1.30 0.74 | 07 (a) Stack Temp. (DEG F) 499 501 500 498 498 498 497 497 500 500 500 500 498 497 | (kg/hr) (ppm) ********** Velocity (ft/sec) 150.27 150.43 147.64 150.2 147.49 144.66 130.01 117.15 117.15 102.34 77.05 | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.85 0.85 0.85 0.32 0.66 0.53 0.53 0.53 0.53 0.41 0.23 | Meter Temp. (Deg F) 82.0 84.0 86.0 88.0 89.5 92.0 92.5 93.5 94.5 96.0 96.0 |
| RULE A) ****** Point (#) 1 2 3 4 5 6 7 8 9 10 11 12 | Veloc. Head (''H2O) 2.80 2.80 2.70 2.80 2.70 2.60 2.10 1.70 1.70 1.30 0.74 0.74 | 07(a) Stack Temp. (DEG F) 499 501 500 498 498 498 498 497 500 500 500 500 498 497 497 500 500 500 498 497 497 500 500 500 500 500 500 500 50 | (kg/hr) (ppm) ********** Velocity | = 13.61 = 2000 ********************************** | Meter Temp. (Deg F) 82.0 84.0 86.0 88.0 87.5 92.0 92.3 93.5 94.5 96.1 96.5 96.5 |
| RULE A) ****** Point (#) 1 2 3 4 5 6 7 8 9 10 11 12 13 | llowable40 Veloc. Head (''H2D) 2.80 2.80 2.70 2.80 2.70 2.60 2.10 1.70 1.70 1.30 0.74 0.74 2.70 | 07(a) Stack Temp. (DEG F) 499 501 500 498 498 498 497 500 500 500 500 498 497 500 500 500 498 497 500 500 500 500 500 500 500 50 | (kg/hr) (ppm) ********** Velocity | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.88 0.88 0.88 0.85 0.32 0.66 0.53 0.53 0.53 0.41 0.23 0.23 0.35 | Meter Temp. (Dey F) 82.0 84.0 86.0 88.0 89.5 72.0 72.5 72.0 72.5 74.5 74.5 76.0 76.5 88.0 |
| RULE A) ****** Point (#) 1 2 3 4 5 6 7 8 9 10 11 12 13 14 | Veloc. Head (''H2D) 2.80 2.80 2.70 2.80 2.70 2.60 2.10 1.70 1.70 1.70 1.30 0.74 0.74 2.70 2.70 | 07 (a) Stack Temp. (DEG F) 499 501 500 498 498 498 497 500 500 500 500 498 497 500 500 500 500 500 500 500 50 | (kg/hr) (ppm) *********************************** | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.88 0.88 0.85 0.32 0.66 0.53 0.53 0.41 0.23 0.23 0.35 0.84 | Meter Temp. (Deg F) 82.0 84.0 86.0 88.0 89.5 92.0 92.5 93.5 94.5 96.0 96.5 88.0 89.5 |
| RULE A) ****** Point (#) 1 2 3 4 5 6 7 8 9 10 11 12 13 | llowable40 Veloc. Head (''H2D) 2.80 2.80 2.70 2.80 2.70 2.60 2.10 1.70 1.70 1.30 0.74 0.74 2.70 | 07 (a) Stack Temp. (DEG F) 499 501 500 498 498 497 500 500 500 500 498 497 500 500 500 500 500 500 500 50 | (kg/hr) (ppm) ********** Velocity | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.88 0.88 0.88 0.85 0.32 0.66 0.53 0.53 0.53 0.41 0.23 0.23 0.35 | Meter Temp. (Deg F) 82.0 84.0 86.0 88.0 89.5 92.0 92.5 93.5 94.5 96.0 96.5 88.0 89.5 95.5 92.0 |
| RULE A) ****** Point (#) 1 2 3 4 5 6 7 8 9 10 11 12 13 14 | Veloc. Head (''H2D) 2.80 2.80 2.70 2.80 2.70 2.60 2.10 1.70 1.70 1.70 1.30 0.74 0.74 2.70 2.70 | 07 (a) Stack Temp. (DEG F) 499 501 500 498 498 498 497 500 500 500 500 498 497 500 500 500 500 500 500 500 50 | (kg/hr) (ppm) *********************************** | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.88 0.88 0.85 0.32 0.66 0.53 0.53 0.41 0.23 0.23 0.35 0.84 | Meter Temp. (Deg F) 82.0 84.0 86.0 88.0 89.5 92.0 92.5 93.5 94.5 96.0 96.5 88.0 89.5 |
| RULE A) ****** Point (#) 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 | Veloc. Head (''H2D) 2.80 2.80 2.70 2.80 2.70 2.60 2.10 1.70 1.70 1.70 1.30 0.74 0.74 0.74 2.70 2.70 2.70 | 07 (a) Stack Temp. (DEG F) 499 501 500 498 498 497 500 500 500 500 498 497 500 500 500 500 500 500 500 50 | (kg/hr) (ppm) *********** Velocity | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.88 0.88 0.85 0.32 0.66 0.53 0.53 0.41 0.23 0.23 0.23 0.84 0.84 | Meter Temp. (Deg F) 82.0 84.0 86.0 88.0 89.5 92.0 92.5 93.5 94.5 96.0 96.5 88.0 89.5 95.5 92.0 |
| RULE A1 ****** Point | Veloc. Head (''H2O) 2.80 2.80 2.70 2.80 2.70 2.60 2.10 1.70 1.70 1.70 1.30 0.74 0.74 2.70 2.70 2.70 2.70 2.70 2.70 2.70 2.70 | 27 (a) ************************************ | (kg/hr) (ppm) *********************************** | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.88 0.88 0.85 0.85 0.32 0.66 0.53 0.53 0.41 0.23 0.23 0.23 0.85 0. | Meter Temp. (Deg F) 82.0 84.0 86.0 88.0 87.5 92.0 92.5 93.5 93.5 94.5 96.0 96.5 88.0 89.5 95.5 92.0 93.5 |
| RULE AI ****** Point (#) 1 2 3 4 5 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 | llowable40 Veloc. Head (''H2D) 2.90 2.80 2.70 2.80 2.70 2.60 2.10 1.70 1.70 1.70 1.30 0.74 0.74 2.70 2.70 2.70 2.70 2.70 2.70 2.70 2.70 | 27 (a) Stack Temp. (DEG F) 499 501 500 498 498 497 500 500 500 500 500 500 500 50 | (kg/hr) (ppm) ********** Velocity | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.85 0.85 0.32 0.66 0.53 0.53 0.53 0.53 0.53 0.41 0.23 0.23 0.23 0.84 0.84 | Meter Temp. (Deg F) 82.0 84.0 86.0 88.0 87.5 72.0 72.5 73.5 74.5 76.1 76.5 88.0 87.5 88.0 87.5 76.5 88.0 87.5 72.0 73.5 75.5 |
| RULE AI ****** Foint (#) 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 | llowable40 Veloc. Head (''H2D) 2.90 2.80 2.70 2.80 2.70 2.60 2.10 1.70 1.70 1.70 1.70 1.30 0.74 0.74 2.70 2.70 2.70 2.70 2.70 2.70 2.70 2.70 | 07 (a) ************************************ | (kg/hr) (ppm) ********** Velocity | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.88 0.85 0.32 0.66 0.53 0.53 0.53 0.53 0.53 0.53 0.53 0.41 0.23 0.23 0.23 0.84 0.84 0.84 0.84 0.84 0.84 0.84 0.75 | Meter Temp. (Dey F) 82.0 84.0 84.0 86.0 88.0 87.5 92.0 92.5 93.5 94.5 96.1 96.5 88.0 89.5 96.5 88.0 89.5 92.0 93.5 95.5 95.5 97.5 97.5 |
| RULE A ****** Point (#) 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 19 20 | llowable40 Veloc. Head (''H2D) 2.90 2.80 2.70 2.80 2.70 2.60 2.10 1.70 1.70 1.70 1.70 1.30 0.74 0.74 2.70 2.70 2.70 2.70 2.70 2.70 2.70 2.70 | 07 (a) ************************************ | (kg/hr) (ppm) ********** Velocity | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.85 0.32 0.66 0.53 0.53 0.53 0.53 0.53 0.53 0.53 0.41 0.23 0.23 0.23 0.23 0.84 0.84 0.84 0.84 0.84 0.84 0.84 0.84 0.75 0.72 | Meter Temp. (Deg F) 82.0 84.0 86.0 88.0 87.5 92.0 92.5 93.5 94.5 96.0 96.5 88.0 87.5 95.5 95.5 97.5 97.5 101.0 |
| RULE A) ****** Point (#) 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 | llowable40 Veloc. Head (''H2D) 2.80 2.70 2.80 2.70 2.60 2.10 1.70 1.70 1.70 1.30 0.74 0.74 2.70 2.70 2.70 2.70 2.70 2.70 2.70 2.70 | 07 (a) Stack Temp. (DEG F) 499 501 500 498 498 498 497 500 500 500 500 500 500 500 50 | (kg/hr) (ppm) ********** Velocity | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.88 0.85 0.32 0.66 0.53 0.72 0.84 0.84 0.84 0.85 0.72 0.84 0.84 0.85 0.72 0.72 0.72 0.72 0.72 | Meter Temp. (Deg F) 82.0 84.0 86.0 88.0 87.5 92.0 92.3 93.5 94.5 96.0 96.5 96.5 88.0 89.5 96.5 88.0 89.5 95.5 95.5 97.5 97.5 101.0 102.0 |
| RULE A) ****** Point (#) 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22 | llowable40 Veloc. Head (''H2D) 2.80 2.80 2.70 2.80 2.70 2.60 2.10 1.70 1.70 1.70 1.70 1.70 2.00 2.00 | 07(a) Stack Temp. (DEG F) 499 501 500 498 498 498 497 497 500 500 500 500 500 500 500 50 | (kg/hr) (ppm) ********** Velocity | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.88 0.85 0.32 0.66 0.53 0.53 0.53 0.53 0.53 0.53 0.53 0.41 0.23 0.23 0.23 0.23 0.23 0.23 0.84 0.84 0.84 0.84 0.84 0.84 0.84 0.84 0.84 0.84 0.84 0.85 0.53 0.54 0.53 0.54 0.54 0.54 0.57 0.72 0.53 0.53 0.53 0.53 0.53 0.53 0.53 0.54 0.54 0.54 0.53 0.57 0.72 0.53 0.53 0.53 0.53 0.53 0.57 0.57 0.57 0.57 0.53 0.55 0. | Meter Temp. (Deg F) 82.0 84.0 86.0 88.0 87.5 92.0 92.3 93.5 94.5 96.0 96.5 96.5 88.0 89.5 96.5 88.0 89.5 95.5 97.5 97.5 97.5 101.0 102.0 103.5 |
| RULE A) ****** Point (#) 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 | llowable40 Veloc. Head (''H2D) 2.80 2.70 2.80 2.70 2.60 2.10 1.70 1.70 1.70 1.30 0.74 0.74 2.70 2.70 2.70 2.70 2.70 2.70 2.70 2.70 | 07 (a) Stack Temp. (DEG F) 499 501 500 498 498 498 497 500 500 500 500 500 500 500 50 | (kg/hr) (ppm) ********** Velocity | = 13.61 = 2000 Drifice Press. (''H2D) 0.88 0.88 0.88 0.88 0.88 0.85 0.32 0.66 0.53 0.72 0.84 0.84 0.84 0.85 0.72 0.84 0.84 0.85 0.72 0.72 0.72 0.72 0.72 | Meter Temp. (Deg F) 82.0 84.0 86.0 88.0 87.5 92.0 92.3 93.5 94.5 96.0 96.5 96.5 88.0 89.5 96.5 88.0 89.5 95.5 95.5 97.5 97.5 101.0 102.0 |

IT-70

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Hit any key to continue ...

Source Test 99-0000 Summary Prepared on 12-17-99 at 13:25:04

| Pitot Correction Factor= Gas Density Correction Factor= Flue Correction Factor (A/B)= Velocity Pressure Correction Factor= Dry Gas Meter Calibration Factor= Magnehelic Calibration Factor= Total Sampling Time(minute) = Gas Volume Metered(dcf) = Corrected Gas Volume Metered(dscf) = Average Wet Mclecular Weight= | 1.200 0.987 1.0231 1 60 30.244 29.55 |
|---|--|
| Average Percent Dxygen | 158947 88543 77260 |

Hit any key to continue +++

Source Test 99-0000 Summary Prepared on 12-17-99 at 13:25:04 RULE 404: Particulate Concentration (gr/dscf) = 0.012(ma/dscm) = 27.5 RULE 405: Solid Emission Rate.....(1b/hr) = 6.22 (kg/hr) = 2.82RULE 407: Average ppm Carbon Monoxide....(CO) = 0 Isokinetic Sampling Rate.....(%) = 97 RULE Allowable.....405(a).....(1b/hr) = 30.00(kg/hr) = 13.61

Hit any key to continue ...

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT

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| Sampling Location FCCU - ESP STACK Alles Sample (Lab Results) Solution (Lab Results) Solution (Lab Results) Solution FILTER (TRIMALC) (ATCH, AS SO2, my <11(4/PD) | | |
|---|---|---|
| (Lab Results) So2 Surver Martis FILTER (TRIMALC) (ATCH, As So3, Mg <1114/80 - 0 - 0 - Calculated By IPA CATCH, As So2 (TITRATINA), Mg 1x64/80 - 1 Calculated By - 1 Calculated By PEROVIDE (ATCH, As So2, Mg 1x64/80 - 1 183 183 PEROVIDE (ATCH, AS So2, Mg TOTAL 183 183 185 | | |
| SAL SAL FILTER (TRIMALC) (ATCH, AS SO3, M3 <1164/80 - 0 IPA CATCH, AS SO2 (TITRATINA), M3 1×64/80 - 1 Calculated By PEROXIDE (ATCH, SO2, M3 1×64/80 TOTAL 1×3 1×3 183 1×3 1×4 | c.s. | |
| EPA CATCH, AS SO2 (TITRATINA), Mg 1×64/80 - 1 1 Catculated by 'EROKIDE (ATCH, SO2, MS 183 183 183 183 TOTAL 183 184 Checked By | C.S. | |
| EROXIDE CATCH, Soz, MS 183 183 183 TOTAL 183 184 184 Checked By | (PA) | |
| | $(\sigma \sim$ | |
| SOURCE TEST CALCULATIONS | | |
| | | |
| SURGIARY | | |
| A. Average Traverse Velocity (Pre-Test) | fps | |
| 3. Average Reference Point Velocity (Pre-Test) | | |
| C. Average Traverse Velocity (During Test) | <u>.7·2</u> fps | |
| | 72 min | |
| 8. Stack Cross Sectional Areaft ² K. Nozzle Cross-Sectional Area | <u> ft² </u> ft² | |
| Barometric Pressure | 1 <u>83_</u> mg 1 <u>84_</u> mg <i>a</i> 60 5 | |
| G. Cas Meter Pressure | <u>ryu</u> mgabe | |
| . Pitot Correction Factor 0. Gas Volume Hetered 3 | 3.07 dcf | |
| | 3.6º dscf | |
| 460 ± 60 | | |
| PERCENT HOISTURE - GAS DENSITY - FROM PM | | |
| Percent Water Vapor in Gas Sample $\frac{4.64 \times N}{(0.0464 \times N) + P}$ TRAIN | 2 <u>74</u> z | |
| . Average, Holecular Weight: | <u>+</u> | |
| v. Whet a Re ⁴ up te catel, met Buc: | | |
| (Component) (Volume Z / 100) x (1 - Z/100) x (Holec. Wt.) = (Wt./ | Hole) | |
| Water 1.00 18.0 | | |
| Carbon Diouida | | |
| Carbon Dioxide Dry Basis 0.9726 44.0 | | |
| Carbon Monoxide Dry Basis 0.8726 28.0 | | |
| Carbon MonoxideDry Basis0.872.628.0OxygenDry Basis6.972.632.0 | | |
| Carbon Monoxide Dry Basis 0.872.6 28.0 | | |
| Carbon MonoxideDry Basis0.872.628.0OxygenDry Basis6.972.632.0 | | |
| Carbon Honoxide Dry Basis 0.872.6 28.0 Oxygen Dry Basis 6.972.6 32.0 Nitrogen & Inerts Dry Basis 6.972.6 28.2 | | |
| Carbon MonoxideDry Basis0.872.628.0OxygenDry Basis6.972.632.0 | | |
| Carbon Monoxide Dry Basis 0.9726 28.0 Oxygen Dry Basis 6.9726 32.0 Nitrogen & Inerts Dry Basis 6.9726 28.2 (Sum) | | |
| Carbon Monoxide Dry Basis 0.2726 28.0 Oxygen Dry Basis 6.9726 32.0 Nitrogen & Inerts Dry Basis 6.9726 28.2 (Sum) | 2. | |
| Carbon Monoxide Dry Basis 0.972.6 28.0 Oxygen Dry Basis 6.972.6 32.0 32.0 Nitrogen & Inerts Dry Basis 6.972.6 28.2 32.0 Nitrogen & Inerts Dry Basis 6.972.6 28.2 32.0 Nitrogen & Inerts Dry Basis 6.972.6 28.2 32.0 Iow Basis 6.972.6 28.2 32.0 32.0 32.0 Cas Density Correction Factor 28.95/R 1.00 1.00 1.00 1.00 | 2 | |
| Carbon Monoxide Dry Basis 0.872.6 28.0 Oxygen Dry Basis 6.972.6 32.0 | | |
| Carbon Monoxide Dry Basis 0.872.6 28.0 Oxygen Dry Basis 6.972.6 32.0 Nitrogen & Inerts Dry Basis 6.972.6 32.0 Nitrogen & Inerts Dry Basis 6.972.6 28.2 Image: State of the state | o 7 fps | |
| Carbon Monoxide Dry Basis $0.272.6$ 28.0 Oxygen Dry Basis $6.472.6$ 32.0 Nitrogen & Inerts Dry Basis $0.472.6$ 32.0 (Sum) LOW RATE Gas Density Correction Factor $\sqrt{28.95/R}$ I 0.6 Velocity Pressure Correction Factor $\sqrt{29.92/H}$ Orgen 2.6 I 0.6 I | 0 7fps 47cfm | |
| Carbon Monoxide Dry Basis 0.872.6 28.0 Oxygen Dry Basis 6.972.6 32.0 Nitrogen & Inerts Dry Basis 0.972.6 28.2 (Sum) LOW RATE Sum 1.00 RATE Sum 1.00 Velocity Correction Factor √28.95/R I.00 Velocity Pressure Correction Factor √28.95/R 0.92/H 0.92/H 0.92/H 0.92/H 0.92/H 0.938 Oxygen 1.00 I.00 | o 7 fps | |
| Carbon MonoxideDry Basis $0.872.6$ 28.0OxygenDry Basis $6.472.6$ 32.0Nitrogen & InertsDry Basis $6.472.6$ 28.2(Sum)LOW RATEGas Density Correction Factor $\sqrt{28.95/R}$ 1.06Flue Correction Factor $\sqrt{28.95/R}$ 0.05 StCorrected Velocity (C x I x S x T x U)105.0Store K ate (W x $\frac{H}{29.92}$ x $\frac{520}{460 + D}$)Store K ate (X x (1 - Q/100)]Store K ate (X x (1 - Q/100)] | 0 7fps 47cfm | |
| Carbon MonoxideDry Basis $0.972.6$ 28.0OxygenDry Basis $6.972.6$ 32.0Nitrogen & InertsDry Basis $6.972.6$ 28.2(Sum)LOW EATEGas Density Correction Factor $\sqrt{28.95/R}$ 1.00Flue Correction Factor $\sqrt{28.95/R}$ 1.00Velocity Pressure Correction Factor $\sqrt{29.92/H}$ Orygen1.00Jow Rate (V x E x 60)Jow Rate (V x E x 60)StateFlow Rate (V x $\frac{H}{29.92}$ x $\frac{520}{460 + D}$)Flow Rate (I x $(1 - Q/100)$)Flow Rate (I x $(1 - Q/100)$) | 0 7 47 47 cfm 43_scfm | |
| Carbon MonoxideDry Basis $0.872.6$ 28.0OxygenDry Basis $a.\sqrt{72.6}$ 32.0Nitrogen & InertsDry Basis $a.\sqrt{72.6}$ 28.2(Sum)(Sum)LOW RATEGas Density Correction Factor $\sqrt{28.95/R}$ 1.00Flue Correction Factor $\sqrt{28.95/R}$ 1.00Velocity Pressure Correction Factor $\sqrt{29.92/H}$ Other StresserOther StresserOther StresserOther StresserOther StresserPlow Rate (W x H 29.92 x $\frac{520}{460 + D}$)R UPSPlow Rate (W x $\frac{H}{29.92}$ x $\frac{520}{460 + D}$)R UPSONCENTRATION - EMISSION RATEOther StresserOncentration StresserOther StresserOther StresserOther StresserNPLE CONCENTRATION - EMISSION RATE | 0 1 47 cfm 43 scfm 60 dscfm | |
| Carbon MonoxideDry Basis $0.872.6$ 28.0 OxygenDry Basis $a. \leq 72.6$ 32.0 Nitrogen & InertsDry Basis $a. \leq 72.6$ 28.2 (Sum)(Sum)LOW RATEGas Density Correction Factor $\sqrt{28.95/R}$ 1.00Flue Correction Factor $\sqrt{28.95/R}$ 1.00Velocity Pressure Correction Factor $\sqrt{29.92/H}$ Orected Velocity (C x I x S x T x U)105 corrected Velocity (C x I x S x T x U)Flow Rate (V x E x 60)Sample Concentration (0.01543 x L/P)Corrector factor $\sqrt{28.95/R}$ 1.00I.00I.00I.00Flow Rate (V x E x 60)Flow Rate (V x E x 60)I x $\frac{520}{460 + D}$ R $\frac{1005}{2}$ Trl. 5 $\frac{50}{2}$ Sample Concentration (0.01543 x L/P) | 0 1 1 1 1 1 1 1 1 1 1 1 1 1 | |
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| Carbon MonoxideDry Basis $0.972.6$ 28.0OxygenDry Basis $6.972.6$ 32.0Nitrogen & InertsDry Basis $0.972.6$ 28.2(Sum)LOW EATEGas Density Correction Factor $\sqrt{28.95/R}$ I.000Flue Correction Factor $\sqrt{28.95/R}$ I.000Flue Correction Factor $\sqrt{28.95/R}$ I.000Correction Factor $\sqrt{28.95/R}$ I.000Flue Correction Factor $\sqrt{29.92/H}$ Other Correction Factor $\sqrt{29.92/H}$ Corrected Velocity (C x I x S x T x U)Flow Rate (V x E x 60)Flow Rate (X x (1 - Q/100))Flow Rate (X x (1 - Q/100))Flow Rate (X x (1 - Q/100))Flow Rate (X x (1 - Q/100))Sample Concentration (0.01543 x L/P)Sample Concentration (0.01543 x L/P)Sample Concentration (0.01543 x X / 64MPICLE CONCENTRATION - EMISSION RATESample Concentration (0.00857 x x x Z) | fps 47_cfm 43_scfm 60_dscfm gr/dscf ppm (dr | |
| Carbon MonoxideDry Basis $0.972.6$ 28.0OxygenDry Basis $6.972.6$ 32.0 Nitrogen & InertsDry Basis $0.972.6$ 28.2 (Sum)(Sum)LOW RATEGas Density Correction Factor $\sqrt{28.95/R}$ 1.000Flue Correction Factor $\sqrt{28.95/R}$ 1.000Velocity Pressure Correction Factor $\sqrt{29.92/H}$ Orgen and the factor $\sqrt{29.92/H}$ <td colspan<="" td=""><td>fps 47_cfm 43_scfm 60_dscfm gr/dscf ppm (dr 1b/hr b/hr</td></td> | <td>fps 47_cfm 43_scfm 60_dscfm gr/dscf ppm (dr 1b/hr b/hr</td> | fps 47_cfm 43_scfm 60_dscfm gr/dscf ppm (dr 1b/hr b/hr |

-25-

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT 9150 Flair Drive, El Monte, California 91731

Test No. 99-0000

Date 11/9/99

SULFUR EVALUATION AND PROCESS MASS FLOW RATE CALCULATION FOR FCCU

| | | TOTAL |
|-----------|---|--------------|
| A. | SO2 flow rate, 1b/hr | 56 |
| B. | Fuel gas flow rate, Miscfd ⁴ | - |
| c. | H ₂ S concentration, ppm | - |
| D. | H ₂ S flow rate (BC/24), scfh | - |
| E. | SO2 flow rate (from fuel), 1b/hr | |
| | $\frac{(D \text{ scf } H_2S/hr)(1 \text{ lb mole } SO_2/lb \text{ mole } H_2S) **(64 \text{ lb } SO_2/lb \text{ mole } SO_2)}{(379 \text{ scf } H_2S/lb \text{ mole } H_2S)} =$ | - |
| Σ. | SO ₂ from FCCU regenerator (A-E), 1bg/hr | 56 |
| G.1 | FCCU Feed rate, Bb1/day* | 1,950 |
| G.2 | FCCU Feed rate, (<u>G.1 x 286 lb/Bbl</u>), lb/hr | 16,490 |
| H. | FCCU Feed rate (G.1/24000), 1000 Bb1/hr, | 1.456 |
| I. | Oxides of Sulfur to the Atmosphere | |
| | From the FCCU regenerator (F/H); 1b\$/1000 Bb1 | 38.5 17.5 |
| J. | Catalyst Recycle Rate, 3.570 | ,000 |
| | 29.75 (tons/min) (2000 lbs/ton) (60 min/hr, lb\$/hr* | |
| K. | Process weight (G.2 + J), 1b/hr | TONT |

* Obtained from CHAMPION

 $** O_2 + H_2S \longrightarrow SO_2 + H_2$

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT 9150 Flair Drive, El Monte, California 91731

Test No. <u>99-0000</u>

Date 11/9/99

RELATIVE ACCURACY OF CONTINUOUS EMISSION MONITOR

| RELATIVE ACCURACY OF CONTINUOUS ENISSION HUNT | |
|--|---|
| Company/Unit | Alpha Specific Resources(FCCU (Cherry)o) |
| Equipment being Monitored | ESP |
| If Time-Shared, Describe Time Sequence of Operation | Continuous |
| Monitor Manufacturer/I.D. Number | KVB Model C84263 |
| Monitor SCAQMD Certification Date | - Thermo Electron |
| NOx Analyzer Manufacturer-Model #, Serial # | 10AR.16803-165 |
| CO Analyzer Manufacturer-Model #, Serial # | |
| 0, Analyzer Manufacturer-Model #, Serial # | Thermox WDG,2-8193 |
| SO, Analyzer Manufacturer-Model #, Serial # | Model_722A/62703 |
| Gas Component Tested for | so ₂ |
| A. Reference Method (AQMD Method 6.1) Value. Corrected, ppm (dry) | 71 ppm |
| B. Reference Method Sampling Time Interval | <u>1:48 - 3:05 P.M.</u> |
| C. Monitor Reading, Average and Corrected, ppm (dry) | 75.5 ppm |
| D. Monitor Recording Time Interval(1327_71= | 1:50 - 2:35 |
| EMaximum Allowable Concentration, ppm (dry) | 243 ppm |
| F. Relative Accuracy, & | |
| Deviation from <u>CA.</u> $\times 100 = \frac{75.5 - 71}{71}$ | x 100 ±†6 .34- |
| Deviation from <u>CA.</u> $x 100 = \frac{75.5 - 71}{243}$ | x 100 =†1.85 |
| · · · · · · · · · · · · · · · · · · · | |

11-75

-27-SOUTH COAST AIR QUALITY MANAGEMENT DISJUICT

ST NO. 99-0000

PAGE____

-DATE 11/9/99

-SAMPLING LOCATION FCCU - ESP STACK

REFINERY PROCESS DATA SHEET/FLUID CATALYTIC CRACKING UNIT

PCCU OPERATING DATA

| | | , | | | | | |
|---|---|---|-------------------------------|---------------|---------------------------------------|--|------------------|
| 1. | Feed Rate, b | bl/day | | | 34,950 | | |
| 2. | Percent Weig | ht Sulfur in 7 | eed | | | 18% | _ |
| | | | | | | 75 | |
| 4. | Coke Burnoff | Rate, 1b/hour | | | 26,794 | | |
| 5. | Regenerator | Air Rate, scfm | | | 5. | 164 X 10 ^b | |
| 6. | Flue Gas Rat | e, (Regenerato | r), scfm | | 5. | 484 X 106 | |
| 7. | Flue Gas Rat | e, (CO Boiler) | , scfm | | N/A | | |
| - | Seastor-Temp | erature; | | | N/A-CO | NFIDENTIAL | |
| 9,== | Reactor Fres | sure, psig | | | N/A-CO | NFIDENTIAL | - |
| 10. | TeSO _x Cataly | st Addition Rai | te, 1b/day | | ~ 40 | | _ |
| 11 | Regenerator | Top-Temperature | e, *F | | | NFIDENTIAL | - |
| 12 | Regenerator- | Top Pressure, | psig | | N/A-CO | NFIDENTIAL | |
| 2. / | ESP Outlet To Ammonia Inje Injection Po | ction Rate and | Location of t | he | | opm <u>.Flue Gas</u> "T" | - _Ductw |
| CET D | <u></u> | | | | | | |
| 1. (| CEM Manufactu | rer <u>KVB</u> | Nodel # | <u>C84263</u> | _Cett. / | · · · · · · · · · · · · · · · · · · · | |
| 4 | Analyzer | Mfg. | Model # | S/N | Reading (Pr) | Time | Ren |
| 2. 1 | NOx (may cons) | Thermo Electr | on 10AR | 16803-165 | 15 pp | m <u>12:10 p.m.</u> | 500 8 |
| | SO ₂ | Western Resea | | 6270-3 | | = <u>12:10 p.m.</u> ≡ <u>12:10 p.m.</u> | |
| | 02 | Therm Ox | WOG CONTROL | 2-8193 | 2.187 * | | - 10% |
| | CO | Beckman Ind. | <u>865</u> | | | ■ <u>12:10 p.m.</u> | |
| | CO ₂ | N/A | N/A | N/A | <u>N/A</u> | - <u>N/A</u> | |
| | ~2 | <u>N/A</u> | <u>N/A</u> | | <u> </u> | N/A | _ |
| со во | DILER -N/A | | | | | | |
| | | | | | | | |
| | | r Rate, sofm. | | | | | |
| 1. 0 | Combustion Ai | r Rate, scfm | Temperature (| •• | | | - |
| 1. C 2. F | Combustion Ai Regenerator F | lue Gas Inlet | Temperature, | •F | | | - |
| 1. C 2. F 3. F | Combustion Ai Regenerator F Regenerator F | lue Gas Inlet lue Gas Inlet | Temperature, ' Pressure, | •F | · · · · · · · · · · · · · · · · · · · | | - |
| 1. C 2. F 3. F | Combustion Ai Regenerator F Regenerator F Inches of Wat | lue Gas Inlet lue Gas Inlet er Column | Temperature, ' Pressure, | •F | | | - |
| 1. C 2. F 3. F 1 4. F | Combustion Ai Regenerator F Regenerator F Inches of Wat Fuel Gas Rate | lue Gas Inlet lue Gas Inlet er Column , 10 ³ scfh | Temperature, ' Pressure, | •F | | | - |
| 1. C 2. F 3. F 4. F 5. P | Combustion Ai Regenerator F Regenerator F Inches of Wat Fuel Gas Rate Trebox Tempe | lue Gas Inlet lue Gas Inlet er Column , 10 ³ scfh rature, 3 P | Temperature, Pressure, | •F | | | - |
| 1. C 2. F 3. F 4. F 5. P | Combustion Ai Regenerator F Regenerator F Inches of Wat Fuel Gas Rate Trebox Tempe | lue Gas Inlet lue Gas Inlet er Column , 10 ³ scfh rature, 3 P | Temperature, Pressure, | •F | | | - |
| 1. C 2. F 3. F 4. F 5. P 6. S | Combustion Ai Regenerator F Regenerator F Inches of Wat Fuel Gas Rate Trebox Tempe | lue Gas Inlet lue Gas Inlet er Column , 10 ³ scfh rature, 3 P | Temperature, Pressure, | •F | | | - |
| 1. C 2. F 3. F 4. F 5. P 6. S RECOR I hav | Combustion Af Regenerator F Regenerator F Inches of Wat Puel Gas Rate Trebox Tempe Steam Rate, 1 RDED BY | lue Gas Inlet lue Gas Inlet er Column , 10 ³ scfh rature, 3 P 0 ³ 1b/hour | Temperature, Pressure, | •F | | | |
| 1. C 2. F 3. F 3. F 5. P 6. S RECOR I hav knowl | Combustion Ai Regenerator F Regenerator F Inches of Wat Fuel Gas Rate Firebox Tempe Steam Rate, 1 RDED BY ve reviewed t | lue Gas Inlet lue Gas Inlet er Column rature, 30 O ³ 1b/hour he above proce | Temperature, Pressure, | •F | accurate, to | o the best of | |

SOUTH COAST AIR QUALITY HANAGENERIT DISTRICT

| Test Ho. | | | | | | | b | ot <i>e</i> : | 11/9/ | 99 | _ | | |
|---------------------------|--|---------------------------------------|--|--|--------------------|------------------|---------------|---------------|------------|--|--|---------------------|--|
| Sampling | ; Locat | ion: 7 | <u>'Cou</u> _ | ESP | STACK | | [šī | mple T | rain / | Sartie | alat | <u>es</u> | |
| | | | TIAV | | OURCE TE | ST DATA | | | | | <u></u> | | |
| Pre-Jest | | | 10aa . | Ki = | D.174 | | | | Lesk C | | 9 11. | | |
| Filler | Filter $\angle 0.005$ cfm @ 15 "Hg vac $K_2 = 0.835$ Filter $\angle .0/cfm @ 5$ "Hg vac Frohe $\angle 0.005$ cfm @ 15 "Hg vac $K_3 = 0.86$ Frohe $\angle .0/cfm @ 5$ "Hg vac | | | | | | | | | | | | |
| Franz Z | (rilot Tube Leak Check of U.L.) V . 1 (rilot Tube Leak Check Of U.D. | | | | | | | | | | | | |
| | | · · · · · · · · · · · · · · · · · · · | | Ka = 1 Ka = 1 | 0.619 | | | | | | · | | |
| Tlar | Samp Polai | Gas Hele | | Jock | | alculate | <u>ed</u> | | Filter | Heler | j Gada | Vacuum | |
| On Off | | Reading (dcf) | Velue (L) Bead | | Velocity (fes) | Sampling Rate | 101 | Li Caula - | lengi. | •! | the second s | *Hg | |
| | | | ("H ₂ /1) | •F | | (cf=) | ("#20) | •F | •F | 14 | thit | | |
| 12.51 | | 597,197 | | | | | | | | | - | | |
| <u>+2.5</u> <u>5.0</u> | ╾┝╾╇ | 569.4 | 2.8 | 499 | 150.9 | | .88 | | 182 | <u>86</u> | 7B RO | 7.5 | |
| 7.6 | -[| 1202.6 | | 500 | | .57 | - 84 | | 196 | | <u>a</u> i | 2.5 | |
| 10.01 | | 603.5 | 2.8 | 448 | 150.2 | .58 | Be | 22 | | 94 | 82 | 3.0 | |
| 12.6 | | 60A.6 | 2.7 | 498 | | - 57 | <u></u> | | 208 | - 26 - | <u>8</u> 3 | <u>. 2.5</u> | |
| 16.0 | ┼╌┿ | 606.7 | 2.6 | 497 | 140.7 | .50 | ·87 .66 | | | | <u>86</u> 86 | 2.5 | |
| 200 | 6 | 608.9 | 1.7 | 500 | 17.2 | 45 | .53 | 220 | | | A2 | 2.0 | |
| | 1 | 610.1 | 1.7 | 500 | 112.2 | .45 | .53 | 213 | 705 | 101 | 88 | 20 | |
| | <u> 0</u> 1 | 612.2 | 1.3 | 448 | 102.3 | <u>40</u> 30 | -41 -25 | 212 | 204 | | 90 91 | 20 | |
| 10.0 130 / | - <u>-</u> ";- | 617.1 | | 494 | | <u></u> | | 222 | _205 | | <u> </u> | 10 | |
| | | | | | | | | | | | | | |
| | ļ | 613.1 | | | | | | | | | | | |
| 311 | <u></u> | 614-1 | 27 | 496 | 147.5 | .57 | ·85 | 206 | | 88 6 90 8 | | 2.5 | |
| | 14 | 613.71 | 2.7 | 500 | 147.6 | 31 | .84 | | | | - | 7.5 | |
| | 16 | 618.7 | 22 | 498 | 147.5 | .57 | .84 | | | | 69 | 25 | |
| | | 620.1 | 2.0 | 498 | 1447 | -54 | <u>_18_</u> _ | 200 | | | | <u> </u> | |
| | 19 | 622.8 | _ | 500 | 147.6 | .57 | <u>-84</u> | 207 | 204 208 | | | 2.5 | |
| | 20 | 626.2 | | 499 | 136.2 | . 53 | .72 | 218 | | | | 2.5 | |
| | 21 | 625.4 | | 497 | 136.1 | .53 | | ZOB | | | | 2.5 | |
| | 27 | 626.6 | 2.0 | 496 | 126.8 | .22 | | <u>203 </u> | | 09 9 | | 2.0 | |
| | 73 | 627.6 | | 495 | 63.4 | .25 | | | | 105 10 | _ | | |
| (Net Vol. Und | | | | 44iB | 129.4 | | .68 | | | | | | |
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| Barometric P | · · · | | .40 | <u></u> " p | y ku Pti | Lot Facl | | | | | 835 | | |
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| Gas Heter No. | | الا ومسكل وسامينا | | 1518 | ∠∦ [] | 1 | | | - | <u> </u> | Dimen | slons | |
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| Heter Corr. F | <u><u><u><u></u></u><u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u><u></u></u></u></u> | 1.0231 | | | ╧╽╽╌ | ┹┝╲ | _/2ª | 二 | - 1 | | | | |
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| Sampl | ing Loc | ation | PCC | <u>10 - E</u> | SP STACK | | SOX | | | | | | |
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| Time | Trav. | 1 | Vel. | Temp. | Calc. | 1 | Vel. | Temp | Calc. | | Vel. | Temp. | Cal |
| | Point | | Head | (°F) | Vel. | . /. | Head | (*F) | Vel. | | Head | (*F) | Vel |
| | | | ("H ₂ O) | F1(76 | (Eps) | VAr | ("H ₂ 0) | | (fps) | <u> </u> | ("H ₂ 0) | | (fp |
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-29-

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT 9150 Flair Drive, Bl Monte, California 91731

-30-

TECHNICAL SERVICES DIVISION LABORATORY SERVICES BRANCE REPORT OF TOTAL CONBUSTION ANALYSIS (TCA) FOR CARBONACEOUS MATTER

| TO: Rod Rock | | Date of Repo | rti12/9/99 | <u> </u> |
|---------------------------|------------------------------|--------------|------------|----------|
| Source Testing | j & Monitoring | Test. Wo.: | 99-0000 | |
| Mame of Company: City: | Champion Petroleum Utopia | Test Date: | 11/9/99 | |
| Equipment Tested: | PCCU, ESP | Lab. No.: | 11111 | |
| | | Ref. Book No | . 22222 | |
| | | Requested By | t C.S. | |

| Sample Identification | Sampling Points | | | | | | | |
|--------------------------|-----------------|-------|-----|---|----------|--|--|--|
| Items | Outlet | | | | | | | |
| Nominal Volume-2 Liters: | · · · | | | 1 | <u> </u> | | | |
| Bulb Identification | 103 | 104 | 105 | | l | | | |
| Bulb Pressure, Torr | -745 | : 747 | 749 | | | | | |
| | | | | | | | | |

for Analysis:

Breakdown of Sample Items Results of Analysis of Samples Listed Above AS PPH CO.

. •

| Bulb Contents: CO ₂ actually present ^{a)} CO actually present | 145000 | 139000 | 144000 | | |
|---|--------|--------|--------|------|--|
| NO2 | 3.4 | 3.3 | 3.3 | | |

a) CO₁ present in sample as such.

None detected.

Approved By:___

...

G. Goodbar, Ph.D. Mauager of Laboratory Services

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT 9150 Flair Drive, Bl Monte, California 91731

TECHNICAL SERVICES DIVISION LABORATORY SERVICES BRANCH REPORT FOR SOURCE TEST

| TOI | Rod R | ock | | LAB REPORT DATE: | December 9, 99 |
|-------------------|-------|--------------------|------------------|------------------|----------------|
| S | ource | e Testing | 6 Monitoring | LABORATORY NO. | 11111 |
| COMPAN CITY: | IX ± | Champion Utopia | Petroleum | REFERENCE NO. | 22222 |
| PROCES | S | | | TEST NO. | 99-0000 |
| EQUIPH | | PCCU | | SOURCE TEST DATE | |
| CONTRO | _ | | | | |
| BQUIPM | BNT : | ESP | | DATE SAMPLE RECE | IVED: 12/9/99 |
| SAMPLE DESCRII | | 1 One | Method 5.2 Train | REQUESTED BY: | <u>_C.S.</u> |

ANALYSIS REQUESTED: Particulates & Moisture Gain

ANALYTICAL WORK PERFORMED, METHOD OF ANALYSIS, AND RESULTS Particulates by SCAQMD Method 5.2L; Moisture gain by SCAQMD Method 4.1L

| Silica gel gain, g Pre-filter recovered volume, mL 30 | 7 6 0 |
|--|-------------|
| Pre-filter recovered volume, mL 30 | - |
| | 0 |
| Pre-filter residue, mg 1 | |
| | 4 |
| Acid, as $H_2SO_2H_2O_2$, mg | 1 |
| Sulfates, as H_2SO_4 .2 H_2O_7 mg | 8 |
| Pilter catch, mg | 4 |
| Acid, as $H_2SO_{2}H_2O_{1}$ mg < | 1 |
| Sulfates, as H ₂ SO2H ₂ O, mg | 2 |
| Post-filter recovered volume, mL 85 | D |
| organic residue, mg | 4 |
| Aqueous residue, mg 13 | D |
| Acid, as H_2SO_{3} .2 H_2O , mg 1 | 2 |
| Sulfates, as $H_1SO_{4.2}H_2O_{7}$ mg 13 | 1 |

Approved By: G. Goodbar, Ph.D. Manager of Laporatory Services

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SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT 9150 Plair Drive, Bl Moste, California 91731

TECHNICAL SERVICES DIVISION LABORATORY SERVICES BRANCH REPORT FOR SOURCE TEST

| TO: Rod Rock | LAB REPORT D | ATE: December 9, 99 |
|----------------------|------------------------|---------------------|
| Source Testing I | | |
| | LABORATORY M | ю |
| COMPANY: Champ n | Petroleum | |
| CITI: Utopia | REFERENCE NO | 22222 |
| PROCESS | TEST NO. | 99-0000 |
| BQUIPMENT: FCCU | | |
| | SOURCE TEST | DATE: 11/9/99 |
| CONTROL | | |
| BQUIPKENT: ESP | DATE SAMPLE | RECEIVED: 12/9/99 |
| SAMPLE | REQUESTED BY | ı <u>C.s.</u> |
| DESCRIPTION: One one | -quart can of fuel oil | |

ANALYSIS REQUESTED: Weight Percent Sulfur

ANALYTICAL WORK PERFORMED, METHOD OF ANALYSIS, AND RESULTS

Weight Percent Sulfur by ASTM D-129-64.

Wt. V Sulfur = 0.15

Approved By:

G. Goodbar, Ph.D. Manager of Laboratory Services

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SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT 9150 Flair Drive, Bi Moste, California 91731

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LABORATORY SERVICES BRANCH REPORT FOR SOURCE TEST

| TO: Rod Rock | LAB REPORT DATE:_ | December 9, 1999 |
|---|-------------------------------|------------------|
| Source Testing & Monitoring | LABORATORY NO. | _11111 |
| COMPANY: Champion Petroleum CITY: Utopia | REFERENCE NO. | 22222 |
| PROCESS | TEST NO. | 99-0000 |
| RONIBWRMI: ACCA | SOURCE TEST DATE: | 11/9/99 |
| Control Bquipment: ESP | DATE SAMPLE RECEIVED: 12/9/99 | |
| SAMPLE DESCRIPTION: <u>One</u> Method 6.1 Train(| REQUESTED BY: | C.S. |
| ANALYSIS REQUESTED: 50, 50, and Moist | ure Gain | |

| Received impinger vol., mL | 490 |
|----------------------------------|-----|
| Impinger gain, mL | 90 |
| Silica gel gain, g | 16 |
| | |
| Thimble catch: | |
| Acid, as SO,, mg | <1 |
| Sulfate, as SO,, mg | 11 |
| 1PA Catchi | |
| Acid, as SU,, mg | 1 |
| Sulfate, as SO ₃ , mg | 50 |
| | |
| Peroxide Catch: | |

Acid, as SO₂, mg 183 Sulfate, as SO₂, mg 192

Approved By:____

G. Goodbar, Ph.D.

Manager of Laboratory Services